# A Simplified Model of Aerosol Removal by Containment Sprays 

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# A Simplified Model of Aerosol Removal by Containment Sprays 

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#### Abstract

Spray systems in nuclear reactor containments are described. The scrubbing of aerosols from containment atmospheres by spray droplets is discussed. Uncertainties are identified in the prediction of spray performance when the sprays are used as a means for decontaminating containment atmospheres. A mechanistic model based on current knowledge of the physical phenomena involved in spray performance is developed. With this model, a quantitative uncertainty analysis of spray performance is conducted using a Monte Carlo method to sample 20 uncertain quantities related to phenomena of spray droplet behavior as well as the initial and boundary conditions expected to be associated with severe reactor accidents. Results of the uncertainty analysis are used to construct simplified expressions for spray decontamination coefficients. Two variables that affect aerosol capture by water droplets are not treated as uncertain; they are (1) ' $Q$ ', spray water flux into the containment, and (2) ' $\mathrm{H}^{\prime}$ ', the total fall distance of spray droplets. The choice of values of these variables is left to the user since they are plant and accident specific. Also, they can usually be ascertained with some degree of certainty. The spray decontamination coefficients are found to be sufficiently dependent on the extent of decontamination that the fraction of the initial aerosol remaining in the atmosphere, $\mathrm{m}_{\mathrm{f}}$, is explicitly treated in the simplified expressions. The simplified expressions for the spray decontamination coefficient are: $$
\lambda\left(\mathrm{hr}^{-1}\right)=\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\left[\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\right]
$$ where $$
\begin{aligned} \ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right) & =\mathrm{A}+\mathrm{B} \ln \mathrm{Q}+\mathrm{CH}+\mathrm{DQ}^{2} \mathrm{H}+\mathrm{EQH}^{2}+\mathrm{FQ} \\ \lambda\left(\mathrm{~m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right) & =\left[\mathrm{a}+\mathrm{b} \log _{10} \mathrm{Q}\right]\left[1-\left[\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right]^{\mathrm{c}}\right]+\left[\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right]^{\mathrm{c}} \end{aligned}
$$

Parametric values for these expressions are found for median, 10 percentile and 90 percentile values in the uncertainty distribution for the spray decontamination coefficient. Examples are given to illustrate the utility of the simplified expressions to predict spray decontamination of an aerosol-laden atmosphere.




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## I. Introduction

Containment sprays have been an important feature of the containments of some pressurized water reactors for many years [1-4]. Drywell sprays, too, have been important engineered safety systems in boiling water reactors [5]. These systems have been installed in reactors as part of the systems to suppress steam pressurization during design basis loss-of-coolant accidents. That is, the systems are intended to supply enormous amounts of water to condense steam quite promptly after a hypothesized rupture of a large pipe in the reactor coolant system.

There has always been some consideration of the source term reduction capabilities of sprays in reactor containments. This attention has focused on the ability of spray droplets to dissolve molecular iodine from the containment atmosphere [1-4,6]. More recently, much greater attention has been given to the capabilities of containment sprays to remove aerosol particles from the atmosphere. Explicit accounting of these aerosol removal processes is taken in many modern severe accident analysis codes such as the Source Term Code Package [7] and CONTAIN [8].

Systematic consideration of the possible steps that could be taken to terminate or at least mitigate severe reactor accidents, so-called "accident management" strategies, have attached great significance to spray systems in reactor containments or drywells [9,10]. These systems can be used to cool the containment atmosphere and to reduce the possibility of long-term overpressurization. The spray systems would be used rather differently for accident management than was envisaged for mitigation of design basis accidents. Water flow rates needed for long-term cooling of the containment atmosphere would be much less than flows used to condense steam pressurization in a design-basis accident. Indeed, the spray systems might be used only intermittently following a severe reactor accident. The spray system could also be used to cleanse the containment atmosphere of radioactive particulate. Thus, even if rupture of the containment in a severe accident could not be prevented, the spray system could reduce substantially the consequences of the accident.

Spray systems have become of enough interest that there is a need for computational tools to analyze spray performance under severe accident conditions. Indeed, such models are found in systemslevel accident analysis codes. These models are, however, inaccessible for routine use in engineering evaluations and regulatory decision making. A simplified equation that could be employed to make quick assessments of spray performance for source term attenuation would be of more use.

The formal differential equation that describes decontamination of an atmosphere by spray droplets is:

$$
\frac{\mathrm{dM}}{\mathrm{dt}}=-\lambda \mathrm{M}+\frac{\mathrm{dS}}{\mathrm{dt}}+\frac{\mathrm{dR}}{\mathrm{dt}}
$$

where
$\mathbf{M}=$ mass of aerosol suspended in the containment atmosphere

## Introduction

$$
\begin{aligned}
\frac{\mathrm{dS}}{\mathrm{dt}}= & \text { rate at which aerosols are injected into the containment atmosphere } \\
\frac{\mathrm{dR}}{\mathrm{dt}}= & \text { rate at which aerosols are removed from the atmosphere by processes other than those } \\
& \text { brought on by the sprays } \\
\lambda= & \text { rate constant for aerosol removal by sprays. }
\end{aligned}
$$

As will become more apparent in the discussions below; the rate of aerosol removal from the containment atmosphere by sprays is so much greater than the rates of removal by other processes in the steady state situations of interest here that dR/dt can be neglected. Similarly, the agglomeration of aerosol particles can be neglected. Removal rates by sprays are so much larger than the rates of agglomeration that the changes in the aerosol size distribution caused by agglomeration can often be neglected in comparison to the apparent changes in the size distribution brought about by spray removal of particles.

Source rates of aerosols into the containment, $\mathrm{dS} / \mathrm{dt}$, are strong functions of time. They vary, often dramatically, from accident-to-accident and plant-to-plant. For most purposes to which a simplified model of spray decontamination would be applied, sources of aerosols to the containment atmosphere would be assumed to be small or zero. That is, a typical issue to be addressed would involve the hypothesis that aerosol material has been injected into the containment atmosphere. It might then be asked how long a spray of some type must operate to achieve a specified decontamination level. This question is answered by:

$$
D F=\exp (+\lambda t)
$$

where

$$
\begin{aligned}
\mathrm{DF}= & \text { the aerosol mass initially in the containment atmosphere divided by the aerosol mass } \\
& \text { present after spray operation for a time } \mathrm{t}
\end{aligned}
$$

DF is usually called the "decontamination factor" and $\lambda$ is often called the "decontamination coefficient."

The time of spray operation required to achieve a specified decontamination factor is given by $t=(1 / \lambda) \ln (D F)$.

A long term, low-level aerosol source rate to the containment atmosphere is also of interest for some purposes. The steady-state aerosol mass in the containment atmosphere if a spray is operating is given by:

$$
\mathrm{M}(\text { steady-state })=(1 / \lambda) \mathrm{dS} / \mathrm{dt}
$$

Clearly, the rate constant for aerosol removal from an atmosphere by a spray, $\lambda$, is a critical quantity. This rate constant will be shown to be a complicated function of the aerosol particle size distribution, the characteristics of the spray and the geometry of the containment. A simplified model of $\lambda$ provides a simplified model of decontamination by sprays. The purpose of this report is to describe such a simplified model that can be used to estimate aerosol removal by sprays without the necessity of using detailed systems codes such as CONTAIN. It is emphasized that the simplified model of aerosol removal by containment sprays developed in this report is not intended to supplant the truly mechanistic models. Rather, the simplified model is intended to provide more readily available estimates of aerosol decontamination along with statistically based uncertainty bounds and confidence limits.

The formulation of a simplified model of decontamination by sprays done here follows a procedure previously used to formulate a simplified model of decontamination by water pools overlying core debris interacting with concrete [11]. A fairly detailed model based on the physical processes involved in decontamination by sprays is first developed. These physical phenomena and processes are discussed in the next chapter of this document. Uncertain features of the model are identified and a Monte-Carlo uncertainty analysis of decontamination by sprays is then conducted. The uncertainties in the model, the ranges of values the influential parameters have, and the distributions of these values are discussed in Chapter III. The Monte Carlo uncertainty analysis of the model predictions is discussed in Chapter IV. The results of the Monte-Carlo analyses are analyzed using non-parametric order statistics. These analyses yield a quantitatively characterized uncertainty distribution for the decontamination that can be achieved by sprays in a volume with a specified height and water flow. Results of analyses for various heights and water flows are used to develop simple expressions for the rate constant for aerosol removal in the fifth chapter of this report.

## II. Phenomena and Processes Involved in Decontamination by Sprays

In this chapter, the phenomena and processes pertinent to spray decontamination are described. An important objective of this chapter is to identify models and quantities in the quantitative descriptions of these phenomena and processes that are uncertain. Uncertainties identified here are used to develop the probability distributions for decontamination by sprays presented in Chapter IV.

## A. Spray Characteristics

A comprehensive survey of the sprays used in U.S. commercial nuclear power plants has not been attempted for this work. Two types of sprays--one type found especially in pressurized water reactors and one type found in some boiling water reactors--are described here to illustrate the nature of the spray systems in nuclear power plants.

A configuration typical for the containment of a pressurized water reactor is to locate spray nozzles on ring headers near the top of the containment. A particular configuration for a four-ring header system is:

| Header | Radius <br> $(\mathrm{m})$ | Elevation <br> $(\mathrm{m})$ |
| :---: | :---: | :---: |
| A | 2.48 | 40.5 |
| B | 7.72 | 39.0 |
| C | 12.87 | 37.3 |
| D | 18.13 | 36.0 |

A configuration found in a Mark III containment of a boiling water reactor is:

Header
B
5.87
12.11
16.48

| Radius | Elevation |
| :---: | :---: |
| $(\mathrm{m})$ | $(\mathrm{m})$ |

25.91
22.56
16.76

Some plants have only two headers. In most pressurized water reactors, either two or three pumps are available to supply water to the headers. Each pump will typically supply 157-189 liters/second. Design flow rates are as high as 330 liters/second. In the Mark III containment, usually, two pumps are available. A single pump can supply about 356 liters/second. With both pumps operating 713 liters/second could be supplied.

More than 300 spray nozzles are mounted on the headers. A Sprayco Model 1713-A or Model 1713 nozzle is widely used. Lists of plants using these nozzles are shown in Tables 1 and 2. The vendor for this nozzle is now Lechler Corporation. The designation for the nozzle is "373.084.xx.BN hollow core, ramp bottom, standard angle spray nozzle." A schematic diagram of the spray nozzle is shown in Figure 1. Also shown in this figure is a schematic diagram of the spray pattern produced by the nozzle when it is pointed downward. In this configuration, droplets emerge from

Table 1 Plants that use the Type 1713-A spray nozzle

| Arkansas Units 1 and 2 | Millstone |
| :--- | :--- |
| Bellefonte Units 1 and 2 | Palisades |
| Braidwood Units 1 and 2 | Prairie Island Units 1 and 2 |
| Byron Units 1 and 2 | Perry Units 1 and 2 |
| Calvert Cliffs Units 1 and 2 | Rancho Seco |
| Catawba Units 1 and 2 | River Bend Units 1 and 2 |
| Clinton Units 1 and 2 | Salem Units 1 and 2 |
| Comanche Peak Unit 1 | San Onofre Units 2 and 3 |
| Crystal River | Seabrook |
| D. C. Cook Units 1 and 2 | Sequoyah Units 1 and 2 |
| Davis Besse Unit 1 | South Texas Project 1 |
| Diablo Canyon Units 1 and 2 | Susquehana Units 1 and 2 |
| Indian Point Units 2 and 3 | Three Mile Island Units 1 and 2 |
| Kewaunee | Watts Bar Units 1 and 2 |
| LaSalle County Units 1 and 2 | WPPSS Unit 1 |

Foreign
Takahama (Japan)
Ringhals Unit 2 (Sweden)
Almaraz Units 1 and 2 (Spain)

Table 2 Plants that use the Type 1713 spray nozzle
Robinson Unit 2
Point Beach Units 1 and 2
Turkey Point Unit 3
Zion Units 1 and 2

Phenomena


Figure 1 Diagram of the Model 1713-A spray nozzle and schematic diagram of the spray pattern
the nozzle within a conical envelope with a half angle of $30^{\circ}$. This angle varies by less than two degrees as the water pressure varies from 0.34 to 2.7 atmospheres. This is the configuration of the nozzle that is usually analyzed for spray performance. It is not, however, the only nozzle configuration used in spray systems. Other configurations are examined below in the discussion of droplet trajectories.

Water flow rate through the Model 1713-A nozzle as a function of water pressure is shown in Figure 2. Water droplets are initially within an annular conical region. Little of the flow is directly downward from the nozzle. As drag reduces the horizontal components of the droplet velocities, the unsprayed central region of the conical pattern begins to be occupied by falling droplets. The spatial variations in the flow claimed by the manufacturer are shown in Figure 3.

As will be discussed at length below, the distribution of droplet sizes varies with distance from the nozzle. The number-weighted size distribution of droplets at a particular location below a spray nozzle is shown in Figure 4. This distribution is distinctly log-normal in nature. Fit of the data shown in Figure 4 to a log-normal distribution yields:

$$
\operatorname{Pr}\left(\mathrm{D}_{\mathrm{d}}(\mathrm{e})<\mathrm{D}\right)=0.5(1+\operatorname{erf}(\mathrm{z}))
$$

where

$$
\left.\begin{array}{rl}
\operatorname{Pr}\left(D_{\mathrm{d}}(\mathrm{e})<\mathrm{D}\right)= & \text { cumulative probability that the volume equivalent spherical diameter of a } \\
& \text { droplet, } \mathrm{D}_{\mathrm{d}}(\mathrm{e}), \text { is less than } \mathrm{D}
\end{array}\right) \begin{aligned}
\operatorname{erf}(\mathrm{z})= & \text { error function of } \mathrm{z}=\frac{2}{\sqrt{\pi}} \int_{0}^{\mathrm{z}} \exp \left(-\mathrm{y}^{2}\right) \mathrm{dy} \\
z= & \ln (\mathrm{D} / \mu) /(\sqrt{(2)} \ln \sigma) \\
\mu= & \text { mean droplet size }=234 \mu \mathrm{~m} \\
\sigma= & \text { geometric standard deviation }=2.196
\end{aligned}
$$

For the purposes of comparison, the size distribution of droplets produced by a similar though not identical nozzle also used in reactor containments (Whirljet Spray Nozzle 15215-1C-304SS-6.3) is shown in Figure 5. This droplet size distribution has a much more distinctly bimodal character than does the distribution of droplet sizes for the Model 1713-A nozzle.

The size distributions shown in Figures 4 and 5 are number distributions. It is not usual to specify spray nozzles for reactor containments in terms of such distributions. It is more common to specify that either the surface-area weighted mean or the volume weighted mean droplet size to be less than some minimum--usually less than $1000 \mu \mathrm{~m}$. Surface area weighted and volume weighted distributions derived from the data in Figure 4 are shown in Figures 6 and 7, respectively. Note that these distributions sharply de-emphasize the contributions made to the distributions by the small

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Figure 2 Volumetric flow rate of water through the Model 1713-A spray nozzle as a function of water pressure


Figure 3 Spatial variation in water flow from a Model 1713-A spray nozzle


Figure 4 Size distribution of water droplets from a Model 1713-A spray nozzle


Figure 5 Size distribution of water droplets produced by a Whirljet Spray Nozzle Model 15215-1C-304SS-6.3


Figure 6 Surface area-weighted size distribution of water droplets from a Model 1713-A spray nozzle


Figure 7 Volume-weighted size distribution of water droplets produced by a Model 1713-A spray nozzle
droplets. Small droplets, however, are important because, as will be described, they can be more efficient than large droplets at trapping aerosol particles.

The distribution shown in Figure 4 was obtained by the manufacturer using a photographic method. Powers and Reid [26] have criticized this method. They adopted a technique in which spray droplets were frozen in liquid nitrogen. The frozen droplets were then size classified with sieves. They found that the spray contained many more small droplets than would be indicated by results of the photographic method. A comparison of the number distribution calculated from their results and the number distribution obtained by photographic methods is shown in Figure 8. Powers and Reid attributed the differences between the distribution obtained with their freeze-and-sieve technique and the distribution obtained by the photographic technique to the inability to resolve small droplets in photographic images and the small sample size used in studies done with the photographic technique.

The freeze-and-sieve technique is, however, not without flaws. A most common source of error that may have affected results is that the sieving process can break particles [27]. This is especially likely to occur if the sieves are very heavily loaded with particulate as they apparently were in the investigations reported by Powers and Reid [26]. No evidence that the usual precautions were taken against particle breakage appears in the documentation of the work.

A remarkable finding of the studies of the 1713-A nozzle using the ${ }^{\text {ffreeze-and-sieve method is that }}$ droplet distributions obtained with a boric acid-sodium hydroxide solution ( 3000 ppm boron; $\mathrm{pH}=9.5$ ) were much coarser than distributions obtained with tap water. Mass fraction distributions obtained in replicate experiments with the two liquids are shown in Table 3 and in Figure 9. Powers and Reid [26] could not offer a ready explanation for the differences in the droplet size distributions. Obvious differences in the properties of the two liquids (density, surface tension, viscosity etc.) seem too small to be responsible for such large differences in the droplet size distributions.

Discrepancies between droplet size distributions obtained by different measurement techniques and the apparent sensitivity of the droplet size distribution to some kinds of water contamination raise uncertainties in the droplet size distributions to be used in the analysis of spray decontamination of containment atmospheres.

A different type of spray nozzle (Spray Systems Co. Model 1-7G25) is shown in Figure 10. This is the type of spray nozzle used in the drywells of some Mark I boiling water reactors. Others use the rather similar Model 1-7G3 nozzle. This type of spray nozzle seems to be better suited than the 1713 or 1713-A nozzle for applications where the droplet fall distances are small. A fairly uniform spatial distribution of droplets is achieved after only a small fall distance. (In the Brown's Ferry Mark I boiling water reactors, headers for the spray nozzles are located 15.84 and 8.53 meters above the drywell floor.) The spray patterns for the nozzles are also shown in Figure 10. About 65 percent of the total water flow from a nozzle is within a central core 3.35 meters ( 11 feet) in diameter at a point 3.35 meters ( 11 feet) below the nozzle. The remaining 35 percent of the flow is in an annular region which has an outside diameter of 5.2 meters ( 17 feet) at 3.35 meters ( 11 feet) below the nozzle.

Flow rates through individual Model 1-7G25 and Model 1-7G3 nozzles as functions of the water pressure are shown in Figure 11. Total spray flow into the Mark I drywell is 517 liters/second in


Figure 8 Comparison of mass-weighted distribution data obtained by the freeze-and-sieve technique and by the photographic technique for the Model 1713-A spray nozzle

Table 3 Droplet size data obtained by the freeze-and-sieve method [26] mass on screen (g)*

| Nozzle | Test 1a 1713-A | $\begin{aligned} & \text { Test 1b } \\ & \text { 1713-A } \end{aligned}$ | $\begin{aligned} & \text { Test 2a } \\ & \text { 1713-A } \end{aligned}$ | $\begin{aligned} & \text { Test 2b } \\ & \text { 1713-A } \end{aligned}$ | $\begin{gathered} \text { Test 3a } \\ 1-7 G 3 \end{gathered}$ | $\begin{gathered} \text { Test 3b } \\ \text { 1-7G3 } \end{gathered}$ | $\begin{gathered} \text { Test 4a } \\ 1-7 \mathrm{G} 3 \end{gathered}$ | $\begin{gathered} \text { Test 4b } \\ \text { 1-7G3 } \end{gathered}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Solution | tap water | tap water | boric acid $-\mathrm{NaOH}$ | boric acid $-\mathrm{NaOH}$ | tap water | tap water | boric acid $-\mathrm{NaOH}$ | boric acid $-\mathrm{NaOH}$ |
| Screen Opening ( $\mu \mathrm{m}$ ) |  |  |  |  |  |  |  |  |
| 2360 | 154.3 | 231.5 | 231.5 | 540.1 |  |  |  |  |
| 1700 | 2546.0 | 3857.5 | 3857.5 | 6403.5 |  |  | 154.3 | 0 |
| 1400 | 4937.6 | 6172.0 | 6094.9 | 8177.9 |  |  | 154.3 | 77.2 |
| 1180 | 6249.2 | 6712.1 | 5400.5 | 6789.2 | 77.2 |  | 231.5 | 77.2 |
| 1000 | 6403.5 | 6326.3 | 4328.4 | 5477.7 | 77.2 | 77.2 | 77.2 | 77.2 |
| 850 | 5786.3 | 5323.4 | 3086.0 | 4089.0 | 231.5 | 154.3 | 231.5 | 231.5 |
| 710 | 4937.6 | 4011.8 | 1851.6 | 2546.0 | 231.5 | 77.2 | 540.1 | 540.1 |
| 600 | 3240.3 | 4011.8 | 1003.0 | 1465.9 | 385.8 | 231.5 | 925.8 | 848.7 |
| 500 | 2777.4 | 2546.0 | 694.4 | 1080.1 | 540.1 | 462.9 | 1311.6 | 1388.7 |
| 355 | 2931.7 | 2160.2 | 462.9 | 848.7 | 1080.1 | 1234.4 | 2468.8 | 3008.9 |
| 300 | 1080.1 | 771.5 | 154.3 | 308.6 | 462.9 | 617.2 | 1080.1 | 1234.4 |
| 250 | 1388.7 | 1003.0 | 231.5 | 385.8 | 462.9 | 462.9 | 462.9 | 462.9 |
| 125 | 1620.2 | 1234.4 | 154.3 | 308.6 | 231.5 | 154.3 | 462.9 | 771.5 |
| pan | 540.1 | 385.8 | 77.2 | 308.6 | 308.6 | 231.5 | 231.5 | 308.6 |
| $\mu^{* *}$ | 899 | 941 | 1295 | 1214 | 426 | 399 | 469 | - |
| $\sigma_{\mathrm{g}}{ }^{* *}$ | 2.192 | 1.928 | 1.637 | 1.710 | 1.654 | 1.490 | 1.577 | - - |

[^0]

Figure 9 Comparison of mass distribution data obtained by the freeze-and-sieve technique for the Model 1713-A spray nozzle using tap water and a boric acid-sodium hydroxide solution



Type 7G
Female connection (mounted on pipe end)

Figure 10 Schematic diagram of the Model 1-7G25 spray nozzle and the spray pattern it produces


Figure 11 Volumetric flow as a function of water pressure for the Model 1-7G25 and the Model 1-7G3 spray nozzles

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Units 1 and 2 at Brown's Ferry and 577 liters/second in Unit 3. These flow rates are not, however, typical for all Mark I drywells. Some plants have reduced the available flow to as low as 57 liters/second to reduce the risk of underpressurization of the drywell. At Brown's Ferry, interlocks prevent actuation of the drywell sprays if the drywell is not at a positive pressure or the core is not at least $2 / 3$ covered with water. Note also that, to the author's knowledge, sprays cannot operate in a Mark I boiling water reactor if off-site electrical power is not available.

The volume-weighted mean droplet size produced by the Model 1-7G25 nozzle as functions of water pressure are shown in Figure 12. Also shown in this figure is the volume weighted mean droplet size produced by the similar, though smaller, Model 1-7G3 nozzle which is also of interest [26,28]. Detailed droplet size data are not available for the Model 1-7G25 spray nozzle. Droplet size data for the Model 1-7G3 nozzle obtained by the freeze-and-sieve method [26] are shown in Table 3 and in Figure 13. Note that the droplets are somewhat smaller for Model 1-7G3 nozzle than for the Model 1713-A nozzle. Again, note that the boric acid-sodium hydroxide solution yielded somewhat larger droplets than did tap water. The effect is, however, not as large as it is for the Model 1713-A spray nozzle.

The distributions of droplet sizes are not readily described in terms of conventional lognormal distributions. In summary, it is evident that the knowledge of these droplet size distributions is not thorough. There is at least some evidence that the size distributions are sensitive to contamination of the liquid. Certainly, when sprays are used to decontaminate containment atmospheres the water will become contaminated with a variety of materials and at concentrations that could be higher than the concentration of the boric acid-sodium hydroxide solution used in the experiments by Powers and Reid. Moreover, in most spray systems, contaminated water is recirculated from a sump in the containment through the spray headers. The effects of contaminants in sump waters on droplets sizes are, of course, not known.

## B. Droplet Shapes

Water droplets falling through a gaseous atmosphere do not adopt a tear-drop shape. If big-enough, the drops can, as a first approximation, be considered to be oblate ellipsoids with semi-major axis a and semi-minor axis b. Pruppacher and Beard [12] have proposed the correlation for droplet eccentricity at atmospheric pressure:

$$
1 / E=b / a= \begin{cases}1.030-0.62 \mathrm{D}_{\mathrm{d}}(\mathrm{e}) & \text { for } 0.1 \leq \mathrm{D}_{\mathrm{d}}(\mathrm{e}) \leq 0.9 \mathrm{~cm} \\ 1.00 & \text { for } D_{d}(\mathrm{e})<0.1 \mathrm{~cm}\end{cases}
$$

where

$$
\begin{aligned}
\mathrm{E} & =\mathrm{a} / \mathrm{b}=\text { eccentricity } \\
\mathrm{D}_{\mathrm{d}}(\mathrm{c}) & =\text { diameter }(\mathrm{cm}) \text { of the spherical droplet that would have the same volume } \\
& =2 \mathrm{a} / \mathrm{I}^{1 / 3}
\end{aligned}
$$



Figure 12 Volume weighted mean droplet sizes produced by the Model 1-7G25 and Model 1-7G3 spray nozzles as functions of water pressure


Figure 13 Mass distribution data obtained by the freeze-and-sieve method for the Model 1-7G3 spray nozzle using tap water and a boric acid-sodium hydroxide solution

The surface area of the oblate ellipsoid is:

$$
A=2 \pi a^{2}+\pi\left\{\frac{a b}{\sqrt{E^{2}-1}} \ln \left[\frac{E+\sqrt{E^{2}-1}}{E-\sqrt{E^{2}-1}}\right]\right\}
$$

This area can be compared to the area of the volume-equivalent sphere which is $4 \pi \mathrm{a}^{2} / \mathrm{E}^{2 / 3}=$ $\pi D_{d}{ }^{2}(\mathrm{e})$.

With the Pruppacher and Beard correlation it is calculated that only the largest droplets produced by reactor sprays are distorted significantly from spherical. Unfortunately, there is no data base to validate this conclusion for conditions different than air at one atmosphere.

A somewhat better approximation for drop shape is to consider the droplet to be formed by two hemi-ellipsoids with semi-minor axes $b_{1}$ and $b_{2}$ and a common semi-major axis a as shown in Figure 14. Correlations for the droplet dimensions are [13]:

$$
\begin{aligned}
& \left(b_{1}+b_{2}\right) / 2 a= \begin{cases}\sim 1.0 & \text { for } E_{0} \leq 0.4 \\
1.0 /\left(1.0+0.18\left(E_{0}-0.4\right)^{0.8}\right) & \text { for } 0.4<E_{0} \leq 8\end{cases} \\
& b_{1} /\left(b_{1}+b_{2}\right)= \begin{cases}0.5 & \text { for } E_{0} \leq 0.5 \\
0.5 /\left(1.0+0.12\left(E_{0}-0.4\right)^{0.8}\right) & \text { for } 0.5<E_{0} \leq 8\end{cases}
\end{aligned}
$$

where

$$
\begin{aligned}
\mathrm{E}_{\mathrm{o}} & =\text { Eotvos number }=\mathrm{g}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) \mathrm{D}_{\mathrm{d}}(\mathrm{e}) / \sigma_{\ell} \\
\mathrm{g} & =\text { acceleration due to gravity } \\
\rho_{\ell} & =\text { density of droplet liquid } \\
\rho_{\mathrm{g}} & =\text { density of the gas phase } \\
\sigma_{\ell} & =\text { surface tension of the droplet liquid }
\end{aligned}
$$



## DIRECTION OF FALL



Figure 14 Schematic diagram of a two hemi-ellipsoid approximation for droplet shape

$$
\begin{aligned}
\mathrm{D}_{\mathrm{d}}(\mathrm{e}) & =2 \mathrm{a} / \mathrm{E}^{\prime 1 / 3} \\
\mathrm{E}^{\prime} & =\text { effective eccentricity }=\left[\left(\mathrm{b}_{1}+\mathrm{b}_{2}\right) / 2 \mathrm{a}\right]
\end{aligned}
$$

The surface area of a two hemi-ellipsoid droplet is given by:

$$
A=2 \pi a^{2}+\frac{\pi}{2}\left\{\left(b_{1}^{2} / e_{1}\right) \ln \left[\frac{1+e_{1}}{1-e_{1}}\right]+\left(b_{2}^{2} / e_{2}\right) \ln \left[\frac{1+e_{2}}{1-e_{2}}\right]\right\}
$$

where

$$
\begin{aligned}
& e_{1}=\left[1-b_{1} 2 / a^{2}\right]^{1 / 2} \\
& e_{2}=\left[1-b_{2}^{2} / a^{2}\right]^{1 / 2}
\end{aligned}
$$

The surface area of the volume-equivalent sphere is $4 \pi \mathrm{a}^{2} / \mathrm{E}^{2 / 3}$.
Surface areas and eccentricities predicted with the two correlations are shown as functions of the diameter of the spherical droplet with the equivalent volume in Figure 15. Again, it is apparent that at atmospheric pressure, droplets of pure water produced by containment sprays distort little. Contamination of the water by species that affect surface tension is predicted to cause more significant distortion of the droplets.

## C. Droplet Terminal Velocities

Clift, Grace and Weber [13] note that the data base for terminal velocities of water droplets is not large. Most of the available data are for raindrops in air. There appear to be no data for water drops falling through atmospheres of the type expected to exist in nuclear reactor containments during severe accidents. Three correlations of the terminal velocities of water drops are:

- Model A: [14]

$$
\begin{aligned}
\operatorname{Re}_{\mathrm{T}} & =\exp \left[-3.126+1.01 \ln \mathrm{~N}_{\mathrm{D}}-0.01912\left(\ln \mathrm{~N}_{\mathrm{D}}\right)^{2}\right] \\
& \text { for } 2.4<\mathrm{N}_{\mathrm{D}}<10^{7} ; 0.1<\mathrm{Re}_{\mathrm{T}}<3550
\end{aligned}
$$

where

$$
\mathrm{Re}_{\mathrm{T}}=\text { terminal Reynolds number }=\mathrm{U}_{\mathrm{T}} \rho_{\mathrm{g}} \mathrm{D}_{\mathrm{d}}(\mathrm{e}) / \mu_{\mathrm{g}}
$$




Figure 15 Comparison of eccentricities $E$ and $E^{\prime}$ and the ratios of the ellipsoidal surface areas to the area of the volume-equivalent sphere for two models of droplet shape

$$
\begin{aligned}
& \mathrm{U}_{\mathrm{T}}=\text { terminal velocity } \\
& \mu_{\mathrm{g}}=\text { viscosity of the gas phase } \\
& \mathrm{N}_{\mathrm{D}}=\text { Best number }=4 \rho_{\mathrm{g}}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) \mathrm{g} \mathrm{D}_{\mathrm{d}}(\mathrm{e})^{3} / 3 \mu_{\mathrm{g}}^{2} \\
& \mathrm{C}_{\mathrm{D}}=\text { drag coefficient }=\mathrm{N}_{\mathrm{D}} / \mathrm{Re}_{\mathrm{T}}^{2}
\end{aligned}
$$

- Model B: [13]

$$
\operatorname{Re}_{\mathrm{T}}= \begin{cases}1.62 \mathrm{E}_{\mathrm{o}}^{0.755} \mathrm{M}^{-0.25} & \text { for } 0.5<\mathrm{E}_{\mathrm{o}} \leq 1.84 \\ 1.83 \mathrm{E}_{\mathrm{o}}^{0.555 \mathrm{M}^{-0.25}} & \text { for } 1.84<\mathrm{E}_{0} \leq 5.0 \\ 2.00 \mathrm{E}_{\mathrm{o}}^{0.5} \mathrm{M}^{-0.25} & \text { for } \mathrm{E}_{\mathrm{O}}>5.0\end{cases}
$$

and for $\mathrm{E}_{\mathrm{o}}<0.5$

$$
\begin{gathered}
\operatorname{Re}_{\mathrm{T}}=\mathrm{N}_{\mathrm{D}} / 24-1.7569 \times 10^{-4} \mathrm{~N}_{\mathrm{D}}^{2}+6.9252 \times 10^{-7} \mathrm{~N}_{\mathrm{D}}^{3}+-2.3027 \times 10^{-10} \mathrm{~N}_{\mathrm{D}}^{4} \\
\text { for } \mathrm{N}_{\mathrm{D}}<73 \text { and } \operatorname{Re}_{\mathrm{T}}<2.37 \\
\log _{10} \operatorname{Re}_{\mathrm{T}}=-1.7095+1.33438 \log _{10} \mathrm{~N}_{\mathrm{D}}-0.11591\left(\log _{10} \mathrm{~N}_{\mathrm{D}}\right)^{2} \\
\text { for } 73<\mathrm{N}_{\mathrm{D}}<580
\end{gathered}
$$

$$
\log _{10} \operatorname{Re}_{T}=-1.81391+1.34671 \log _{10} N_{D}-0.12427\left(\log _{10} N_{D}\right)^{2}+0.006344\left(\log _{10} N_{D}\right)^{3}
$$

$$
\text { for } N_{D}>580
$$

where

$$
\begin{aligned}
\mathrm{M} & =\text { Morton number }=\mathrm{g} \mu_{\mathrm{g}}^{4}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) / \rho_{\mathrm{g}}{ }^{2} \sigma_{\ell}{ }^{3} \\
\mathrm{C}_{\mathrm{D}} & =4 \rho_{\mathrm{g}}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) \mathrm{g} \mathrm{D}_{\mathrm{d}}(\mathrm{e})^{3} / 3 \mu_{\mathrm{g}}^{2} \operatorname{Re}_{\mathrm{T}}^{2}
\end{aligned}
$$

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- Model C: [13]

$$
\operatorname{Re}_{\mathrm{T}}= \begin{cases}0.766 \mathrm{E}_{\mathrm{O}}^{0.66} \mathrm{M}^{-028} & \text { for } \mathrm{E}_{\mathrm{O}} \leq 164 \mathrm{M}^{1 / 6} \\ 1.37 \mathrm{E}_{\mathrm{O}}^{0.55} \mathrm{M}^{-0.26} & \text { for } \mathrm{E}_{\mathrm{O}}>164 \mathrm{M}^{1 / 6}\end{cases}
$$

where, again:

$$
\mathrm{C}_{\mathrm{D}}=4 \rho_{\mathrm{g}}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) \mathrm{g} \mathrm{D}_{\mathrm{d}}(\mathrm{e})^{3} / 3 \mu_{\mathrm{g}}^{2} \operatorname{Re}_{\mathrm{T}}^{2}
$$

Terminal velocities calculated from these models for water droplets falling through air at 1 atmosphere pressure and 298 K are shown in Figure 16. Physical properties of air and water used in these calculations are shown in Table 4. The essential result shown by these models is that droplets of different sizes fall at different velocities. As a result, spray droplets not only sweep aerosols from the atmosphere, they also sweep other spray droplets from the atmosphere. Most importantly, the smallest droplets, which will be shown below to be most efficient at the capture of aerosol particles, are swept out by larger droplets as the spray droplets fall. Thus, the ability of a spray to cleanse a containment of particulate decreases with increasing fall distances.

## D. Aerosol Capture by Water Droplets

In the most general situation hypothesized to develop in a severe reactor accident, the containment or drywell spray would be actuated at a time when the containment atmosphere was very hot and rich in steam. Evaporation of the initial drops expelled by the spray would reduce any superheating of the atmosphere. Steam would then begin to condense on the droplets. The flux of steam condensing on the droplets would carry aerosol particles into the droplets. There would be, also initially, a thermophoretic force that would drive particles into the droplets. These highly dynamic conditions would be of short duration. A steady-state situation in which the atmosphere composition and temperature come close to equilibrium with the droplets of the spray would be established rather quickly. This is the situation that is of interest here. Under these quasi steady-state conditions the predominant modes of aerosol capture are:

- impaction,
- interception, and
- diffusion.

Impaction and interception of aerosol particles are affected by the atmosphere hydrodynamics. As a droplet falls through the atmosphere, a flow field develops around the droplet. This flow field will carry along aerosol particles. The flow field will, ideally, carry the aerosols around falling droplets. Some aerosols will, however, be too massive to respond to the sudden accelerations in the gas flow in the vicinity of the falling droplet. Inertia will carry these particles across streamlines of the flow so that the particles impact on the droplet surface. It is assumed here that contact between a droplet


Figure 16 Terminal velocities for falling water droplets

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## Table 4 Physical properties of air and water

Water Density $\left(\mathrm{g} / \mathrm{cm}^{3}\right)$

$$
\rho_{\ell}=1 /\left(1.236866-1.828945 \times 10^{-3} \mathrm{~T}(\mathrm{~K})+3.509325 \times 10^{-6} \mathrm{~T}(\mathrm{~K})^{2}\right)
$$

Water Surface Tension (dyne/cm)

$$
\sigma_{\ell}=34.6(\mathrm{~T}(\mathrm{~K}) / 704)^{-0.8373}
$$

Water Viscosity (Poise)

$$
\log _{10}\left(\mu_{\ell}\right)=\log _{10}(0.01002)+\left[\frac{1.3272(293-\mathrm{T}(\mathrm{~K}))-1.52 \times 10^{-3}(\mathrm{~T}(\mathrm{~K})-293)^{2}}{(\mathrm{~T}(\mathrm{~K})-168)}\right]
$$

Air Density ( $\mathrm{g} / \mathrm{cm}^{3}$ )

$$
\rho_{\mathrm{g}}(\text { air })=28.91 \mathrm{P}(\text { atms }) / 82.06 \mathrm{~T}(\mathrm{~K})
$$

Air Viscosity (Poise)

$$
\mu_{\mathrm{g}}(\mathrm{air})=2.3013 \times 10^{-6} \mathrm{~T}(\mathrm{~K})^{0.768}
$$

Saturation Pressure of Water Vapor (atms):

$$
\begin{aligned}
& \log _{10} \frac{P(\mathrm{atms})}{218.167}=\frac{-x}{T(\mathrm{~K})}\left[\frac{3.2437814+5.86826 \times 10^{-3} \mathrm{x}+1.1702379 \times 10^{-8} \mathrm{x}^{3}}{1+2.1878462 \times 10^{3} \mathrm{x}}\right] \\
& \mathrm{x}=647.27-\mathrm{T}(\mathrm{~K})
\end{aligned}
$$

and a particle is sufficient to cause capture of the aerosol particle. Surface tension and Van der Waals forces are sufficient to keep the particle in contact with the droplet even if the material that makes up the particle is not soluble in the droplet.

If the center of mass of an aerosol particle can follow the streamlines of the flow field around a falling droplet, the finite size of the aerosol particle may lead, nevertheless, to contact between the droplet and the particle. This interception mechanism is quite important for non-spherical aerosol particles. Again, contact with the droplet is probably sufficient to assure capture of the particle because of the surface tension and Van der Waals forces.

Very small particles are more able to follow the streamlines of the flow field around a droplet and are, therefore, less susceptible to capture by impaction or interception. But, these very small particles respond to the stochastic impulses of collisions with gas molecules. Because these impulses are not perfectly balanced on the time scales of interest during the passage of a droplet, there is an apparent diffusion of aerosol particles that can carry the aerosols across streamlines of the flow, leading to aerosol contact with the droplet and, consequently, aerosol capture. Convection of the gas can enhance this diffusive flux of particles into the droplet.

The diffusive flux of particles into the droplets is complicated by the vaporization of water from the falling droplet. Even if the atmosphere is nominally in equilibrium with water, it will not be in equilibrium with a droplet. The curvature of the droplet surface means that it will have a slightly higher vapor pressure than does a large body of water. The vapor pressure over a surface with a radius of curvature $r$ relative to the vapor pressure over a flat surface is given by:

$$
\ln \frac{\mathrm{P}(\mathrm{r})}{\mathrm{P}(\infty)}=\frac{2 \mathrm{M} \sigma_{\ell}}{\mathrm{RT} \rho_{\ell} \mathrm{r}}
$$

where $M$ is the molecular weight of the vapor. Thus, the vapor pressure of the droplets increases with decreasing size. There will be, then, a tendency for small droplets to evaporate and large droplets to grow in a cloud of droplets even if the atmosphere is nominally saturated. For droplets of the size of interest here ( $>100 \mu \mathrm{~m}$ ) the effect is not large.' It is ameliorated further by the tendency of the evaporating droplet to cool slightly [29]. Any effect of the vapor flux coming off small droplets on the ability of the droplet to capture particles is probably overwhelmed by local turbulence effects. Therefore, the effect is ignored here.

It is possible for aerosol particles and water droplets to become electrostatically charged. The relatively powerful electrostatic forces could greatly accentuate or reduce the trapping of aerosols by droplets depending on whether charges on the droplets and the particles were different or were the same. Radiation fields can efficiently discharge both droplets and particles. It is assumed here that electrostatic effects can be neglected. There is no entirely satisfactory proof that this assumption is valid (but, see Reference 25). The difficulty is that even if particles are neutral, overall fluctuations in the charge densities or non-zero variances in charge density could affect the trapping process.

For the purposes of this work, only the three steady-state aerosol capture mechanisms discussed above--impaction, interception, and diffusion--are considered. The quantitative descriptions of these particle-capture processes presented below are based on analyses for isolated spherical droplets.

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From the discussions above, it is apparent that the droplets will not always be spherical and they are never isolated. This introduces some uncertainty in the prediction of decontamination of containment atmospheres by sprays.

Consider a sphere of diameter $\mathrm{D}_{\mathrm{d}}(\mathrm{e})$ falling through space. After falling a distance X , the sphere will sweep out a volume of gas given by:

$$
\text { Volume }=\frac{\pi}{4} D_{d}(e)^{2} X
$$

If the gas contains a concentration of $n(i)$ particles of diameter $d_{p}(i)$, then in the absence of hydrodynamic phenomena, the falling sphere would sweep out:

$$
\frac{\pi}{4} \mathrm{D}_{\mathrm{d}}(\mathrm{e})^{2} \mathrm{X} \cdot \mathrm{n}(\mathrm{i})
$$

of the particles. A convenient definition of the particle capture efficiency is the ratio of the actual number of particles of size $d_{p}(i)$ captured to the number captured in the hypothetical situation:

$$
\in\left(D_{d}(e), d_{p}(i)\right)=4 \Delta N(i) / \pi D_{d}(e)^{2} n(i) X
$$

where

$$
\begin{aligned}
\in\left(D_{d}(e), d_{p}(i)\right)= & \begin{array}{l}
\text { efficiency with which a drop of diameter } D_{d}(e) \text { captures particles of } \\
\\
\\
\text { diameter } d_{p}(i)
\end{array} \\
\Delta N(i)= & \begin{array}{l}
\text { actual number of particles of diameter } d_{p}(i) \text { captured in a fall of } \\
\text { distance } X
\end{array}
\end{aligned}
$$

Hydrodynamic effects cannot be neglected in the analysis of aerosol capture by falling water droplets. The efficiency with which droplets capture aerosol particles depends on the nature of flow around the droplet. Analytic results are, however, available only for the limiting flow regimes of viscous flow $(\operatorname{Re} \rightarrow 0)$ and of potential flow $(\operatorname{Re} \rightarrow \infty)$. Pemberton [14] has argued that in view of the substantial size differences between aerosols of interest (diameters less than $10 \mu \mathrm{~m}$ ) and droplets of interest (diameters greater than $100 \mu \mathrm{~m}$ ), flow around the droplets is well approximated by potential flow. Others $[8,15]$ have felt it necessary to consider some means for interpolating between viscous and potential flow to predict real decontamination rates. Not everyone has agreed with the interpolation methods that have been described in the literature [16].

Widely used expressions for the efficiency of aerosol collection as a result of impaction are:
a. Potential Flow Regime

$$
\begin{array}{ll}
\in(\mathrm{imp}, \text { pot })=0 & \text { for Stk } \leq 0.0833 \\
\epsilon(\mathrm{imp}, \text { pot })=[\mathrm{Stk} /(\mathrm{Stk}+\delta)]^{2} & \text { for Stk } \geq 0.2 \\
\epsilon(\mathrm{imp}, \text { pot })=8.57[\mathrm{Stk} /(\mathrm{Stk}+\delta)]^{2}(\mathrm{Stk}-0.083336) & \text { for } 0.08333<\text { Stk }<0.2
\end{array}
$$

b. Viscous Flow Regime

$$
\begin{array}{ll}
\in(\mathrm{imp}, \text { visc })=0 & \text { for Stk } \leq 1.214 \\
\in(\mathrm{imp}, \text { visc })=\left[1+\frac{0.75 \ln (2 \text { Stk })}{(\text { Stk - 1.214)}}\right]^{-2} & \text { for Stk }>1.214
\end{array}
$$

c. Transition Flow Regime

$$
\epsilon(\mathrm{imp}, \text { trans })=\frac{\in(\mathrm{imp}, \text { visc })+\operatorname{Re}_{\mathrm{d}} \in(\mathrm{imp}, \text { pot }) / 60}{1+\operatorname{Re}_{\mathrm{d}} / 60}
$$

where

$$
\begin{aligned}
\mathrm{Stk} & =\mathrm{d}_{\mathrm{p}}^{2} \rho_{\mathrm{g}} \mathrm{U}_{\mathrm{T}} / 9 \mu_{\mathrm{g}} \mathrm{D}_{\mathrm{d}}(\mathrm{e}) \chi \\
\mathrm{Re}_{\mathrm{d}} & =\mathrm{U}_{\mathrm{T}} \rho_{\mathrm{g}} \mathrm{D}_{\mathrm{d}}(\mathrm{e}) / \mu_{\mathrm{g}} \\
\chi & =\text { dynamic shape factor for the particles } \\
\delta & =\text { uncertain constant cited to have values between } 0.25 \text { and } 0.75
\end{aligned}
$$

Note there are really two models here. All real flows are in the transition regime. One model is based on the assumption that real flows are similar to potential flows so the impaction efficiency is given by $\in$ (imp, pot). The other model uses $\in$ (imp, trans) for the impaction efficiency. Plots of $E$ (imp, pot) and $\in$ (imp, trans) against aerosol particle size are shown in Figure 17 for droplets of various sizes falling through air at 298 K and 1 atmosphere pressure.

Expressions for the efficiency of aerosol capture by interception are:
a. Potential Flow Regime

$$
\epsilon(\text { int, pot })=3 \gamma \mathrm{~d}_{\mathrm{p}} / \mathrm{D}_{\mathrm{d}}(\mathrm{e})
$$

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Figure $17 \epsilon$ (imp, trans) and $\epsilon(\operatorname{imp}, p o t)$ as functions of aerosol particle size for a $\mathbf{6 0 0} \boldsymbol{\mu m}$ drop
b. Viscous Flow Regime

$$
E(\text { int, visc })=1.5\left(\gamma \mathrm{~d}_{\mathrm{p}} / \mathrm{D}_{\mathrm{d}}(\mathrm{e})\right)^{2} /\left(1+\gamma \mathrm{d}_{\mathrm{p}} / \mathrm{D}_{\mathrm{d}}(\mathrm{e})\right)^{1 / 3}
$$

## c. Transition Flow Regime

$$
\epsilon(\text { int, trans })=\frac{\in(\text { int, visc })+\operatorname{Re}_{\mathrm{d}} \in(\text { int, pot }) / 60}{1+\operatorname{Re}_{\mathrm{d}} / 60}
$$

where $\gamma$ is the collision shape factor for the aerosol particles.
The capture efficiency for the viscous flow regime deserves comment. Lee and Gieseke [21] have reviewed the various approximations for interception efficiency. Under Stokes-flow conditions, the efficiency is given by:

$$
\epsilon(\text { int, visc })=(1+\mathrm{I})^{2}\left[1-1.5 /(1+\mathrm{I})+0.5 /(1+\mathrm{I})^{2}\right]
$$

where

$$
\mathrm{I}=\gamma \mathrm{d}_{\mathrm{p}} / \mathrm{D}_{\mathrm{d}}^{\prime}(\mathrm{e})
$$

Lee and Gieseke note the following approximations that have been made to this expression:

- $1.5 \mathrm{I}^{2}-0.25 \mathrm{I}^{3} /(1+\mathrm{I})$
- $1.45 \mathrm{I}^{2}$
- $1.5 \mathrm{I}^{2}$
- $1.5 \mathrm{I}^{2} /(1+\mathrm{I})^{\mathrm{m}}+\frac{(3 \mathrm{~m}-1)}{4}\left[\frac{\mathrm{I}^{3}}{(1+\mathrm{I})^{\mathrm{m}}+\mathrm{I}}\right]$

Lee and Gieseke [21] recommended the last of these approximations with $m=1 / 3$ as the better approximation to the actual Stokes flow efficiency. They also note that the presence of many collectors affects the collection efficiency. For an array of collectors occupying a volume fraction $\alpha$, they cite as the collection efficiency:

$$
\in(\text { int, visc })=\left(1 / \mathrm{K}_{\mathrm{s}}\right)\left[(1+\mathrm{l})^{2}-1.5(1+\mathrm{I})+0.5 /(1+\mathrm{I})+\mathrm{f}(\alpha)\right]
$$

where

$$
\mathrm{K}_{\mathrm{s}}=1-(9 / 5) \alpha^{1 / 3}+\alpha-0.2 \alpha^{2}
$$

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$$
\mathrm{f}(\alpha)=\alpha\left[0.2 /(1+\mathrm{I})+0.5(1+\mathrm{I})^{2}-0.3(1+\mathrm{I})^{4}\right]
$$

Plots of the interception efficiency calculated with various models are shown in Figure 18.
Aerosol capture by diffusion processes presents some conceptual problems involving the treatment of convection. Some of the expressions available for the efficiency of aerosol capture by diffusion are:

$$
\begin{aligned}
& \epsilon(\text { dif })=2.18 \mathrm{Pe}^{-1 / 2} \text { for } \mathrm{d}_{\mathrm{p}} / \mathrm{D}_{\mathrm{d}}(\mathrm{e})<0.3 \mathrm{Pe}^{-1 / 2} \\
& \epsilon(\text { dif })=\left[2 \mathrm{Pe} \mathrm{D}_{\mathrm{d}}(\mathrm{e})\right]^{-1 / 2} \\
& \in(\text { dif })=3.18 \mathrm{Pe}^{-2 / 3} \\
& \in(\text { dif })=(4 / \mathrm{Pe})\left(2+0.557 \mathrm{Re}_{\mathrm{d}}{ }^{1 / 2} \mathrm{Sc}^{3 / 8}\right)
\end{aligned}
$$

where

$$
\begin{aligned}
\mathrm{Pe} & =\text { Peclet number }=\mathrm{Re}_{\mathrm{d}} \mathrm{Sc} \\
\mathrm{Sc} & =\text { Schmidt number }-\mu_{\mathrm{g}} / \rho_{\mathrm{g}} \widetilde{\mathscr{D}}_{\mathrm{p}} \\
\widetilde{\mathscr{D}}_{\mathrm{p}} & =\text { diffusion coefficient of particles } \\
& =\overline{\mathrm{c}} \mathrm{kT} / 3 \pi \mu_{\mathrm{g}} \mathrm{~d}_{\mathrm{g}} \\
\mathrm{k} & =\text { Boltzmann's constant }=1.38 \times 10^{-16} \mathrm{ergs} / \mathrm{K} \\
\overline{\mathrm{c}} & =\text { Cunningham slip correction } \\
& =1+\left[\frac{2 \lambda}{\mathrm{~d}_{\mathrm{p}}}\right]\left[1.257+0.4 \exp \left(-0.55 \mathrm{~d}_{\mathrm{p}} / \lambda\right)\right] \\
\lambda(\mathrm{cm}) & =\text { mean free path in the gas phase } \cong 2.3 \times 10^{-8} \mathrm{~T}(\mathrm{~K}) / \mathrm{P}(\mathrm{~atm})
\end{aligned}
$$

Great confidence cannot be placed in any of these expressions. The expressions are based on isolated spheres. There is, however, substantial evidence that in an array of spheres mass transport to one of the spheres is less than to an isolated sphere in the same flow conditions [22, 23]. Detailed results are available only for cases involving two equal size spheres [22-24]. At the limit of $\mathrm{Pe} \rightarrow 0$ where the Sherwood number for an isolated sphere is 2 , the Sherwood number for a paired sphere as a function of the separation is [24]:


Figure $18 \in$ (int, trans) and $\in$ (int, pot) as functions of aerosol particle size and water drop size

| Separation Divided <br> by Sphere Radius | Sherwood |
| :---: | :--- |
| $\infty$ | Number |

Where the Sherwood number is $\mathrm{k}_{\mathrm{m}} \mathrm{D}_{\mathrm{d}}(\mathrm{e}) / \mathscr{D}$ and $\mathrm{k}_{\mathrm{m}}$ is the mass transport coefficient.
Thus, the deviation increases as the spheres become closer. The obvious limit of 1.0 for the spheres is not reached until the two spheres are combined. The presence of the adjacent sphere drastically affects the angular distribution of the local Sherwood number around the sphere.

Useful results for randomly dispersed spheres with varying diameters do not appear to be available. The issue is troublesome because it can be anticipated that the wakes of large fast falling droplets could disturb the trajectories and the aerosol capture efficiencies of smaller droplets which are the most efficient at decontaminating the atmosphere.

The problem of combining the effects of all three aerosol capture mechanisms must also be addressed. Traditionally, it would be assumed that the three mechanisms would be completely independent. Then,

$$
\epsilon(\text { total })=\Theta(\mathrm{imp})+\in(\text { int })+\in(\text { dif })
$$

It is manifestly apparent that the three aerosol capture mechanisms are not entirely independent. An alternate expression for the overall efficiency of aerosol capture is [17]:

$$
\epsilon^{\prime}(\text { total })=1-(1-\in(\text { imp }))(1-\in(\text { int }))(1-\in(\text { dif }))
$$

Plots of $\epsilon^{\prime}$ (total) and $\in$ (total) against aerosol particle size for water drops 200, 400, 1000 and $2500 \mu \mathrm{~m}$ in diameter are shown in Figure 19. Note that there is a minimum in the overall efficiency of aerosol capture when plotted against aerosol particle size. At this minimum, aerosol particles are too big to be affected significantly by Brownian motion which is responsible for aerosol capture by diffusion. Yet, the aerosol particles are still small enough to have a high probability of eluding capture by impaction or interception.

A great deal of significance has been attached to this minimum in the aerosol capture efficiency. Though sprays may be effective agents for cleansing an atmosphere of general aerosols, they may be less effective at removing aerosols with sizes in the vicinity of the minimum. This minimum size, not coincidently, is the aerosol size most likely to be injected into the containment atmosphere by sources previously subjected to other decontamination processes such as decontamination by an


Figure $19 E^{\prime}$ (total), the compound model, and $\in$ (total), the additive model, as functions of aerosol particle size and water drop size

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overlying water pool or aerosol deposition during transport through the reactor coolant system. It is also the most likely aerosol particle size to be expected when vapors produced by revaporization in the reactor coolant system condense upon entering the cooler containment atmosphere.

Note, however, that the minimum in the overall efficiency curve is dependent on droplet size. The minimum in the overall efficiency curve for $200 \mu \mathrm{~m}$ droplets is shifted substantially from the minima in the efficiency curves for larger droplets. Much of the concern that some aerosols may be resistent to capture by sprays arises from analyses with models that describe sprays in terms of a single monodisperse droplet size [8]. Were these models to use a more realistic description of the spray in terms of a distribution of droplet sizes including droplets of about $200 \mu \mathrm{~m}$ diameter, much of the concern would disappear.

The discussions of aerosol capture efficiency also show that spray performance will depend very strongly on the size distribution of aerosols in the containment. Both the mean size and the breadth of the aerosol size distribution will affect the predicted performance of the containment spray. Further, the spray will alter the size distribution because very large and very small particles will be removed more efficiently than are particles near the size of minimum capture efficiency. The effectiveness of the spray will decrease as decontamination progresses.

Though the aerosol size distribution will significantly affect spray performance, the discussion of this uncertainty is deferred to Chapter III of this report. Suffice it here to say that two classes of aerosol size distributions need to be considered. The first class includes those aerosols injected into the containment from the original source without any significant modification by some aerosol attenuation system. The second class of aerosols are those injected into containment after first passing through some aerosol attenuation system such as a water pool or a filter system.

## E. Droplet Trajectories

Analyses of decontamination of containment atmospheres by spray droplets usually consider the droplet motion to be strictly downward and at the droplet terminal velocity. Certainly after a long fall distance, the droplet motions will be well-represented by this simple description. Before reaching this steady-state situation, the droplet motions are a good deal more complex. The first source of the complexity is that the nozzles need not be mounted so that they point directly downward. Indeed, the Model 1713-A (or Model 1713) nozzles are frequently mounted so that the centerlines of the nozzles point in a variety of directions to achieve more complete coverage of the containment cross-sectional area. Consequently, initial motions of the drops follow ballistic arcs.

The classic differential equations of droplet motions are [22]:

$$
\begin{aligned}
\frac{\mathrm{d} \mathrm{U}(\mathrm{x})}{\mathrm{dx}} & =-0.75 \rho_{\mathrm{g}}|\mathrm{U}| C_{D} \mathrm{U}(\mathrm{x}) / \rho_{\ell} D_{\mathrm{d}}(\mathrm{e}) \\
\frac{\mathrm{d} \mathrm{U}(\mathrm{y})}{\mathrm{dt}} & =\mathrm{g}\left(\rho_{\ell}-\rho_{\mathrm{g}}\right) / \rho_{\ell}-0.75 \rho_{\mathrm{g}}|\mathrm{U}| C_{D} \mathrm{U}(\mathrm{y}) / \rho_{\ell} D_{\mathrm{d}}(\mathrm{e}) \\
\frac{\mathrm{dx}}{\mathrm{dt}} & =\mathrm{U}(\mathrm{x}) \\
\frac{\mathrm{dy}}{\mathrm{dt}} & =\mathrm{U}(\mathrm{y})
\end{aligned}
$$

where

$$
\begin{aligned}
C_{D} & =\text { drag coefficient } \\
\mathrm{g} & =\text { acceleration due to gravity }=980 \mathrm{~cm} / \mathrm{s}^{2} \\
\mathrm{U}(\mathrm{x}) & =\text { radial component of droplet velocity } \\
\mathrm{U}(\mathrm{y}) & =\text { axial component of droplet velocity } \\
|\mathrm{U}| & =\text { droplet speed }=\sqrt{\left(\mathrm{U}(\mathrm{x})^{2}+\mathrm{U}(\mathrm{y})^{2}\right)} \\
\mathrm{x} & =\text { radial position relative to the nozzle } \\
y & =\text { axial position relative to the nozzle }
\end{aligned}
$$

The initial conditions for the differential equations for position are:

$$
\begin{aligned}
& x(t=0)=0 \\
& y(t=0)=0
\end{aligned}
$$

The initial conditions for the velocity equations are not as obvious. In principle, the initial speeds of the droplets are given by:

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$$
|U|=Q / A_{h} C
$$

where

$$
\begin{aligned}
& \mathrm{Q}=\text { volumetric flow rate } \cong 956 \mathrm{~cm}^{3} / \mathrm{s} \\
& \mathrm{~A}_{\mathrm{h}}=\text { nozzle flow area } \cong 0.713 \mathrm{~cm}^{2} \\
& \mathrm{C}=\text { discharge coefficient. }
\end{aligned}
$$

The discharge coefficients for the nozzles might be between 0.6 and 1. A discharge coefficient of about 0.75 has apparently been used in the study of spray trajectories reported in Reference 22. The observed pattern of the sprays can, in principle, be used to back-calculate a discharge coefficient. Available data on the spray patterns are, however, quite limited. Back-calculation of the discharge coefficient is somewhat sensitive to the droplet size used to define the spray pattern. Here, a discharge coefficient of 0.6 is assumed for the Model 1713-A and Model 1713 spray nozzles [59].

Droplet trajectories for droplets with diameters of 200 to $1000 \mu \mathrm{~m}$ are shown in Figures 20-22. Trajectories for a nozzle with its axis pointed directly downward are shown in Figure 20. Droplets larger than about $600 \mu \mathrm{~m}$ follow trajectories that conform well to the manufacturer's indicated spray pattern. Drag forces cause smaller droplets to lose quickly their horizontal components of motion. These smaller droplets follow trajectories that "fill-in" the hollow cone area of the initial spray envelope. Were a single, isolated spray nozzle of interest, it is evident that the droplet size distribution would be calculated to vary radically across the cross-section of the spray pattern. The trajectories of the small droplets separate the small droplets from larger droplets. Sweepout of small droplets by larger droplets could occur only in a small region of space.

Trajectories for water droplets of various sizes produced by a Model 1713-A nozzle with its axis pointed horizontally are shown in Figure 21. The envelope of the spray pattern is not defined by droplets of a particular size. Larger droplets travel for extended horizontal distances. Small droplets quickly lose their horizontal motion and fall across the trajectories of the larger droplets. The opportunities for collisions between small and large droplets are greater in this situation than in the situation with the nozzle pointed downward.

An even more complicated set of trajectories for droplets formed by a nozzle with its axis pointed at an angle $45^{\circ}$ above horizontal is shown in Figure 22.

The spray patterns for droplets produced by individual spray nozzles are not simple especially when nozzles can have orientations that are different than simply downward. Spray patterns and the opportunities for droplets to interact become even more complicated to analyze when the overlaps of the spray patterns produced by adjacent spray nozzles are considered. The elliptical cross-sections of spray envelopes defined by $800 \mu \mathrm{~m}$ droplets in horizontal planes about 3 m below nozzles on various headers in a particular spray system are shown in Figures 23 to 25. Patterns produced by only 13 of the nozzles on a header are shown in these figures. Inclusion of patterns from all nozzles on a header would produce an indecipherable figure. Overlaps of the patterns have been

## MODEL 1713-A SPRAY NOZZLE O DEG. CONFIGURATION



Figure 20 Trajectories of droplets of various sizes from a Model 1713-A spray nozzle pointed downward. Trajectories were calculated for droplets in air at 1 atmosphere pressure and 298 K .

## MODEL 1713-A SPRAY NOZZLE 90 DEG. CONFIGURATION



Figure 21 Trajectories of droplets of various sizes from a Model 1713-A spray nozzle pointed horizontally. Trajectories were calculated for droplets in air at 1 atmosphere pressure and 298 K .

## MODEL 1713-A SPRAY NOZZLE 45 DEG. CONFIGURATION



Figure 22 Trajectories of droplets of various sizes from a Model 1713-A spray nozzle pointed upward at a $45^{\circ}$ angle. Trajectories were calculated for droplets in air at 1 atmosphere pressure and 298 K.


Figure 23 Cross-sections for spray patterns produced by 13 nozzles on Header B in a particular containment spray system. Cross-sections are for a plane 3 m below the nozzles.


Figure 24 Cross-sections for spray patterns produced by 13 nozzles on Header D in a particular containment spray system. Cross-sections are for a plane 3 m below the nozzles.

Figure 25 Cross-sections for spray patterns produced by 13 nozzles on Header $\mathbf{F}$ in a particular containment spray system. Cross-sections are for a plane 3 m below the nozzles.
deliberately designed into the spray system. Projections of the cross-sections of all 3 header systems are shown in Figure 26.

The various headers in the spray system considered in making these figures are located at different elevations. Droplets produced by nozzles on one header would have lost much if not all of their horizontal motions by the time they arrive at the elevation of the next header. There is, then, an additional complication in the analysis of droplet trajectories and the opportunities for spray droplets to interact. Droplets produced by nozzles on higher headers will fall through the developing spray patterns produced by nozzles on headers at lower elevations. Again, complicated opportunities for droplet collisions would develop in regions immediately below the lower header.

Some efforts to mechanistically model spray droplet behavior have been undertaken [33]. These analyses include hydrodynamic effects of the reverse flow of gas caused by droplets falling through the atmosphere. This reverse flow can disturb the droplet trajectories from the simple ballistic trajectories discussed here. The gas flow is, however, affected by structures in the containment. Gas and droplet motions are also strongly coupled near the spray nozzles where droplet concentrations are high. Coupling of the gas and droplet motions could be expected to affect the efficiency of sweepout of smaller droplets by larger droplets. The detailed analysis of this hydrodynamic problem is, however, not yet entirely feasible and is not attempted here.

## F. Droplet Agglomeration

Because of drag and the overlap of spray patterns there is relative motion among droplets. This creates the opportunity for droplet collisions. Analyses of droplet collisions often portray the process as involving simple sweepout of slowly falling smaller droplets by larger, faster moving droplets. The discussion of droplet trajectories above make it evident that the interactions of droplets, at least in the vicinity of the spray nozzles, is not so simple. Collisions of droplets can take place because of differences in their horizontal components of velocity as well as differences in their vertical velocity components.

For this work, collisions of droplets in the regions where droplets have significant horizontal components of motion are neglected. It is regrettable that this approximation has to be made. But, the details of droplet motions and the interactions among droplets in this region appear to constitute a problem too difficult to address in this work. Solution of this problem would be peculiar to the spray system in question and very difficult to generalize on an overall basis. The effects of dropletdroplet interactions in the vicinity of spray nozzles and in the regions of pattern overlaps would distort the droplet size distribution from that observed to be produced by a single, isolated spray nozzle. As discussed above, the size distribution of spray droplets produced by even a single nozzle is uncertain. Droplet-droplet interactions in multiple nozzle systems add further to this uncertainty. The uncertainty is in the contributions to the distribution made by smaller droplets-those with diameters less than $200 \mu \mathrm{~m}$. Coalescence of droplets removes these fine droplets from the size spectrum. But, high velocity collisions of droplets can also generate such fine droplets [51,55]. Here the effects of droplet trajectories are considered only as implicit contributors to the uncertainty in the initial size distribution of droplets.

Analyses of the evolution of the droplet size distribution are restricted to an idealized situation in which all of the droplets are falling vertically at terminal velocities. Once below the region of


Figure 26 Projection of the spray pattern cross-sections of all three headers. Note that pattems are shown for only a subset of adjacent nozzles on each beader.
dynamic, transient droplet motion, which is the first few meters below the nozzle, droplet motions are just in the downward direction. During the fall of droplets through the containment atmosphere, larger droplets will sweep out smaller droplets. A steady-state droplet size distribution will develop in the containment atmosphere. Consider $N_{0}$ droplets with a distribution in sizes such that there are $N(i)=f(i) N_{0}$ droplets with diameters between $D_{d}(i)$ and $D_{d}(i+1)$. For calculational purposes, it is convenient to assume initially that all droplets in size class i , that is, droplets with diameters between $\mathrm{D}_{\mathrm{d}}(\mathrm{i})$ and $\mathrm{D}_{\mathrm{d}}(\mathrm{i}+1)$ have the same diameter. The droplet size distribution will change as droplets fall and collide with each other. The sizes of droplets within a given size class will become distributed rather than constant because of coalescence of droplets of various sizes. Assume that the aerodynamic properties of all droplets in a size class $i$ are well represented by a droplet with radius $R(i)$. In general, the volumetric properties of droplets in the $i^{\text {th }}$ size class will not be represented well by a droplet of this size. These volumetric properties are therefore taken to be represented by a different droplet of radius, $S(i)$. Initially $R(i)$ and $S(i)$ are nearly equal. As the fall of the droplets progresses and droplet collisions resulting in coalescence occur, these representative droplet radii will change.

Since it has been assumed that all horizontal motions of the droplets have ceased, at least over some suitable time average, the containment and droplet fall can be treated one dimensionally. Mass balance requires that at a horizontal plane in the containment atmosphere:

$$
\sum_{i=1}^{N} n(i) V(i) \frac{4}{3} \pi S(i)^{3}=Q
$$

where
$N=$ number of droplet size classes
$\mathrm{n}(\mathrm{i})=$ number concentration of droplets in class i
$\mathrm{V}(\mathrm{i})=$ terminal velocity of a droplet of radius $\mathrm{R}(\mathrm{i})$
$S(i)=$ volume characteristic droplet radius for size class $i$
$\mathrm{Q}=$ volume flux of water into the containment produced by sprays.
A cross-sectional area for size class $i$ is defined by

$$
A(i)=\sum_{i=1}^{N} n(i) \pi R(i)^{2}
$$

Consider a subvolume defined by two horizontal planes at x and $\mathrm{x}+\mathrm{dx}$. A number balance of droplets of size class $j$ in this region is:

Number of $j$ class droplets that enter the volume in time dt

| Number of $\mathbf{j}$ class <br> droplets that <br> leave the volume <br> in time dt |
| :--- |$=$| Number of $\mathbf{j}$ class |
| :--- |
| droplets removed |
| by agglomeration |
| in time dt |$\quad-$| Number of $\mathbf{j}$ class |
| :--- |
| droplets created by |
| agglomeration in |
| time dt |

or

$$
[n(j, x)-n(j, x+d x)] V(j) A d t=\Delta N(j)-\psi(j)
$$

where

$$
\begin{aligned}
\mathrm{n}(\mathrm{j}, \mathrm{x}) & =\text { number concentration of } \mathrm{j} \text { class droplets at plane } \mathrm{x} \\
\mathrm{~V}(\mathrm{j}) & =\text { terminal velocity of } \mathrm{j} \text { class droplets } \\
\Delta \mathrm{N}(\mathrm{j}) & =\text { number of } \mathrm{j} \text { class droplets removed by agglomeration in time dt } \\
\psi(\mathrm{j}) & =\text { number of } \mathrm{j} \text { class droplets created by agglomeration in time } \mathrm{dt}
\end{aligned}
$$

A single droplet of size class $i$ such that $R(i)>R(j)$ falling a distance $d x$ will encounter $\Delta n(i, j)$ droplets of size class $j$ given by:

$$
\Delta n(i, j)=\pi(R(i)+R(j))^{2} n(j, x) \frac{V(i)-V(j)}{V(i)} d x
$$

During the period dt the number of i class droplets that enters the volume is given by:

$$
\mathrm{n}(\mathrm{i}, \mathrm{x}) \mathrm{V}(\mathrm{i}) \mathrm{Adt}
$$

If the efficiency with which a collision of $i$ and $j$ class droplets results in agglomeration is $\in(i, j)$, then from the above it is found that the number of j class droplets lost by sweepout by the larger i class droplets is:

$$
\Delta N(i>j)=\sum_{i=j+1}^{N} \in(i, j) \pi[R(i)+R(j)]^{2} n(j, x) n(i, x)[V(i)-V(j)] A d t d x
$$

By analogous arguments the number of j class droplets lost by collisions with smaller droplets is:

$$
\Delta N(j>k)=\sum_{k=1}^{j-1} \epsilon^{\prime}(j, k) \pi[R(j)+R(k)]^{2} n(j, x) n(k, x)[V(j)-V(k)] A d t d x
$$

where $\epsilon^{\prime}(\mathrm{j}, \mathrm{k})$ includes an additional term that indicates whether the agglomeration of a j class droplet and a k class droplet creates a droplet that is outside the range of sizes for the j class.

Were all the droplets within a size class to have exactly the same diameter, then, under the idealized assumptions for this analysis, there would be no collisions of droplets from the same size class. Because droplets within a class are not all the same size, and because rather large size ranges are used to define the boundaries of a size class, there can be collisions of droplets within the same size class. Coalescence of two droplets within a size class may yield a droplet that is outside the size range for the class. This type of collision reduces the population of the size class by 2 . On the other hand, depending on the upper and lower boundaries defining a size class, collisions of two droplets within the same size class may only yield a slightly larger droplet that is still within the size class. The population of the size class is then reduced by one.

Considering the limits for a size class, the expression of the loss of j class droplets by collisions with other $j$ class droplets can be constructed by analogy with expressions for collisions between droplets of different size classes. Recognizing that a collision can remove two droplets from the size class yields:

$$
\Delta \mathrm{N}(\mathrm{j}=\mathrm{j})=\epsilon^{\prime \prime}(\mathrm{j}, \mathrm{j}) \frac{\pi}{2}\left[\mathrm{D}_{\mathrm{d}}(\mathrm{j}+1)+\mathrm{D}_{\mathrm{d}}(\mathrm{j})\right]^{2} \mathrm{n}(\mathrm{j}, \mathrm{x})^{2} \Delta \mathrm{~V}(\mathrm{j}) A d x d t
$$

where

$$
\begin{aligned}
\Delta V & =\mathrm{V}\left(\mathrm{D}_{\mathrm{d}}(\mathrm{j}+\mathrm{i})-\mathrm{V}\left(\mathrm{D}_{\mathrm{d}}(\mathrm{j})\right)\right. \\
\mathrm{V}\left(\mathrm{D}_{\mathrm{d}}(\mathrm{j})\right) & =\text { terminal velocity of a droplet of diameter } \mathrm{D}_{\mathrm{d}}(\mathrm{j})
\end{aligned}
$$

The efficiency term, $\in$ " $(j, j)$, includes an expression for the probability that a collision results in coalescence and a term that indicates if the droplet produced by coalescence is outside the specified size limits for the $\mathrm{j}^{\text {th }}$ size class.

Then, the total number of j class droplets lost by collision in the spatial interval x to $\mathrm{x}+\mathrm{dx}$ is:

$$
\Delta N(j)=\Delta N(i>k)+\Delta N(j>k)+\Delta N(j=j)
$$

Formation of j class droplets by collisions of droplets in size classes k and l such that $\mathrm{j}>\mathrm{k}>\mathrm{l}$ can be analyzed in a similar fashion to yield:

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$$
\begin{aligned}
\psi(\mathrm{j})= & \sum_{\mathrm{k}=2}^{\mathrm{j}-1} \sum_{\ell=1}^{\mathrm{k}-1} \epsilon^{\prime}(\mathrm{k}, \ell) \pi[\mathrm{R}(\mathrm{k})+\mathrm{R}(\ell)]^{2} \mathrm{n}(\mathrm{k}, \mathrm{x}) \mathrm{n}(\ell, \mathrm{x})[\mathrm{V}(\mathrm{k})-\mathrm{V}(\ell)] A \mathrm{dt} \mathrm{dx} \\
& +\sum_{\mathrm{k}=1}^{\mathrm{j}-1} \epsilon^{\prime}(\mathrm{k}, \mathrm{k}) \frac{\pi}{4}\left[\mathrm{D}_{\mathrm{d}}(\mathrm{k}+1)+\mathrm{D}_{\mathrm{d}}(\mathrm{k})\right]^{2} \mathrm{n}(\mathrm{k}, \mathrm{x})^{2} \Delta \mathrm{~V}(\mathrm{k}) \mathrm{A} d t \mathrm{dx}
\end{aligned}
$$

Formation of j class droplets by collisions of two k class droplets can be estimated as was done for the loss of j class droplets by collisions of two j class droplets. Then, from a number balance on droplets of size class j :

$$
\begin{aligned}
\frac{-d n(j, x)}{d x}= & \sum_{i=j+1}^{N} \in(i, j) \pi[R(i)+R(j)]^{2} n(j, x) n(i, x) \frac{[V(i)-V(j)]}{V(j)} \\
& +\sum_{k=1}^{j-1} \epsilon(j, k) \pi[R(j)+R(k)]^{2} n(k, x) n(j, x) \frac{[V(j)-V(k)]}{V(j)} \\
& +\epsilon^{\prime}(j, j) \frac{\pi}{2}\left[D_{d}(j+1)+D_{d}(j)\right]^{2} n(j, x)^{2} \frac{\Delta V(j)}{V(j)} \\
& -\sum_{k=2} \sum_{\ell=1}^{k-1} \epsilon^{\prime}(k, \ell) \pi[R(k)+R(\ell)]^{2} n(\ell, x) n(k, x) \frac{[V(k)-V(\ell)]}{V(j)} \\
& \quad j-1 \\
& -\sum_{k=1} \epsilon^{\prime}(k, k) \frac{\pi}{4}\left[D_{d}(k+1)+D_{d}(k)\right]^{2} n(k, x)^{2} \frac{\Delta V(k)}{V(j)}
\end{aligned}
$$

Differential equations of this type for $\mathrm{j}=1$ to N were solved by an explicit, Eulerian method to obtain the spatial distribution in droplet sizes. Term-by-term examinations were necessary to account for the changes in the water volume and total cross-sectional area in a size class. Values of $R(j)$ and $S(j)$ for each size class were adjusted at the end of each spatial step to reflect these changes. Mass balance was maintained by adjusting $N_{0}$ such that

$$
\frac{N_{0}^{\prime} \sum_{j=1}^{N} n(j, x) V(j) \frac{4}{3} \pi S(j)^{3}}{\Omega}=Q
$$

where

$$
\Omega=\sum_{i=1}^{N} n(i, x)
$$

Values of $n(j, x)$ for the next spatial step were calculated from

$$
\mathrm{n}(\mathrm{j}, \mathrm{x}+\mathrm{dx})=\mathrm{N}_{\mathrm{O}} \mathrm{n}(\mathrm{j}, \mathrm{x}) / \Omega
$$

Plots of the various terms in the differential equation are shown in Figure 27 for an example distribution with essentially a constant number density of particles across the size spectrum (see Figure 28). Sweepout of droplets by larger droplets is the largest term in the equation for droplets smaller than about $1000 \mu \mathrm{~m}$. The next largest terms for this example are losses and gains of droplets in a class by agglomeration with smaller droplets. These terms become the dominant terms for the largest droplets in the distribution. Agglomeration processes within a droplet size class do make contributions to the evolution of the size distribution of droplets. These contributions are, however, about one order of magnitude less than other contributions.

The evolution of an example droplet size distribution during free fall is shown in Figure 28. This figure is a plot of the quantity

$$
\left[\mathrm{f}_{\mathrm{i}}(\mathrm{~N}) / \log _{10} \Delta \mathrm{D}\right]
$$

where

$$
\begin{aligned}
& f_{i}(N)=\text { fraction of the total number of droplets in the size class } i \\
& \Delta D=D(i+1) / D(i)
\end{aligned}
$$

against the characteristic diameter of droplets in the $\mathrm{i}^{\text {th }}$ size class. For the example, an initial distribution was selected such that the plotted quantity was the same for all size classes. Dramatic changes in the distribution occur in the first 50 cm of free fall as the larger droplets sweep out smaller droplets. Evolution in the distribution of droplet sizes slows once droplets smaller than about $100 \mu \mathrm{~m}$ have been removed. After free fall of about 1050 cm , nearly all droplets smaller than $200 \mu \mathrm{~m}$ have been eliminated from the distribution.


Figure 27 Terms in the differential equation for the steady state number distribution of droplets in containment. These terms are calculated for the initial size distribution shown in Figure 28.


Figure 28 Evolution of a droplet size distribution during free fall. The vertical axis is the logarithm of the fraction of the total number of droplets in a size bin, $f(N)$, divided by the logarithm of the ratio of the droplet sizes defining the bin limits. Curves are labelled by the distance from the start of free fall.

The evolution of a more realistic droplet size distribution is shown in Figure 29. The initial number distribution was formulated from a hypothesized log-normal mass distribution:

$$
f(M)=0.5(1+\operatorname{erf}(p))
$$

where

$$
\begin{aligned}
\mathrm{f}(\mathrm{M}) & =\text { fraction of the mass of droplets with sizes less than } \mathrm{D} \\
\mathrm{p} & =\ln (\mathrm{D} / \mu) / \sqrt{(2)} \ln \sigma \\
\mu & =\text { mean droplet size }=426 \mu \mathrm{~m} \\
\sigma & =\text { geometric standard deviation }=1.654 \\
\operatorname{erf}(\mathrm{p}) & =\text { error function of } \mathrm{p}=\frac{2}{\sqrt{\pi}} \int_{0}^{\mathrm{p}} \exp \left(-\mathrm{y}^{2}\right) \mathrm{dy}
\end{aligned}
$$

It is evident from these results why there might be difficulty in obtaining reliable droplet size data from single spray nozzles. In the region of 0-3 meters below the nozzle, the distribution is undergoing very significant changes as a result of droplet-droplet interactions. Measurements of droplet size distributions in this region will be complicated because spatial variations in the distribution are so large. In particular, the contributions to the distribution made by droplets $200 \mu \mathrm{~m}$ and less in size vary dramatically in this region. Needless to say, it is precisely in this region that most attempts to measure the droplet size have been made.

## G. Efficiency of Droplet-Droplet Interactions

Simple contact between water droplets does not necessarily result in the coalescence of the droplets. Colliding water droplets may recoil, splatter or otherwise be disrupted as well as coalescing [53]. Droplet-droplet collisions that are not head-on collisions are likely not to coalesce even at low, terminal velocities [47-52]. The greatest diversity of behavior occurs for droplets of nearly equal size. A criterion for coalescence of droplets is that the collision energy be less than 15 ergs [54]. At terminal velocities of interest here, the collisions nearly always satisfy this criterion. The same could not be said for droplet collisions in the immediate vicinity of the spray nozzle. Even when the energy criterion is satisfied, the efficiency with which collision of droplets results in coalescence is not unity. A commonly cited efficiency for coalescence during water droplet collisions is [47]:

$$
\in(i, j)=\frac{R(i)^{2}}{[R(i)+R(j)]^{2}} \quad \text { for } R(i)>R(j)
$$

The evolution in the size distributions of droplets discussed in the previous subsection were computed using this expression for the efficiency with which droplet-droplet interactions result in


Figure 29 Evolution of a realistic spray droplet size distribution using for the efficiency of dropletdroplet interactions $\in(i, j)=1 /(1+R(j) / R(i))^{2}$

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coalescence. This expression for the efficiency of collisions yielding coalescence indicates that the minimum efficiency is 0.25 . Experimental evidence indicates that lower efficiencies can occur [48]. Efficiencies calculated based on theoretical arguments [48] and supported by the limited data that are available are compared in Figure 30 to the efficiencies calculated with the usual expression. As droplets become of similar size, the efficiency of collisions falls below that calculated with the simple expression above. An alternate bound on the efficiencies shown in the figure is given by:

$$
\in(i, j)= \begin{cases}1-8 R(j) / R(i) & \text { for } R(j) / R(i)<0.125 \\ 0 & \text { otherwise }\end{cases}
$$

The evolution of the initial droplet size distribution shown in Figure 31 is based on this efficiency. In comparison to the case calculated with the usual description of the coalescence of colliding droplets, this case of a lower bound efficiency yields much less change in the droplet size distribution. Still, this alternate description of collision efficiency indicates that droplets smaller than $100 \mu \mathrm{~m}$ in diameter are removed from the distribution quite quickly.

## H. Droplet-Structure Interactions

Reactor containment buildings are not simple, open volumes. Immediately below spray headers there is often a substantial open space. But, eventually, falling drops begin to encounter equipment, structures and operating floor of the reactor. The drywells of Mark I containments are well-known for the congestion that can interfere in the free fall of water droplets.

The flooring in many reactor containments is grating or so-called "expanded sheet metal." Below the flooring are large volumes which, in a severe reactor accident, would hold aerosol-contaminated gas. It is of interest to know, then, if spray droplets, after hitting structures and the open flooring, would continue to sweep aerosols from the containment atmosphere. Certainly, in the case of the design basis analysis of iodine removal from containment atmospheres, it has been traditional to assume droplets are ineffective once they have hit a structure or the flooring.

Baker et al. [42] have reviewed the observed behaviors of droplets of all sorts when they contact surfaces. The behaviors observed are of three types:

- droplets can bounce off the structure,
- droplets can spread on the surface, or
- droplets can splash.

Droplets bounce because of an "air cushion" that forms as they interact with the solid surface. Spreading and coalescence of droplets on surfaces of interest for the analysis of spray performance would lead, eventually, to the reformation of droplets as the liquid film formed by the droplets drained off the structure surface. Splashing of droplets can lead to the formation of more, smaller drops.


Figure 30 Comparison of the usual collision efficiency (bold line) to theoretical analyses of the collision efficiency of a $500 \mu \mathrm{~m}$ droplet (symbols) and the alternate model $\in=$ 1-8 R(j)/R(i) (dashed line)


Figure 31 Evolution of droplet size distribution calculated using as the efficiency of droplet coalescence $\in(i, j)=1-8 R(j) / R(i)$ for $R(j) / R(i)<0.125$. The evolution shown in this figure should be compared to that in Figure 29.

The behaviors of water droplets when they encounter solid surfaces can be categorized into regimes according to the Weber number of the drop, We, given by:

$$
\mathrm{We}=\mathrm{D}_{\mathrm{d}}(\mathrm{e}) \rho_{\ell} \mathrm{U}_{\mathrm{T}}^{2} / \sigma_{\ell}
$$

An example of categorization is shown in Figure 32. For low Weber numbers, typically We $<5$, droplets bounce when they hit structures [43]. The droplets retain only about 6 percent of their incident kinetic energy when they bounce off structures [44]. At higher Weber numbers, the droplets coalesce with the water film. Water that coalesces to form a film on surfaces is lost for decontamination purposes unless it can contribute to drips off the surface. Baker et al. [42] indicate the drops formed by dripping have a diameter calculated from Taylor instability given by:

$$
\mathrm{D}_{\mathrm{d}}(\mathrm{e})=3 \sqrt{\frac{\sigma}{\rho_{\ell} \mathrm{g}}}
$$

Such drops are huge in comparison to the drops formed by spray nozzles and would be ineffective at removing aerosols. Baker et al. noted, however, that when these drops detach from the surface, four or five smaller droplets are formed as the liquid filaments rupture. These smaller drops might be more effective at decontamination.

At Weber numbers of about 65, water droplets striking wet surfaces begin to splash. About 50 percent of the incident water droplet mass is splashed [44, 45, 46] in droplets with median diameters of about 0.1 to 0.05 cm at Weber numbers of about 1500. At a Weber number of 3000 essentially 100 percent of the incident water volume is splashed. The splashed water droplets would be effective at removing aerosols, but few spray droplets would have such high Weber numbers at their terminal velocities.

Clearly, there are opportunities for water to continue to be effective at atmosphere decontamination even after the water in the form of droplets has encountered a structure. Because of the wide diversity of reactor containments and the structures housed within these containments, no attempt has been made in this work to include analyses of droplet interactions with structures.

## I. Summary of the Uncertainties in the Spray Decontamination Process

The subsections above describe the essential physical processes that lead to aerosol removal from a containment atmosphere by spray droplets. The processes depend on the number and size distribution of the spray droplets, the size distribution of the aerosols and the distance the droplets fall within a containment atmosphere. There is sufficient understanding of the many physical phenomena involved in aerosol removal by sprays, that a detailed, mechanistic model of the process can be formulated. The major modeling difficulties arise in describing the interactions among droplets and the complex droplet trajectories in the immediate vicinity of spray nozzles.


Figure 32 Regimes of droplet behavior on impact with surfaces

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Predictions of the efficiency of spray removal of aerosol obtained with the detailed mechanistic model would, however, still be uncertain. The uncertainty arises from several sources. There is, of course, omnipresent uncertainty about the atmosphere conditions that will exist in reactor containments during severe reactor accidents. Containment temperatures, pressures, and the amount of water available to drive the sprays depend on details of both the reactor and the reactor accident. The exact size distribution of the aerosols suspended in the containment is another uncertainty that depends on the details of the rector accidents that are known only to within fairly large, uncertainty limits. Definitive measurements of the size distribution of spray droplets have not been made.

There are also phenomenological uncertainties. The proper model to describe aerosol capture by processes such as interception is not known. The summation of the efficiencies of various aerosol capture processes is not known. The efficiency with which two colliding droplets will coalesce to form a larger droplet is not well known.

These and the other uncertainties that afflict the prediction of spray performance are summarized in Table 5. In the next chapter of this report, a quantitative analysis of the uncertainty in predictions of spray performance is described.

Some phenomena that lead to aerosol capture have been neglected. Notably, the diffusiophoretic deposition of particles on droplets as steam produced by decay heat condenses on droplets has been neglected. Steam produced late in an accident condenses on both structures and spray droplets. The relative importance of deposition on droplets depends on the details of the accident and the extent to which the structures have been heated during the accident. Analysis of the diffusiophoretic deposition of particles late in an accident is too dependent on the specific design of the reactor to be considered here. In any event, the contribution of this diffusiophoretic deposition late in the accident is thought to be small.

Table 5 Summary of uncertain quantities

| Symbols | Description | Range | Probability density function |
| :---: | :---: | :---: | :---: |
| a | Parameter to change the mix of fine and coarse droplets in the initial size distribution of the water droplets | 0-1 | uniform |
| $\mathbf{P}$ | Total pressure in containment (atms) | 1.1-9.0 | uniform |
| $\mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right)$ | Partial pressure of steam in the containment atmosphere (atms) | 0.1-7.9 | uniform |
| $\boldsymbol{\delta}(\mathrm{H})$ | $\left[\mathrm{P}(\mathrm{CO})+\mathrm{P}\left(\mathrm{CO}_{2}\right)\right] / \mathrm{P}\left(\mathrm{H}_{2}\right)$ in the containment atmosphere | 0.02 to 3 | log-uniform |
| $\delta(C)$ | $\mathrm{P}(\mathrm{CO}) / \mathrm{P}\left(\mathrm{CO}_{2}\right)$ in the containment atmosphere | $10^{-4}-1$ | log-uniform |
| $\mu_{p}$ | Mean size of aerosols in the containment atmosphere |  |  |
| Case 1 <br> Case 2 |  | $\begin{gathered} 1.5-5.5 \\ 0.15-0.65 \end{gathered}$ | uniform uniform |
| $\boldsymbol{\sigma}^{\mathbf{p}}$ | Geometric standard deviation of aerosols in the containment atmosphere |  |  |
| Case 1 |  | 1.6-3.7 | uniform |
| Case 2 |  | 1.1-1.6 | correlated to the mean |
| $\chi$ | Dynamic shape factor for aerosols | 1-4 | $\begin{aligned} & \text { log-normal } \\ & \mu=0.3 \end{aligned}$ |
| $\boldsymbol{\gamma}$ | Collision shape factor for aerosols |  | $\sigma=3.04$ |
| $\delta \sigma_{\boldsymbol{l}}$ | Uncertainty in the surface tension of water | -0.1 to 0.1 | uniform |
| $\delta \rho_{\ell}$ | Uncertainty in the density of water | 0 to 0.05 | uniform |

Table 5 Summary of uncertain quantities (Concluded)

| Symbols | Description | Range | Probability density function |
| :---: | :---: | :---: | :---: |
| $\delta \mu_{\mathrm{g}}$ | Uncertainty in the estimated viscosity of the containment gases | -0.04 to 0.04 | uniform |
| $\epsilon(1)$ | Uncertainty in the model of droplet shape | 0-1 | uniform |
| $\epsilon(2)$ | Uncertainty in the terminal velocities of droplets | 0-1 | uniform |
| $\delta(\mathrm{i})$ | Uncertainty in the applicable flows regime model for aerosol capture by impaction and interception | 0-1 | uniform |
| $\delta(t)$ | Uncertainty in the interpolation between viscous and potential flow regimes |  | $\begin{aligned} & \text { log-normal } \\ & \mu=60 \\ & \sigma=4 \end{aligned}$ |
| $\boldsymbol{\delta}$ | Uncertain parameter in impaction efficiency model | 0.25-0.75 | uniform |
| $\delta($ dif $)$ | Uncertainty in the model for aerosol capture by diffusion | 0-1 | uniform |
| $\delta$ (sum) | Uncertainty in the summation of aerosol capture efficiencies by impaction, interception and diffusion | 0-1 | uniform |
| $\delta($ drop ) | Uncertainty in the efficiency with which dropletdroplet interactions result in coalescence of the drops | 0-1 | uniform |

## III. Uncertainty Analysis

## A. Overview of the Approach to Uncertainty

The discussions presented in Chapter II show that there are many uncertainties in the modeling of aerosol capture by spray droplets. In addition to the phenomenological uncertainties, there are, of course, also uncertainties in the boundary and initial conditions. These uncertainties in the boundary and initial conditions originate in the analyses of accident scenarios and are propagated into the analysis of spray performance. These accident-dependent uncertainties include such things as the pressure in the containment or the drywell and the availability of pumps to drive the sprays.

The "expert opinion" approach to uncertainty has been avoided here. Instead, an approach to develop quantitative uncertainty analysis first articulated by Theofanous [31] and pursued by Powers [32] has been adopted. The approach involves six steps.

The first two steps in this approach are:

1) develop a mechanistic description of the phenomenon or process of interest, and
2) identify uncertain parameters or submodels in this description of the phenomenon or process.

These first two steps for the analysis of uncertainties in the prediction of spray decontamination of an aerosol-laden containment atmosphere are described in the previous chapter (Chapter II) of this report.

The next two steps in the uncertainty analysis process are:
3) define ranges for the uncertain parameters in the model, and
4) develop probability density functions for the values of uncertain parameters within these ranges.

These two steps are described for the spray decontamination process in this chapter (Chapter III).
The final two steps in the uncertainty analysis are:
5) conduct multiple evaluations of the phenomenon or process with the mechanistic model (described in Step 1) while sampling from the distributions to obtain parameter values used in each calculation, and
6) accumulate the results of the model predictions to develop a quantitative description of the uncertainty.

These last two steps are described for spray decontamination in Chapter IV of this report.
Some of the mechanical details of this uncertainty analysis are described elsewhere [11]. The approach does not completely avoid expert opinion. Expert opinion is, in fact, essential in the development of a mechanistic model and in the definition of ranges for uncertain parameter values
and the definition of alternate models for critical phenomena contributing to the issue of interest. This use of expert opinion is inherently different than the use of expert opinion in more traditional approaches to uncertainty. Expert opinion is here focused on detailed phenomenological issues for which there are data and, consequently, real expertise can be developed. Often, questions requiring the opinions of experts can be of sufficient detail that the "opinions" can be drawn from the scientific literature as they have been, in the main, here.

This chapter presents a summary of the uncertainties that arise in the prediction of aerosol removal by sprays. The uncertainties that are examined include phenomenological uncertainties discussed in Chapter II and uncertainties in boundary or initial conditions. Ranges for the uncertain quantities are defined based on literature data or limitations imposed by physical laws. Finally, probability density functions are developed for values of the uncertain quantities within their respective ranges. These probability density functions are used in the Monte Carlo uncertainty analysis described in the next chapter of this report.

Many of the uncertain features of spray performance are readily ascribed to individual parameters with uncertain values. It is, however, also important to recognize uncertainty in the predictions of spray performance that arise because of uncertainties concerning which model to use to describe processes and phenomena that affect spray performance. To incorporate this type of uncertainty into the Monte Carlo uncertainty analyses discussed in Chapter IV, it is convenient to define a parameter that reflects uncertainty in the applicable model. This is done here in one of two ways. The first of these is a weighted averaging of model predictions. This averaging method is applied when there are two or more available models that could be used to describe the same phenomena or process but the models have different parameterization or different functional dependencies. A typical example might be different correlations of the convective enhancement of diffusive mass transport to a sphere. Denote the prediction of the models to be used in the evaluation of spray performance as $\pi$. Let the value predicted by model A to be $\pi(\mathrm{A})$ and the value predicted by model B be $\pi(\mathrm{B})$. Then, a parameter $\xi$ is defined to have values uniformly distributed over the range of 0 to 1 and the value of the model predictions used in the analysis is given by:

$$
\pi=\xi \pi(\mathrm{A})+(1-\xi) \pi(\mathrm{B})
$$

The second method used to account for model uncertainty is applied when the competing models are based on different views of the physical processes responsible for the predicted quantities. Again, define the predictions of models $A$ and $B$ to be $\pi(A)$ and $\pi(B)$, respectively. Then, a parameter $\delta$ is defined to have values uniformly distributed between 0 and 1 . The value of the quantity of interest used in an analysis of spray performance is given by:

$$
\pi= \begin{cases}\pi(\mathrm{A}) & \text { for } 0<\delta \leq 0.5 \\ \pi(\mathrm{~B}) & \text { for } 0.5<\delta \leq 1.0\end{cases}
$$

Definition of probability density functions to be used for uncertain quantities is a subjective process. The authors know of no algorithm or non-controversial way to do this. There have been attempts reported in the literature to define optimal approaches to the definition of these probability density

## Uncertainty

functions [34]. A rule-based approach is adopted here. All parameters used here are non-negative. Three possible types of probability density functions are considered:

- the uniform distribution,
- the log-uniform distribution, and
- the $\log$-normal distribution.

The uniform distribution has a constant probability density within the range of values defined for the parameter of interest. The log-uniform distribution has a constant probability density for the logarithm of the parameter of interest within its specified range. The probability densities for the uniform and log-uniform distributions are, of course, zero for values of the parameters outside their respective ranges. The third distribution used here is the log-normal function. For a parametric quantity, Z , the probability density is given by:

$$
f(\mathrm{Z})=\frac{1}{\ln \sigma \sqrt{(2 \pi)}} \exp \left[-\frac{(\ln (\mathrm{Z} / \mu))^{2}}{2(\ln \sigma)^{2}}\right]
$$

where

$$
\begin{aligned}
& \mu=\text { mean of the distribution } \\
& \sigma=\text { geometric standard deviation }
\end{aligned}
$$

The log-normal distribution specifies finite probability densities for all positive values of the parametric quantity even if the values are outside the probable ranges for values discussed above. Here, the lower limit of the specified range is taken to be the 1 percentile of the cumulative distribution and the upper limit is taken to be the 99 percentile value when the distribution function is log-normal. Thus, the upper limit, $\mathrm{x}(\mathrm{u})$, and the lower limit, $\mathrm{x}(\mathrm{L})$, of the range of parametric values specify the mean and standard deviation of the distribution:

$$
\begin{aligned}
& \ln \mu=(1 / 2)(\ln x(\mathrm{u})+\ln \mathrm{x}(\mathrm{~L})) \\
& \ln \sigma=\ln (\mathrm{x}(\mathrm{u}) / \mathrm{x}(\mathrm{~L})) / 4.65269
\end{aligned}
$$

The three probability density functions used here are shown schematically in Figure 33. Note that the log-uniform density function would, if plotted against the logarithms of the parameter values, be a constant. When plotted against the actual parameter values, the probability density varies with the reciprocal of the parameter value.

The "rules" adopted here for the selection of the distribution functions are as follows:

1. The log-normal distribution is selected for those parameters for which values are known well enough that means and standard deviations can be meaningfully calculated.

# Assumed <br> Probability Densities for the Uncertain Variables 



Figure 33 Schematic illustrations of the probability density functions used for the uncertainty analyses

## Uncertainty

2. Uniform distributions are used for uncertain parameters whose meaningful values span a range of less than one order of magnitude.
3. The log-uniform distribution is used when meaningful values of the parameter span more than one order of magnitude.

The various parameters and quantities considered to be uncertain in the analyses presented here are summarized in Table 5. Allowable ranges for the values of these quantities and the probability density functions assumed for the values within the ranges are also indicated in the table. Some effort has been made to decompose issues sufficiently that the uncertainties are uncorrelated. Where it has not been possible to entirely avoid correlations among uncertain quantities, the necessary modifications to the density functions are described below as part of the discussions of each of the individual uncertain quantities.

## B. Discussion of Individual Uncertainties

Fourteen areas of uncertainty involving 20 uncertain quantities have been identified as possibly affecting predictions of spray performance. In the subsections below, each of the uncertainties considered in the analysis of spray performance is discussed. The principal objectives of the discussions are to define the ranges of values the uncertain quantities can assume along with the probability density functions defined for values within the ranges. The bases for the ranges of values have often been defined in the discussion of phenomena and processes in Chapter II. Only when some elaboration is thought necessary is there further discussion of the bases for the ranges.

## 1. Uncertainty in the Initial Droplet Size

The complexities and uncertainties in the initial droplet size of the spray have been discussed at length in Chapter II. In summary, these uncertainties arise because:

- different measurement techniques yield different spray droplet size distributions,
- the size distributions are, apparently, sensitive to the purity of the water, and
- overlap of spray patterns of adjacent nozzles provides the opportunity for larger droplets to sweep out smaller droplets.

The primary uncertainty is the contribution to the spray made by small droplets. The question is, are droplets less than $200 \mu \mathrm{~m}$ in diameter as numerous as is indicated by spray size distributions obtained by the freeze-and-sieve technique with tap water or are they less abundant as indicated by results obtained with boric acid-sodium hydroxide solution? To reflect this uncertainty, it is assumed here that the spray droplet size distribution can be resolved into two modified log-normal components. The mix between these components is taken to be uncertain. The modifications made to the log-normal distributions are to truncate the components at lower and upper limits to the sizes of droplets that can initially be present. The upper limit is taken to be $3000 \mu \mathrm{~m}$. This is a limit drawn simply from the empirical èvidence presented in Chapter II that there appear to be few droplets larger than this. The lower limit is taken to be $39 \mu \mathrm{~m}$ based on the experience that it takes special effort to form droplets smaller than about this size.

The two component distributions are taken to have means of $125 \mu \mathrm{~m}$ and $650 \mu \mathrm{~m}$, respectively, and geometric standard deviations of 2.0. These parameters are admittedly somewhat arbitrary. At best they are based on a qualitative inspection of the data on spray size distributions shown in Chapter II. It is possible to consider these parameters as uncertain. But, a sufficient account of the uncertainty concerning the initial size distribution of water droplets is probably provided by varying the contributions the two components make to the overall distribution.

The cumulative number distribution of spray droplets is then given by:

$$
\mathrm{F}\left(\mathrm{D}_{\mathrm{d}}(\mathrm{e})<\mathrm{D}\right)=\frac{\mathrm{aN}_{1}}{2}\left\{0.90712+\operatorname{erf}\left(\mathrm{Z}_{1}\right)\right\}+\frac{(1-\mathrm{a}) \mathrm{N}_{2}}{2}\left\{0.99996+\operatorname{erf}\left(\mathrm{Z}_{2}\right)\right\}
$$

where

$$
\left.\begin{array}{rl}
\mathrm{a} & =\text { uncertain parameter uniformly distributed between } 0 \text { and } 1 \\
\mathrm{~N}_{1}= & \text { normalization factor to account for the cutoff of the distribution at } 39 \text { and } \\
& 3000 \mu \mathrm{~m}=1.0487
\end{array}\right\} \begin{aligned}
& \mathrm{N}_{2}=\begin{array}{l}
\text { normalization factor to account for the cutoff of the distribution at } 39 \text { and } \\
3000 \mu \mathrm{~m}=1.0139
\end{array} \\
& \mathrm{Z}_{1}=\ln (\mathrm{D} / 125) / \sqrt{2} \ln 2 \\
& \mathrm{Z}_{2}=\ln (\mathrm{D} / 650) / \sqrt{2} \ln 2 \\
& \mathrm{D}= \\
& \text { critical droplet } \operatorname{size} \text { in } \mu \mathrm{m} .
\end{aligned}
$$

$\operatorname{erf}(Z)=$ error function of $Z=\frac{2}{\sqrt{\pi}} \int_{0}^{Z} \exp \left(-y^{2}\right) d y$
Plots of the number distribution against droplet size for various values of the parameter a are shown in Figure 34. As the parameter varies from 0 to 1 the importance of fine droplets in the distribution increases.

## 2. Uncertainty in the Droplet Shape

Only the largest water droplets of interest here distort significantly from spherical during fall through the containment atmosphere. Typically, at atmospheric pressure, only droplets larger than 0.1 cm distort. Two models for the distortion are described in Chapter II. A simple model developed by Pruppacher and Beard [12] considers distortion of droplets larger than 0.1. This model can be designated model A. A more complicated model that considers distortions when the Eotvos


Figure 34 Variations in the droplet size distribution with variations in the uncertain parameter a. Cumulative probability is in percent.
number, $\mathrm{E}_{\mathrm{O}}$, is greater than 0.4 is designated model B . An uncertain parameter, $\in(1)$, which is uniformly distributed over the range of 0 to 1 , is used to select between these models. Model $\mathbf{A}$ is used when $\in(1)<0.5$ and Model B is used otherwise. Note that the distorted geometry of the droplets is not used in the computations of the terminal velocities. The droplet distortions are implicitly considered in the correlations for terminal velocities.

## 3. Uncertainty in the Droplet Terminal Velocities

There is a limited data base for the terminal velocities of water droplets for conditions more extreme than those encountered in weather systems. That is, the elevated temperatures and pressures in reactor containment atmospheres under severe accident conditions have not been considered in the development of the data base for the terminal velocities of water droplets. Three models for the terminal velocities of water droplets are described in Chapter II of this report. Model C in these discussions is really restricted in its applications to droplets that are larger than those of interest here. Consequently, Model $C$ is not considered here. Model A is the best fit model for terminal velocities of water droplets in air and Model B has been used by others to extrapolate the data base[13]:

- Model A:

$$
\operatorname{Re} \stackrel{(\mathrm{A})}{\mathrm{T}}=\exp \left[-3.126+1.013 \ln \mathrm{~N}_{\mathrm{D}}-0.01912\left(\ln \mathrm{~N}_{\mathrm{D}}\right)^{2}\right]
$$

- Model B:

$$
\operatorname{Re}_{\mathrm{T}}^{(\mathrm{B})}= \begin{cases}1.62 \mathrm{E}_{\mathrm{O}}^{0.755} \mathrm{M}^{-0.25} & \text { for } 0.5<\mathrm{E}_{\mathrm{O}} \leq 1.84 \\ 1.83 \mathrm{E}_{\mathrm{O}}^{0.555} \mathrm{M}^{-0.25} & \text { for } 1.84<\mathrm{E}_{\mathrm{O}} \leq 5.0 \\ 2.0 \mathrm{E}_{\mathrm{O}}^{0.5} \mathrm{M}^{-0.25} & \text { for } \mathrm{E}_{\mathrm{O}}>5\end{cases}
$$

$$
\begin{aligned}
\operatorname{Re} \stackrel{(\mathrm{B})}{\mathrm{T}}= & \mathrm{N}_{\mathrm{D}} / 24-1.7569 \times 10^{-4} \mathrm{~N}_{\mathrm{D}}^{2}+6.9252 \times 10^{-7} \mathrm{~N}_{\mathrm{D}}{ }^{3} \\
& -2.3027 \times 10^{-10} \mathrm{~N}_{\mathrm{D}}^{4} \quad \text { for } \mathrm{N}_{\mathrm{D}}<73 ; \mathrm{E}_{\mathrm{O}} \leq 0.5 ; \operatorname{Re}_{\mathrm{T}}<2.37
\end{aligned}
$$

## Uncertainty

$$
\begin{gathered}
\log _{10} \operatorname{Re}_{\mathrm{T}}^{(\mathrm{B})}=-1.7095+1.33438 \log _{10} \mathrm{~N}_{\mathrm{D}}-0.11591\left(\log _{10} \mathrm{~N}_{\mathrm{D}}\right)^{2} \\
\text { for } 73<\mathrm{N}_{\mathrm{D}}<580 ; \mathrm{E}_{\mathrm{O}} \leq 0.5 ; 2.37<\operatorname{Re}_{\mathrm{T}}<12.2 \\
\log _{10} \mathrm{Re}_{\mathrm{T}}^{(\mathrm{B})}=-1.81391+1.34671 \log _{10} \mathrm{~N}_{\mathrm{D}}-0.12427\left(\log _{10} \mathrm{~N}_{\mathrm{D}}\right)^{2} \\
\\
+0.006344\left(\log _{10} \mathrm{~N}_{\mathrm{D}}\right)^{3} \\
\text { for } \mathrm{N}_{\mathrm{D}}>580 ; \mathrm{E}_{\mathrm{O}} \leq 0.5 ; 12.2<\operatorname{Re}_{\mathrm{T}}<6350
\end{gathered}
$$

To account for the uncertainty in the extrapolation of water droplet terminal velocities, an uncertain parameter $\in(2)$ which is uniformly distributed over the range 0 to 1 is defined. The terminal velocity is then calculated from:

$$
\operatorname{Re}_{\mathrm{T}}=\epsilon(2) \operatorname{Re}_{\mathrm{T}}^{(\mathrm{A})}+[1-\epsilon(2)] \operatorname{Re}_{\mathrm{T}}^{(\mathrm{B})}
$$

## 4. Uncertainty in the Surface Tension of Water

The surface tension of water in the droplets affects the deformation and consequently the drag on the droplets as they fall through the atmosphere. Surface tension effects may be responsible for the changes in the water droplet size distributions when boric acid-sodium hydroxide solutions are used rather than tap water in sprays (see Chapter II).

The surface tension of pure water at temperatures of interest here is quite well known. The effects of additives such as boric acid, sodium hydroxide and the like as well as the effects of contaminants that accumulate in the waters during spray operation are the sources of uncertainty in the surface tension of water. None of the additives or contaminants usually considered to be in the spray waters is a particularly strong surface-active agent. Rather, the effects of these species, when dissolved in water, are milder bulk chemistry effects. As discussed elsewhere [11], dissolved species can either increase or decrease the surface tension of water. At the concentrations expected to arise in spray waters, the magnitude of the effect ought not be greater than a 10 percent increase or reduction in the surface tension of pure water. Here the surface tension of the spray water is taken to be:

$$
\sigma_{\ell}=\sigma(\mathrm{w})\left(1+\delta \sigma_{\ell}\right)
$$

where

$$
\begin{aligned}
\sigma(w) & =\text { surface tension of pure water } \\
\delta \sigma_{\ell} & =\text { uncertain parameter uniformly distributed over the range of } 0.1 \text { to }-0.1
\end{aligned}
$$

## 5. Uncertainty in the Density of Water

The density of pure water is, of course, very well known. The temperature-dependent density of pure water is shown in Table 4. But, water used in sprays is likely to contain additives such as boric acid at concentrations of up to 4000 ppm . In most reactor systems, the containment sprays operate in a recirculation mode. As decontamination progresses, the water used for the sprays becomes more heavily contaminated with dissolved and suspended materials. Consequently, the water density is taken here to be given by:

$$
\rho(\ell)=\rho \text { (pure water) }\left[1+\delta \rho_{\ell}\right]
$$

where $\delta \rho_{\ell}$ is an uncertain variable with values uniformly distributed over the range of 0 to 0.05 .

## 6. Uncertainty in the Viscosities of Gas Mixtures

The viscosity of the gas phase has a pervasive effect on spray performance. Viscosity affects droplet sizes, shapes, and terminal velocities. Fairly complicated gas mixtures of air, steam, and the gaseous products of concrete decomposition can develop in reactor containments under severe accident conditions. The viscosities of individual constituents of the gas phase have been measured with reasonable accuracy. The viscosities of the mixtures thought to be possible during severe accidents have not been studied. To estimate the viscosities of mixtures the Herning-Zipperer formula is used

$$
\mu_{\mathrm{g}}(\text { mixture })=\frac{\sum_{\mathrm{i}}(\mathrm{P}(\mathrm{i}) / \mathrm{P}) \mu_{\mathrm{g}}(\mathrm{i}) \sqrt{(\mathrm{Mw}(\mathrm{i}))}}{\sum_{\mathrm{i}}(\mathrm{P}(\mathrm{i}) / \mathrm{P}) \sqrt{(\mathrm{Mw}(\mathrm{i}))}}
$$

where the summations are over the constituents of the mixture (taking air as a constituent species) and $\mathrm{Mw}(\mathrm{i})$ is the molecular weight of the $\mathrm{i}^{\text {th }}$ gas species. This estimation formula has proven to give results accurate to about 2 percent for $\mathrm{CO}-\mathrm{H}_{2}$ gas mixtures at 298 K [36]. Another test of the estimation formula is to compare its predictions for air-steam mixtures to the more involved formula suggested by Knudsen [35]:

$$
\mu(\text { mixture })=\frac{\mu(\text { air })}{1+\mathrm{P}(\text { steam }) \phi / \mathrm{P}(\text { air })}+\frac{\mu(\text { steam })}{1+\mathrm{P}(\text { air }) \psi / \mathrm{P}(\text { steam })}
$$

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where

$$
\begin{aligned}
\mu \text { (air) } & =2.3013 \times 10^{-6} \mathrm{~T}^{0.768} \text { poises } \\
\mu \text { (steam) } & =9.75 \times 10^{-7} \mathrm{~T} /(1+207 / \mathrm{T}) \text { poises } \\
\phi & =\frac{\left\{1+\left[\frac{\mu \text { (air) }}{\mu(\text { steam })}\right]^{1 / 2} 0.884\right\}^{2}}{4.56525} \\
\psi & =\frac{\left\{1+\left[\frac{\mu \text { (steam) }}{\mu(\text { air })}\right]^{1 / 2} 1.134\right\}^{2}}{3.60331}
\end{aligned}
$$

Results obtained in this comparison are shown in Table 6. Again, it is found that the HerningZipperer formula produces predictions that agree to within about 4 percent with predictions obtained with the presumedly more accurate correlation developed by Knudsen specifically for air-steam mixtures.

Predictions of the Herning-Zipperer formula are uniformly higher than those of the Knudsen Model. It is, however, not apparent that this systematic difference will occur for all mixtures. To account for uncertainty in the estimates of gas mixture viscosities, estimates of viscosity obtained from the Herning-Zipperer formula are considered uncertain by $\pm 4$ percent of the estimated value. The uncertainty is considered to be uniformly distributed over this range.

Viscosities of $\mathrm{CO}, \mathrm{CO}_{2}$, and $\mathrm{H}_{2}$ used in the Herning-Zipperer formula are:

$$
\begin{gathered}
\mu_{\mathrm{g}}(\mathrm{CO})=14.151 \times 10^{-6} \mathrm{~T}^{0.502012} /(1+117.178 / \mathrm{T}) \text { poise } \\
\mu_{\mathrm{g}}\left(\mathrm{CO}_{2}\right)=15.957 \times 10^{-6} \mathrm{~T}^{0.457212} /(1+246.744 / \mathrm{T}) \text { poise } \\
\mu_{\mathrm{g}}\left(\mathrm{H}_{2}\right)=1.5765 \times 10^{-6} \mathrm{~T}^{0.705712} /(1-3.378 / \mathrm{T}) \text { poise }
\end{gathered}
$$

## 7. Uncertainty in Droplet-Droplet Interactions

Sweepout of small water droplets by larger water droplets is an important factor in the prediction of the performance of containment sprays. Simple contact between two droplets does not necessarily lead to coalescence of the droplets. Two limiting models of the efficiency with which droplet collisions result in coalescence are described in Chapter II:

Table 6 Comparison of predictions of the viscosities of air/steam mixtures

|  | Total <br> pressure <br> (atms) | Steam partial <br> pressure <br> (atms) | Gas viscosity from <br> Herning-Zipperer model <br> (Poise) | Gas viscosity from <br> Knudsen model <br> (Poise) | Percent <br> difference |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 298 | 1.031 | 0.031 | $1.807 \times 10^{-4}$ | $1.798 \times 10^{-4}$ | 0.5 |
| 310 | 1.061 | 0.061 | $1.842 \times 10^{-4}$ |  | $1.826 \times 10^{-4}$ |

$$
E(A)=\frac{R(i)^{2}}{(R(i)+R(j))^{2}}
$$

and

$$
\epsilon(B)=\left\{\begin{array}{ll}
1-8 \frac{R(j)}{R(i)} & \text { for } R(j) / R(i)<0.125 \\
0 & \text { for } R(j) / R(i) \geq 0.125
\end{array} .\right.
$$

An uncertain parameter, $\delta$ (drop), is defined here to have values uniformly distributed over the range of 0 to 1 . This parameter is used to evaluate the efficiency of droplet coalescence in collisions from

$$
\epsilon=\delta(\text { drop }) \in(\mathrm{A})+[1-\delta(\text { drop })] \in(\mathrm{B})
$$

## 8. Uncertainty in Containment Pressure and Temperature

The pressure and the temperature in reactor containments is affected by operation of the sprays. The sprays can, of course, cool the atmosphere and condense steam. How much reduction in the pressure and temperature can be achieved with containment sprays depends on other aspects of the accident. In particular, the non-condensible gases generated during the accident are important and for this analysis they are considered uncertain. For this analysis, it is clear that pressures above the containment failure pressure are not of interest. The difficulties of estimating the ultimate failure pressures of reactor containments are well beyond the scope of this work. It is clear that few containments are capable of withstanding pressures in excess' of 9 atmospheres. Even if global analyses of a containment structure indicate higher pressure capabilities, it is likely that flaws or errors in construction would restrict pressure capabilities to less than 9 atmospheres.

Pressure in the reactor containment is determined by the amount of air originally in the containment, the vapor pressure of water, and the amount of non-condensible gas produced during core degradation and during core debris interactions with concrete. The concentrations of steam and noncondensible gas in the containment atmosphere vary markedly over the range of severe accidents that are hypothesized to occur at the various types of reactor containments found in the country. Prediction of these concentrations is still the subject of debate within the reactor safety community.

To account for the uncertainty in the pressure and composition of the containment atmosphere during spray operation, the following steps are taken:

1. the total pressure, P , in the containment is taken to be uncertain over the range of 1.1 to 9.0 atmospheres,
2. the partial pressure of steam is taken to be uncertain over the range of 0.1 to 7.8 atmospheres but is always less than the total pressure minus one atmosphere to account for the original air in containment,
3. the temperature of the atmosphere during spray operation is taken to be that temperature which yields the selected value of the steam partial pressure,
4. the partial pressures of hydrogen, carbon monoxide and carbon dioxide produced during core degradation complete the description of the composition of the containment atmosphere.

Note that the containment atmosphere is assumed to be saturated during spray operations. The transient period when sprays just begin to operate and to condense steam from the atmosphere is neglected in this work. It is assumed that the atmosphere can become quite hot to sustain steam partial pressures of up to 7.9 atmospheres because containment sprays do operate in a recirculation mode especially if they are used to attenuate the potential source term in the long-term phase of a severe accident. Sprays can draw water from sumps containing large inventories of radionuclides that heat the water by radioactive decay. The temperature of the containment atmosphere is calculated from a simple correlation of vapor pressure data for water:

$$
\ln \mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right)=-7.938 .16 / \mathrm{T}+88.912-12.1215 \ln (\mathrm{~T})+0.011079 \mathrm{~T}
$$

where $\mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right)$ is the partial pressure of water vapor in atmospheres.
Hydrogen is produced during severe reactor accidents predominantly by metal-water reactions as the core degrades within the reactor coolant system or as the core debris interacts with concrete. Metalwater reactions during steam explosions [56] or during other energetic events such as direct containment heating [57] can also produce hydrogen in the containment atmosphere. Radiolysis and corrosion of metals in the containment are negligible sources of hydrogen in severe reactor accidents [58]. Carbon monoxide and carbon dioxide in the containment atmosphere are thought to come from the interaction of core debris with concrete. Some carbon monoxide and carbon dioxide may also come from pyrolysis of organic materials in the containment under severe reactor accident conditions. The authors are not aware of any detailed analysis of this possible source of carbonaceous gases but suspect that this source is small in comparison to the production of carbon monoxide and carbon dioxide during core debris interactions with concrete.

The sum of the partial pressures of carbon monoxide and carbon dioxide relative to the partial pressure of hydrogen is affected by the extent to which hydrogen is produced during core degradation as well as by the composition of concrete used to construct the reactor. Concretes that use siliceous materials as the aggregate contain only about 1 weight percent carbon dioxide in the form of carbonates. Concretes that use calcareous aggregate can contain as much as 36 weight percent carbon dioxide in the form of carbonates that will decompose during interactions with high temperature core debris.

Carbon dioxide liberated from the concrete sparges through and reacts with core debris. The reactions produce carbon monoxide. Core debris of depths greater than $5-10 \mathrm{~cm}$ is capable of reacting with evolved carbon dioxide to the point that essentially an equilibrium mixture of carbon

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monoxide and carbon dioxide is formed. The partial pressure ratio of carbon monoxide and carbon dioxide in this equilibrium mixture depends on the reactivity of metals in the core debris. When metallic zirconium is present in the core debris interacting with the concrete, reactions of carbon dioxide to form carbon monoxide are nearly complete. The equilibrium partial pressure ratio is quite large:

$$
\frac{1}{\delta(\mathrm{C})}=\frac{\mathrm{P}(\mathrm{CO})}{\mathrm{P}\left(\mathrm{CO}_{2}\right)} \cong 10^{4}
$$

If chemical reactions have depleted the core debris of reactive metals such as zirconium and chromium so that iron is the most reactive metal remaining in the core debris, the reaction of carbon dioxide to form carbon monoxide is much less complete:

$$
\frac{1}{\delta(\mathrm{C})}=\frac{\mathrm{P}(\mathrm{CO})}{\mathrm{P}\left(\mathrm{CO}_{2}\right)} \cong 1
$$

The water content of concrete depends on the humidity of the atmosphere to which the concrete is exposed during operation of the reactor. Typically structural concretes in nuclear reactors are found to contain 5 to 8 weight percent water. When core debris interacts with concrete, this water is vaporized, sparges through the core debris and reacts to form hydrogen. Again, the extent of reaction of water vapor released from the concrete to form hydrogen depends on the reactivity of the core debris. Nearly complete reduction of water vapor occurs when metallic zirconium is present. Only about $2 / 3$ of the evolved water vapor is converted to hydrogen when iron is the most reactive constituent of core debris.

If core debris interactions with concrete were the only sources of hydrogen, carbon monoxide and carbon dioxide to the containment atmosphere, the partial pressure ratio

$$
\left[\mathrm{P}\left(\mathrm{CO}_{2}\right)+\mathrm{P}(\mathrm{CO})\right] / \mathrm{P}\left(\mathrm{H}_{2}\right)
$$

could be as high as 3 in the case of calcareous aggregate concrete. In the case of siliceous aggregate concrete, the ratio might be as low as 0.05 . Consideration of other sources of hydrogen production during severe reactor accidents leads to the conclusion that this ratio might be even lower.

Based on these considerations, the contributions to the atmospheric composition that are made by hydrogen, carbon monoxide and carbon dioxide are found from the following equations:

$$
\begin{aligned}
\mathrm{P}\left(\mathrm{H}_{2}\right) & =\Delta /(1+\delta(\mathrm{H})) \\
\mathrm{P}(\mathrm{CO}) & =\delta(\mathrm{H}) \Delta /[(1+\delta(\mathrm{H}))(1+\delta(\mathrm{C}))] \\
\mathrm{P}\left(\mathrm{CO}_{2}\right) & =\delta(\mathrm{C}) \delta(\mathrm{H}) \Delta /[(1+\delta(\mathrm{H}))(1+\delta(\mathrm{C}))]
\end{aligned}
$$

where

$$
\begin{aligned}
\Delta & =\mathrm{P}-\frac{\mathrm{T}}{298}-\mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right) \\
\mathrm{P} & =\text { total pressure in the containment } \\
\mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right) & =\text { partial pressure of steam } \\
\delta(\mathrm{H}) & =\left(\mathrm{P}(\mathrm{CO})+\mathrm{P}\left(\mathrm{CO}_{2}\right)\right) / \mathrm{P}\left(\mathrm{H}_{2}\right) \\
& =\text { uncertain parameter with a log-uniform distribution over the interval from } 0.02 \\
& \text { to } 3 \\
\delta(\mathrm{C}) & =\mathrm{P}\left(\mathrm{CO}_{2}\right) / \mathrm{P}(\mathrm{CO}) \\
& =\begin{array}{l}
\text { uncertain parameter with a log-uniform distribution over the range from } 1 \text { to } \\
\end{array}
\end{aligned}
$$

One of the biggest safety concerns that has been raised over spray operations during severe reactor accidents deals with the issue of hydrogen combustion. Sprays condense steam and can eliminate the so-called "steam-inerting" of containment atmospheres which increases the likelihood of hydrogen combustion [58]. The effect of hydrogen combustion events is to reduce the contributions made by oxygen and hydrogen to the containment atmosphere since, by postulate, hydrogen combustion events are assumed not to rupture containment. Relative to other factors that might affect the composition of the atmosphere, the changes that a hydrogen combustion event might have on the atmospheric composition during steady state spray operation are thought to be negligible.

## 9. Uncertainty in the Aerosol Size

Aerosols in the containment atmosphere can come from a variety of sources such as:

- in-vessel core degradation
- ex-vessel core debris interactions
- revaporization of volatile materials from the reactor coolant system.

Within the containment, the size spectrum of the aerosols will evolve as smaller particles agglomerate and larger particles deposit from the atmosphere. A number of computer codes have been developed to predict the evolution in aerosol particle sizes [37-41]. Where it has been possible to compare predictions to data, the evidence is that these codes are quite accurate at least for the purposes of reactor safety analyses. With continuing sources of aerosols to the reactor containment that are not too intense, a stable distribution of particle sizes is established in the containment

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atmosphere. While the distributions of aerosol sizes are not precisely log-normal, they are usually rather well approximated by such a distribution.

Some example size distributions for aerosols in containments during severe reactor accidents calculated with the Source Term Code Package are shown in Figure 35. The distributions indicate the aerosols in containment to be relatively large. Based on these results and results from the QUEST study [61], the aerosol size distributions present in containment are assumed here to be lognormally distributed in size with uncertain means and geometric standard deviations. The mass mean aerosol size is taken to be uniformly distributed over the size range of 1.5 to $5.5 \mu \mathrm{~m}$. The geometric standard deviation is taken to be uniformly distributed over the range of 1.6 to 3.7 .

It might be expected that the geometric standard deviation and the mass mean size are correlated. No evidence to support this suspicion could be found. Breadth in the size distribution as indicated by a large geometric standard deviation is more readily correlated with a continuing source of aerosol material to the containment atmosphere.

Dedicated attempts to mitigate the consequences of a severe reactor accident will affect the total mass suspended in the reactor containment atmosphere as well as the particle sizes of the containment aerosol. For instance, a water pool overlying core debris that is interacting with concrete will significantly reduce the total amount of aerosol that is lofted into the containment atmosphere by these ex-vessel interactions. The aerosol mass that is lofted will, however, be shifted to a particle size, $\sim 0.3 \pm 0.15 \mu \mathrm{~m}$, that resists additional filtration or removal. That is, the aerosol that emerges from a water pool can be highly persistent in the atmosphere. Further, the aerosol will have a very narrow distribution in sizes--geometric standard deviations of 1.1 to 1.6 depending on such factors as the depth of the water pool and the sub-cooling of the pool. The nearly monodisperse nature of the aerosol as well as its low concentration greatly slows agglomeration of the particles to sizes that can be easily removed from the atmosphere by natural and engineered processes. One of the principal interests in the performance of containment spray systems is, in fact, ability of spray systems to remove persistent, low concentration aerosols.

Consequently, a second "case" is defined here for the size distribution of aerosols in the containment atmosphere. This fine-particle case is based on considering the mean aerosol particle size to be uncertain within the range of 0.15 to $0.65 \mu \mathrm{~m}$ and the geometric standard deviation to be uncertain within the range of 1.4 and 3.2. The geometric standard deviation is taken to be linearly correlated with the mean size:

$$
\sigma=0.860+3.6 \mu
$$

where the mean particle size, $\mu$, is given in micrometers.

## 10. Uncertainty in Aerosol Shape Factors

The physical phenomena that lead to decontamination of an atmosphere by spray droplets have been described in Chapter II. The models presented in that chapter have been derived under the assumption that aerosol particles are spheres. It is unlikely that aerosols in the reactor containment under severe accident conditions will be spheres. The traditional and rather


Figure 35 Some examples of aerosol size distribution calculated to exist in containment atmospheres during severe reactor accidents

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approximate approach adopted in aerosol science to correct for the fact aerosols are not necessarily spheres is to introduce shape factors [16]. Two shape factors are pertinent to the discussions here:

- the dynamic shape factor $=\chi$, and
- the collision shape factor $=\gamma$.

These shape factors are defined by:

$$
\begin{aligned}
& \chi=\rho_{\mathrm{p}} \mathrm{~d}_{\mathrm{p}}^{2}(\mathrm{~m}) / \rho_{\mathrm{o}} \mathrm{~d}_{\mathrm{p}}(\mathrm{ae})^{2} \\
& \gamma=\mathrm{d}_{\mathrm{p}}(\mathrm{c}) / \mathrm{d}_{\mathrm{p}}(\mathrm{~m})
\end{aligned}
$$

where

$$
d_{p}(m)=\begin{aligned}
& \text { diameter of the nonporous spherical particle having the same mass as the particle } \\
& \text { of interest }
\end{aligned}
$$

$\mathrm{d}_{\mathrm{p}}(\mathrm{ae})=$ diameter of the unit density spherical particle with the same aerodynamic characteristics as the particle of interest
$\begin{aligned} \mathrm{d}_{\mathrm{p}}(\mathrm{c})= & \text { diameter of the spherical particle that would have the same collision characteristics } \\ & \text { as the particle of interest }\end{aligned}$

$$
\rho_{0}=1 \mathrm{~g} / \mathrm{cm}^{3}
$$

Brockman [19] has reviewed the data available on dynamic shape factors for aerosols of the type expected in reactor containments under severe accident conditions. Values of $\chi$ from nearly 1 to 9 have been observed. There have been no measurements of the collision shape factors for aerosols of the type of interest here. Values of the collision shape factor have been estimated based on the rates of agglomeration and settling of aerosols. Values as high as 10 have been suggested.

Very large values of the dynamic and collision shape factors are obtained only under dry conditions. Under high humidity conditions that are of interest here, water vapor can condense in the concave interstices created by the agglomeration of aerosol particles. The surface tension of the condensed water tends to compact the particles into spheres. Shape factors, then, reflect the packing density that can be achieved in agglomerated particles. Based on tests with $\mathrm{U}_{3} \mathrm{O}_{8}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$ aerosols [20], Kress [19] has suggested that under high humidity conditions an upper bound for both $\chi$ and $\gamma$ is 3 . Further, under these high humidity conditions $\chi=\gamma$. Values of the shape factors are especially likely to approach the theoretical packing limit for spheres [19] or about 1.1 in aerosols that are hygroscopic or deliquescent. The hygroscopicity of the aerosolized materials in a reactor containment is expected to be highly variable and is definitely uncertain [20].

The preponderance of data cited by Brockmann [19] indicates that the dynamic and the collision shape factors will be equal under conditions of high humidity. Then, here, it is assumed:

$$
\chi=\gamma
$$

Further, the high humidity limits the range of values the shape factors can assume. Typically values will not be greatly different from 1. Brockmann suggests the range of values is 1 to 4 [19], but notes large values are unusual. Here the dynamic and collision shape factors are assumed to have uncertain values log-normally distributed with means of 1.3 and geometric standard deviations of 3.04 so $\chi=\gamma=4$ is the 99 th percentile of the cumulative distribution. Then,

$$
\chi=\gamma=1+\delta(\mathrm{s})
$$

where $\delta(\mathrm{s})$ is lognormally distributed with a mean of 0.3 and a standard deviation of 3.04.

## 11. Uncertainty in the Collection Efficiency by Impaction and Interception

In the discussions of aerosol capture by impaction and interception in Chapter II, it is noted that correlations are known only for viscous and potential flow. Some have argued that because of the size disparity between droplets and the aerosol particles, potential flow results are adequate to describe the efficiency of aerosol capture by impaction and interception under real flow conditions. Others have argued some interpolation, which is itself uncertain as discussed below, between viscous and potential flow efficiencies is needed for real flow conditions.

To account for this uncertainty in the use of potential or transition flow approximations for aerosol capture efficiency, a parameter $\delta(i)$ is defined and taken to be uniformly distributed over the range of 0 to 1 . The impaction and interception efficiencies are then taken to be:

$$
\begin{aligned}
& \epsilon(\text { imp })= \begin{cases}\epsilon(\text { imp,pot }) & \text { for } \delta(i) \leq 0.5 \\
\epsilon(\text { imp,trans }) & \text { for } 0.5<\delta(i) \leq 1.0\end{cases} \\
& \epsilon(\text { int })= \begin{cases}\epsilon(\text { int,pot }) & \text { for } \delta(i) \leq 0.5 \\
\in(\text { int,trans }) & \text { for } 0.5<\delta(i) \leq 1.0\end{cases}
\end{aligned}
$$

Note that the selections of impaction and interception models are completely correlated. The uncertainty being described here is the applicability of potential flow as a descriptor of real flow conditions. The collection efficiencies are then determined by the decision on the applicability of the flow model. Note that the expression for $\in$ (imp,pot) includes another uncertain parameter $\delta$ discussed in Chapter II.

## Uncertainty

## 12. Uncertainty in the Collection Efficiencies in the Transition Flow Regime

The Langmuir interpolation [15] between results for the viscous flow regime and results for the potential flow regime is used in models for the efficiency of impaction and the efficiency of interception. The efficiencies of these processes for flows in the transition regime are given by:

$$
\in(\text { transition })=\frac{\in(\text { viscous })+\in(\text { potential }) R e_{d} / \delta(t)}{1+\operatorname{Re}_{\mathrm{d}} / \delta(\mathrm{t})}
$$

where

$$
\left.\begin{array}{rl}
\epsilon(\text { transition })= & \text { efficiency of impaction or interception at real Reynolds numbers } \\
\epsilon(\text { viscous })= & \text { efficiency of impaction or interception at Reynolds numbers approaching } \\
& \text { zero }
\end{array}\right\} \begin{aligned}
\epsilon(\text { potential })= & \begin{array}{l}
\text { efficiency of impaction or interception at Reynolds numbers approaching } \\
\\
\text { infinity }
\end{array} \\
\operatorname{Re}_{\mathrm{d}}= & \mathrm{U}_{\mathrm{T}} \mathrm{D}_{\mathrm{d}}(\mathrm{e}) \rho_{\mathrm{g}} / \mu_{\mathrm{g}}=\text { Reynolds number }
\end{aligned}
$$

In the Langmuir interpolation, $\delta(t)=60$. There is, however, no particular virtue to this selection. Here $\delta(t)$ is taken to be an uncertain parameter log-normally distributed with a mean value of 60 and a geometric standard deviation of 4 .

## 13. Uncertainty in the Collection Efficiency by Diffusion

Several possible models of aerosol collection by water droplets as a result of particle diffusion are described in Chapter II. Diffusion is by far the most uncertain of the aerosol capture processes. Yet, diffusion is an important mechanism for the removal of very small, low concentration aerosols. To account for uncertainty in the diffusion, a parameter, $\delta$ (dif), is defined and is considered to be uncertain over the range of $0-1$. The efficiency of aerosol capture by diffusion is then taken to be:

$$
\begin{array}{ll}
\epsilon(\text { dif })=\left[2 \mathrm{Pe} D_{\mathrm{d}}(\mathrm{e})\right]^{-1 / 2} & \text { for } 0<\delta(\text { dif }) \leq 2 / 3 \\
\epsilon(\text { dif })=3.18 \mathrm{Pe}^{-2 / 3} & \text { for } 1 / 3<\delta(\text { dif }) \leq 2 / 3 \\
\epsilon(\text { dif })=(4 / \mathrm{Pe})\left(2+0.557 \mathrm{Re}_{\mathrm{d}} 1 / 2 \mathrm{Sc}^{3 / 8}\right) & \text { for } 2 / 3<\delta(\text { dif }) \leq 1.0
\end{array}
$$

Note that the term $0.557 \mathrm{Re}_{\mathrm{d}}{ }^{1 / 2} \mathrm{Sc}^{3 / 8}$ in the third model of diffusion efficiency is, itself, uncertain. This uncertainty in the convective enhancement of diffusion is thought to be accounted for by the consideration of other models for diffusion efficiency.

## 14. Uncertainty in the Summation of Efficiencies

The uncertainty in summing aerosol collection efficiencies by diffusion, impaction and interception is whether these processes are adequately approximated as independently acting processes. To account for this uncertainty, two models are considered. The choice between these models is based on the value of the uncertain parameter $\delta($ sum ) which is uniformly distributed over the range of $0-1$ :

$$
\epsilon(\text { total })= \begin{cases}\epsilon(\text { dif })+\epsilon(\mathrm{imp})+\epsilon(\text { int }) & \text { for } 0<\delta(\text { sum }) \leq 0.5 \\ 1-(1-\epsilon(\text { dif }))(1-\epsilon(\text { imp }))(1-\epsilon(\text { int })) & \text { for } 0.5<\delta(\text { sum }) \leq 1.0\end{cases}
$$

## C. Summary Concerning Individual Uncertainties

The fourteen areas of uncertainty discussed above are represented by 20 uncertain quantities. Nine of these uncertain quantities stem from uncertainties in the details of the accident or the design of the plant in question:

1. containment pressure, $\mathbf{P}$
2. steam partial pressure, $\mathrm{P}\left(\mathrm{H}_{2} \mathrm{O}\right)$
3. ratio of partial pressures of carbonaceous gases to hydrogen in the containment atmosphere, $\delta(\mathrm{H})$
4. ratio of carbon monoxide partial pressure to the carbon dioxide partial pressure in the containment atmosphere, $\delta(\mathrm{C})$
5. the mean of the aerosol particle size distribution, $\mu_{\mathrm{p}}$
6. the geometric standard deviation of the aerosol particle size distribution, $\sigma_{\mathrm{p}}$
7. the dynamic shape factor of the aerosol, $\chi$
8. the collision shape factor of the aerosol, $\gamma$, and
9. the distribution of spray droplets between fine and coarse modes, a.

Three of the uncertain quantities have to do with properties of water and gas:
10. uncertainty in the surface tension of contaminated water, $\delta \sigma_{\ell}$
11. uncertainty in the density of contaminated water, $\delta \rho_{\ell}$, and
12. uncertainty in the predicted viscosity of a gas mixture, $\delta \mu_{\mathrm{g}}$.

## Uncertainty

Eight of the uncertain quantities have to do with the phenomena of droplet behavior and droplet aerosol interactions:
13. uncertainty in the appropriate model of droplet shape, $\in(\ell)$
14. uncertainty in the appropriate model for predicting terminal velocities of water droplets under severe accident conditions, $\in(2)$
15. uncertainty in the applicable flow regime for droplet particle interactions, $\delta(i)$
16. uncertainty in the interpolation of impaction and interception efficiencies in the transition flow regime, $\delta(t)$
17. uncertainty in the impaction efficiency model, $\delta$
18. uncertainty in the efficiency of droplet-particle interaction by diffusion, $\delta$ (diff)
19. uncertainty in the summation of efficiencies of droplet-particle interactions by impaction, interception and diffusion, $\delta$ (sum), and
20. uncertainty in the efficiency of droplet-droplet interactions, $\delta$ (drop).

Justifiable ranges for the values of these uncertain quantities and probability density functions for values within the ranges are summarized in Table 5. Exept for the treatment of aerosol size distribution parameters in Case 2 (see below), the uncertain parameters are assumed to be uncorrelated. These uncertain quantities are considered in the Monte Carlo analysis of uncertainty in spray performance described in the next chapter of this report.

## IV. Results of the Monte Carlo Uncertainty Analysis

The first objective of this report is to review the technical bases for the mechanistic calculation of aerosol removal from reactor containment atmospheres by sprays. This first objective has been addressed in Chapters II and III. Physical phenomena involved in the capture of aerosol particles by falling water drops were discussed at length in Chapter II. As part of these discussions, uncertain parameters and variables that will affect predictions of the aerosol removal process were identified. In Chapter III, realistic ranges for the values of these uncertain parameters and variables were determined and probability density functions for values within these ranges were defined. The uncertain parameters, the credible ranges for their values and the associated probability density functions are summarized in Table 5.

The second objective of this work is to apply a mechanistic model of spray removal of aerosols to a wide range of reactor accident conditions to obtain a meaningful sampling of atmosphere decontamination that can be achieved by sprays. The mechanistic model of spray removal of aerosols is described in this chapter (Chapter IV).

In Chapter V analyses of spray performance are discussed. The results of these analyses are used to construct cumulative probability distributions from which spray decontamination of containment atmospheres can be estimated with specified conservatism at known confidence levels.

The extent to which sprays will decontaminate an aerosol-laden atmosphere depends, of course, on the number of spray droplets falling through the atmosphere and the distance the water droplets fall. The water droplet flux into the containment atmosphere is under the control of the plant operators. The fall distance of water droplets is dependent on the particular containment design. These two variables which so strongly affect spray performance--water flux and fall distance--are not treated as uncertain variables. To facilitate applications of results obtained here, calculations are done for a variety of specific water fluxes and fall distances.

Calculations are done for three values of the volumetric water flux Q , i.e., $\mathrm{Q}=0.25,0.01$, and $0.001 \mathrm{~cm}^{3} \mathrm{H}_{2} \mathrm{O} / \mathrm{cm}^{2}$-s. Typical spray systems in pressurized water reactors produce water fluxes in the range of 0.01 to $0.06 \mathrm{~cm}^{3} \mathrm{H}_{2} \mathrm{O} / \mathrm{cm}^{2}-\mathrm{s}$. The lowest value of Q used in the calculations, $\mathrm{Q}=$ $0.001 \mathrm{~cm}^{3} \mathrm{H}_{2} \mathrm{O} / \mathrm{cm}^{2}-\mathrm{s}$, was taken to be indicative of the performance of a degraded spray system or one whose water discharge rate had been reduced as part of a strategy to manage severe accidents. The highest value of Q used in the calculations, $\mathrm{Q}=0.25 \mathrm{~cm}^{3} \mathrm{H}_{2} \mathrm{O} / \mathrm{cm}^{2}-\mathrm{s}$, is an upper bound on the capacity of spray systems in nuclear reactor containments known to the authors.

For each of the selected water fluxes, analyses were done for eight fall distances H , i.e., $\mathrm{H}=500$, $853,1000,1584,2000,3000,4000$ and 5000 cm . These values of the fall distances are believed to span the range of fall distances open to spray droplets in commercial nuclear power plants.

The mechanistic model of aerosol removal by sprays is built upon the knowledge of how a single droplet falling through an aerosol-laden containment atmosphere would scavenge particles. The scavenging process depends on (1) the properties and behavior of the water droplet, (2) the properties of the aerosol, and (3) the nature and properties of the containment atmosphere under accident conditions. Many of these things that affect the scavenging process are not now predictable to high accuracy for reactor accident conditions. There is, then, some uncertainty in predictions of spray performance for specified values of the water flux, Q , and the droplet fall distance, H . To

## Results

account for these uncertainties, a large number (400) of calculations were done with the mechanistic model for specific values of $\mathbf{Q}$ and $\mathbf{H}$ and varying values of the uncertain parameters. For each calculation, a set of parameter values was selected from the prescribed ranges weighted according to the probability density functions summarized in Table 5. Each result of a calculation is a sample of the uncertainty distribution for spray performance at the specified values of $Q$ and $H$. Results of the many calculations were accumulated to develop an estimate of the uncertainty distribution for spray performance at specific values of the water flux and fall distance. It was found in the analyses that spray performance is also dependent on the extent of atmosphere decontamination. Analyses were done, then, for six specific values of the extent of atmosphere decontamination. Altogether, 144 uncertainty distributions for spray removal of aerosols from a containment atmosphere were developed. An additional 48 uncertainty distributions for spray performance in conjunction with water pools overlying core debris were derived.

The uncertainty distributions produced in these analyses are then used in Chapter V of this report to develop simplified models of spray removal of aerosols. These simplified models permit interpolation of the results of calculations with the mechanistic model to other values of water flux, fall distance and the extent of decontamination. Because the simplified models are based on quantitative uncertainty distributions for spray performance obtained with the detailed mechanistic model, they can be used to provide estimates of spray performance at specified levels of conservatism.

## A. Model Description

The mechanistic model of aerosol removal by sprays used for the uncertainty analysis is based on the phenomena and correlations presented in Chapter II.

A number of simplifying assumptions have been made to make the analyses of spray removal of aerosols more tractable. It is assumed that in the spatial region of the containment where spray decontamination is occurring, all droplets have lost any horizontal components of their motions and are falling vertically downward at their terminal velocities. Droplet position, x , is measured downward from a horizontal plane of origin to the containment floor at position H . It is assumed that the aerosol suspended in the containment atmosphere is homogeneously distributed so that the size distribution of the aerosol is independent of location in the sprayed region. Aerosol agglomeration and aerosol removal by processes other than the action of spray (such as settling, diffusiophoresis to the walls, etc.) is neglected.

Major steps in the calculation of spray performance are:

- select, randomly, the values of uncertain quantities,
- calculate the steady-state population and size distribution of water droplets throughout the containment atmosphere,
- evaluate the rates of capture of aerosol particles in various size classes by water droplets, and
- accumulate the results in terms of an overall rate of aerosol removal.

This analysis sequence is done for each of the 24 combinations of fall distance and water flux described above. As will be discussed further below, the efficiency of spray removal of aerosol particles from the atmosphere depends on the extent to which the aerosol size distribution has been altered by the actions of spray droplets earlier. Analyses were done for six levels of decontamination, $\mathrm{DF}=1.1,2,3.3,10,100$, and 1000.

Uncertain parameters and models that affect predictions of spray performance are discussed at length in Chapter II of this report. Values of the uncertain parameters used in each calculation were selected according to the probability density function hypothesized for each parameter. The selection was done by solving the equation below for $\mathrm{X}_{\mathrm{o}}$ :

$$
\text { nnd } \#=\operatorname{Pr}\left(\mathrm{x}<\mathrm{X}_{\mathrm{o}}\right)
$$

where

$$
\begin{aligned}
\text { mad } \# & =\text { random number between } 0 \text { and } 1.0 \\
\mathrm{x} & =\text { value of the uncertain quantity } \\
\mathrm{X}_{\mathrm{o}} & =\text { selected value of the uncertain quantity } \\
\operatorname{Pr}\left(\mathrm{x}<\mathrm{X}_{\mathrm{o}}\right) & =\text { cumulative probability that } \mathrm{x} \text { is less than or equal to } \mathrm{X}_{\mathrm{o}}
\end{aligned}
$$

The inversion needed to obtain the selected parameter values from this equation was done with a Newton-Raphson root-solving routine. The random numbers needed in the selection process were obtained with a congruent, sequential random number generator. Numbers produced by this generator were "shuffled" randomly to avoid any periodicity in the generator's characteristics [62].

As described in Chapter II, the number density and size distribution of water droplets change with distance from the origin plane. These changes affect the efficiency with which the spray removes aerosol particles. Because large spray droplets collide with smaller droplets, the spray becomes less efficient with increasing fall distance. The steady-state, spatial, size distribution of water droplets was calculated at horizontal planes in the sprayed volume using an explicit, Eulerian, differential equation solver. The initial droplet size distribution was divided into 18 "bins" or size intervals. The limits on these bins are listed in Table 7. The volumetric properties of droplets within a bin were taken to be represented initially by a droplet whose diameter is given by

$$
\mathrm{D}_{\mathrm{d}}(\mathrm{v})=\left\{\left[\mathrm{D}(\mathrm{i})^{3}+\mathrm{D}(\mathrm{i}+1)^{3}\right] / 2\right\}^{1 / 3}
$$

where $D(i)$ and $D(i+1)$ are the upper and lower limits of the size bin. The hydrodynamic and aerosol capture properties of droplets in a particular bin were taken to be represented initially by a droplet whose diameter is given by:

Results

Table 7 Droplet size "bins"

| Bin <br> number | Size range <br> $(\mu \mathrm{m})$ |
| :---: | :---: |
| 1 | $2000-3000$ |
| 2 | $1587-2000$ |
| 3 | $1260-1587$ |
| 4 | $1000-1260$ |
| 5 | $794-1000$ |
| 6 | $630-794$ |
| 7 | $500-630$ |
| 8 | $397-500$ |
| 9 | $315-397$ |
| 10 | $250-315$ |
| 11 | $198-250$ |
| 12 | $157-198$ |
| 13 | $125-157$ |
| 14 | $99-125$ |
| 15 | $79-99$ |
| 16 | $62-79$ |
| 17 | $50-62$ |
| 18 | $39-50$ |

$$
D_{\mathrm{d}}(\mathrm{~h})=\left\{\left[\mathrm{D}(\mathrm{i})^{2}+\mathrm{D}(\mathrm{i}+1)^{2}\right] / 2\right\}^{1 / 2}
$$

Values of $D_{d}(v)$ and $D_{d}(h)$ were adjusted as droplets were added to or removed from the bin during the fall through the sprayed volume. Calculations of the size distributions were done at spatial intervals selected so that the population of any bin did not change by more than 25 percent. Spatial intervals were limited, however, to be smaller than 20 cm and larger than 1 cm . Some numerical tests showed that the size distributions calculated to be present at distances greater than 500 cm below the starting point of droplet fall were not significantly sensitive to the details of these limits on the changes in the droplet size distribution. Care was taken throughout the calculation of the droplet size distribution to assure water volume was conserved.

Capture of aerosol particulate by falling water droplets was also done using an explicit Eulerian solver. The calculations of aerosol capture were done for the same spatial intervals used in the calculation of the droplet size distribution. For these calculations, the droplet size distribution calculated for the bottom of the spatial interval was assumed to exist over the entire interval. Calculations using the droplet size distribution present at the top of the spatial interval did not yield significantly different results.

For the analysis of aerosol capture, the aerosol size distributions were divided into 20 size bins. The limits on these size bins were selected so that initially each bin contained 5 percent of the aerosol mass. The properties of particles within each bin were assumed to be represented by a particle with the mass average diameter of particles in the bin.

Capture rates were computed for aerosols in each size bin by droplets of each size class. The results were then summed to determine the overall rate of aerosol removal. That is, the decontamination coefficient for aerosols in the $\mathrm{j}^{\text {th }}$ size class is defined by

$$
-\frac{1}{M(j)} \frac{d M(j)}{d t}=\lambda(j)
$$

where $M(j)$ is the mass concentration of aerosols in the $\mathrm{j}^{\text {th }}$ size class. The value of $\lambda(\mathrm{j})$ is determined by the capture efficiencies of droplets in all size classes and the fall distance:

$$
\lambda(j)=\sum_{i=1}^{18} \sum_{k} \frac{\Delta x(k)}{H} \pi R(i)^{2} n(i, x) V(i, x) \in(i, j)
$$

where

$$
\begin{aligned}
\Delta x(k) & =\text { length of the } k^{\text {th }} \text { spatial step } \\
n(i, x) & =\text { number concentration of droplets in the } i^{\text {th }} \text { size class in the } k^{\text {th }} \text { spatial node }
\end{aligned}
$$

Results
$\mathrm{V}(\mathrm{i}, \mathrm{x})=$ terminal velocity of the droplets in the $\mathrm{i}^{\text {th }}$ size class in the $\mathrm{k}^{\text {th }}$ spatial node

$$
\begin{aligned}
\mathrm{x} & =\sum_{\mathrm{j}=1}^{\mathrm{k}} \Delta \mathrm{x}(\mathrm{j}) \\
\mathrm{R}(\mathrm{i}) & =\mathrm{D}_{\mathrm{d}}(\mathrm{~h}) / 2 \\
\mathrm{H} & =\text { total fall distance available }=\sum_{\mathbf{k}} \Delta \mathrm{x}(\mathrm{k})
\end{aligned}
$$

It has been assumed here that the aerosols are well mixed so that the droplet velocity term in the above equation need not be adjusted by the settling velocities of the aerosols with respect to the terminal velocities of the droplets. The overall decontamination coefficient is calculated from:

$$
\frac{\mathrm{dM}}{\mathrm{dt}}=-\lambda(\text { overall }) \mathrm{M}=-\sum_{j=1}^{20} \lambda(j) M(j)
$$

where

$$
M=\sum_{j=1}^{20} M(j)
$$

Calculations were done for fixed amounts of aerosol in the containment volume and assuming any unsprayed volume was negligible. Discussion of the results presented below indicates how the calculated results may be used when either of these assumptions is invalid.

## B. Some Representative Results

The decontamination factors produced by sprays for three particular cases are shown in Figure 36. These three cases were chosen simply to illustrate the magnitude of decontamination that can be achieved by sprays. The cases shown in the figure are not statistically representative of all the results. Decontamination is initially quite rapid. As decontamination progresses, the rate of aerosol removal slows. The reasons for this are readily apparent when the size distribution of the aerosol remaining suspended in the atmosphere is examined. The size distributions of the remaining aerosol after decontamination factors of 10,100 , and 1000 have been reached are shown in Figure 37. The amount of mass in any size bin falls as decontamination progresses. The rate of removal of aerosol mass is greater for very large and very small aerosol particles. Removal of aerosol particles with diameters of 0.1 to $0.4 \mu \mathrm{~m}$ is slower than removal of larger or smaller particles. Therefore, as decontamination of the atmosphere by a spray progresses, the size distribution of the aerosol remaining in the atmosphere changes. The mean size of the remaining aerosol shifts toward the particle size that is removed most slowly. The breadth of the aerosol size distribution is also


Figure 36 Three examples of the predicted decontamination by a spray for $\mathbf{H}=3000 \mathrm{~cm}$, $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$


Figure 37 Evolution of the aerosol size distribution as decontamination progresses
narrowed. As the easily removed aerosol particles are captured, the remaining aerosol becomes progressively more difficult to remove.

Continued operation of a spray can, given sufficient time, produce any desired level of decontamination. For the purposes of this work, it is not useful to speak in terms of the decontamination factor that can be achieved with a spray. It is more useful to discuss the rate of decontamination characterized by the decontamination coefficient, $\lambda$. The values of $\lambda$ that were used to calculate decontamination for the three cases shown in Figure 36 are plotted in Figure 38. The decontamination coefficient $\lambda$ varies with the fraction of aerosol mass remaining in the containment, $m_{f}$. $\lambda$ decreases approximately linearly with $m_{f}$ for values of $m_{f}$ greater than about 0.1 . For smaller values of $m_{f}, \lambda$ approaches a constant value. The changes in $\lambda$ with $m_{f}$ are simply the result of changes in size distribution of aerosol remaining in the atmosphere as decontamination progresses.

Detailed results are presented below for $m_{f}=0.9,0.5,0.3,0.1,0.01$, and $10^{-3}$. The value of $\lambda$ at $\mathrm{m}_{\mathrm{f}}=0.9$ is taken to be indicative of the initial rate of decontamination when aerosol is first exposed to the action of a spray. This is the value of $\lambda$ that would be applied to the analysis of the decontamination of a steady source of aerosols to the containment atmosphere which is one of the principal issues addressed in Chapter I of this report. Values of $\lambda$ at $m_{f}=0.5,0.1,0.01$ and $10^{-3}$ correspond to values at decontamination factors of $2,10,100$, and 1000 .

The decontamination coefficient at a fixed level of decontamination (or, equivalently, a fixed value of $\mathrm{m}_{\mathrm{f}}$ ) decreases with increasing fall distance. Some examples of the variations in $\lambda$ with fall

[^1]Regulatory descriptions of $\lambda$ use the definition [63]:

$$
\lambda=\frac{1.5 \mathrm{HF}}{\mathrm{~V}}\left[\frac{\mathrm{E}}{\mathrm{D}}\right]
$$

where

$$
\begin{aligned}
& \mathrm{F}=\text { total water flow rate } \\
& \mathrm{H}=\text { fall distance } \\
& \mathrm{V}=\text { containment volume } \\
& \frac{\mathrm{E}}{\mathrm{D}}=\text { capture efficiency divided by the droplet diameter }
\end{aligned}
$$

For droplets $1000 \mu \mathrm{~m}$ in diameter a value of $E / D=10 \mathrm{~m}^{-1}$ has been recommended [63]. This value is further recommended to be reduced to $1 \mathrm{~m}^{-1}$ once the mass fraction of aerosol remaining in the containment has been reduced to 0.02 . Values of $\lambda$ cited here in units of $\mathrm{hr}^{-1}$ may be converted to $\mathrm{E} / \mathrm{D}$ ratios in units of $\mathrm{m}^{-1}$ by:

$$
\frac{E}{D}\left(\mathrm{~m}^{-1}\right)=\frac{\lambda\left(\mathrm{hr}^{-1}\right) 0.01852}{\mathrm{Q}\left(\mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}\right)}
$$



Figure 38 Variations of the decontamination coefficients as decontamination progresses for three cases
distance, $H$, are shown in Figures 39 and 40 for $m_{f}=0.9$ and $m_{f}=0.01$, respectively. Again, these examples were chosen simply to be illustrative of the range of variation of $\lambda$ with $m_{f}$. In some cases, $\lambda$ changes fairly significantly as the fall distance goes from 500 cm to 5000 cm . In other cases, the change is not so great though $\lambda$ still decreases as the fall distance increases. The decrease in $\lambda$ with increasing fall distance comes about because the droplet size distribution becomes increasingly coarse with distance from the spray nozzle. Larger droplets less efficiently trap aerosols than do smaller droplets. The variability in the sensitivity of $\lambda$ to fall distance comes about because of the uncertainty in the efficiency with which large droplets sweep out small droplets during the fall through the containment atmosphere.

The decontamination coefficient, $\lambda$, also varies with the volumetric water flux, Q . All this sensitivity of $\lambda$ presents a challenge in presenting the results of the calculations done for the uncertainty analysis. Quite a lot of results must be examined to understand how $\lambda$ varies with the known quantities, Q and H as well as $\mathrm{m}_{\mathrm{f}}$.

## C. Detailed Results of the Uncertainty Analysis

About 400 calculations of $\lambda$ were done for each of the three values of water flux, Q , the eight values of fall distance, $H$, and for $m_{f}=0.9,0.5,0.3,0.1,0.01$, and $10^{-3}$. The sets of values of $\lambda$ for fixed values of $\mathrm{Q}, \mathrm{H}$, and $\mathrm{m}_{\mathrm{f}}$ were analyzed to formulate uncertainty distributions for $\lambda(\mathrm{Q}, \mathrm{H}$, $m_{f}$ ) using a non-parametric, order statistics method. This method of analysis has been described in detail elsewhere [11]. The Monte Carlo method samples the distribution of values of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$. Because only a finite number of samples is selected at given values of $Q, H$, and $m_{f}$, the actual distribution of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$ is known only to a selected confidence level. Here, attentions are focused on the confidence levels of 50,90 , and 95 percent. Enough information is provided in the Tables in Appendix A to compute quantities of interest at other confidence levels.

The non-parametric, order statistics used to analyze the results of the Monte Carlo calculation yields cumulative probability distributions for $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$. A range of values of $\lambda$ define each percentile of the cumulative distribution. The range is indicative of the stochastic uncertainty that exists because of the finite sample used to estimate the uncertainty distribution of $\lambda^{*}$. The cumulative distribution is the result of phenomenological uncertainty and uncertainty in initial and boundary conditions in spray operations. One of the most desirable features of the order statistical analysis procedure is that it separates stochastic uncertainty from the phenomenological, initial condition and boundary condition uncertainty. An example of the product of this analysis for $\mathrm{Q}=$ $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{H}=3000 \mathrm{~cm}$, and $\mathrm{m}_{\mathrm{f}}=0.9$ is shown in Table 8. Other tables for other values of $\mathrm{Q}, \mathrm{H}$, and $\mathrm{m}_{\mathrm{f}}$ are collected in Appendix A.

Some example distributions of $\lambda$ are shown in Figures 41 to 44 . The first of these figures shows the variations in the distributions with the extent of decontamination. Note that percentile levels in the cumulative probability plot are shown in the figure for confidence levels of 50 percent (bars) and 95 percent (dashed lines). The next figure illustrates the dependence of the distributions of $\lambda$ on fall

[^2]

Figure 39 Some examples of the calculated variations in the decontamination coefficient with fall distance for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s and $m_{f}=0.9$


Figure 40 Some examples of the calculated variations in the decontamination coefficient with fall distance for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ and $\mathrm{m}_{\mathrm{f}}=0.01$

Table 8 Cumulative uncertainty distribution for $\lambda\left(Q, H, m_{f}\right)$ for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{H}=3000$, and $\mathrm{m}_{\mathrm{f}}=0.9$ for confidence levels of 95,90 and 50 percent

|  | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |  |
| :--- | :---: | :---: | :---: | :--- | :--- |
|  | Quantile <br> $(\%)$ | $95 \%$ | $90 \%$ | $50 \%$ |  |
| Mean $=9.740$ | 5 | $2.087-2.760$ | $2.172-2.739$ | $2.492-2.672$ | Water Flux $=$ |
|  | 10 | $2.755-3.713$ | $2.782-3.487$ | $2.990-3.290$ | $0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | $3.359-4.307$ | $3.400-4.286$ | $3.837-4.152$ |  |
| Std. Dev. $=7.537$ | 20 | $4.150-5.174$ | $4.202-5.042$ | $4.310-4.609$ |  |
|  | 25 | $4.554-5.761$ | $4.650-5.711$ | $5.080-5.452$ |  |
|  | 30 | $5.377-6.403$ | $5.434-6.330$ | $5.687-6.182$ | Fall Distance $=3000 \mathrm{~cm}$ |
| Sample Size $=400$ | 35 | $5.986-6.985$ | $6.092-6.886$ | $6.310-6.661$ |  |
|  | 40 | $6.467-7.698$ | $6.605-7.661$ | $6.807-7.182$ |  |
|  | 45 | $7.021-8.200$ | $7.141-8.040$ | $7.519-7.796$ |  |
|  | 50 | $7.746-8.952$ | $7.775-8.760$ | $7.922-8.394$ |  |
|  | 55 | $8.223-9.794$ | $8.316-9.704$ | $8.668-9.256$ | Aerosol Mass Fraction |
|  | 60 | $9.052-10.510$ | $9.244-10.388$ | $9.533-10.116$ | Remaining $=0.9$ |
|  | 70 | $9.816-11.363$ | $9.930-10.995$ | $10.354-10.676$ |  |
|  | 75 | $10.586-12.327$ | $10.641-12.086$ | $10.930-11.722$ |  |
|  | 80 | $12.612-14.230$ | $12.689-14.111$ | $12.897-13.564$ |  |
|  | 85 | $13.566-15.957$ | $13.605-15.702$ | $14.220-15.060$ |  |
|  | 90 | $15.321-18.215$ | $15.626-18.039$ | $16.291-17.459$ |  |
|  | 95 | $18.197-24.898$ | $18.288-24.150$ | $20.524-22.776$ |  |



Figure 41 Cumulative distributions of $\lambda$ for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{H}=3000 \mathrm{~cm}$ and $m_{f}=0.9,0.01$, and 0.001 Note that the cumulative probability is given in percent.


Figure 42 Cumulative distributions of $\lambda$ for $\mathrm{Q}=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{m}_{\mathrm{f}}=0.9$ and $\mathrm{H}=853$ and 5000 cm . Bars indicate 50 percent confidence intervals for $\lambda$. Cumulative probability is given in percent.


Figure 43 Cumulative distribution of $\lambda$ for $Q=0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{H}=3000 \mathrm{~cm}$ and $m_{f}=0.9,0.01$, and 0.001 . Cumulative probability is given in percent.


Figure 44 Cumulative distribution of $\lambda$ for $Q=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \mathrm{H}=3000 \mathrm{~cm}$ and $\mathrm{m}_{\mathrm{f}}=0.9,0.1$, and 0.001 . Cumulative probability is given in percent.
distance. The next two figures show the sensitivity of the distribution to water flux. Were the distributions shown in the figures log-normal distributions, the percentile levels would fall on straight lines. Clearly, the distributions for the spray decontamination coefficients found here are more complicated than the well-known log-normal distribution.

Introduction of confidence level to which the uncertainty distributions are known as well as the distributions themselves creates challenges in the succinct presentation of the results of the analyses done here. The distributions for $\lambda$ at various values of water flux, fall distance and the mass fraction of aerosol remaining in the atmosphere can be quite broad because of uncertainties in quantities that affect spray performance. Notably the size distribution of the aerosol initially present in the atmosphere, the initial size distribution of the spray droplets and the efficiency with which droplets collisions result in coalescence of droplets are uncertainties that contribute significantly to the breadth of the distribution of predicted values of the spray decontamination coefficient, $\lambda$. Attentions are restricted in the rest of the discussion presented here to only certain percentiles of the distributions. It is thought by the authors that of most immediate interest is the median or 50 percentile of the distributions. ${ }^{*}$ It is assumed by the authors that analyses done using the medians of the uncertainty distributions for $\lambda$ would not have especially stringent demands with regard to confidence level. Therefore, the medians at only 50 percent confidence level [ 50 percent confidence that the true median lies within the indicated range] are discussed below.. For other purposes, the extremes of the distribution for $\lambda$ may be more appropriate. It might be, for instance, that conservative predictions of the aerosol removal are appropriate to use. Then, the lower percentiles of the distributions might be of greater interest than the median. If, on the other hand, the intended use of results presented here is to develop a conservative estimate of the amount of radioactivity in containment sump waters, then higher percentiles of the distributions for $\lambda$ might be of interest. For the purposes of the remainder of the discussions, the authors have selected the 10 and 90 percentiles of the distributions as reasonable lower and upper bounds, respectively, of the values of $\lambda$ for particular conditions. It has been assumed that when extremes of the distributions are of interest there are also demands for high levels of confidence. The 10 and 90 percentiles at 90 percent confidence [ 90 percent confidence that the true values of the 10 and 90 percentiles lie within the indicated range] are discussed here.

Sufficient information is presented in Appendix A for the interested reader to examine other percentiles of the distributions at other confidence levels.

Summaries of the ranges of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$ corresponding to

- the median at 50 percent confidence level,
- the 10 percentile or reasonable lower bound at 90 percent confidence level, and
- the 90 percentile or reasonable upper bound at 90 percent confidence level

[^3]Results
are shown in Tables 9 to 17. Again, information on other quantiles at other confidence levels can be derived from tables assembled in Appendix A of this report.

The median values of $\lambda(\mathrm{Q}, \mathrm{H})$ for $\mathrm{m}_{\mathrm{f}}=0.9$ and for $\mathrm{m}_{\mathrm{f}}=0.01$ are shown as functions of fall distance $H$ and water flux Q in Figures 45 and 46. Note that the decontamination coefficients do decrease with increasing fall distance. The sensitivity of $\lambda$ to fall distance increases with increasing water flux. As the concentration of water droplets increases, the rates at which the water droplets collide and coalesce increase during the fall of these droplets through the containment atmosphere. At water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}, \lambda$ is practically insensitive to fall distance.

The sensitivity of the 90 percentile values of $\lambda$ to fall distance is only slightly greater than the sensitivity of the median values of $\lambda$. The 10 percentile values of $\lambda$ are less sensitive than the median values to fall distance.

A plot of values of $\lambda$ at $m_{f}=0.9$ for a fall distance of 3000 cm distance against water flux, Q , is shown in Figure 47. The values of $\lambda$ vary essentially linearly with water flux from $Q=0.001$ to $\mathrm{Q}=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s. At water fluxes of $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ some non-linear effects appear. The efficiency of aerosol removal is reduced from what would be expected based on linear extrapolation. This reduction in the efficiency of capture occurs because of changes in the water droplet size distribution during free fall through the containment atmosphere. The coalescence of water droplets proceeds at a rate that is approximately proportional to the square of droplet concentration whereas aerosol capture proceeds at a rate proportional to the droplet concentration. At the highest concentrations studied here, extensive coalescence of droplets occurs to form larger droplets that are less efficient at aerosol capture.

Plots of the median values of $\lambda$ for various values of fall distance and water flux against the mass fraction of the aerosol remaining in the atmosphere are shown in Figures 48 to 50. These plots show that $\lambda$ decreases as decontamination progresses. These plots must, however, be carefully interpreted. There is a correlation among sampled values of $\lambda$ with $m_{f}$ at fixed $Q$ and $H$. That is, for circumstances in which $\lambda$ with $m_{f}=0.9$ is large, there is a high probability that $\lambda$ at other values of $m_{f}$ will also be relatively large. This correlation among values of $\lambda$ for fixed water flux and fall height but varying values of $m_{f}$ is demonstrated in the plot of $\lambda\left(m_{f}=0.01\right)$ against $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ for $\mathrm{Q}=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ and $\mathrm{H}=3000 \mathrm{~cm}$ shown in Figure 51. Some of the correlation can be eliminated by considering the ratio $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$. The lower correlation between $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ and $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ can be seen by the plot of sampled values shown in Figure 52. Distributions of the ratios $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ are more nearly independent than are the distributions of $\lambda\left(m_{f}\right)$. Results of the Monte Carlo sampling were reanalyzed in terms of the ratios $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ for $\mathrm{m}_{\mathrm{f}}=0.5,0.3,0.1,0.01$, and 0.001 . Results of the analyses are summarized in Tables 18 to 26 . Note that the ratios are dependent on $m_{f}$ and $Q$ but are essentially independent of the fall distance, $H$. Cumulative probability plots of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ are shown in Figures 53 to 55.

Table 9 Median decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 50 percent confidence level for a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$



Table 1010 Percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 90 percent confidence level for a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

|  | $\begin{aligned} & \text { Fall distance } \\ & \text { (cm) } \end{aligned}$ | Mass fraction of aerosol remaining in the containment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
|  | 500 | 3.138-3.990 | 2.514-3.068 | 2.128-2.584 | 1.596-1.832 | 1.019-1.138 | 0.747-0.902 |
|  | 853 | 3.089-3.865 | 2.467-3.023 | 2.119-2.552 | 1.594-1.820 | 0.982-1.117 | 0.733-0.878 |
|  | 1000 | 3.119-3.872 | 2.439-2.964 | 2.113-2.526 | 1.588-1.817 | 0.982-1.124 | 0.732-0.870 |
| っ | 1584 | 3.053-3.742 | 2.395-2.879 | 2.035-2.468 | 1.540-1.776 | 0.965-1.105 | 0.718-0.862 |
|  | 2000 | 2.939-3.644 | 2.337-2.851 | 1.968-2.436 | 1.505-1.749 | 0.938-1.094 | 0.710-0.852 |
|  | 3000 | 2.782-3.487 | 2.277-2.746 | 1.938-2.304 | 1.465-1.678 | 0.898-1.050 | 0.703-0.812 |
|  | 4000 | 2.695-3.282 | 2.227-2.720 | 1.900-2.182 | 1.459-1.628 | 0.877-1.014 | 0.672-0.778 |
|  | 5000 | 2.619-3.295 | 2.171-2.615 | 1.824-2.150 | 1.430-1.581 | 0.850-0.995 | 0.651-0.741 |

Table 1190 percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 90 percent confidence level for a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Fall distance (cm) | Mass fraction of aerosol remaining in the containment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 16.837-20.735 | 12.294-14.242 | 9.907-11.745 | 7.410-8.923 | 4.708-6.311 | 3.894-4.952 |
| 853 | 16.892-20.443 | 12.052-14.136 | 9.688-11.655 | 7.266-8.352 | 4.596-6.114 | 3.880-4.864 |
| 1000 | 16.449-20.125 | 11.957-14.046 | 9.648-11.628 | 7.233-8.286 | 4.687-6.148 | 3.937-5.301 |
| 1584 | 16.074-19.231 | 11.656-13.522 | 9.354-11.224 | 7.118-8.197 | 4.594-5.852 | 3.814-4.787 |
| 2000 | 16.044-19.098 | 11.441-13.419 | 9.323-10.930 | 6.985-8.194 | 4.550-5.758 | 3.754-4.745 |
| 3000 | 15.626-18.039 | 10.940-12.943 | 9.208-10.664 | 6.760-7.983 | 4.499-5.625 | 3.681-4.605 |
| 4000 | 15.166-17.419 | 10.879-12.889 | 8.980-10.431 | 6.644-7.834 | 4.420-5.650 | 3.515-4.586 |
| 5000 | 15.088-17.299 | 10.600-12.647 | 8.868-10.371 | 6.590-7.649 | 4.388-5.611 | 3.404-4.565 |

Table 12 Median decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at a confidence level of 50 percent for a water flux of $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Mass fraction of aerosol remaining in the contaimment atmosphere |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| distance (cm) | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 144.302-158.520 | 109.629-118.793 | 89.046-93.558 | 63.361-65.174 | 37.780-40.456 | 29.481-30.926 |
| 853 | 128.227-138.510 | 95.617-102.228 | 77.661-82.729 | 53.885-57.275 | 33.343-36.243 | 25.743-28.456 |
| 1000 | 121.340-136.124 | 89.496-99.013 | 74.114-81.176 | 50.931-55.178 | 31.844-34.513 | 24.370-27.429 |
| 1584 | 108.094-118.246 | 78.832-86.987 | 63.324-70.572 | 43.873-49.038 | 28.567-30.560 | 22.411-23.651 |
| 2000 | 96.826-110.243 | 70.160-79.865 | 58.499-65.342 | 41.186-45.819 | 25.847-28.431 | 20.030-21.962 |
| 3000 | 83.989-91.291 | 60.442-68.414 | 48.749-55.514 | 36.021-38.510 | 22.498-23.609 | 16.882-18.893 |
| 4000 | 73.854-84.354 | 53.575-59.184 | 43.660-48.285 | 31.066-36.164 | 19.421-22.569 | 14.826-16.922 |
| 5000 | 65.440-76.867 | 47.699-53.529 | 39.577-43.410 | 28.085-33.663 | 17.208-21.212 | 13.505-16.358 |

Table 1310 percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at a 90 percent confidence level for a water flux of $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$


Table 1490 percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at a 90 percent confidence level for a water flux of $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Fall distance (cm) | Mass fraction of aerosol remaining in the containment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 318.316-366.868 | 218.596-258.747 | 182.084-207.701 | 130.062-156.260 | 80.724-98.823 | 63.224-78.441 |
| 853 | 296.267-348.861 | 207.498-249.353 | 175.959-199.056 | 121.338-148.608 | 77.239-95.992 | 60.560-75.928 |
| 1000 | 287.074-346.965 | 205.097-244.232 | 173.763-196.900 | 120.046-146.943 | 76.400-95.113 | 59.776-75.256 |
| 1584 | 272.434-336.391 | 194.375-237.302 | 167.435-188.991 | 115.276-139.034 | 73.762-92.430 | 57.034-72.418 |
| 2000 | 267.688-334.389 | 189.821-231.738 | 164.554-185.425 | 112.953-136.156 | 70.545-89.629 | 54.451-70.048. |
| 3000 | 252.802-313.652 | 182.912-223.418 | 157.956-175.482 | 105.802-130.606 | 67.533-87.285 | 52.521-68.300 |
| 4000 | 248.930-309.229 | 180.940-216.779 | 154.402-171.409 | 101.459-127.837 | 66.120-85.082 | 51.447-66.678 |
| 5000 | 246.726-305.904 | 177.006-212.539 | 151.242-168.371 | 99.381-124.472 | 66.520-83.500 | 51.393-64.798 |

Table 15 Median decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 50 percent confidence level for a water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Fall distance (cm) | Mass fraction of aerosol remaining in the containment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 0.834-0.859 | 0.644-0.694 | 0.539-0.559 | 0.379-0.412 | 0.235-0.252 | 0.181-0.193 |
| 853 | 0.832-0.856 | 0.644-0.693 | 0.537-0.559 | 0.378-0.411 | 0.234-0.251 | 0.180-0.193 |
| 1000 | 0.831-0.855 | 0.643-0.693 | 0.536-0.559 | 0.377-0.411 | 0.234-0.251 | 0.180-0.193 |
| 1584 | 0.828-0.854 | 0.643-0.691 | 0.533-0.556 | 0.373-0.411 | 0.234-0.250 | 0.179-0.192 |
| 2000 | 0.826-0.854 | 0.643-0.688 | 0.531-0.554 | 0.372-0.411 | 0.233-0.248 | 0.178-0.192 |
| 3000 | 0.822-0.853 | 0.643-0.685 | 0.528-0.549 | 0.369-0.411 | 0.231-0.247 | 0.177-0.190 |
| 4000 | 0.818-0.844 | 0.640-0.677 | 0.527-0.548 | 0.368-0.409 | 0.231-0.244 | 0.177-0.190 |
| 5000 | 0.815-0.832 | 0.636-0.669 | 0.519-0.545 | 0.365-0.406 | 0.231-0.241 | 0.177-0.190 |

Table 1610 percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 90 percent confidence level for a water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

|  | Mass fraction of aerosol remaining in the containment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| (cm) | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 0.355-0.424 | 0.296-0.327 | 0.240-0.279 | 0.162-0.195 | 0.097-0.116 | 0.072-0.087 |
| 853 | 0.353-0.424 | 0.295-0.326 | 0.239-0.278 | 0.162-0.195 | 0.097-0.116 | 0.071-0.086 |
| 1000 | 0.353-0.424 | 0.294-0.326 | 0.238-0.278 | 0.162-0.195 | 0.097-0.116 | 0.071-0.086 |
| 1584 | 0.352-0.424 | 0.293-0.325 | 0.237-0.277 | 0.162-0.194 | 0.097-0.116 | 0.071-0.086 |
| 2000 | 0.352-0.424 | 0.291-0.325 | 0.236-0.276 | 0.162-0.194 | 0.097-0.115 | 0.071-0.086 |
| 3000 | 0.349-0.424 | 0.289-0.324 | 0.234-0.275 | 0.162-0.192 | 0.097-0.114 | 0.070-0.086 |
| 4000 | 0.349-0.424 | 0.288-0.322 | 0.230-0.274 | 0.160-0.190 | 0.097-0.112 | 0.070-0.084 |
| 5000 | 0.351-0.423 | 0.286-0.321 | 0.228-0.273 | 0.159-0.189 | 0.093-0.111 | 0.069-0.084 |

Table 1790 percentile decontamination coefficient, $\lambda\left(\mathrm{hr}^{-1}\right)$, at 90 percent confidence level for a water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| $\begin{aligned} & \text { Fall distance } \\ & \text { (cm) } \end{aligned}$ | Mass fraction of aerosol remaining in the contaimment atmosphere |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 0.9 | 0.5 | 0.3 | 0.1 | 0.01 | 0.001 |
| 500 | 1.788-2.364 | 1.227-1.552 | 0.997-1.196 | 0.719-0.904 | 0.508-0.596 | 0.411-0.489 |
| 853 | 1.788-2.356 | 1.225-1.550 | 0.992-1.196 | 0.718-0.901 | 0.507-0.596 | 0.411-0.489 |
| 1000 | 1.788-2.352 | 1.224-1.550 | 0.991-1.196 | 0.717-0.900 | 0.506-0.596 | 0.411-0.489 |
| 1584 | 1.785-2.339 | 1.221-1.548 | 0.987-1.195 | 0.715-0.896 | 0.503-0.596 | 0.409-0.488 |
| 2000 | 1.780-2.329 | 1.218-1.542 | 0.983-1.195 | 0.715-0.893 | 0.500-0.595 | 0.409-0.488 |
| 3000 | 1.768-2.304 | 1.212-1.527 | 0.975-1.194 | 0.712-0.885 | 0.491-0.594 | 0.407-0.486 |
| 4000 | 1.755-2.281 | 1.206-1.512 | 0.969-1.192 | 0.707-0.878 | 0.486-0.594 | 0.406-0.482 |
| 5000 | 1.747-2.257 | 1.203-1.496 | 0.966-1.190 | 0.705-0.871 | 0.482-0.594 | 0.404-0.478 |



Figure 45 Median ( 50 percentile) $\lambda$ at 50 percent confidence level for $\mathrm{m}_{\mathrm{f}}=0.9$ as a function of water flux, $\mathbf{Q}$, and fall distance, $H$


Figure 46 Median ( 50 percentile) $\lambda$ at 50 percent confidence level for $m_{f}=0.01$ as a function of water flux, $Q$, and fall distance, $H$


Figure 47 Median ( 50 percentile), 10 percentile and 90 percentile values of $\lambda$ for $m_{f}=0.9$ as functions of water flux, $Q$, for $H=3000 \mathrm{~cm}$


Figure 48 Median ( 50 percentile) $\lambda$ for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ as a function of the mass fraction of acrosol remaining in the atmosphere


Figure 49 Median ( 50 percentile) $\lambda$ for $Q=0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s as a function of the mass fraction of aerosol remaining in the atmosphere


Figure 50 Median ( 50 percentile) $\lambda$ for $Q=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s as a function of the mass fraction of aerosol remaining in the atmosphere


Figure 51 Correlation between values of $\lambda\left(m_{f}=0.01\right)$ and values of $\lambda\left(m_{f}=0.9\right)$ for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ and $\mathrm{H}=3000 \mathrm{~cm}$


Figure 52 Values of $\lambda\left(m_{f}=0.01\right) / \lambda\left(m_{f}=0.9\right)$ plotted against values of $\lambda\left(m_{f}=0.9\right)$ for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-8$ and $H=3000 \mathrm{~cm}$

Table 18 Median ( 50 percentile) values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 50 percent confidence for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

Table 1910 percentile value of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 90 percent confidence for $Q=0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$


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Table 21 Median ( 50 percentile) values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 50 percent confidence for $Q=0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Fall distance (cm) | $\mathrm{m}_{\mathrm{f}}=0.5$ | $\mathrm{m}_{\mathrm{f}}=0.3$ | $\begin{gathered} \left.n_{f}\right) / \lambda\left(m_{f}=0.9\right) \\ m_{f}=0.1 \end{gathered}$ | $\mathrm{m}_{\mathrm{f}}=0.01$ | $\mathrm{m}_{\mathrm{f}}=0.001$ |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 500 | 0.741-0.751 | 0.600-0.615 | 0.419-0.437 | 0.247-0.262 | 0.191-0.202 |
| 853 | 0.742-0.754 | 0.602-0.617 | 0.420-0.437 | 0.250-0.262 | 0.191-0.201 |
| 1000 | 0.741-0.752 | 0.601-0.617 | 0.421-0.438 | 0.249-0.264 | 0.192-0.200 |
| 1584 | 0.745-0.757 | 0.602-0.617 | 0.420-0.436 | 0.252-0.264 | 0.191-0.199 |
| 2000 | 0.744-0.754 | 0.601-0.618 | 0.422-0.439 | 0.251-0.264 | 0.190-0.199 |
| 3000 | 0.749-0.756 | 0.601-0.618 | 0.423-0.438 | 0.252-0.263 | 0.191-0.199 |
| 4000 | 0.748-0.756 | 0.602-0.618 | 0.423-0.438 | 0.253-0.263 | 0.191-0.199 |
| 5000 | 0.742-0.754 | 0.600-0.616 | 0.422-0.436 | 0.252-0.264 | 0.190-0.199 |

*Equivalent to $\frac{E}{D}\left(m_{f}\right) / \frac{E}{D}\left(m_{f}=0.9\right)$

|  | Table 2210 percentile values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 90 percent confidence for $Q=0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Fall distance (cm) | $\mathrm{m}_{\mathrm{f}}=0.5$ | $\mathrm{m}_{\mathrm{f}}=0.3$ | $\begin{gathered} \lambda\left(m_{f}\right) / \lambda\left(m_{f}=0\right. \\ m_{f}=0.1 \end{gathered}$ | $\mathrm{m}_{\mathrm{f}}=0.01$ | $\mathrm{m}_{\mathrm{f}}=0.001$ |
|  | 500 | 0.591-0.622 | 0.429-0.459 | 0.258-0.274 | 0.128-0.138 | 0.092-0.101 |
|  | 853 | 0.595-0.621 | 0.430-0.459 | 0.258-0.274 | 0.128-0.139 | 0.091-0.101 |
|  | 1000 | 0.596-0.619 | 0.431-0.459 | 0.258-0.274 | 0.128-0.139 | 0.091-0.101 |
|  | 1584 | 0.597-0.618 | 0.432-0.458 | 0.257-0.274 | 0.128-0.139 | 0.091-0.101 |
| 岕 | 2000 | 0.596-0.618 | 0.432-0.457 | 0.257-0.273 | 0.128-0.138 | 0.091-0.101 |
|  | 3000 | 0.598-0.619 | 0.432-0.460 | 0.257-0.275 | 0.128-0.140 | 0.091-0.101 |
|  | 4000 | 0.598-0.619 | 0.432-0.459 | 0.258-0.275 | 0.128-0.140 | 0.091-0.101 |
|  | 5000 | 0.598-0.618 | 0.432-0.454 | 0.258-0.273 | 0.128-0.140 | 0.091-0.101 |
|  | *Equivalent to $\frac{E}{D}\left(m_{f}\right) / \frac{E}{D}\left(m_{f}=0.9\right)$ |  |  |  |  |  |

Table 2390 percentile values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 90 percent confidence for $Q=0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

|  | Fall distance (cm) | $\mathrm{m}_{\mathrm{f}}=0.5$ | $\mathrm{m}_{\mathrm{f}}=0.3$ | $\begin{array}{r} \lambda\left(m_{f}\right) / \lambda\left(m_{f}=\right. \\ m_{f}=0.1 \end{array}$ | $\mathrm{m}_{\mathrm{f}}=0.01$ | $\mathrm{m}_{\mathrm{f}}=0.001$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 500 | 0.890-0.906 | 0.814-0.837 | 0.685-0.725 | 0.527-0.571 | 0.438-0.501 |
|  | 853 | 0.890-0.908 | 0.815-0.841 | 0.692-0.733 | 0.528-0.576 | 0.437-0.492 |
|  | 1000 | 0.893-0.908 | 0.818-0.841 | 0.684-0.731 | 0.527-0.576 | 0.437-0.488 |
|  | 1584 | 0.892-0.907 | 0.815-0.841 | 0.685-0.731 | 0.529-0.577 | 0.439-0.489 |
| W | 2000 | 0.892-0.907 | 0.815-0.843 | 0.685-0.732 | 0.529-0.578 | 0.439-0.490 |
|  | 3000 | 0.891-0.906 | 0.815-0.842 | 0.685-0.732 | 0.530-0.577 | 0.439-0.488 |
|  | 4000 | 0.891-0.907 | 0.818-0.844 | 0.687-0.731 | 0.529-0.577 | 0.440-0.487 |
|  | 5000 | 0.891-0.907 | 0.816-0.842 | 0.687-0.731 | 0.529-0.577 | 0.440-0.487 |
|  | *Equivalent to $\frac{\mathrm{E}}{\mathrm{D}}\left(\mathrm{m}_{\mathrm{f}}\right) / \frac{\mathrm{E}}{\mathrm{D}}\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ |  |  |  |  |  |


|  | Table 24 Median values ( 50 percentile) of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 50 percent confidence for $\mathrm{Q}=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Fall distance (cm) | $\mathrm{m}_{\mathrm{f}}=0.5$ | $\mathrm{m}_{\mathrm{f}}=0.3$ | $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ $m_{f}=0.1$ | $\mathrm{m}_{\mathrm{f}}=0.01$ | $\mathrm{m}_{\mathrm{f}}=0.001$ |
|  | 500 | 0.749-0.776 | 0.612-0.645 | 0.436-0.465 | 0.276-0.291 | 0.214-0.225 |
|  | 853 | 0.749-0.776 | 0.612:0.645 | 0.436-0.465 | 0.276-0.292 | 0.214-0.225 |
|  | 1000 | 0.749-0.776 | 0.612-0.645 | 0.436-0.465 | 0.276-0.292 | 0.214-0.225 |
|  | 1584 | 0.750-0.775 | 0.612-0.645 | 0.436-0.465 | 0.276-0.292 | 0.214-0.225 |
| $\stackrel{\sim}{+}$ | 2000 | 0.750-0.776 | 0.612-0.645 | 0.437-0.465 | 0.276-0.292 | 0.214-0.225 |
|  | 3000 | 0.750-0.775 | 0.612-0.645 | 0.436-0.465 | 0.276-0.292 | 0.213-0.225 |
|  | 4000 | 0.751-0.775 | 0.612-0.644 | 0.435-0.463 | 0.276-0.290 | 0.212-0.223 |
|  | 5000 | 0.750-0.775 | 0.609-0.644 | 0.432-0.463 | 0.270-0.290 | 0.212-0.223 |
|  | *Equivalent to $\frac{\mathrm{E}}{\mathrm{D}}\left(\mathrm{m}_{\mathrm{f}}\right) / \frac{\mathrm{E}}{\mathrm{D}}\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ |  |  |  |  |  |

Table 24 Median values ( 50 percentile) of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 50 percent confidence for $Q=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

Table 2510 percentile values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at 90 percent confidence for $Q=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$


|  | Table 2690 percentile values of $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at 90 percent confidence for $\mathrm{Q}=0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| , | Fall distance (cm) | $\mathrm{m}_{\mathrm{f}}=0.5$ | $\mathrm{m}_{\mathrm{f}}=0.3$ | $\begin{gathered} \left(m_{f}\right) / \lambda\left(m_{f}=0 .\right. \\ m_{f}=0.1 \end{gathered}$ | $\mathrm{m}_{\mathrm{f}}=0.01$ | $\mathrm{m}_{\mathrm{f}}=0.001$ |
|  | 500 | 0.896-0.909 | 0.820-0.839 | 0.690-0.720 | 0.521-0.558 | 0.431-0.467 |
|  | 853 | 0.896-0.909 | 0.820-0.839 | 0.690-0.720 | 0.521-0.556 | 0.431-0.465 |
|  | 1000 | 0.896-0.909 | 0.819-0.839 | 0.690-0.720 | 0.521-0.556 | 0.431-0.465 |
|  | 1584 | 0.896-0.908 | 0.820-0.839 | 0.690-0.720 | 0.520-0.556 | 0.430-0.465 |
| 山̈ 心 | 2000 | 0.896-0.908 | 0.820-0.839 | 0.690-0.720 | 0.520-0.556 | 0.430-0.465 |
|  | 3000 | 0.896-0.908 | 0.820-0.839 | 0.690-0.720 | 0.520-0.556 | 0.429-0.466 |
|  | 4000 | 0.896-0.908 | 0.820-0.840 | 0.690-0.720 | 0.520-0.556 | 0.429-0.466 |
|  | 5000 | 0.896-0.908 | 0.820-0.839 | 0.690-0.720 | 0.520-0.556 | 0.429-0.466 |
|  | *Equivalent to $\frac{E}{D}\left(m_{f}\right) / \frac{E}{D}\left(m_{f}=0.9\right)$ |  |  |  |  |  |



Figure 53 Cumulative probability plots for the distributions of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for various values of $m_{f}$ and a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$. Percentile levels are shown for 50 percent confidence (bars) and 95 percent confidence (dashed lines). These distributions are for the case $\mathbf{H}=\mathbf{3 0 0 0} \mathbf{c m}$. Distributions for other fall distances are very similar (see Appendix B).


Figure 54 Cumulative probability plots for the distributions of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for various values of $m_{f}$ and a water flux of $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$. Percentile levels are shown for 50 percent confidence (bars) and 95 percent confidence (dashed lines). These distributions are for the case $\mathbf{H}=3000 \mathrm{~cm}$. Distributions for other fall distances are very similar (see Appendix B).


Figure 55 Cumulative probability plots for the distributions of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for various values of $m_{f}$ and a water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s. Percentile levels are shown for 50 percent confidence (bars) and 95 percent confidence (dashed lines). These distributions are for the case $\mathbf{H}=3000 \mathrm{~cm}$. Distributions for other fall distances are very similar (see Appendix B).

## Results

A quantity of regulatory interest is the change in $\lambda$ between the start of decontamination (here represented by $\lambda\left(m_{f}=0.9\right)$ ) and $\lambda$ when the decontamination factor has reached about 100 (here represented by $\left.\lambda\left(m_{f}=0.01\right)\right)$. Plots of the distributions of $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.01\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ for various water fluxes are shown in Figure 56. These distributions in the value of $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.01\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=\right.$ 0.9 ) can be compared to the fixed value 0.1 that has been recommended [68].

From the discussion above, it is evident that $\lambda\left(m_{f}=0.9\right)$ is essentially a linear function of fall distance and a quadratic function of water flux. The ratio $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda(0.9)$ is independent of the fall distance. The ratio does depend on the water flux but the dependence is weak. Essentially, the ratio $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ approaches a limiting value dependent on the water flux into the containment atmosphere as the mass fraction of the aerosol remaining in the atmosphere approaches zero. The ratio is quite dependent on the mass fraction of the aerosol remaining in the containment atmosphere especially when the extent of decontamination is small. Once $\mathrm{m}_{\mathrm{f}}$ falls below 0.01 ( $\mathrm{DF}=100$ ) the dependence of the ratio on $\mathrm{m}_{\mathrm{f}}$ is small.

These results suggest that a simplified model for spray performance can be devised by developing a correlation for $\lambda\left(m_{f}=0.9\right)$ in terms of water flux and fall distance and a correlation for $\lambda\left(m_{f}\right)$ / $\lambda\left(m_{f}=0.9\right)$ in terms of water flux and the mass fraction of aerosol remaining in the containment atmosphere. Such a simplified model is developed in Chapter V.

## D. Effect of Unsprayed Volume

The decontamination coefficients have been calculated here assuming that the entire containment volume is exposed to the action of the spray. This, of course, can never be entirely true. Compartments in a reactor below the operating floor will not be exposed to the spray. At best, relatively large droplets produced by liquid films draining from surfaces will fall through atmospheres of the lower compartments. In some reactors there can be unsprayed space above the spray headers (of course, in many reactors the spray nozzles are configured so that some spray droplets go upward to penetrate areas above the spray headers).

The spray does produce a significant amount of gas circulation in the containment atmosphere (see, for example, discussions in Reference 33). The turbulent, circulating atmosphere can penetrate into regions that are not exposed to the spray. If it is assumed that this circulation is rapid in comparison to the decontamination rate, then, the decontamination coefficients for a containment with unsprayed volumes, $\lambda$ (real) are easily related to the decontamination coefficients calculated here:

$$
\lambda(\text { real })=\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}\right) /(1+\alpha)
$$

where
$\lambda($ real $)=$ actual decontamination coefficients for an atmosphere in a containment with unsprayed volumes


Figure 56 Variation of $\lambda\left(m_{f}=0.01\right) / \lambda\left(m_{f}=0.9\right)$ with water flux. The median values of $\lambda\left(m_{f}=\right.$ $0.01) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ are shown at 50 percent confidence. The 90 percentile and 10 percentile values are shown at 90 percent confidence.

Results

$$
\begin{aligned}
\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}\right) & =\text { decontamination coefficient calculated here } \\
\alpha & =\mathrm{v}(\text { unsprayed }) / \mathrm{v} \text { (sprayed) } \\
\mathrm{v}(\text { unsprayed }) & =\text { volume of containment not exposed to the spray } \\
\mathrm{v}(\text { sprayed }) & =\text { volume of containment exposed to the spray }
\end{aligned}
$$

If, on the other hand, circulation of gas from the unsprayed volumes into the volume exposed to the spray is slow relative to rate of decontamination by the spray, then the gas circulation rate determines the overall rate of decontamination of the entire containment. The values of $\lambda(\mathrm{Q}, \mathrm{H}$, $\mathrm{m}_{\mathrm{f}}$ ) computed here can still be used in an analysis of the containment response by treating the slow circulation of gas from unsprayed volumes as a source of aerosol to the sprayed volume.

## E. Combined Effects of Water Pools and Sprays

All the calculated results discussed above have been for the removal of rather coarse aerosol subjected only to attenuation by sprays. The aerosols considered thus far have size distributions expected for materials discharged directly to the containment atmosphere from the reactor coolant system or as a result of core debris interactions with concrete in the reactor cavity. Sprays may, however, not be the only system being used to mitigate.the amount of radioactivity suspended in the reactor containment atmosphere. Sprays may, in fact, be used to augment the aerosol attenuation achieved by other means. A likely, additional, method to attenuate the potential severe accident source term is to maintain a water pool over core debris that has penetrated the reactor coolant system and is interacting with structural concrete [11].

Water pools overlying core debris interacting with concrete will scrub aerosols from the gases evolved during these interactions. The efficiency of aerosol scrubbing by a water pool depends on the size of the aerosol particles. As a result of this size selective scrubbing, aerosols that emerge into the containment atmosphere from a water pool are expected to be much smaller than the aerosol considered thus far in the analysis of spray performance. The aerosol must also have a narrower distribution of sizes. Since the removal of aerosol particles by sprays is size selective, the decontamination that can be achieved by sprays would be expected to be less when the spray is used in conjunction with a water pool than when a spray is used alone.

To demonstrate this reduction in spray effectiveness at removal of aerosols subjected to the actions of a water pool, a second set of calculations was done for a spray producing a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$. For these calculations, the range of mean aerosol particle sizes was taken to be 0.15 to $0.65 \mu \mathrm{~m}$ (see Case 2 in Table 7). This is the range of mean aerosol particle sizes calculated to emerge from water pools of depths of 30 to 500 cm and subcooling of 0 to 70 K overlying core debris interacting with concrete [11]. The aerosols emerging from the water pool to be subjected to the action of the spray are assumed to be log-normally.distributed in size. Because the smaller sizes
of these aerosols are the result of size selective scrubbing, it is assumed that the geometric standard deviation of the aerosol size distribution is completely correlated to the mean size. The maximum value of the geometric standard deviation, which corresponds to a mean aerosol particle size of $0.65 \mu \mathrm{~m}$, is taken to be 3.2. The minimum geometric standard deviation, corresponding to a mean aerosol size of $0.15 \mu \mathrm{~m}$, is taken to be 1.4. Values of the geometric standard deviation for other mean aerosol particle sizes are calculated from:

$$
\sigma_{\mathrm{g}}=0.86+3.6 \mu
$$

where $\mu$ is the mean aerosol particle size in units of micrometers.
Calculations of the spray decontamination factor for aerosol previously subjected to the actions of a water pool were done in a manner completely analogous to other uncertainty analyses described in this report. Results of the calculations are summarized in Tables 27 and 28 . Values of $\lambda\left(\mathrm{m}_{\mathrm{f}}=\right.$ 0.9 ) corresponding to 10,50 , and 90 th percentiles of the uncertainty distributions at confidence levels of 95,90 , and 50 percent for various fall distances are shown in Table 27. Values of $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ for a fall distance of 3000 cm are shown in Table 28. Values listed in the table are, of course, ranges at confidence levels of 95,90 and 50 percent corresponding to the 10,50 , and 90 th percentile of the distributions for $\mathrm{m}_{\mathrm{f}}=0.5,0.3,0.1,0.01$, and 0.001 ( $\mathrm{DF}=2,3.3,10$, 100 , and 1000). Values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for other fall distances are nearly identical to those listed in Table 28 for a fall distance of 3000 cm since the ratio of spray decontamination coefficients is insensitive to fall distance.

The values of $\lambda\left(m_{f}=0.9\right)$ are plotted against fall distances in Figure 57. Values corresponding to the median of the uncertainty distribution (at 50 percent confidence) and the 10 and 90 percentiles of the distribution (at 90 percent confidence) are shown in this figure. Similar values of $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ obtained for coarser aerosol injected directly into the containment atmosphere without passing through a water pool are also shown in this figure. Comparison of the values of the $\lambda\left(m_{f}=0.9\right)$ for the two cases shows that the effectiveness of a spray at particle removal is substantially reduced for particles that have emerged from the water pool. Again, this reduction in spray effectiveness is simply, because the particles that do emerge from a water pool have size distributions that are centered near the size of minimum aerosol capture efficiency by falling water droplets.

Values of $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ are plotted against $\mathrm{m}_{\mathrm{f}}$ in Figure 58. Values of this ratio obtained in the calculations described above for coarse aerosols injected directly into the containment atmosphere without passing through a water pool are also shown in this figure. The ratios $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ found for aerosols that had been subjected to scrubbing by a water pool are somewhat less sensitive to the extent of atmosphere decontamination than are the ratios for aerosols not subjected to scrubbing. The reason for this relative insensitivity is that scrubbing by a water pool narrows the spread in the particle size distribution. The shape of the distribution is not changed greatly as atmosphere decontamination progresses.

Table 27 Summary of the uncertainty distributions found for $\lambda\left(m_{f}=0.9\right)$ for the case of aerosols subjected to pool scrubbing and spray decontamination at a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$

| Fall distance$(\mathrm{cm})$ | Percentile of distribution | Range of values of $\lambda\left(m_{f}=0.9\right)\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |
| :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |
| 500 | 10 | 0.440-0.534 | 0.445-0.522 | 0.470-0.503 |
|  | 50 | 1.013-1.128 | 1.026-1.125 | 1.061-1.086 |
|  | 90 | 2.036-2.361 | 2.055-2.313 | 2.180-2.262 |
| 853 | 10 | 0.435-0.523 | 0.440-0.511 | 0.466-0.497 |
|  | 50 | 1.000-1.117 | 1.011-1.109 | 1.045-1.080 |
|  | 90 | 1.991-2.299 | 2.016-2.271 | 2.166-2.203 |
| 1000 | 10 | 0.431-0.518 | 0.438-0.507 | 0.462-0.492 |
|  | 50 | 0.995-1.116 | 1.002-1.101 | 1.040-1.078 |
|  | 90 | 1.977-2.277 | 2.010-2.264 | 2.147-2.200 |
| 1584 | 10 | 0.413-0.506 | 0.424-0.498 | 0.450-0.477 |
|  | 50 | 0.972-1.095 | 0.985-1.076 | 1.008-1.059 |
|  | 90 | 1.920-2.251 | 1.995-2.198 | 2.050-2.166 |
| 2000 | 10 | 0.401-0.495 | 0.418-0.494 | 0.440-0.462 |
|  | 50 | 0.967-1.082 | 0.970-1.071 | 0.990-1.039 |
|  | 90 | 1.913-2.242 | 1.955-2.233 | 2.013-2.157 |
| 3000 | 10 | 0.384-0.472 | 0.388-0.467 | 0.423-0.444 |
|  | 50 | 0.932-1.054 | 0.941-1.049 | 0.964-1.017 |
|  | 90 | 1.821-2.169 | 1.853-2.161 | 1.953-2.116 |
| 4000 | 10 | 0.374-0.451 | 0.380-0.444 | 0.399-0.432 |
|  | 50 | 0.901-1.036 | 0.910-1.027 | 0.947-0.987 |
|  | 90 | 1.804-2.144 | 1.808-2.134 | 1.887-1.441 |
| 5000 | 10 | 0.366-0.438 | 0.374-0.432 | 0.381-0.420 |
|  | 50 | 0.866-0.999 | 0.891-0.988 | 0.930-0.965 |
|  | 90 | 1.754-2.118 | 1.787-2.103 | 1.853-1.988 |

Table 28 Summary of the uncertainty distribution for $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for the case of aerosols subjected to water pool scrubbing and spray decontamination at a water flux of $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ and a fall distance of 3000 cm

| Percentile of <br> the distribution | Mass fraction of <br> initial aerosol <br> remaining $\left(m_{f}\right)$ | Range of values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at a confidence level of |  |  |
| :---: | :---: | :---: | :---: | :---: |
|  | 0.5 | $95 \%$ | $90 \%$ | $50 \%$ |
|  | 0.3 | $0.727-0.750$ | $0.728-0.747$ | $0.731-0.740$ |
|  | 0.1 | $0.590-0.621$ | $0.592-0.620$ | $0.599-0.610$ |
|  | 0.01 | $0.431-0.477$ | $0.433-0.475$ | $0.445-0.462$ |
|  | 0.001 | $0.304-0.357$ | $0.307-0.355$ | $0.318-0.337$ |
|  |  | $0.261-0.309$ | $0.261-0.305$ | $0.272-0.288$ |
|  | 0.5 |  |  |  |
| 50 | 0.3 | $0.857-0.894$ | $0.861-0.892$ | $0.870-0.882$ |
|  | 0.1 | $0.773-0.831$ | $0.775-0.824$ | $0.795-0.810$ |
|  | 0.01 | $0.666-0.734$ | $0.670-0.732$ | $0.681-0.705$ |
|  | 0.001 | $0.565-0.635$ | $-0.567-0.618$ | $0.576-0.602$ |
|  |  | $0.510-0.582$ | $0.515-0.572$ | $0.532-0.556$ |
|  | 0.5 |  |  |  |
|  | 0.3 | $0.981-0.993$ | $0.983-0.993$ | $0.987-0.990$ |
|  | 0.1 | $0.968-0.987$ | $0.369-0.987$ | $0.977-0.983$ |
|  | 0.01 | $0.943-0.976$ | $0.946-0.974$ | $0.960-0.968$ |
|  | 0.001 | $0.907-0.960$ | $0.914-0.957$ | $0.934-0.947$ |
|  |  | $0.886-0.949$ | $0.896-0.945$ | $0.916-0.934$ |



Fall Distance (cm)

Figure 57 Comparison of $\lambda\left(m_{f}=0.9\right)$ for aerosols subjected to scrubbing by a water pool (solid lines) to $\lambda$ ( $\mathrm{m}_{\mathrm{f}}=0.9$ ) for aerosol injected directly into the containment atmosphere (dashed lines). For both cases the water flux is $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$. Symbols on curves for the 10 and 90 percentiles represent 90 percent confidence intervals. Symbols on the 50 percentile curve indicate 50 percent confidence intervals.


Figure 58 Comparison of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ for aerosols subjected to scrubbing by a water pool (prescrubbed aerosol) to $\lambda\left(m_{f}\right) \lambda\left(m_{f}=0.9\right)$ for aerosols injected directly into the containment atmosphere (coarse aerosol). For both cases the water flux is $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s and the fall distance is 3000 cm . Curves are shown for 90 , and 50 , and 10 percentiles of the uncertainty distributions.

## Results

The results of the calculations done here for the combined effects of a water pool and a containment spray show that decontamination factors associated with two mitigation systems cannot be simply multiplied to obtain an overall decontamination factor. Such a multiplication would overestimate the decontamination factor achieved by the combined attenuation systems. The overestimation comes about because aerosol removal is dependent on aerosol size.

A useful, approximate, method can be suggested to estimate the effectiveness of a spray operating on aerosols that had been previously exposed to the scrubbing actions of a water pool. If the water pool produces a decontamination factor DF, the spray effectiveness can be calculated using for the spray decontamination coefficient $\lambda\left(m_{f}=1 / D F\right)$ where $\lambda\left(m_{f}\right)$ is taken from the results of analyses for coarse aerosols presented above. The value of $\lambda$ used in such combined analyses will decrease with increasing decontamination effectiveness. The value of $\lambda$ will approach an asymptotic value corresponding to the minimum in the capture efficiency for the distribution of spray droplets.

## V. Development of a Simplified Model

The results of the uncertainty analysis can be used to develop a simplified description of the decontamination coefficient for aerosol removal by sprays. The procedure to develop this model is to correlate results described in Chapter IV in terms of the known quantities, water flux, Q , and fall distance, $H$. Because the decontamination coefficient depends on the extent of decontamination, $\mathrm{m}_{\mathrm{f}}$ must also be included in the correlation. The resulting description of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$ can be used in a simple differential equation to calculate decontamination:

$$
\frac{\mathrm{dm}_{\mathrm{f}}}{\mathrm{dt}}=-\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}\right) \mathrm{m}_{\mathrm{f}}
$$

Based on the discussions in Chapter IV it is evident that separate correlations are needed for $\lambda(Q$, $\left.\mathrm{H}, \mathrm{m}_{\mathrm{f}}=0.9\right)$ and $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$. Further, it is useful to have correlations for different percentiles of the uncertainty distributions of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$.

Here, attentions are restricted to:

- the medians ( 50 percentile values) at 50 percent confidence
- the 90 percentile values at 90 percent confidence, and
- the 10 percentile values at 90 percent confidence.

Some readers might find it more useful to have a model cast in terms of the E/D ratios used in regulatory evaluations of spray performance (see Reference 63 and Chapter IV). The values of $\lambda\left(m_{f}=0.9\right)$ have been converted to $E / D\left(m_{f}=0.9\right)$ values and the results are shown in Tables 29, 30 and 31 for spray fluxes of $0.01,0.25$, and $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$, respectively. In comparing the values of $E / D\left(m_{f}=0.9\right)$ in these tables to the regulatory recommendation of $10 \mathrm{~m}^{-1}$, bear in mind that the tabulated values do not account for unsprayed volume. The regulatory guidance probably accounts for some regions of the containment volume not being exposed to the spray. As discussed in Section $D$ of Chapter IV, an unsprayed volume causes some reduction in the apparent value of $\lambda$ or E/D.

The ratio of $E / D\left(m_{f}\right) / E / D\left(m_{f}=0.9\right)$ is identical to the ratio $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$. These ratios are unaffected by the existence of an unsprayed volume and can be compared to the regulatory guidance of 0.1 for $\mathrm{m}_{\mathrm{f}}$ less than 0.02 .

The strategy for developing a simple representation for the many results obtained in the uncertainty study is to correlate values of $\lambda\left(m_{f}=0.9\right)$ and $E / D\left(m_{f}=0.9\right)$ at specific percentiles in the uncertainty distribution in terms of the fall distance, $H$, and the water flux, Q . Then, the ratios $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at specific percentiles in the distribution are correlated with $\mathrm{m}_{\mathrm{f}}$ and Q . Results obtained in this correlation process are:

Table 29 Median values of $\mathrm{E} / \mathrm{D}\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at 50 percent confidence level

|  | E/D (meters ${ }^{-1}$ ) at water fluxes of: |  |  |
| :---: | :---: | :---: | :---: |
| Fall distance (cm) | $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ | $\mathbf{0 . 0 1 \mathrm { cm } ^ { 3 } / \mathrm { cm } ^ { 2 } - \mathrm { s }}$ | $\mathbf{0 . 0 0 1 \mathrm { cm } ^ { 3 } / \mathrm { cm } ^ { 2 } - \mathrm { s }}$ |
| 500 | $10.689-11.742$ | $16.412-17.156$ | $15.445-15.908$ |
| 853 | $9.498-10.260$ | $16.169-16.982$ | $15.408-15.852$ |
| 1000 | $8.988-10.084$ | $16.130-16.971$ | $15.389-15.834$ |
| 1584 | $8.007-8.759$ | $15.641-16.434$ | $15.334-15.815$ |
| 2000 | $7.172-8.166$ | $15.391-16.213$ | $15.297-15.815$ |
| 3000 | $6.222-6.762$ | $14.671-15.545$ | $15.223-15.797$ |
| 4000 | $5.471-6.249$ | $14.256-15.089$ | $15.148-15.630$ |
| 5000 | $4.848-5.694$ | $13.889-14.615$ | $15.093-15.408$ |

Table 3010 percentile values of $E / D\left(m_{f}=0.9\right)$ at 90 percent confidence

|  | . | E/D (meters ${ }^{-1}$ ) at water fluxes of: |  |
| :---: | :---: | :---: | :---: |
| Fall Distance (cm) | $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ | $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ | $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ |
| 500 | $4.040-4.586$ | $5.811-7.389$ | $6.574-7.852$ |
| 853 | $3.418-3.915$ | $5.720-7.158$ | $6.537-7.852$ |
| 1000 | $3.209-3.904$ | $5.776-7.170$ | $6.537-7.852$ |
| 1584 | $2.605-3.235$ | $5.544-6.854$ | $6.519-7.852$ |
| 2000 | $2.289-2.870$ | $5.433-6.748$ | $6.519-7.852$ |
| 3000 | $1.868-2.247$ | $5.152-6.458$ | $6.463-7.852$ |
| 4000 | $1.591-1.942$ | $4.991-6.078$ | $6.463-7.852$ |
| 5000 | $1.402-1.727$ | $4.850-6.102$ | $6.500-7.834$ |

Table 3190 percentile values of $\mathrm{E} / \mathrm{D}\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at 90 percent confidence

|  |  | E/D (meters ${ }^{-1}$ ) at water fluxes of: |  |
| :---: | :---: | :---: | :---: |
| Fall distance $(\mathrm{cm})$ | $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ | $0.01 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$ | $\mathbf{0 . 0 0 1 \mathrm { cm } ^ { 3 } / \mathrm { cm } ^ { 2 } - \mathrm { s }}$ |
| 500 | $23.580-27.176$ | $31.180-38.399$ | $33.112-43.779$ |
| 853 | $21.946-25.842$ | $32.275-37.858$ | $33.112-43.631$ |
| 1000 | $21.265-25.702$ | $30.462-37.269$ | $33.112-43.557$ |
| 1584 | $20.181-24.918$ | $29.845-36.242$ | $33.056-43.316$ |
| 2000 | $19.829-24.770$ | $29.712-35.368$ | $32.964-43.131$ |
| 3000 | $18.726-23.234$ | $28.938-33.406$ | $32.742-42.668$ |
| 4000 | $18.440-22.906$ | $28.086-32.258$ | $32.501-42.242$ |
| 5000 | $18.276-22.660$ | $27.941-32.036$ | $32.353-41.797$ |

- Median Values at 50 Percent Confidence

$$
\begin{aligned}
\ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)= & 6.83707+(1.0074 \pm 0.0079) \ln \mathrm{Q} \\
& -(4.1731 \pm 0.5658) \times 10^{-3} \mathrm{Q}^{2} \mathrm{H} \\
& -(1.2478 \pm 0.2311) \mathrm{Q} \\
& -(2.4045 \pm 0.5562) \times 10^{-5} \mathrm{H} \\
& +(9.006 \pm 2.578) \times 10^{-8} \mathrm{QH}^{2} \\
& \quad \text { standard error }=0.0471 \\
\mathrm{E} / \mathrm{D}\left(\mathrm{~m}_{\mathrm{f}}=0.9\right)= & 21.4006-(21.8270 \pm 2.2819) \mathrm{Q} \\
& -(9.6074 \pm 1.6614) \times 10^{-3} \mathrm{QH} \\
& +(4.17724 \pm 1.14024) \times 10^{-6} \mathrm{Q}^{2} \mathrm{H}^{2} \\
& +(0.2542 \pm 0.00828) \ln \mathrm{Q} \\
& -(0.5466 \pm 0.1235 \ln \mathrm{H} \\
& \text { standard error }=0.4387
\end{aligned}
$$

- 90 Percentile Values at 90 Percent Confidence

$$
\begin{aligned}
\ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)= & 7.10927-(8.0868 \pm 2.8048) \times 10^{-4} \mathrm{Q}^{2} \mathrm{H} \\
& +(0.92549 \pm 0.01060) \ln \mathrm{Q} \\
& \text { standard error }=0.1185 \\
\mathrm{E} / \mathrm{D}\left(\mathrm{~m}_{\mathrm{f}}=0.9\right)= & 31.593-(2.8237 \pm 0.2417) \ln \mathrm{Q} \\
& -(1.7102 \pm 0.7236) \ln \mathrm{H} \\
& \text { standard error }=3.792
\end{aligned}
$$

- 10 Percentile Values at 90 Percent Confidence

$$
\begin{aligned}
\ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)= & 5.5750+(0.94362 \pm 0.01322) \ln \mathrm{Q} \\
& -(7.327 \pm 3.000) \times 10^{-7} \mathrm{QH}^{2} \\
& -(6.9821 \pm 1.0186) \times 10^{-3} \mathrm{Q}^{2} \mathrm{H} \\
& +(3.555 \pm 1.273) \times 10^{-6} \mathrm{Q}^{2} \mathrm{H}^{2} \\
& \text { standard error }=0.1066
\end{aligned}
$$

Development

$$
\begin{aligned}
\mathrm{E} / \mathrm{D}\left(\mathrm{~m}_{\mathrm{f}}=0.9\right)= & 4.36525-(6.0860 \pm 1.5091) \times 10^{-3} \mathrm{QH} \\
& +(2.7906) \pm 1.1523) \times 10^{-6} \mathrm{Q}^{2} \mathrm{H}^{2} \\
& -(0.4080 \pm 0.0780) \ln \mathrm{Q} \\
& \text { standard error }=0.6241
\end{aligned}
$$

Values of the ratio $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ fit well the general expression:

$$
\frac{\lambda\left(\mathrm{m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}=\left[\mathrm{a}+\mathrm{b} \log _{10} \mathrm{Q}\right]\left[1-\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{\mathrm{c}}\right]+\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{\mathrm{c}}
$$

Where $a, b$, and $c$ are parameters that depend on the percentile of the uncertainty distribution for the ratio $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ and the confidence level of interest. For the three cases of interest here:

- Median ( 50 percentile) at 50 Percent Confidence

$$
\frac{\lambda\left(m_{f}\right)}{\lambda\left(m_{f}=0.9\right)}=\left(0.1815-0.01153 \log _{10} Q\right)\left[1-\left(\frac{m_{f}}{0.9}\right)^{0.5843}\right]+\left[\frac{m_{f}}{0.9}\right)^{0.5843}
$$

## - 10 Percentile at 30 Percent Confidence

$$
\frac{\lambda\left(m_{f}\right)}{\lambda\left(m_{f}=0.9\right)}=\left(0.1108-0.00201 \log _{10} Q\right)\left[1-\left(\frac{m_{f}}{0.9}\right)^{0.8945}\right]+\left(\frac{m_{f}}{0.9}\right)^{0.8945}
$$

- 90 Percentile at 90 Percent Confidence

$$
\frac{\lambda\left(m_{f}\right)}{\lambda\left(m_{f}=0.9\right)}=\left(0.3751+0.00648 \log _{10} Q\right)\left[1-\left(\frac{m_{f}}{0.9}\right)^{0.2786}\right]+\left(\frac{m_{f}}{0.9}\right)^{0.2786}
$$

For approximate work the weak dependence of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ on $Q$ may be neglected.
Predictions obtained with these correlation expressions are compared to results of the mechanistic analyses in Figures 59 to 67.


Figure 59 Comparison of median ( 50 percentile) values of $\lambda\left(m_{f}=0.9\right)$ (in units of $\mathrm{hr}^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 50 percent confidence intervals for medians in the distributions calculated with the mechanistic model.


Figure 60 Comparison of 90 percentile values of $\lambda\left(m_{f}=0.9\right)$ (in units of $\mathrm{hr}^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 90 percentile values in the distributions calculated with the mechanistic model.


Figure 61 Comparison of 10 percentile values of $\lambda\left(m_{f}=0.9\right)$ (in units of $\mathrm{hr}^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 10 percentile values in the distributions calculated with the mechanistic model.


Figure 62 Comparison of median ( 50 percentile) values of $\mathrm{E} / \mathrm{D}\left(\mathrm{m}_{\mathrm{f}}=0.9\right.$ ) (in units of meters ${ }^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the $\mathbf{5 0}$ percent confidence intervals for median values in the distributions calculated with the mechanistic model.


Figure 63 Comparison of 90 percentile values of $E / D\left(m_{f}=0.9\right)$ (in units of meters ${ }^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 90 percentile values in the distributions calculated with the mechanistic model.


Figure 64 Comparison of the 10 percentile values of $E / D\left(m_{f}=0.9\right)$ (in units of meters ${ }^{-1}$ ) calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 10 percentile values in the distributions calculated with the mechanistic model.


Figure 65 Comparison of the median ( 50 percentile) values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 50 percent confidence intervals for the median values in the distributions calculated with the mechanistic model.


Figure 66 Comparison of the 90 percentile values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 90 percentile values in the distributions calculated with the mechanistic model.


Figure 67 Comparison of the 10 percentile values of $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ calculated with the correlation to values calculated with the mechanistic model. Bars indicate the 90 percent confidence intervals for the 10 percentile values in the distributions calculated with the mechanistic model.

## Development

The value of the decontamination coefficient for any set of conditions (values of $\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}$ ) can be calculated from:

$$
\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}\right)=\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\left[\frac{\lambda\left(\mathrm{m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}\right]
$$

When unsprayed volumes are significant and there is rapid mixing of the sprayed and unsprayed volumes:

$$
\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}, \alpha\right)=\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{~m}_{\mathrm{f}}\right) /(1+\alpha)
$$

where $\alpha$ is the ratio of unsprayed volume divided by the sprayed volume.

## VI. Examples of the Use of the Simplified Model of Spray Removal of Aerosols

The simplified models of spray removal of aerosols derived in Chapter 5 provide a convenient way to calculate spray decontamination of a containment at known levels of conservatism. Two examples illustrating the use of the simplified models are presented below.

## Example 1:

Consider a containment with spray headers located 3000 cm above the operating floor. Hypothesize that during a severe reactor accident this containment has an atmospheric loading of aerosols of $10 \mathrm{~g} / \mathrm{m}^{3}$ at the end of significant radionuclide release. Assume the sprays provide a water flux of $0.10 \mathrm{~cm}^{3} \mathrm{H}_{2} \mathrm{O} / \mathrm{cm}^{2}$-s. The spray droplets pass through half the containment volume. What is the best estimate of the time required of spray operation to reduce the aerosol concentration to 0.1 $\mathrm{g} / \mathrm{m}^{3}$ ? What are reasonable upper and lower bounds on this time?

## Analysis:

The example asks for a best estimate of the time required to achieve a DF of 100 with sprays for a situation in which there is no continuing release of material into the containment atmosphere. Assume that settling of the aerosols is negligible on the time scales of interest. Assume, further, that the median value of spray performance is, by definition, the best estimate. The differential equation for this problem is:

$$
\frac{\mathrm{dM}}{\mathrm{dt}}=\frac{-\lambda \mathrm{M}}{(1+\alpha)}
$$

where M is the mass of aerosol in the containment. The parameter $\alpha$ is just the ratio of the containment volume that is not contacted by spray droplets to the volume that is contacted by spray droplets:

$$
\alpha=\frac{\mathrm{V}(\text { unsprayed })}{\mathrm{V}(\text { sprayed })}
$$

In this case $\alpha=1$.
Divide through the differential equation by the total mass of aerosol initially suspended in the containment atmosphere:

$$
\frac{d\left[\frac{M(t)}{M(0)}\right]}{\mathrm{dt}}=\frac{\mathrm{dm}_{\mathrm{f}}(\mathrm{t})}{\mathrm{dt}}=\frac{-\lambda}{(1+\alpha)} \frac{\mathrm{M}(\mathrm{t})}{\mathrm{M}(\mathrm{o})}=\frac{-\lambda}{(1+\alpha)} \mathrm{m}_{\mathrm{f}}(\mathrm{t})
$$

## Development

where
$m_{f}(t)=\begin{aligned} & \text { mass fraction of the initially-presented aerosol that remains suspended in the } \\ & \text { containment atmosphere }\end{aligned}$
$\mathrm{M}(\mathrm{t}) \quad=$ total mass of aerosol suspended in the containment atmosphere at time t
$M(0)=$ total mass of aerosol suspended in the containment atmosphere at time zero Note that $\mathrm{m}_{\mathrm{f}}(\mathrm{t})$ is related to the decontamination factor, DF , by:

$$
1 / \mathrm{m}_{\mathrm{f}}(\mathrm{t})=\mathrm{DF}
$$

From the discussions in Chapter $V$, the decontamination coefficient, $\lambda$, is given by:

$$
\lambda=\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\left[\frac{\lambda\left(\mathrm{m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}\right]
$$

where median values of these quantities are:

$$
\begin{aligned}
\ln \left[\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\right]= & 6.83707+1.0074 \ln \mathrm{Q}-4.1731 \times 10^{-3} \mathrm{Q}^{2} \mathrm{H} \\
& -1.2478 \mathrm{Q}-2.4045 \times 10^{-5} \mathrm{H}+9.006 \times 10^{-8} \mathrm{QH}^{2} \\
\frac{\lambda\left(\mathrm{~m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)} & =\left(0.1815-0.01153 \log _{10} \mathrm{Q}\right)\left[1-\left[\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right]^{0.5843}\right] \\
& +\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)
\end{aligned}
$$

For the conditions specified here $(H=3000 \mathrm{~cm}$ and $\mathrm{Q}=0.10)$ :

$$
\ln \left[\lambda\left(m_{f}=0.9\right)\right]=4.2764
$$

or

$$
\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=71.980 \mathrm{hr}^{1}
$$

and

$$
\begin{aligned}
\frac{\lambda\left(m_{f}\right)}{\lambda\left(m_{f}=0.9\right)} & =0.193\left[1-\left(\frac{m_{f}}{0.9}\right]^{0.5843}\right]+\left(\frac{m_{f}}{0.9}\right]^{0.5843} \\
& =0.193+0.8582 \mathrm{~m}_{\mathrm{f}} 0.5843
\end{aligned}
$$

The differential equation is then:

$$
\begin{aligned}
\frac{\mathrm{dm}_{\mathrm{f}}(\mathrm{t})}{\mathrm{dt}} & =-\frac{71.98}{2}\left[0.193+0.8582 \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{0.5843}\right] \mathrm{m}_{\mathrm{f}}(\mathrm{t}) \\
& =-6.946 \mathrm{~m}_{\mathrm{f}}(\mathrm{t})-30.887 \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{1.5843}
\end{aligned}
$$

This equation is easily solved numerically to give the time to achieve $D F=1 / \mathrm{m}_{\mathrm{f}}(\mathrm{t})=100$ to be 0.31 hours. Times required to reach other levels of decontamination are shown in Table 32.

Assume that a reasonable upper bound for the time required to achieve $\mathrm{DF}=100$ is the 90 percentile value. A reasonable lower bound for the time is similarly assumed to be the 10 percentile value. Because of the reciprocal relationship between time and the spray decontamination coefficient, the 90 percentile and 10 percentile times to achieve a specified decontamination are found using the 10 percentile and 90 percentile values of the spray decontamination coefficient, respectively. Then, the appropriate differential equation for determining the reasonable upper bound time is:

$$
\frac{\mathrm{dm}_{\mathrm{f}}(\mathrm{t})}{\mathrm{dt}}=-\frac{\lambda(10 \text { Percentile })}{(1+\alpha)} \mathrm{m}_{\mathrm{f}}(\mathrm{t})
$$

where $\lambda(10$ percentile $)$ is found from:

$$
\begin{aligned}
\lambda & =\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\left[\frac{\lambda\left(\mathrm{m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}\right] \\
\ln \left[\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\right]^{\circ}= & 5.5750+0.94362 \ln \mathrm{Q}-7.327 \times 10^{-7} \mathrm{QH}^{2} \\
& -6.9821 \times 10^{-3} \mathrm{Q}^{2} \mathrm{H}+3.555 \times 10^{-6} \mathrm{Q}^{2} \mathrm{H}^{2}
\end{aligned}
$$

## Development

$$
\begin{aligned}
\frac{\lambda\left(m_{f}\right)}{\lambda\left(m_{f}=0.9\right)} & =\left(0.1108-0.00201 \log _{10} \mathrm{Q}\right)\left[1-\left(\frac{m_{f}(t)}{0.9}\right)^{0.8945}\right] \\
& +\left(\frac{m_{f}(t)}{0.9}\right]^{0.8945}
\end{aligned}
$$

For the conditions of the example:

$$
\begin{gathered}
\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=17.345 \mathrm{hr}^{-1} \\
\frac{\lambda\left(\mathrm{~m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}=0.1128+0.9749 \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{0.8945}
\end{gathered}
$$

Then, the differential equation for the reasonable upper bound (90 percentile) time is:

$$
\frac{\mathrm{dm}_{\mathrm{f}}(\mathrm{t})}{\mathrm{dt}}=-\frac{1.9565}{2} \mathrm{~m}_{\mathrm{f}}(\mathrm{t})-\frac{16.9091}{2} \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{1.8945}
$$

Similarly, the reasonable lower bound ( 10 percentile) time is given using the 90 percentile values of the decontamination coefficient, and the appropriate equations are:

$$
\begin{aligned}
\ln \left[\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)\right]= & 7.10927-8.0868 \times 10^{-4} \mathrm{Q}^{2} \mathrm{H}+0.92549 \ln \mathrm{Q} \\
& \lambda\left(\mathrm{~m}_{\mathrm{f}}=0.9\right)=141.7 \mathrm{hr}^{-1} \\
\frac{\lambda\left(\mathrm{~m}_{\mathrm{f}}\right)}{\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)}= & \left(0.3751+0.00648 \log _{10} \mathrm{Q}\right)\left[1-\frac{\mathrm{m}_{\mathrm{f}}(\mathrm{t})^{0.2786}}{0.9}\right] \\
+ & \left(\frac{\mathrm{m}_{\mathrm{f}}(\mathrm{t})}{0.9}\right)^{0.2786} \\
= & 0.3686+0.6502 \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{0.2786} \\
\frac{d m_{\mathrm{f}}(\mathrm{t})}{\mathrm{dt}}= & -\frac{52.231}{2} \mathrm{~m}_{\mathrm{f}}(\mathrm{t})-\frac{92.132}{2} \mathrm{~m}_{\mathrm{f}}(\mathrm{t})^{0.2786}
\end{aligned}
$$

Results obtained with these equations are also summarized in Table 32.

Table 32 Results for example 1

|  | Time (hours) to reach DF |  |  |
| :---: | :---: | :---: | :---: |
| DF | Median | $\mathbf{9 0}$ Percentile | $\mathbf{1 0}$ Percentile |
| 10 | 0.10 | 0.61 | 0.05 |
| 100 | 0.31 | 2.27 | 0.14 |
| 1000 | 0.60 | 4.49 | 0.22 |
| 10000 | 0.91 | 6.83 | 0.31 |

## Example 2:

For the second example, the containment is considered to have a total volume of $50,000 \mathrm{~m}^{3}$. At time zero the containment is taken to contain no aerosol of safety significance. Also, at time zero an aerosol source of $1000 \mathrm{~g} / \mathrm{s}$ is hypothesized to arise and to operate for one hour. If agglomeration, settling and deposition of the aerosols are neglected, this source will produce an aerosol concentration of $72 \mathrm{grams} / \mathrm{m}^{3}$. What effect will sprays at an elevation of 3000 cm and a water flow rate of $0.1 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s have on the aerosol concentration in containment? Again, sprays are considered to contact only half the containment volume.

## Analysis

The appropriate differential equation for this example is:

$$
\frac{d M(t)}{d t}=-\frac{\lambda M(t)}{(1+\alpha)}+\frac{1}{V} \frac{d S}{d t}
$$

where

$$
\mathrm{M}(\mathrm{t})=\text { aerosol concentration in } \mathrm{g} / \mathrm{m}^{3}
$$

$\frac{\mathrm{dS}}{\mathrm{dt}}=$ aerosol source rate into the containment (g/hr)
$\mathrm{V} \quad=$ containment volume $\left(\mathrm{m}^{3}\right)$
This differential equation has a steady-state asymptote. At the steady-state the mass concentration of aerosol suspended in the containment is given by:

Development

$$
M(\infty)=\frac{\mathrm{dS} / \mathrm{dt}(1+\alpha)}{\lambda \mathrm{V}}
$$

The only difficulty that arises is the selection of the value of $\lambda$. The correlations developed in Chapter V did not consider a continuing source. The correlations have $\lambda$ dependent on the mass fraction of aerosol remaining in the containment atmosphere. But, this concept on mass fraction remaining becomes difficult to define in the face of a continuing source.

It can be recalled that the reason $\lambda$ is dependent on the mass fraction of aerosol remaining in the atmosphere is that sprays not only trap aerosol particles, they also change the size distribution of the aerosols remaining in the atmosphere in such a way that what aerosols are left become progressively harder for sprays to remove. In the case of a continuing source, the size distribution is being renewed by the additional particulate being injected into the atmosphere. An approximate value for $\lambda$ to use for a continuing source is then $\lambda\left(m_{f}=0.9\right)$. The reason that $\lambda\left(m_{f}=0.9\right)$ is such a surprisingly good approximate value is because, with a continuing source, most of the material suspended in the atmosphere at any one time is fresh material provided by the source. More accurate values of $\lambda$ would have to consider the magnitude of the source and the magnitude of the water flux.

Using $\lambda\left(m_{\mathrm{f}}=0.9\right)$, the calculated steady-state mass concentrations in the containment atmosphere while the source is operating are:

- Median value:
$M(\mathrm{t})=2.0 \mathrm{~g} / \mathrm{m}^{3}$
- 90 percentile value: $\mathrm{M}(\mathrm{t})=8.3 \mathrm{~g} / \mathrm{cm}^{3}$
- 10 percentile value: $\mathrm{M}(\mathrm{t})=1.0 \mathrm{~g} / \mathrm{m}^{3}$

The median value corresponds to a decontamination factor of 36 when compared to the concentration of aerosol the source would produce in the absence of any aerosol deposition mechanisms. The 10 percentile and 90 percentile values of the decontamination factor similarly defined are 8.7 and 72 , respectively.

The differential equation shown above can be solved numerically to show the fully dynamic behavior of aerosol concentration in the containment with both a source and the sprays operating. Results of such calculations are shown in Figure 68. In preparing this figure, correlations for $\lambda$ that included the dependence on the mass fraction of aerosol remaining suspended in the atmosphere were used once the source stopped at one hour. Once the source is no longer providing fresh material to the containment atmosphere, the spray system rapidly decontaminates the atmosphere.


Figure 68 Dynamic analysis of aerosol concentration in the containment for example 2

## VII. Conclusions

A description of the phenomena that affect the removal of aerosols by containment sprays has been presented. A mechanistic model of the aerosol removal process has been developed. An important feature of this model is that it recognizes both the distribution in size of spray droplets and the evolution of the droplet size distribution as the droplets fall through the atmosphere. The model has been used to conduct a quantitative uncertainty analysis for the spray decontamination coefficient, $\lambda$, used in the simple differential equation for prediction of aerosol mass removal from the containment atmosphere:

$$
\frac{\mathrm{dm}_{\mathrm{f}}}{\mathrm{dt}}=-\lambda \mathrm{m}_{\mathrm{f}}
$$

where $\mathrm{m}_{\mathrm{f}}$ is the mass fraction remaining in the containment atmosphere.
The decontamination coefficient has been shown to be a function of the water flux into the containment, the fall distance of droplets and the fraction of aerosol removed.

Uncertainty distributions for $\lambda$ have been found for

- water flux $=Q=0.001,0.01$, and $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$,
- fall distance $=\mathrm{H}=500,853,1000,1584,2000,3000,4000$, and 5000 cm , and
- mass fraction of aerosol remaining in the containment atmosphere $=\mathrm{m}_{\mathrm{f}}=0.9,0.5,0.3,0.1$, 0.01 , and 0.001 .

It has been shown that the decontamination coefficient $\lambda$, decreases with increasing decontamination. At a confidence level of 50 percent, the median value of the ratio $\lambda\left(m_{f}=0.01\right) / \lambda\left(m_{f}=0.9\right)$ is between 0.252 and 0.292 for the range of water fluxes considered here. The 90th percentile value of this ratio (at 90 percent confidence) is between 0.520 and 0.580 . The 10th percentile value (again at 90 percent confidence) is between 0.128 and 0.146 .

Simplified models of the spray process have been developed by correlating $\lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ and $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ with water flux, $Q$, fall distance, $H$, and the mass fraction of aerosol remaining in the containment, $\mathrm{m}_{\mathrm{f}}$. Median values of these quantities are given by:

$$
\begin{gather*}
\ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=6.83707+1.0074 \ln \mathrm{Q}-4.1731 \times 10^{-3} \mathrm{Q}^{2} \mathrm{H} \\
-1.2478 \mathrm{Q}-2.4045 \times 10^{-5} \mathrm{H}+9.006 \times 10^{-8} \mathrm{QH}^{2} \\
\lambda\left(\mathrm{~m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=\left(0.1815-0.01153 \log _{10} \mathrm{Q}\right)\left[1-\left[\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right]^{0.5843}\right]+\left[\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right]^{0}
\end{gather*}
$$

The 90 percentile values are given by:

$$
\begin{gathered}
\ln \lambda\left(m_{f}=0.9\right)=7.10927-8.0868 \times 10^{-4} \mathrm{Q}^{2} \mathrm{H}+0.92549 \ln \mathrm{Q} \\
\lambda\left(\mathrm{~m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=\left(0.3751+0.00648 \log _{10} \mathrm{Q}\right)\left[1-\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{0.2786}\right]+\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{0.2786}
\end{gathered}
$$

The 10 percentile values are given by:

$$
\begin{aligned}
& \ln \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)= 5.5750+0.94362 \ln \mathrm{Q} \\
&-7.327 \times 10^{-7} \mathrm{Q} \mathrm{H}^{2}-6.9821 \times 10^{-3} \mathrm{Q}^{2} \mathrm{H} \\
&+3.555 \times 10^{-6} \mathrm{Q}^{2} \mathrm{H}^{2} \\
& \lambda\left(\mathrm{~m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)=\left(0.1108-0.00201 \log _{10} \mathrm{Q}\right)\left[1-\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{0.8945}\right]+\left(\frac{\mathrm{m}_{\mathrm{f}}}{0.9}\right)^{0.8945}
\end{aligned}
$$

These simple expressions have been shown to effectively represent the predictions of the more detailed mechanistic analyses of spray removal of aerosol from a reactor containment atmosphere. Information necessary to prepare similar simple representations of the detailed analyses for different percentiles of the uncertainty distributions or different confidence levels is provided in this document.

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## Appendix A

## Uncertainty Distributions for $\boldsymbol{\lambda}\left(\mathbf{Q}, \mathbf{H}, \mathbf{m}_{\mathbf{f}}\right)$

Uncertainty distributions for the decontamination coefficient $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$ at confidence levels of 50 , 90 , and 95 percent are collected in this appendix. Distributions are presented for

$$
\begin{aligned}
\mathrm{Q} & =0.001,0.01, \text { and } 0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s} \\
\mathrm{H} & =500,853,1000,1584,2000,3000,4000 \text { and } 5000 \mathrm{~cm} \\
\mathrm{~m}_{\mathrm{f}} & =0.9,0.5,0.3,0.1,0.01, \text { and } 0.001
\end{aligned}
$$

where
$\mathrm{Q}=$ volummetric water flux into the containment
$\mathrm{H}=$ fall distance for water droplets
$\mathrm{m}_{\mathrm{f}}=$ mass fraction of aerosol remaining in the containment.
Distribution are presented as ranges of values of $\lambda\left(\mathrm{Q}, \mathrm{H}, \mathrm{m}_{\mathrm{f}}\right)$ that define the percentiles of a cumulative probability distribution. Ranges for percentiles of 5 to 95 percent at 5 percent intervals are tabulated. Means and standard deviations for the distributions are also shown in the tables in this appendix. In the case of a water flux of $0.001 \mathrm{~cm}^{3} / \mathrm{cm}^{2}-\mathrm{s}$, uncertainty distributions are tabulated only for fall distances of 500 and 5000 cm . Results for this low water flux are very insensitive to fall distance. Linear interpolation of the tabulated results yields distributions for other fall distances that are in quite good agreement with the actual calculated distributions.

|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=10.726$ | 5 | 2.298-3.122 | 2.324-3.095 | 2.607-2.926 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 3.120-4.010 | 3.138-3.990 | 3.314-3.730 |  |
|  | 15 | 3.795-4.874 | 3.950-4.770 | 4.105-4.411 |  |
|  | 20 | 4.410-5.615 | 4.487-5.553 | 4.875-5.322 |  |
|  | 25 | 5.235-6.510 | 5.361-6.421 | 5.577-5.928 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =8.358 \end{aligned}$ | 30 | 5.819-6.958 | 5.897-6.890 | 6.409-6.736 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =500 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 6.599-7.716 | 6.668-7.570 | 6.877-7.233 |  |
|  | 40 | 7.145-8.556 | 7.182-8.270 | 7.440-7.906 |  |
|  | 45 | 7.780-9.056 | 7.852-9.019 | 8.008-8.758 |  |
|  | 50 | 8.582-9.731 | 8.697-9.651 | 8.862-9.264 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 9.114-10.594 | 9.182-10.493 | 9.495-10.055 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.9$ |
|  | 60 | 9.835-11.097 | 9.883-11.054 | 10.404-10.766 |  |
|  | 65 | 10.628-12.252 | 10.722-11.967 | 10.908-11.616 |  |
|  | 70 | 11.327-12.991 | 11.565-12.933 | 11.926-12.626 |  |
|  | 75 | 12.467-14.554 | 12.550-14.264 | 12.913-13.279 |  |
|  | 80 | 13.121-15.970 | 13.463-15.517 | 14.358-14.988 |  |
|  | 85 | 15.022-17.511 | 15.278-17.296 | 15.949-16.625 |  |
|  | 90 | 16.744-20.863 | 16.837-20.735 | 17.670-18.212 |  |
|  | 95 | 20.851-27.940 | 21.063-27.010 | 22.113-25.449 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=6.387$ | 5 | 1.682-2.124 | 1.714-2.112 | 1.770-1.979 | WATER FLUX = |
|  | 10 | 2.123-2.626 | 2.128-2.584 | 2.216-2.503 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.546-2.968 | 2.576-2.917 | 2.663-2.779 |  |
|  | 20 | 2.778-3.416 | 2.806-3.379 | 2.979-3.226 |  |
|  | 25 | 3.207-3.780 | 3.237-3.713 | 3.396-3.619 |  |
| STD. DEV. = | 30 | 3.547-4.180 | 3.596-4.101 | $3.713-3.884$ | FALL DISTANCE = |
| $=4.550$ | 35 | 3.824-4.510 | 3.876-4.493 | $4.079-4.335$ | $=500 \mathrm{~cm}$ |
|  | 40 | 4.276-5.122 | 4.310-5.060 | 4.463-4.742 |  |
|  | 45 | 4.590-5.517 | 4.616-5.444 | 4.960-5.369 |  |
|  | 50 | 5.184-5.973 | 5.252-5.936 | 5.412-5.799 |  |
| SAMPLE SIZE = | 55 | 5.591-6.372 | 5.690-6.339 | 5.880-6.099 | AEROSOL MASS |
| $=400$ | 60 | 5.983-6.851 | 6.075-6.654 | $6.197-6.513$ | FRACTION REMAINING $=$ |
|  | 65 | 6.420-7.234 | 6.476-7.165 | 6.580-6.992 | $=0.3$ |
|  | 70 | 6.885-7.756 | 6.951-7.621 | 7.100-7.403 |  |
|  | 75 | 7.332-8.442 | $7.386-8.255$ | $7.572-7.980$ |  |
|  | 80 | 7.888-9.141 | 8.016-9.124 | 8.266-8.946 |  |
|  | 85 | 8.959-10.046 | 9.042-9.969 | 9.141-9.655 |  |
|  | 90 | 9.785-11.990 | 9.907-11.745 | 10.267-11.007 |  |
|  | 95 | 11.979-18.196 | 12.567-17.734 | 13.082-14.430 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.592$ | 5 | 1.203-1.548 | 1.243-1.510 | 1.358-1.466 | WATER FLUX = |
|  | 10 | 1.546-1.860 | 1.596-1.832 | 1.687-1.770 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.785-2.168 | 1.813-2.144 | 1.905-2.016 |  |
|  | 20 | 2.016-2.398 | 2.028-2.373 | 2.169-2.281 |  |
|  | 25 | 2.223-2.642 | 2.282-2.558 | 2.378-2.492 |  |
| STD. DEV. $=$ | 30 | 2.474-2.830 | 2.487-2.803 | 2.555-2.743 | FALL DISTANCE $=$ |
| $=3.262$ | 35 | 2.707-3.207 | 2.741-3.173 | 2.786-3.080 | $=500 \mathrm{~cm}$ |
|  | 40 | 2.952-3.611 | 3.006-3.528 | 3.152-3.317 |  |
|  | 45 | 3.226-3.822 | 3.274-3.783 | 3.460-3.676 |  |
|  | 50 | 3.629-4.058 | 3.661-4.028 | $3.765-3.930$ |  |
| SAMPLE SIZE = | 55 | 3.844-4.441 | 3.889-4.353 | 3.982-4.154 | AEROSOL MASS |
| $=400$ | 60 | 4.068-4.769 | 4.136-4.659 | 4.319-4.494 | FRACTION REMAINING $=$ |
|  | 65 | 4.461-5.228 | 4.484-5.170 | 4.607-4.946 | $\doteq 0.1$ |
|  | 70 | 4.860-5.564 | 4.938-5.486 | 5.091-5.385 |  |
|  | 75 | 5.318-6.215 | 5.377-6.127 | 5.485-5.837 |  |
|  | 80 | 5.733-6.848 | 5.852-6.727 | 6.170-6.489 |  |
|  | 85 | 6.499-7.464 | 6.557-7.449 | 6.843-7.232 |  |
|  | 90 | 7.330-9.214 | 7.410-8.923 | 7.524-8.003 |  |
|  | 95 | 9.134-13.779 | 9.432-13.409 | 10.425-11.803 |  |

Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.922$ | 5 | 0.732-1.009 | 0.760-1.002 | 0.876-0.955 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 1.008-1.141 | 1.019-1.138 | 1.032-1.104 |  |
|  | 15 | 1.130-1.300 | 1.134-1.281 | 1.204-1.242 |  |
|  | 20 | 1.241-1.476 | 1.249-1.448 | 1.301-1.405 |  |
|  | 25 | 1.393-1.621 | 1.409-1.610 | 1.456-1.556 |  |
| STD. DEV. $=$$=2.162$ | 30 | 1.512-1.797 | 1.540-1.776 | 1.607-1.684 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =500 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 1.644-1.906 | 1.667-1.888 | $1.753-1.832$ |  |
|  | 40 | 1.805-2.068 | 1.824-2.040 | 1.869-1.953 |  |
|  | 45 | 1.918-2.183 | 1.933-2.166 | 2.021-2.099 |  |
|  | 50 | 2.072-2.429 | 2.093-2.411 | 2.141-2.261 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 2.193-2.691 | 2.212-2.658 | 2.378-2.532 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 2.434-3.001 | 2.461-2.933 | 2.587-2.813 |  |
|  | 65 | 2.706-3.243 | 2.786-3.230 | 2.908-3.118 |  |
|  | 70 | 3.026-3.580 | 3.077-3.527 | 3.204-3.324 |  |
|  | 75 | 3.290-3.970 | 3.322-3.916 | 3.500-3.810 |  |
|  | 80 | 3.787-4.432 | 3.814-4.388 | 3.929-4.230 |  |
|  | 85 | 4.231-5.056 | 4.252-4.930 | 4.429-4.579 |  |
|  | 90 | 4.609-6.428 | 4.708-6.311 | 5.242-5.675 |  |
|  | 95 | 6.419-9.424 | 6.588-9.272 | 7.474-8.518 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.284$ | 5 | 0.585-0.742 | 0.616-0.738 | 0.659-0.720 | WATER FLUX = |
|  | 10 | 0.740-0.912 | 0.747-0.902 | 0.815-0.862 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.869-1.009 | 0.882-1.000 | 0.924-0.970 |  |
|  | 20 | 0.970-1.164 | 0.979-1.141 | 1.010-1.075 |  |
|  | 25 | 0.107-1.255 | 1.077-1.253 | 1.156-1.225 |  |
| STD. DEV. = | 30 | 1.193-1.332 | 1.215-1.324 | 1.253-1.293 | FALL DISTANCE $=$ |
| $=1.727$ | 35 | 1.277-1.441 | 1.293-1.436 | 1.319-1.391 | $=500 \mathrm{~cm}$ |
|  | 40 | 1.340-1.582 | 1.371-1.573 | 1.431-1.523 |  |
|  | 45 | 1.476-1.692 | 1.501-1.656 | 1.557-1.616 |  |
|  | 50 | 1.593-1.813 | 1.597-1.797 | 1.640-1.740 |  |
| SAMPLE SIZE = | 55 | 1.694-2.098 | 1.717-2.068 | 1.760-1.877 | AEROSOL MASS |
| $=400$ | 60 | 1.821-2.304 | 1.845-2.252 | 2.042-2.142 | FRACTION REMAINING $=$ |
|  | 65 | 2.114-2.559 | 2.127-2.526 | 2.231-2.426 | $=0.001$ |
|  | 70 | 2.349-2.725 | 2.381-2.720 | 2.516-2.642 |  |
|  | 75 | 2.583-3.121 | 2.638-3.075 | 2.716-2.927 |  |
|  | 80 | 2.873-3.480 | 2.934-3.431 | 3.085-3.291 |  |
|  | 85 | 3.296-4.136 | 3.333-3.970 | 3.475-3.715 |  |
|  | 90 | 3.802-5.383 | 3.894-4.952 | 4.286-4.623 |  |
|  | 95 | 5.359-7.455 | 5.404-7.227 | 5.679-6.791 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=10.511$ | 5 | 2.212-3.061 | 2.275-2.995 | 2.538-2.802 | WATER FLUX = |
|  | 10 | 3.051-3.945 | 3.089-3.865 | 3.222-3.530 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.603-4.760 | $3.770-4.591$ | 4.032-4.386 |  |
|  | 20 | 4.386-5.484 | 4.396-5.399 | 4.770-5.221 |  |
|  | 25 | 5.153-6.431 | 5.234-6.364 | 5.407-5.805 |  |
| STD. DEV. $=$ | 30 | 5.692-6.877 | 5.803-6.754 | 6.273-6.597 | FALL DISTANCE $=$ |
| $=8.130$ | 35 | 6.510-7.556 | 6.575-7.372 | 6.734-7.112 | $=853 \mathrm{~cm}$. |
|  | 40 | 6.936-8.363 | 7.090-8.000 | 7.325-7.765 |  |
|  | 45 | 7.579-8.854 | 7.670-8.828 | 7.969-8.579 |  |
|  | 50 | 8.371-9.624 | 8.466-9.458 | 8.731-9.170 |  |
| SAMPLE SIZE = | 55 | 8.860-10.422 | 9.005-10.313 | 9.396-9.893 | AEROSOL MASS |
| $=400$ | 60 | 9.630-11.003 | 9.745-10.836 | 10.281-10.619 | FRACTION REMAINING $=$ |
|  | 65 | 10.475-11.976 | 10.519-11.876 | 10.771-11.463 | $=0.9$ |
|  | 70 | 11.071-12.918 | 11.224-12.825 | 11.823-12.513 |  |
|  | 75 | 12.250-14.376 | 12.503-14.060 | 12.776-13.299 |  |
|  | 80 | 13.067-15.648 | 13.539-15.488 | 14.112-14.919 |  |
|  | 85 | 14.943-17.384 | 15.130-17.060 | 15.631-16.407 |  |
|  | 90 | 16.582-20.912 | 16.892-20.443 | 17.428-18.443 |  |
|  | 95 | 20.740-28.004 | 21.200-27.560 | 21.985-24.831 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.714$ | 5 | 1.922-2.427 | 2.015-2.399 | 2.129-2.260 | WATER FLUX = |
|  | 10 | 2.414-3.058 | 2.467-3.023 | 2.648-2.870 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.936-3.577 | 2.973-3.518 | 3.133-3.356 |  |
|  | 20 | 3.355-4.226 | 3.446-4.098 | 3.586-3.864 |  |
|  | 25 | 3.787-4.647 | 3.872-4.591 | 4.133-4.479 |  |
| STD. DEV. = | 30 | 4.443-5.143 | 4.463-5.008 | 4.579-4.789 | FALL DISTANCE $=$ |
| $=5.607$ | 35 | 4.692-5.703 | 4.771-5.504 | 4.953-5.280 | $=853 \mathrm{~cm}$ |
|  | 40 | 5.174-6.137 | 5.207-6.084 | 5.451-5.841 |  |
|  | 45 | 5.734-6.682 | 5.786-6.616 | 6.000-6.278 |  |
|  | 50 | 6.143-7.432 | 6.200-7.139 | 6.428-6.887 |  |
| SAMPLE SIZE = | 55 | 6.684-7.934 | 6.777-7.854 | 7.050-7.537 | AEROSOL MASS |
| $=400$ | 60 | 7.441-8.348 | 7.510-8.241 | 7.726-8.017 | FRACTION REMAINING = |
|  | 65 | 7.936-8.694 | 7.981-8.674 | 8.170-8.455 | $=0.5$ |
|  | 70 | 8.429-9.298 | 8.449-9.229 | 8.620-8.874 |  |
|  | 75 | 8.777-10.260 | 8.871-10.081 | 9.216-9.694 |  |
|  | 80 | 9.616-10.918 | 9.702-10.856 | 10.142-10.529 |  |
|  | 85 | 10.535-12.226 | 10.627-12.094 | 10.914-11.631 |  |
|  | 90 | 11.960-14.150 | 12.052-14.136 | 12.513-13.450 |  |
|  | 95 | 14.148-20.575 | 14.597-20.344 | 15.164-17.496 |  |



|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.509$ | 5 | 1.180-1.546 | 1.227-1.508 | 1.320-1.449 | WATER FLUX = |
|  | 10 | 1.544-1.855 | 1.594-1.820 | 1.648-1.754 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.758-2.114 | 1.785-2.098 | 1.877-1.994 |  |
|  | 20 | 1.994-2.377 | 2.014-2.342 | 2.115-2.218 |  |
|  | 25 | 2.198-2.578 | 2.231-2.532 | 2.347-2.464 |  |
| STD. DEV. = | 30 | 2.420-2.803 | 2.457-2.752 | 2.510-2.656 | FALL DISTANCE = |
| $=3.203$ | 35 | 2.631-3.174 | 2.642-3.126 | 2.723-3.050 | $=853 \mathrm{~cm}$ |
|  | 40 | 2.855-3.555 | 2.943-3.427 | 3.108-3.270 |  |
|  | 45 | 3.196-3.774 | 3.252-3.751 | 3.379-3.646 |  |
|  | 50 | 3.562-4.018 | 3.593-3.958 | 3.705-3.850 |  |
| SAMPLE SIZE $=$ | 55 | 3.786-4.331 | 3.827-4.267 | 3.936-4.110 |  |
| $=400$ | 60 | 4.033-4.682 | 4.063-4.614 | 4.227-4.480 | FRACTION REMAINING $=$ |
|  | 65 | 4.346-5.114 | 4.453-5.055 | 4.551-4.930 | $=0.1$ |
|  | 70 | 4.762-5.461 | 4.868-5.391 | 5.020-5.224 |  |
|  | 75 | 5.178-6.074 | 5.223-6.013 | 5.376-5.656 |  |
|  | 80 | 5.604-6.671 | 5.674-6.568 | 6.041-6.377 |  |
|  | 85 | 6.380-7.360 | 6.421-7.304 | 6.666-7.118 |  |
|  | 90 | 7.215-8.971 | 7.266-8.352 | 7.411-7.902 |  |
|  | 95 | 8.940-13.736 | 9.074-13.381 | 10.100-11.517 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.865$ | 5 | 0.702-0.981 | 0.727-0.979 | 0.861-0.920 | WATER FLUX = |
|  | 10 | 0.980-1.134 | 0.982-1.117 | 1.020-1.087 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.100-1.276 | 1.109-1.249 | 1.165-1.213 |  |
|  | 20 | 1.212-1.450 | 1.230-1.425 | 1.277-1.391 |  |
|  | 25 | 1.360-1.604 | 1.395-1.581 | 1.427-1.509 |  |
| STD. DEV. = | 30 | 1.486-1.756 | 1.503-1.737 | 1.573-1.668 | FALL DISTANCE = |
| $=2.130$ | 35 | 1.623-1.872 | 1.640-1.855 | 1.725-1.806 | $=853 \mathrm{~cm}$ |
|  | 40 | 1.770-2.009 | 1.797-1.994 | 1.836-1.915 |  |
|  | 45 | 1.882-2.164 | 1.904-2.136 | 1.980-2.056 |  |
|  | 50 | 2.010-2.381 | 2.019-2.349 | 2.112-2.210 |  |
| SAMPLE SIZE = | 55 | 2.173-2.609 | 2.194-2.594 | 2.316-2.450 |  |
| $=400$ | $60$ | $2.392-2.906$ | $2.418-2.883$ | $2.576-2.766$ | FRACTION REMAINING = |
|  | 65 | $2.639-3.197$ | $2.708-3.181$ | $2.862-3.029$ | $=0.01$ |
|  | 70 | 2.965-3.550 | 3.007-3.443 | 3.174-3.280 |  |
|  | 75 | 3.230-3.892 | 3.272-3.844 | 3.433-3.728 |  |
|  | 80 | 3.687-4.365 | 3.730-4.263 | 3.857-4.103 |  |
|  | 85 | 4.109-4.927 | 4.142-4.804 | 4.351-4.504 |  |
|  | 90 | 4.550-6.275 | 4.596-6.114 | 5.116-5.603 |  |
|  | 95 | 6.248-9.346 | 6.432-9.095 | 7.320-8.372 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.251$ | 5 | 0.573-0.730 | 0.605-0.726 | 0.654-0.709 | WATER FLUX = |
|  | 10 | 0.729-0.898 | 0.733-0.878 | 0.788-0.850 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.863-0.990 | 0.870-0.985 | 0.913-0.959 |  |
|  | 20 | 0.957-1.147 | 0.968-1.118 | 0.991-1.067 |  |
|  | 25 | 1.049-1.248 | 1.068-1.236 | 1.137-1.200 |  |
| STD. DEV. $=$ | 30 | 1.187-1.311 | 1.198-1.296 | 1.233-1.266 | FALL DISTANCE $=$ |
| $=1.705$ | 35 | 1.257-1.426 | 1.265-1.413 | 1.291-1.379 | $=853 \mathrm{~cm}$ |
|  | 40 | 1.328-1.552 | 1.360-1.532 | 1.404-1.503 |  |
|  | 45 | 1.442-1.673 | 1.474-1.649 | 1.526-1.592 |  |
|  | 50 | 1.557-1.793 | 1.568-1.755 | 1.630-1.696 |  |
| SAMPLE SIZE = | 55 | 1.677-2.051 | 1.687-2.031 | 1.746-1.853 | AEROSOL MASS |
| $=400$ | 60 | 1.802-2.288 | 1.830-2.225 | 2.013-2.119 | FRACTION REMAINING $=$ |
|  | 65 | 2.071-2.514 | 2.098-2.475 | 2.181-2.372 | $=0.001$ |
|  | 70 | 2.341-2.715 | 2.356-2.698 | 2.457-2.608 |  |
|  | 75 | 2.555-3.108 | 2.577-3.026 | 2.688-2.841 |  |
|  | 80 | 2.798-3.429 | 2.855-3.408 | 3.046-3.250 |  |
|  | 85 | 3.252-4.049 | 3.263-3.949 | 3.427-3.661 |  |
|  | 90 | 3.746-5.346 | 3.880-4.864 | 4.268-4.524 |  |
|  | 95 | 5.334-7.439 | 5.383-7.141 | 5.653-6.731 |  |

Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=10.455$ | 5 | 2.248-3.083 | 2.305-3.025 | 2.589-2.878 | WATER FLUX = |
|  | 10 | 3.059-3.967 | 3.119-3.872 | 3.249-3.543 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.753-4.751 | 3.802-4.660 | 4.064-4.382 |  |
|  | 20 | 4.382-5.535 | 4.393-5.367 | 4.755-5.209 |  |
|  | 25 | 5.055-6.411 | 5.217-6.347 | 5.387-5.816 |  |
| STD. DEV. = | 30 | 5.733-6.871 | 5.799-6.775 | $6.251-6.534$ | FALL DISTANCE = |
| $=8.086$ | 35 | 6.492-7.497 | 6.504-7.369 | $6.739-7.131$ | $=1000 \mathrm{~cm}$ |
|  | 40 | 6.914-8.277 | 7.052-7.996 | 7.330-7.818 |  |
|  | 45 | 7.528-8.839 | 7.615-8.764 | 7.957-8.553 |  |
|  | 50 | 8.326-9.621 | 8.457-9.430 | 8.710-9.164 |  |
| SAMPLE SIZE = | 55 | 8.840-10.402 | 8.979-10.305 | 9.378-9.880 | AEROSOL MASS |
| $=400$ | 60 | 9.628-11.019 | 9.738-10.824 | 10.200-10.579 | FRACTION REMAINING $=$ |
|  | 65 | 10.460-11.900 | 10.511-11.831 | 10.751-11.449 | $=0.9$ |
|  | 70 | 11.075-12.874 | 11.204-12.732 | 11.762-12.447 |  |
|  | 75 | 12.234-14.141 | 12.439-13.900 | 12.716-13.094 |  |
|  | 80 | 13.004-15.486 | 13.204-15.412 | 13.942-14.739 |  |
|  | 85 | 14.759-17.162 | 14.966-16.712 | 15.483-16.191 |  |
|  | 90 | 16.360-20.363 | 16.449-20.125 | 17.333-17.965 |  |
|  | 95 | 20.335-27.421 | 20.956-26.632 | 21.306-24.326 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.651$ | 5 | 1.856-2.398 | 1.930-2.339 | 2.112-2.234 | WATER FLUX = |
|  | 10 | 2.397-3.023 | 2.439-2.964 | 2.562-2.837 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.870-3.520 | 2.944-3.499 | 3.082-3.326 |  |
|  | 20 | 3.324-4.115 | 3.380-4.071 | 3.523-3.811 |  |
|  | 25 | 3.735-4.626 | 3.815-4.568 | 4.082-4.434 |  |
| STD. DEV. = | 30 | 4.381-5.080 | 4.422-4.931 | 4.566-4.752 | FALL DISTANCE = |
| $=5.587$ | 35 | 4.677-5.558 | 4.733-5.454 | 4.885-5.230 | $=1000 \mathrm{~cm}$ |
|  | 40 | 5.121-6.055 | 5.178-6.021 | 5.379-5.784 |  |
|  | 45 | 5.670-6.665 | 5.728-6.453 | 5.904-6.218 |  |
|  | 50 | 6.082-7.377 | 6.143-7.084 | 6.379-6.802 |  |
| SAMPLE SIZE $=$ | 55 | 6.676-7.871 | $6.690-7.723$ | 7.010-7.513 | AEROSOL MASS |
| $=400$ | 60 | 7.389-8.274 | 7.439-8.181 | $7.647-7.956$ | FRACTION REMAINING $=$ |
|  | 65 | 7.921-8.599 | 7.733-8.548 | 8.107-8.437 | $=0.5$ |
|  | 70 | 8.381-9.204 | 8.428-9.163 | 8.525-8.851 |  |
|  | 75 | 8.692-10.217 | 8.825-10.058 | 9.151-9.557 |  |
|  | 80 | 9.486-10.896 | 9.581-10.838 | 10.113-10.504 |  |
|  | 85 | 10.510-12.155 | 10.600-12.048 | 10.888-11.592 |  |
|  | 90 | 11.862-14.134 | 11.957-14.046 | 12.452-13.379 |  |
|  | 95 | 14.124-20.561 | 14.583-20.329 | 15.153-17.350 |  |

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|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.485$ | 5 | 1.177-1.545 | 1.221-1.508 | 1.302-1.448 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 1.544-1.839 | 1.588-1.817 | 1.644-1.751 |  |
|  | 15 | 1.757-2.103 | 1.784-2.064 | 1.866-1.980 |  |
|  | 20 | 1.978-2.360 | 2.014-2.339 | 2.106-2.216 |  |
|  | 25 | 2.196-2.562 | 2.221-2.499 | 2.344-2.461 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =3.188 \end{aligned}$ | 30 | 2.402-2.794 | 2.453-2.750 | 2.498-2.633 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =1000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 2.613-3.166 | 2.620-3.120 | 2.706-3.047 |  |
|  | 40 | 2.841-3.487 | 2.938-3.382 | 3.097-3.260 |  |
|  | 45 | 3.193-3.748 | 3.240-3.718 | 3.370-3.607 |  |
|  | 50 | 3.522-3.982 | 3.562-3.951 | 3.665-3.823 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 3.751-4.294 | 3.804-4.230 | 3.905-4.088 | AEROSOL MASS FRACTION REMAINING = $=0.1$ |
|  | 60 | 4.017-4.649 | $4.040-4.589$ | $4.181-4.477$ |  |
|  | 65 | 4.338-5.043 | 4.450-5.013 | $4.532-4.911$ |  |
|  | 70 | 4.729-5.443 | 4.858-5.385 | 4.993-5.170 |  |
|  | 75 | 5.149-6.029 | 5.169-5.968 | 5.363-5.574 |  |
|  | 80 | 5.563-6.604 | 5.603-6.548 | 5.974-6.291 |  |
|  | 85 | 6.304-7.324 | 6.395-7.298 | 6.602-7.045 |  |
|  | 90 | 7.184-8.957 | 7.233-8.286 | 7.376-7.870 |  |
|  | 95 | 8.929-13.722 | 9.012-13.371 | 10.089-11.463 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.858$ | 5 | 0.717-0.980 | 0.746-0.973 | 0.864-0.924 | WATER FLUX = |
|  | 10 | 0.979-1.137 | 0.982-1.124 | 1.019-1.076 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.100-1.277 | 1.106-1.258 | 1.166-1.212 |  |
|  | 20 | 1.211-1.446 | 1.226-1.426 | 1.278-1.394 |  |
|  | 25 | 1.378-1.607 | 1.394-1.585 | 1.437-1.504 |  |
| STD. DEV. $=$ | 30 | 1.490-1.744 | 1.501-1.732 | $1.582-1.658$ | FALL DISTANCE $=$ |
| $=2.112$ | $35$ | $1.621-1.877$ | $1.638-1.851$ | $1.723-1.807$ | $=1000 \mathrm{~cm}$ |
|  | $40$ | $1.771-2.005$ | $1.793-1.976$ | 1.838-1.924 |  |
|  | $45$ | $1.895-2.163$ | $1.911-2.151$ | 1.964-2.076 |  |
|  | 50 | 2.010-2.388 | 2.016-2.360 | 2.120-2.233 |  |
| SAMPLE SIZE $=$ | 55 | 2.172-2.645 | 2.206-2.586 | 2.306-2.493 | AEROSOL MASS |
| $=400$ | 60 | 2.409-2.924 | 2.431-2.878 | 2.574-2.766 | FRACTION REMAINING $=$ |
|  | 65 | 2.684-3.217 | 2.725-3.171 | 2.860-3.033 | $=0.01$ |
|  | 70 | 2.984-3.570 | 3.004-3.499 | 3.160-3.300 |  |
|  | 75 | 3.259-3.888 | 3.285-3.841 | 3.461-3.676 |  |
|  | 80 | 3.643-4.348 | 3.696-4.248 | 3.861-4.082 |  |
|  | 85 | 4.084-5.017 | 4.114-4.809 | 4.346-4.487 |  |
|  | 90 | 4.569-6.322 | 4.687-6.148 | 5.212-5.656 |  |
|  | 95 | 6.304-9.289 | 6.428-9.066 | 7.250-8.304 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.235$ | 5 | 0.568-0.723 | 0.602-0.720 | 0.652-0.703 | WATER FLUX = |
|  | 10 | 0.722-0.880 | 0.732-0.870 | 0.777-0.847 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.851-0.985 | 0.865-0.983 | 0.908-0.952 |  |
|  | 20 | 0.952-1.142 | 0.960-1.103 | 0.985-1.065 |  |
|  | 25 | 1.046-1.238 | 1.067-1.229 | 1.127-1.196 |  |
| STD. DEV. = | 30 | 1.181-1.314 | 1.193-1.292 | 1.228-1.263 | FALL DISTANCE $=$ |
| $=1.691$ | 35 | 1.248-1.424 | 1.256-1.417 | 1.290-1.371 | $=1000 \mathrm{~cm}$ |
|  | 40 | 1.330-1.540 | 1.358-1.529 | 1.396-1.489 |  |
|  | 45 | 1.438-1.658 | 1.461-1.652 | 1.520-1.592 |  |
|  | 50 | 1.552-1.792 | 1.567-1.752 | 1.631-1.702 |  |
| SAMPLE SIZE $=$ | 55 | 1.664-2.047 | 1.682-2.022 | 1.731-1.852 | AEROSOL MASS |
| $=400$ | 60 | 1.800-2.272 | 1.821-2.212 | 1.973-2.102 | FRACTION REMAINING $=$ |
|  | 65 | 2.057-2.503 | 2.082-2.445 | 2.174-2.366 | $=0.001$ |
|  | 70 | 2.331-2.712 | 2.344-2.686 | 2.431-2.604 |  |
|  | 75 | 2.539-3.097 | 2.571-3.001 | 2.674-2.806 |  |
|  | 80 | 2.762-3.415 | 2.835-3.374 | 3.024-3.217 |  |
|  | 85 | 3.225-4.204 | 3.294-3.954 | 3.413-3.671 |  |
|  | 90 | 3.791-5.370 | 3.937-5.301 | 4.278-4.497 |  |
|  | 95 | 5.347-7.472 | 5.394-7.434 | 5.719-6.760 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=10.204$ | 5 | 2.206-2.968 | 2.250-2.928 | 2.532-2.794 | WATER FLUX = |
|  | 10 | 2.943-3.898 | 3.053-3.742 | 3.126-3.471 | $=0.010 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.633-4.537 | 3.695-4.505 | 3.976-4.327 |  |
|  | 20 | 4.319-5.384 | 4.377-5.202 | 4.545-4.941 |  |
|  | 25 | 4.897-6.128 | 4.981-6.044 | 5.224-5.685 |  |
| STD. DEV. = | 30 | 5.578-6.717 | 5.668-6.680 | 5.989-6.413 | FALL DISTANCE $=$ |
| $=7.895$ | 35 | 6.360-7.280 | 6.398-7.190 | $6.637-6.864$ | $=1584 \mathrm{~cm}$ |
|  | 40 | 6.783-7.976 | 6.816-7.930 | 7.128-7.619 |  |
|  | 45 | 7.289-8.647 | 7.355-8.550 | 7.856-8.289 |  |
|  | 50 | 7.981-9.399 | 8.228-9.350 | 8.446-8.874 |  |
| SAMPLE SIZE $=$ | 55 | 8.659-10.253 | 8.773-10.034 | 9.232-9.647 | AEROSOL MASS |
| $=400$ | 60 | 9.439-10.780 | 9.573-10.690 | 9.928-10.463 | FRACTION REMAINING $=$ |
|  | 65 | 10.262-11.840 | 10.362-11.690 | 10.672-11.032 | $=0.9$ |
|  | 70 | 10.919-12.723 | 10.997-12.559 | 11.622-12.133 |  |
|  | 75 | 11.895-13.724 | 12.130-13.493 | 12.461-12.933 |  |
|  | 80 | 12.899-14.993 | 12.961-14.805 | 13.527-14.431 |  |
|  | 85 | 14.454-16.590 | 14.595-16.169 | 14.977-15.682 |  |
|  | 90 | 15.965-19.667 | 16.074-19.231 | 16.719-17.739 |  |
|  | 95 | 19.618-26.092 | 19.974-25.715 | 20.725-23.225 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.496$ | 5 | 1.896-2.374 | 1.994-2.348 | 2.101-2.221 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 2.370-2.956 | 2.395-2.879 | 2.590-2.799 |  |
|  | 15 | 2.829-3.507 | 2.844-3.463 | 3.021-3.259 |  |
|  | 20 | 3.257-4.059 | 3.322-4.020 | 3.509-3.736 |  |
|  | 25 | 3.724-4.551 | 3.752-4.481 | 4.045-4.356 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =5.450 \end{aligned}$ | 30 | 4.248-4.902 | 4.326-4.855 | 4.481-4.664 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =1584 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 4.634-5.423 | 4.650-5.365 | 4.824-5.138 |  |
|  | 40 | 4.967-5.932 | 5.102-5.856 | 5.291-5.593 |  |
|  | 45 | 5.439-6.453 | 5.524-6.411 | 5.750-6.167 |  |
|  | 50 | 5.965-7.156 | 6.068-7.021 | 6.342-6.651 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 6.504-7.645 | 6.566-7.560 | 6.870-7.370 | AEROSOL MASS <br> FRACTION REMAINING = $=0.5$ |
|  | 60 | 7.212-8.071 | 7.293-7.984 | 7.521-7.867 |  |
|  | 65 | 7.667-8.517 | 7.817-8.428 | 7.962-8.226 |  |
|  | 70 | 8.138-9.044 | 8.216-8.934 | 8.402 - 8.710 |  |
|  | 75 | 8.631-9.893 | 8.680-9.741 | 8.912-9.334 |  |
|  | 80 | 9.250-10.765 | 9.354-10.644 | 9.770-10.303 |  |
|  | 85 | 10.306-11.917 | 10.337-11.741 | 10.756-11.316 |  |
|  | 90 | 11.469-14.009 | 11.656-13.522 | 12.094-13.000 |  |
|  | 95 | 13.990-20.255 | 14.099-19.850 | 15.090-16.821 |  |

## Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=6.117$ | 5 | 1.658-2.021 | 1.665-2.006 | 1.738-1.911 | WATER FLUX = |
|  | 10 | 2.018-2.496 | 2.035-2.468 | 2.134-2.367 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.406-2.882 | 2.424-2.828 | 2.525-2.679 |  |
|  | 20 | 2.677-3.312 | 2.765-3.281 | 2.886-3.129 |  |
|  | 25 | 3.100-3.626 | 3.141-3.590 | 3.287-3.474 |  |
| STD. DEV. = | 30 | 3.428-3.944 | 3.456-3.871 | 3.573-3.742 | FALL DISTANCE = |
| $=4.362$ | 35 | 3.677-4.373 | $3.700-4.340$ | 3.869-4.083 | $=1584 \mathrm{~cm}$ |
|  | 40 | 3.988-4.889 | 4.038-4.829 | 4.257-4.471 |  |
|  | 45 | 4.376-5.353 | 4.450-5.280 | 4.777-5.091 |  |
|  | 50 | 4.930-5.785 | 5.014-5.722 | 5.222-5.495 |  |
| SAMPLE SIZE = | 55 | 5.359-6.135 | 5.390-6.080 | 5.675-5.859 |  |
| $=400$ | 60 | 5.791-6.451 | 5.808-6.414 | $6.050-6.283$ | FRACTION REMAINING $=$ |
|  | 65 | 6.184-6.940 | 6.233-6.810 | $6.391-6.579$ | $=0.3$ |
|  | 70 | 6.483-7.290 | 6.554-7.233 | 6.785-7.056 |  |
|  | 75 | 7.014-8.249 | 7.052-8.086 | 7.202-7.440 |  |
|  | 80 | 7.426-9.007 | 7.481-8.854 | 8.141-8.590 |  |
|  | 85 | 8.601-9.867 | 8.738-9.645 | 9.002-9.114 |  |
|  | 90 | 9.328-11.658 | 9.354-11.224 | 9.999-10.479 |  |
|  | 95 | 11.628-17.391 | 11.801-16.839 | 12.507-14.170 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.382$ | 5 | 1.164-1.540 | 1.182-1.505 | 1.266-1.445 | $\begin{aligned} & \text { WATER FLUX = } \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 1.539-1.786 | 1.540-1.776 | 1.600-1.722 |  |
|  | 15 | 1.748-2.024 | - 1.753-2.012 | 1.840-1.912 |  |
|  | 20 | 1.911-2.300 | 1.956-2.289 | 2.025-2.198 |  |
|  | 25 | 2.171-2.472 | 2.201-2.459 | 2.295-2.387 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =3.120 \end{aligned}$ | 30 | 2.372-2.758 | 2.384-2.699 | 2.457-2.547 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =1584 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 2.489-3.104 | 2.538-3.067 | 2.634-2.948 |  |
|  | 40 | 2.798-3.354 | 2.901-3.328 | 3.034-3.196 |  |
|  | 45 | 3.122-3.641 | 3.156-3.620 | 3.294-3.496 |  |
|  | 50 | 3.361-3.918 | 3.416-3.848 | 3.594-3.744 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 3.658-4.218 | 3.724-4.118 | 3.819-3.975 | AEROSOL MASS FRACTION REMAINING = $=0.1$ |
|  | 60 | 3.923-4.575 | 3.947-4.507 | 4.067-4.411 |  |
|  | 65 | 4.275-4.909 | 4.327-4.869 | 4.486-4.729 |  |
|  | 70 | 4.642-5.325 | 4.715-5.187 | 4.861-5.058 |  |
|  | 75 | 4.979-5.861 | 5.021-5.780 | 5.180-5.525 |  |
|  | 80 | 5.448-6.492 | 5.529-6.402 | 5.784-6.138 |  |
|  | 85 | 6.152-7.184 | 6.258-7.161 | 6.483-6.823 |  |
|  | 90 | 6.941-8.835 | 7.118-8.197 | 7.280-7.770 |  |
|  | 95 | 8.746-13.389 | 8.926-13.285 | 9.812-11.291 |  |

Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.799$ | 5 | 0.695-0.952 | 0.728-0.934 | 0.853-0.900 | WATER FLUX = |
|  | 10 | 0.943-1.124 | 0.965-1.105 | 1.012-1.068 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$. |
|  | 15 | 1.087-1.264 | 1.099-1.245 | 1.134-1.198 |  |
|  | 20 | 1.197-1.403 | 1.204-1.392 | 1.266-1.346 |  |
|  | 25 | 1.337-1.574 | 1.354-1.551 | 1.396-1.480 |  |
| STD. DEV. = | 30 | 1.452-1.699 | 1.471-1.675 | 1.550-1.618 | FALL DISTANCE = |
| $=2.076$ | 35 | 1.593-1.824 | 1.616-1.812 | 1.666-1.760 | $=1584 \mathrm{~cm}$ |
|  | 40 | 1.722-1.914 | 1.740-1.905 | 1.804-1.862 |  |
|  | 45 | 1.829-2.139 | 1.846-2.107 | 1.894-2.001 |  |
|  | 50 | 1.937-2.322 | 1.990-2.273 | 2.083-2.182 |  |
| SAMPLE SIZE = | 55 | 2.144-2.572 | 2.167-2.544 | 2.220-2.400 |  |
| $=400$ | 60 | 2.357-2.850 | 2.384-2.795 | $2.535-2.674$ | FRACTION REMAINING $=$ |
|  | 65 | 2.595-3.150 | 2.622-3.114 | 2.762-2.962 | $=0.01$ |
|  | 70 | 2.870-3.424 | 2.901-3.414 | 3.050-3.242 |  |
|  | 75 | 3.186-3.758 | 3.221-3.744 | 3.409-3.580 |  |
|  | 80 | $3.563-4.225$ | $3.591-4.171$ | 3.751-3.918 |  |
|  | 85 | 3.920-4.896 | $3.943-4.772$ | $4.224-4.455$ |  |
|  | $90$ | 4.547-6.228 | $4.594-5.852$ | $5.042-5.585$ |  |
|  | 95 | 6.138-8.930 | 6.409-8.887 | 7.006-7.951 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=10.061$ | 5 | 2.170-2.926 | 2.205-2.880 | 2.529-2.763 | WATER FLUX = |
|  | 10 | 2.923-3.845 | 2.939-3.644 | 3.114-3.421 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.532-4.490 | 3.590-4.395 | $3.956-4.316$ |  |
|  | 20 | 4.311-5.345 | 4.356-5.223 | 4.495-4.887 |  |
|  | 25 | 4.823-5.979 | 4.895-5.925 | $5.235-5.657$ |  |
| STD. DEV. = | 30 | 5.566-6.643 | 5.633-6.596 | 5.908-6.367 | FALL DISTANCE $=$ |
| $=7.775$ | 35 | 6.238-7.230 | 6.351-7.131 | 6.565-6.844 | $=2000 \mathrm{~cm}$ |
|  | 40 | $6.678-7.938$ | 6.776-7.891 | 7.063-7.415 |  |
|  | 45 | 7.250-8.481 | 7.344-8.423 | 7.816-8.111 |  |
|  | 50 | $7.951-9.334$ | 8.019-9.127 | 8.311-8.755 |  |
| SAMPLE SIZE = | 55 | 8.511-10.112 | 8.631-9.894 | $9.104-9.576$ |  |
| $=400$ | $60$ | $9.346-10.656$ | $9.508-10.599$ | $9.779-10.401$ | FRACTION REMAINING $=$ |
|  | 65 | $10.201-11.650$ | $10.286-11.498$ | $10.552-10.920$ | $=0.9$ |
|  | 70 | 10.679-12.670 | 10.787-12.545 | $11.466-11.918$ |  |
|  | 75 | 11.816-13.524 | 11.899-13.456 | 12.472-12.871 |  |
|  | 80 | 12.820-14.792 | 12.887-14.645 | 13.469-14.246 |  |
|  | 85 | 14.253-16.413 | 14.337-16.082 | 14.782-15.412 |  |
|  | 90 | 15.709-19.403 | 16.044-19.098 | 16.635-17.700 |  |
|  | 95 | 19.335-25.853 | 19.485-25.452 | 21.032-23.236 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.386$ | 5 | 1.881-2.330 | 1.972-2.320 | 2.054-2.203 | WATER FLUX |
|  | 10 | 2.327-2.893 | 2.337-2.851 | 2.530-2.770 | $=0.010 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.782-3.486 | 2.804-3.424 | 2.970-3.222 |  |
|  | 20 | 3.215-3.995 | 3.297-3.926 | 3.490-3.696 |  |
|  | 25 | 3.676-4.491 | 3.710-4.469 | 3.946-4.260 |  |
| STD. DEV. = | 30 | 4.149-4.823 | 4.239-4.767 | 4.447-4.636 | FALL DISTANCE = |
| $=5.375$ | 35 | 4.568-5.298 | 4.618-5.264 | 4.758-5.110 | $=2000 \mathrm{~cm}$ |
|  | 40 | 4.879-5.867 | 4.966-5.744 | 5.247-5.452 |  |
|  | 45 | 5.338-6.361 | 5.399-6.310 | 5.679-6.118 |  |
|  | 50 | 5.924-6.997 | 6.056-6.970 | 6.264-6.593 |  |
| SAMPLE SIZE = | 55 | 6.373-7.522 | 6.430-7.467 | 6.747-7.248 |  |
| $=400$ | 60 | $7.009-7.973$ | $7.151-7.897$ | $7.416-7.658$ | FRACTION REMAINING $=$ |
|  | 65 | $7.539-8.447$ | $7.635-8.371$ | $7.867-8.142$ | $=0.5$ |
|  | 70 | 8.059-8.924 | 8.131-8.812 | $8.361-8.583$ |  |
|  | 75 | 8.503-9.676 | 8.530-9.580 | 8.800-9.170 |  |
|  | 80 | 9.144-10.570 | 9.218-10.496 | 9.610-10.193 |  |
|  | 85 | 10.199-11.753 | 10.250-11.494 | 10.566-11.044 |  |
|  | 90 | 11.336-13.712 | 11.441-13.419 | 11.933-12.704 |  |
|  | 95 | 13.649-20.193 | 13.967-19.443 | 15.049-16.606 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=6.019$ | 5 | 1.631-1.962 | 1.651-1.950 | 1.724-1.885 | WATER FLUX = |
|  | 10 | 1.961-2.468 | 1.968-2.436 | 2.122-2.277 | $=0.010 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.339-2.812 | 2.365-2.792 | 2.492-2.631 |  |
|  | 20 | 2.621-3.291 | 2.743-3.269 | 2.813-3.106 |  |
|  | 25 | 3.085-3.558 | 3.110-3.516 | 3.277-3.414 |  |
| STD. DEV. = | 30 | 3.358-3.857 | 3.397-3.824 | 3.516-3.712 | FALL DISTANCE = |
| $=4.303$ | 35 | 3.628-4.285 | 3.662-4.249 | 3.789-4.024 | $=2000 \mathrm{~cm}$ |
|  | 40 | 3.893-4.814 | 3.963-4.726 | 4.235-4.437 |  |
|  | 45 | 4.319-5.265 | 4.360-5.181 | 4.657-4.985 |  |
|  | 50 | 4.831-5.641 | 4.922-5.577 | 5.138-5.364 |  |
| SAMPLE SIZE $=$ | 55 | 5.279-6.043 | 5.334-6.032 | 5.563-5.782 | AEROSOL MASS |
| $=400$ | 60 | $5.683-6.376$ | $5.727-6.328$ | $5.997-6.124$ | FRACTION REMAINING $=$ |
|  | 65 | $6.066-6.759$ | $6.077-6.686$ | $6.264-6.455$ | $=0.3$ |
|  | 70 | 6.408-7.123 | 6.446-7.094 | $6.591-6.927$ |  |
|  | 75 | 6.846-8.071 | 6.920-7.980 | 7.081-7.403 |  |
|  | 80 | 7.354-8.835 | 7.408-8.770 | 7.988-8.403 |  |
|  | 85 | 8.406-9.850 | 8.468-9.529 | 8.833-9.063 |  |
|  | 90 | 9.182-11.396 | 9.323-10.930 | 9.935-10.429 |  |
|  | 95 | 11.335-17.150 | 11.580-16.273 | 12.340-14.138 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.319$ | 5 | 1.139-1.501 | 1.157-1.494 | 1.250-1.443 |  |
|  | 10 | 1.499-1.769 | 1.505-1.749 | 1.596-1.689 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.722-2.008 | 1.746-1.993 | 1.808-1.889 |  |
|  | 20 | 1.888-2.281 | 1.913-2.250 | 2.008-2.175 |  |
|  | 25 | 2.143-2.431 | 2.179-2.392 | 2.260-2.360 |  |
| STD. DEV. = | 30 | 2.334-2.741 | 2.354-2.674 | 2.390-2.501 | FALL DISTANCE = |
| $=3.081$ | 35 | 2.479-3.066 | $2.484-3.028$ | $2.614-2.878$ | $=2000 \mathrm{~cm}$ |
|  | 40 | 2.786-3.303 | 2.828-3.245 | 2.980-3.168 |  |
|  | 45 | 3.093-3.611 | 3.117-3.589 | 3.232-3.398 |  |
|  | 50 | 3.318-3.832 | 3.342-3.799 | 3.527-3.691 |  |
| SAMPLE SIZE = | $55^{*}$ | 3.624-4.150 | 3.665-4.060 | 3.755-3.910 | AEROSOL MASS |
| $=400$ | 60 | 3.835-4.524 | 3.876-4.486 | 4.011-4.324 | FRACTION REMAINING $=$ |
|  | 65 | 4.196-4.838 | 4.264-4.768 | 4.474-4.611 | $=0.1$ |
|  | 70 | 4.562-5.239 | 4.603-5.154 | 4.738-4.952 |  |
|  | 75 | 4.921-5.758 | 4.946-5.654 | 5.128-5.429 |  |
|  | 80 | 5.383-6.408 | 5.460-6.356 | 5.678-6.060 |  |
|  | 85 | 6.067-7.169 | 6.176-6.999 | 6.406-6.771 |  |
|  | 90 | 6.836-8.829 | 6.985-8.194 | 7.258-7.591 |  |
|  | 95 | 8.773-13.269 | 8.853-13.021 | 9.672-11.053 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.150$ | 5 | 0.536-0.700 | 0.579-0.688 | 0.639-0.666 | WATER FLUX = |
|  | 10 | 0.698-0.859 | 0.710-0.852 | 0.754-0.813 | $=0.01 \mathrm{~cm}^{3} / \mathrm{S}-\mathrm{cm}^{2}$ |
|  | 15 | 0.828-0.956 | 0.841-0.950 | - $0.869-0.928$ |  |
|  | 20 | 0.927-1.077 | 0.935-1.065 | 0.956-1.022 |  |
|  | 25 | 1.007-1.178 | 1.024-1.165 | 1.065-1.143 |  |
| STD. DEV. $=$ | 30 | 1.127-1.281 | 1.136-1.267 | 1.164-1.228 | FALL DISTANCE $=$ |
| $=1.637$ | 35 | 1.192-1.364 | 1.221-1.356 | 1.253-1.302 | $=2000 \mathrm{~cm}$ |
|  | 40 | 1.285-1.501 | 1.294-1.455 | 1.332-1.408 |  |
|  | 45 | 1.364-1.593 | 1.393-1.575 | 1.440-1.517 |  |
|  | 50 | 1.504-1.749 | 1.508-1.708 | 1.552-1.632 |  |
| SAMPLE SIZE $=$ | 55 | 1.595-1.931 | 1.610-1.902 | 1.684-1.810 | AEROSOL MASS |
| $=400$ | 60 | 1.776-2.182 | 1.784-2.120 | 1.841-2.041 | FRACTION REMAINING $=$ |
|  | 65 | 1.950-2.367 | 2.028-2.326 | 2.103-2.247 | $=0.001$ |
|  | 70 | 2.226-2.642 | 2.234-2.617 | 2.321-2.517 |  |
|  | 75 | 2.474-2.900 | 2.502-2.864 | 2.611-2.710 |  |
|  | 80 | 2.691-3.260 | 2.716-3.191 | 2.883-3.085 |  |
|  | 85 | 3.090-3.905 | 3.126-3.806 | 3.256-3.473 |  |
|  | 90 | 3.643-5.232 | 3.754-4.745 | 4.017-4.343 |  |
|  | 95 | 5.081-6.876 | 5.347-6.838 | 5.548-6.263 |  |

Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(3 r^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=9.740$ | 5 | 2.087-2.760 | 2.172-2.739 | 2.492-2.672 | WATER FLUX = |
|  | 10 | 2.755-3.713 | 2.782-3.487 | 2.990-3.290 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.359-4.307 | 3.400-4.286 | 3.837-4.152 |  |
|  | 20 | 4.150-5.174 | 4.202-5.042 | 4.310-4.609 |  |
|  | 25 | 4.554-5.761 | 4.650-5.711 | 5.080-5.452 |  |
| STD. DEV. $=$ | 30 | 5.377-6.403 | $5.434-6.330$ | $5.687-6.182$ | $\text { FALL DISTANCE }=$ |
| $=7.537$ | $35$ | $5.986-6.985$ | $6.092-6.886$ | $6.310-6.661$ | $=3000 \mathrm{~cm}$ |
|  | 40 | 6.467-7.698 | 6.605-7.661 | 6.807-7.182 |  |
|  | 45 | $7.021-8.200$ | 7.141-8.040 | 7.519-7.796 |  |
|  | 50 | 7.746-8.952 | 7.775-8.760 | 7.922-8.394 |  |
| SAMPLE SIZE = | 55 | 8.223-9.794 | 8.316-9.704 | 8.668-9.256 | AEROSOL MASS |
| $=400$ | 60 | 9.052-10.510 | 9.244-10.388 | 9.533-10.116 | FRACTION REMAINING $=$ |
|  | 65 | 9.816-11.363 | 9.930-10.995 | 10.354-10.676 | $=0.9$ |
|  | 70 | 10.586-12.327 | 10.641-12.086 | 10.930-11.722 |  |
|  | 75 | 11.583-13.053 | 11.692-12.893 | 12.019-12.673 |  |
|  | 80 | 12.612-14.230 | 12.689-14.111 | 12.897-13.564 |  |
|  | 85 | 13.566-15.957 | 13.605-15.702 | 14.220-15.060 |  |
|  | 90 | 15.321-18.215 | 15.626-18.039 | 16.291-17.459 |  |
|  | 95 | 18.197-24.898 | 18.288-24.150 | 20.524-22.776 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.130$ | 5 | 1.802-2.250 | 1.859-2.232 | 1.967-2.152 | WATER FLUX = |
|  | 10 | 2.243-2.791 | 2.277-2.746 | 2.402-2.561 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.647-3.340 | 2.688-3.283 | 2.866-3.061 |  |
|  | 20 | 3.039-3.818 | 3.199-3.735 | 3.342-3.653 |  |
|  | 25 | 3.636-4.346 | 3.659-4.251 | 3.769-4.008 |  |
| STD. DEV. $=$ | 30 | 3.945-4.633 | 4.005-4.607 | 4.231-4.492 | FALL DISTANCE $=$ |
| $=5.228$ | 35 | 4.408-5.091 | 4.462-5.059 | 4.602-4.856 | $=3000 \mathrm{~cm}$ |
|  | 40 | 4.710-5.734 | 4.818-5.537 | 5.004-5.229 |  |
|  | 45 | 5.129-6.203 | 5.160-6.093 | 5.340-5.914 |  |
|  | 50 | 5.740-6.688 | 5.824-6.611 | 6.032-6.294 |  |
| SAMPLE SIZE $=$ | 55 | 6.204-7.208 | 6.264-7.158 | 6.552-6.875 | AEROSOL MASS |
| $=400$ | 60 | 6.689-7.795 | 6.816-7.708 | 7.070-7.402 | FRACTION REMAINING $=$ |
|  | 65 | 7.242-8.190 | 7.330-8.124 | 7.597-7.883 | $=0.5$ |
|  | 70 | 7.813-8.659 | 7.846-8.620 | 8.098-8.350 |  |
|  | 75 | 8.299-9.404 | 8.335-9.211 | 8.596-8.878 |  |
|  | 80 | 8.821-10.163 | 8.896-10.149 | 9.234-9.851 |  |
|  | 85 | 9.854-11.418 | 9.903-11.225 | 10.162-10.847 |  |
|  | 90 | 10.885-13.248 | 10.940-12.943 | 11.700-12.347 |  |
|  | 95 | 13.170-19.235 | 13.840-18.164 | 14.620-15.944 |  |

Appendix A

|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=5.837$ | 5 | 1.585-1.899 | 1.609-1.874 | 1.703-1.797 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 1.891-2.357 | 1.938-2.304 | 2.088-2.160 |  |
|  | 15 | 2.220-2.770 | 2.245-2.729 | 2.420-2.579 |  |
|  | 20 | 2.557-3.176 | 2.600-3.122 | 2.771-3.058 |  |
|  | 25 | 2.952-3.458 | 3.066-3.406 | 3.126-3.292 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =4.187 \end{aligned}$ | 30 | 3.270-3.702 | 3.288-3.671 | 3.405-3.599 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =3000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 3.490-4.103 | 3.566-4.030 | 4.640-3.879 |  |
|  | 40 | 3.765-4.663 | 3.835-4.507 | 4.013-4.332 |  |
|  | 45 | 4.186-5.110 | 4.246-5.019 | 4.450-4.787 |  |
|  | 50 | 4.693-5.539 | 4.762-5.375 | 4.953-5.247 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 5.132-5.838 | 5.192-5.811 | 5.311-5.653 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | $5.545-6.211$ | 5.591-6.153 | 5.772-5.970 |  |
|  | 65 | 5.869-6.448 | 5.909-6.419 | 6.061-6.275 |  |
|  | 70 | 6.219-7.057 | 6.239-7.014 | 6.408-6.617 |  |
|  | 75 | 6.530-7.750 | 6.607-7.669 | 6.998-7.344 |  |
|  | 80 | 7.307-8.573 | 7.351-8.442 | 7.679-8.105 |  |
|  | 85 | 8.117-9.414 | 8.179-9.325 | $8.561-9.001$ |  |
|  | 90 | 9.070-10.773 | 9.208-10.664 | 9.495-10.258 |  |
|  | 95 | 10.759-15.976 | 11.429-15.125 | 11.821-13.760 |  |



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|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.664$ | 5 | 0.651-0.884 | 0.688-0.880 | 0.797-0.850 | WATER FLUX = |
|  | 10 | 0.884-1.057 | 0.898-1.050 | 0.966-1.012 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.035-1.208 | 1.044-1.202 | 1.090-1.133 |  |
|  | 20 | 1.132-1.374 | 1.171-1.342 | 1.208-1.266 |  |
|  | 25 | 1.254-1.475 | 1.268-1.468 | 1.347-1.420 |  |
| STD. DEV. = | 30 | 1.395-1.611 | 1.416-1.604 | 1.465-1.532 | FALL DISTANCE = |
| $=1.994$ | 35 | 1.489-1.710 | 1.526-1.701 | 1.596-1.655 | $=3000 \mathrm{~cm}$ |
|  | 40 | 1.634-1.869 | 1.648-1.808 | 1.689-1.760 |  |
|  | 45 | 1.715-2.066 | 1.728-2.005 | 1.793-1.896 |  |
|  | 50 | 1.872-2.184 | 1.889-2.168 | 1.985-2.102 |  |
| SAMPLE SIZE = | 55 | 2.070-2.485 | 2.077-2.407 | 2.158-2.311 | AEROSOL MASS |
| $=400$ | 60 | 2.191-2.673 | 2.236-2.642 | 2.369-2.546 | FRACTION REMAINING $=$ |
|  | 65 | 2.492-3.000 | 2.525-2.938 | 2.588-2.775 | $=0.01$ |
|  | 70 | 2.701-3.260 | 2.755-3.236 | 2.880-3.142 |  |
|  | 75 | 3.095-3.534 | 3.140-3.519 | 3.223-3.393 |  |
|  | 80 | $3.377-3.920$ | $3.399-3.902$ | $3.524-3.717$ |  |
|  | 85 | 3.721-4.600 | $3.763-4.534$ | $3.918-4.390$ |  |
|  | 90 | 4.486-6.148 | 4.499-5.625 | 4.813-5.331 |  |
|  | 95 | 5.966-8.378 | 6.340-8.246 | 6.839-7.656 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.082$ | 5 | 0.510-0.686 | 0.555-0.662 | 0.605-0.640 | WATER FLUX = |
|  | 10 | 0.676-0.824 | 0.703-0.812 | 0.725-0.785 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.803-0.931 | 0.809-0.922 | 0.848-0.888 |  |
|  | 20 | 0.888-1.048 | 0.898-1.040 | 0.931-0.980 |  |
|  | 25 | 0.976-1.142 | 0.989-1.136 | 1.044-1.068 |  |
| STD. DEV. $=$ | 30 | 1.058-1.234 | 1.066-1.229 | 1.133-1.177 | FALL DISTANCE $=$ |
| $=1.597$ | 35 | 1.162-1.311 | 1.171-1.292 | 1.222-1.264 | $=3000 \mathrm{~cm}$ |
|  | 40 | 1.239-1.415 | 1.247-1.410 | 1.283-1.360 |  |
|  | 45 | 1.322-1.542 | 1.349-1.534 | 1.390-1.468 |  |
|  | 50 | 1.422-1.691 | 1.430-1.672 | 1.494-1.599 |  |
| SAMPLE SIZE = | 55 | 1.546-1.859 | 1.587-1.827 | 1.649-1.760 | AEROSOL MASS |
| $=400$ | 60 | 1.696-2.088 | 1.735-2.069 | 1.789-1.960 | FRACTION REMAINING $=$ |
|  | 65 | 1.904-2.307 | 1.937-2.257 | 2.059-2.147 | $=0.001$ |
|  | 70 | 2.096-2.598 | 2.126-2.564 | 2.251-2.363 |  |
|  | 75 | 2.328-2.748 | 2.355-2.714 | 2.536-2.655 |  |
|  | 80 | 2.625-3.217 | 2.669-3.167 | 2.720-2.930 |  |
|  | 85 | 2.937-3.798 | 3.053-3.769 | 3.216-3.440 |  |
|  | 90 | 3.591-5.078 | 3.681-4.605 | 3.847-4.298 |  |
|  | 95 | 4.911-6.745 | 5.153-6.680 | 5.368-5.855 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=9.476$ | 5 | 2.020-2.659 | 2.109-2.647 | 2.427-2.591 | WATER FLUX = |
|  | 10 | 2.654-3.320 | 2.695-3.282 | 2.854-3.106 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 3.135-4.165 | 3.228-4.111 | 3.518-3.955 |  |
|  | 20 | 3.952-4.994 | 4.030-4.870 | 4.166-4.468 |  |
|  | 25 | 4.365-5.662 | 4.489-5.530 | 4.945-5.207 |  |
| STD. DEV. $=$ | 30 | 5.177-6.272 | 5.204-6.131 | 5.496-5.836 | FALL DISTANCE $=$ |
| $=7.358$ | 35 | 5.738-6.743 | 5.806-6.682 | 6.027-6.452 | $=4000 \mathrm{~cm}$ |
|  | 40 | 6.325-7.348 | 6.379-7.297 | 6.642-7.068 |  |
|  | 45 | 6.776-7.824 | 6.936-7.745 | 7.199-7.512 |  |
|  | 50 | 7.350-8.667 | 7.426-8.535 | 7.698-8.148 |  |
| SAMPLE SIZE = | 55 | 7.864-9.467 | 7.942-9.339 | 8.333-9.020 |  |
| $=400$ | 60 | 8.678-10.280 | $8.833-10.189$ | $9.244-9.899$ | FRACTION REMAINING $=$ |
|  | 65 | 9.508-10.923 | 9.650-10.872 | $10.168-10.498$ | $=0.9$ |
|  | 70 | 10.364-12.094 | 10.450-11.820 | 10.855-11.365 |  |
|  | 75 | 11.220-12.680 | 11.318-12.624 | 11.751-12.382 |  |
|  | 80 | 12.331-13.737 | 12.450-13.531 | 12.636-13.010 |  |
|  | 85 | 13.034-15.875 | 13.238-15.274 | 13.711-14.725 |  |
|  | 90 | 14.976-17.559 | 15.166-17.419 | 16.019-17.087 |  |
|  | 95 | 17.546-24.641 | 17.568-23.566 | 19.497-21.952 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=6.958$ | 5 | 1.783-2.206 | 1.829-2.192 | 1.918-2.124 | WATER FLUX = |
|  | 10 | 2.206-2.774 | 2.227-2.720 | 2.315-2.509 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.532-3.298 | 2.606-3.223 | 2.781-3.045 |  |
|  | 20 | 3.043-3.685 | 3.077-3.652 | 3.311-3.586 |  |
|  | 25 | 3.538-4.180 | 3.587-4.113 | 3.660-3.948 |  |
| STD. DEV. = | 30 | 3.856-4.592 | 3.922-4.537 | 4.068-4.366 | FALL DISTANCE = |
| $=5.108$ | 35 | 4.265-4.945 | 4.336-4.826 | 4.528-4.679 | $=4000 \mathrm{~cm}$ |
|  | 40 | 4.622-5.540 | 4.647-5.351 | 4.814-5.122 |  |
|  | 45 | 4.979-6.020 | 5.051-5.957 | 5.277-5.749 |  |
|  | 50 | $5.569-6.502$ | 5.704-6.384 | 5.914-6.229 |  |
| SAMPLE SIZE = | 55 | 6.038-6.940 | 6.128-6.865 | 6.353-6.617 | AEROSOL MASS |
| $=400$ | 60 | $6.508-7.530$ | 6.577-7.441 | 6.804-7.258 | FRACTION REMAINING $=$ |
|  | 65 | 7.146-8.062 | 7.195-7.990 | 7.382-7.760 | $=0.5$ |
|  | 70 | 7.676-8.464 | 7.738-8.435 | $7.959-8.262$ |  |
|  | 75 | 8.226-9.171 | 8.255-9.064 | 8.420-8.799 |  |
|  | 80 | 8.702-10.091 | 8.825-9.992 | 9.072-9.433 |  |
|  | 85 | 9.438-11.159 | 9.620-11.117 | 10.089-10.495 |  |
|  | 90 | 10.663-13.139 | 10.879-12.889 | 11.206-12.000 |  |
|  | 95 | 13.064-18.066 | 13.417-17.117 | 14.538-15.475 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=5.674$ | 5 | 1.526-1.854 | 1.574-1.814 | 1.672-1.732 | WATER FLUX = |
|  | 10 | 1.851-2.232 | 1.900-2.182 | 1.967-2.123 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.141-2.672 | 2.147-2.646 | 2.296-2.492 |  |
|  | 20 | 2.491-3.081 | 2.508-3.070 | 2.676-2.895 |  |
|  | 25 | 2.848-3.340 | 2.904-3.285 | 3.075-3.188 |  |
| STD. DEV. = | 30 | 3.114-3.629 | 3.166-3.587 | $3.283-3.440$ | FALL DISTANCE = |
| $=4.106$ | $35$ | $3.389-3.935$ | $3.426-3.878$ | $3.555-3.737$ | $=4000 \mathrm{~cm}$ |
|  | $40$ | $3.662-4.434$ | $3.697-4.381$ | $3.830-4.173$ |  |
|  | $45$ | $3.971-4.943$ | $4.085-4.797$ | $4.308-4.634$ |  |
|  | 50 | 4.471-5.278 | $4.498-5.245$ | 4.757-5.060 |  |
| SAMPLE SIZE = | 55 | 4.948-5.709 | 4.980-5.603 | 5.180-5.481 | AEROSOL MASS |
| $=400$ | 60 | $5.351-5.973$ | $5.382-5.958$ | 5.525-5.798 | FRACTION REMAINING $=$ |
|  | 65 | 5.715-6.328 | 5.782-6.240 | 5.924-6.060 | $=0.3$ |
|  | 70 | 6.004-6.991 | 6.047-6.921 | 6.227-6.447 |  |
|  | 75 | 6.372-7.366 | 6.438-7.317 | 6.910-7.194 |  |
|  | 80 | 7.157-8.515 | 7.210-8.214 | 7.323-7.778 |  |
|  | 85 | 7.787-9.132 | 8.020-9.011 | 8.487-8.921 |  |
|  | 90 | 8.955-10.685 | 8.980-10.431 | 9.284-9.854 |  |
|  | 95 | 10.675-15.031 | 10.908-14.381 | 11.653-13.363 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=4.071$ | 5 | 1.049-1.438 | 1.084-1.430 | 1.145-1.321 |  |
|  | 10 | 1.436-1.635 | 1.459-1.628 | 1.502-1.580 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.591-1.922 | 1.604-1.888 | 1.659-1.815 |  |
|  | 20 | 1.813-2.102 | 1.832-2.089 | 1.927-2.016 |  |
|  | 25 | 2.008-2.327 | 2.022-2.315 | 2.092-2.186 |  |
| STD. DEV. = | 30 | 2.154-2.552 | 2.178-2.523 | 2.283-2.444 | FALL DISTANCE $=$ |
| $=2.939$ | 35 | 2.370-2.828 | 2.415-2.784 | 2.511-2.687 | $=4000 \mathrm{~cm}$ |
|  | 40 | 2.592-3.102 | 2.668-3.064 | 2.763-2.960 |  |
|  | 45 | 2.845-3.289 | 2.922-3.261 | 3.043-3.180 |  |
|  | 50 | 3.109-3.655 | 3.134-3.612 | 3.236-3.469 |  |
| SAMPLE SIZE = | 55 | 3.299-3.931 | 3.324-3.885 | 3.546-3.735 |  |
| $=400$ | 60 | 3.681-4.211 | 3.699-4.180 | $3.816-4.035$ | FRACTION REMAINING $=$ |
|  | 65 | 3.947-4.460 | 3.988-4.450 | $4.142-4.368$ | $=0.1$ |
|  | 70 | 4.261-4.928 | 4.319-4.886 | $4.440-4.712$ |  |
|  | 75 | 4.563-5.411 | 4.665-5.329 | 4.857-5.095 |  |
|  | 80 | 5.080-6.004 | 5.119-5.887 | 5.353-5.590 |  |
|  | 85 | 5.593-6.801 | 5.688-6.713 | 5.996-6.428 |  |
|  | 90 | 6.614-7.973 | 6.644-7.834 | 7.101-7.440 |  |
|  | 95 | 7.960-11.831 | 8.058-11.637 | 9.185-10.158 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.591$ | 5 | 0.627-0.853 | 0.663-0.848 | 0.761-0.804 | WATER FLUX = |
|  | 10 | 0.852-1.048 | 0.877-1.014 | 0.945-0.994 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.999-1.174 | 1.005-1.143 | 1.057-1.120 |  |
|  | 20 | 1.120-1.324 | 1.123-1.313 | 1.174-1.238 |  |
|  | 25 | 1.219-1.419 | 1.249-1.417 | 1.315-1.376 |  |
| STD. DEV. = | 30 | 1.368-1.563 | 1.372-1.547 | 1.416-1.486 | FALL DISTANCE $=$ |
| $=1.955$ | 35 | 1.450-1.637 | 1.462-1.620 | 1.542-1.603 | $=4000 \mathrm{~cm}$ |
|  | 40 | 1.588-1.803 | 1.598-1.780 | 1.618-1.706 |  |
|  | 45 | 1.648-1.978 | 1.687-1.970 | 1.768-1.872 |  |
|  | 50 | 1.805-2.153 | 1.827-2.142 | 1.922-2.045 |  |
| SAMPLE SIZE = | 55 | 1.984-2.394 | 2.032-2.349 | $2.088-2.219$ |  |
| $=400$ | $60$ | $2.158-2.559$ | $2.193-2.545$ | $2.318-2.478$ | FRACTION REMAINING $=$ |
|  | $65$ | $2.402-2.905$ | $2.460-2.833$ | $2.531-2.679$ | $=0.01$ |
|  | 70 | $2.601-3.193$ | $2.642-3.162$ | $2.801-3.052$ |  |
|  | 75 | 2.998-3.452 | $3.039-3.370$ | $3.143-3.253$ |  |
|  | 80 | 3.231-3.817 | 3.283-3.747 | 3.379-3.680 |  |
|  | 85 | 3.686-4.516 | 3.698-4.465 | 3.809-4.347 |  |
|  | 90 | 4.384-5.940 | 4.420-5.650 | 4.713-5.193 |  |
|  | 95 | 5.836-8.009 | 6.188-7.797 | 6.668-7.527 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.026$ | 5 | 0.491-0.670 | 0.525-0.658 | 0.577-0.623 | WATER FLUX = |
|  | 10 | 0.670-0.805 | 0.672-0.778 | 0.699-0.748 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.756-0.911 | 0.773-0.890 | 0.821-0.868 |  |
|  | 20 | 0.867-1.002 | 0.876-0.989 | 0.911-0.964 |  |
|  | 25 | 0.950-1.105 | 0.966-1.085 | 0.991-1.046 |  |
| STD. DEV. = | 30 | 1.025-1.196 | 1.043-1.170 | 1.073-1.138 | FALL DISTANCE $=$ |
| $=1.566$ | 35 | 1.126-1.278 | 1.136-1.274 | 1.164-1.233 | $=4000 \mathrm{~cm}$ |
|  | 40 | 1.208-1.383 | 1.227-1.359 | 1.269-1.315 |  |
|  | 45 | 1.286-1.529 | 1.302-1.498 | 1.339-1.408 |  |
|  | 50 | 1.387-1.662 | 1.404-1.643 | 1.484-1.577 |  |
| SAMPLE SIZE $=$ | 55 | 1.533-1.819 | 1.540-1.797 | 1.614-1.715 | AEROSOL MASS |
| $=400$ | 60 | 1.668-2.019 | 1.684-2.006 | 1.757-1.942 | FRACTION REMAINING $=$ |
|  | 65 | 1.823-2.220 | 1.893-2.182 | 1.994-2.094 | $=0.001$ |
|  | 70 | 2.049-2.503 | 2.074-2.490 | 2.160-2.327 |  |
|  | 75 | 2.301-2.659 | 2.319-2.657 | 2.487-2.598 |  |
|  | 80 | 2.586-3.078 | 2.602-3.062 | 2.657-2.800 |  |
|  | 85 | 2.804-3.602 | 2.893-3.578 | 3.078-3.365 |  |
|  | 90 | 3.436-4.804 | 3.515-4.586 | 3.722-4.252 |  |
|  | 95 | 4.735-6.708 | 4.846-6.644 | 5.307-5.662 |  |

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|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=7.215$ | 5 | 1.948-2.589 | 2.040-2.578 | 2.236-2.496 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 2.586-3.446 | 2.619-3.295 | 2.894-3.090 |  |
|  | 15 | 3.170-4.071 | 3.265-4.039 | 3.564-3.897 |  |
|  | 20 | 3.896-4.806 | 3.910-4.755 | 4.076-4.458 |  |
|  | 25 | 4.354-5.465 | 4.478-5.424 | 4.774-5.085 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =9.247 \end{aligned}$ | 30 | 5.019-6.070 | 5.066-5.972 | 5.415-5.698 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =5000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 5.516-6.641 | 5.646-6.582 | 5.899-6.312 |  |
|  | 40 | 6.203-7.070 | 6.289-7.055 | 6.547-6.888 |  |
|  | 45 | 6.704-7.715 | 6.815-7.658 | 7.008-7.274 |  |
|  | 50 | 7.078-8.476 | 7.167-8.286 | 7.500-7.892 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 7.721-9.422 | 7.828-9.204 | 8.192 - 8.859 | AEROSOL MASS FRACTION REMAINING $=$ $=0.9$ |
|  | 60 | $8.509-10.192$ | 8.634-10.130 | 9.127-9.638 |  |
|  | 65 | 9.461-10.704 | 9.538-10.612 | 10.017-10.389 |  |
|  | 70 | 10.273-11.708 | 10.332-11.628 | 10.563-11.210 |  |
|  | 75 | 10.828-12.503 | 11.151-12.404 | 11.617-12.043 |  |
|  | 80 | 12.018-13.509 | 12.051-13.292 | 12.417-12.725 |  |
|  | 85 | 12.733-15.520 | 12.766-15.200 | 13.476-14.373 |  |
|  | 90 | 14.904-17.385 | 15.088-17.299 | 15.740-16.511 |  |
|  | 95 | 17.366-24.322 | 17.477-23.405 | 18.850-21.430 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=6.793$ | 5 | 1.733-2.149 | 1.778-2.136 | 1.886-2.066 | WATER FLUX = |
|  | 10 | 2.142-2.654 | 2.171-2.615 | 2.211-2.409 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 2.489-3.260 | 2.540-3.187 | 2.713-2.944 |  |
|  | 20 | 2.942-3.639 | 2.971-3.605 | 3.267-3.449 |  |
|  | . 25 | 3.406-3.992 | 3.452-3.940 | 3.608-3.807 |  |
| STD. DEV. = | 30 | 3.721-4.445 | 3.800-4.416 | 3.937-4.259 | FALL DISTANCE = |
| $=5.017$ | 35 | 4.103-4.778 | 4.210-4.696 | 4.400-4.587 | $=5000 \mathrm{~cm}$ |
|  | 40 | 4.503-4.778 | 4.550-5.249 | 4.671-5.026 |  |
|  | 45 | 4.831-5.279 | 4.952-5.854 | 5.168-5.556 |  |
|  | 50 | 5.390-6.250 | 5.491-6.192 | 5.671-6.042 |  |
| SAMPLE SIZE = | 55 | 5.914-6.841 | 5.977-6.755 | 6.148-6.447 | AEROSOL MASS |
| $=400$ | 60 | 6.288-7.375 | 6.380-7.310 | 6.602-6.950 | FRACTION REMAINING $=$ |
|  | 65 | 6.860-7.913 | 6.903-7.866 | 7.223-7.622 | $=0.5$ |
|  | 70 | 7.432-8.420 | 7.513-8.366 | 7.823-8.124 |  |
|  | 75 | 7.991-8.969 | 8.081-8.954 | 8.326-8.622 |  |
|  | 80 | 8.586-9.908 | 8.641-9.693 | 8.963-9.193 |  |
|  | 85 | 9.217-10.798 | 9.349-10.714 | 9.881-10.446 |  |
|  | 90 | 10.545-12.824 | 10.600-12.647 | 10.967-11.678 |  |
|  | 95 | 12.792-17.104 | 12.888-16.628 | 14.287-15.135 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=5.545$ | 5 | 1.470-1.813 | 1.512-1.780 | 1.618-1.705 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 1.811-2.213 | 1.824-2.150 | 1.910-2.074 |  |
|  | 15 | 2.098-2.636 | 2.137-2.561 | 2.225-2.475 |  |
|  | 20 | 2.474-2.991 | 2.492-2.939 | 2.652-2.779 |  |
|  | 25 | 2.760-3.259 | 2.789-3.216 | 2.951-3.084 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =4.027 \end{aligned}$ | 30 | 3.069-3.563 | 3.079-3.528 | 3.215-3.365 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =5000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 3.309-3.876 | 3.349-3.813 | 3.500-3.655 |  |
|  | 40 | 3.584-4.346 | 3.610-4.280 | 3.746-4.141 |  |
|  | 45 | 3.920-4.749 | 4.020-4.717 | 4.249-4.469 |  |
|  | 50 | 4.362-5.170 | 4.436-5.124 | 4.687-4.936 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 4.796-5.555 | 4.868-5.489 | 5.088-5.286 | AEROSOL MASS FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | 5.212-5.827 | 5.240-5.762 | $5.465-5.687$ |  |
|  | 65 | 5.562-6.288 | 5.661-6.148 | $5.748-5.928$ |  |
|  | 70 | 5.894-6.835 | 5.926-6.742 | 6.110-6.398 |  |
|  | 75 | 6.339-7.262 | 6.374-7.208 | 6.717-6.980 |  |
|  | 80 | 6.963-8.296 | $6.990-8.048$ | 7.217-7.668 |  |
|  | 85 | 7.681-8.934 | 7.822-8.908 | 8.266-8.618 |  |
|  | 90 | 8.836-10.464 | 8.868-10.371 | 9.058-9.752 |  |
|  | 95 | 10.454-14.467 | 10.487-13.912 | 11.597-13.301 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=3.972$ | 5 | 1.035-1.424 | 1.048-1.388 | 1.124-1.250 | WATER FLUX $=$ |
|  | 10 | 1.424-1.587 | 1.430-1.581 | $1.458-1.517$ | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 1.540-1.854 | 1.577-1.842 | 1.615-1.774 |  |
|  | 20 | 1.774-2.029 | 1.814-2.002 | 1.855-1.960 |  |
|  | 25 | 1.943-2.296 | 1.962-2.251 | 2.009-2.136 |  |
| STD. DEV. = | 30 | 2.092-2.484 | 2.122-2.441 | 2.247-2.370 | FALL DISTANCE $=$ |
| $=2.893$ | 35 | 2.323-2.721 | 2.361-2.688 | 2.423-2.563 | $=5000 \mathrm{~cm}$ |
|  | 40 | 2.521-3.037 | 2.548-2.963 | 2.677-2.801 |  |
|  | 45 | 2.744-3.208 | 2.777-3.154 | 2.940-3.082 |  |
|  | 50 | 3.043-3.559 | 3.063-3.529 | 3.131-3.292 |  |
| SAMPLE SIZE = | 55 | 3.228-3.805 | 3.257-3.795 | 3.514-3.660 | AEROSOL MASS |
| $=400$ | 60 | 3.571-4.075 | 3.617-4.022 | 3.734-3.907 | FRACTION REMAINING $=$ |
|  | 65 | 3.834-4.435 | 3.886-4.401 | 3.977-4.225 | $=0.1$ |
|  | 70 | 4.109-4.823 | 4.191-4.791 | 4.392-4.547 |  |
|  | 75 | 4.490-5.220 | 4.532-5.188 | 4.772-4.991 |  |
|  | 80 | 4.975-5.910 | 5.014-5.761 | 5.191-5.471 |  |
|  | 85 | 5.474-6.722 | 5.570-6.627 | 5.897-6.287 |  |
|  | 90 | 6.461-7.810 | 6.590-7.649 | 7.078-7.357 |  |
|  | 95 | 7.792-11.381 | 7.926-11.168 | 8.978-10.100 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=2.530$ | 5 | 0.604-0.846 | 0.642-0.802 | 0.727-0.768 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 0.846-1.016 | 0.850-0.995 | 0.902-0.961 |  |
|  | 15 | 0.983-1.125 | 0.993-1.121 | 1.042-1.080 |  |
|  | 20 | 1.080-1.298 | 1.088-1.269 | 1.126-1.211 |  |
|  | 25 | 1.195-1.383 | 1.215-1.368 | 1.285-1.328 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =1.924 \end{aligned}$ | 30 | 1.311-1.506 | 1.327-1.486 | 1.366-1.448 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =5000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 1.421-1.600 | 1.440-1.581 | 1.475-1.534 |  |
|  | 40 | 1.523-1.766 | 1.528-1.741 | 1.553-1.683 |  |
|  | 45 | 1.609-1.931 | 1.644-1.881 | 1.733-1.814 |  |
|  | 50 | 1.772-2.108 | 1.795-2.092 | 1.872-2.007 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 1.936-2.332 | 1.964-2.294 | 2.066-2.162 | AEROSOL MASS <br> FRACTION REMAINING = $=0.01$ |
|  | 60 | $2.117-2.513$ | $2.142-2.482$ | $2.261-2.391$ |  |
|  | 65 | 2.341-2.838 | 2.371-2.783 | $2.461-2.582$ |  |
|  | 70 | 2.534-3.109 | 2.558-3.069 | 2.737-2.947 |  |
|  | 75 | 2.880-3.363 | 2.939-3.324 | 3.047-3.173 |  |
|  | 80 | 3.161-3.740 | 3.178-3.695 | 3.338-3.532 |  |
|  | 85 | 3.536-4.446 | 3.563-4.435 | 3.739-4.296 |  |
|  | 90 | 4.340-5.664 | 4.388-5.611 | 4.581-5.166 |  |
|  | 95 | 5.638-7.681 | 5.962-7.607 | 6.471-7.198 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=1.977$ | 5 | 0.479-0.646 | 0.505-0.637 | 0.552-0.607 | WATER FLUX = |
|  | 10 | 0.644-0.765 | 0.651-0.741 | 0.694-0.720 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.738-0.888 | 0.740-0.876 | 0.802-0.850 |  |
|  | 20 | 0.850-0.965 | 0.855-0.960 | 0.888-0.938 |  |
|  | 25 | 0.931-1.054 | 0.938-1.047 | 0.962-1.016 |  |
| STD. DEV. = | 30 | 0.997-1.163 | 1.011-1.136 | 1.046-1.098 | FALL DISTANCE = |
| $=1.541$ | 35 | 1.071-1.259 | 1.093-1.246 | 1.130-1.205 | $=5000 \mathrm{~cm}$ |
|  | 40 | 1.183-1.333 | 1.202-1.314 | 1.230-1.270 |  |
|  | 45 | 1.262-1.474 | 1.267-1.457 | 1.302-1.387 |  |
|  | 50 | 1.335-1.612 | 1.348-1.600 | 1.428-1.536 |  |
| SAMPLE SIZE = | 55 | 1.485-1.758 | $1.520 \div 1.743$ | 1.575-1.668 | AEROSOL MASS |
| $=400$ | 60 | 1.626-1.973 | 1.641-1.924 | 1.723-1.847 | FRACTION REMAINING $=$ |
|  | 65 | 1.792-2.151 | 1.823-2.105 | 1.911-2.028 | $=0.001$ |
|  | 70 | 1.995-2.442 | 2.014-2.372 | 2.081-2.281 |  |
|  | 75 | 2.209-2.624 | 2.277-2.586 | 2.363-2.521 |  |
|  | 80 | 2.496-3.065 | 2.526-3.050 | 2.588-2.718 |  |
|  | 85 | 2.731-3.557 | 2.862-3.456 | 3.063-3.335 |  |
|  | 90 | 3.385-4.590 | 3.404-4.565 | 3.733-4.218 |  |
|  | 95 | 4.581-6.624 | 4.607-6.557 | 5.285-5.516 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=179.373$ | 5 | 42.275-54.420 | 42.841-54.320 | 44.552-51.580 | WATER FLUX = |
|  | 10 | 54.326-62.650 | 54.533-61.904 | 56.655-59.630 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 60.106-80.544 | 60.426-79.700 | 63.180-75.151 |  |
|  | 20 | 74.830-88.356 | 76.214-87.602 | 80.504-85.783 |  |
|  | 25 | 85.155-96.986 | 85.720-96.555 | 87.574-92.811 |  |
| STD. DEV. = | 30 | 90.902-110.376 | $92.727-108.186$ | $95.443-101.244$ | $\text { FALL DISTANCE }=$ |
| $=121.228$ | 35 | 97.854-125.942 | $99.912-122.281$ | $107.115-114.005$ | $=500 \mathrm{~cm}$ |
|  | 40 | 111.136-135.726 | 111.912-133.949 | 116.361-129.597 |  |
|  | 45 | 125.814-150.031 | 126.751-148.549 | 132.704-141.580 |  |
|  | 50 | 135.278-166.429 | 136.196-165.840 | 144.302-158.520 |  |
| SAMPLE SIZE = | 55 | 148.858-184.184 | 153.727-181.451 | 161.844-170.938 | AEROSOL MASS |
| $=360$ | 60 | 166.326-202.022 | 166.733-199.098 | 176.866-188.765 | FRACTION REMAINING $=$ |
|  | 65 | 184.023-214.980 | 186.118-213.849 | 195.213-206.437 | $=0.9$ |
|  | 70 | 202.907-228.962 | 204.920-227.891 | 211.865-224.063 |  |
|  | 75 | 216.793-254.651 | 221.382-244.374 | 226.980-236.431 |  |
|  | 80 | 233.937-288.557 | 236.359-286.482 | 243.209-269.213 |  |
|  | 85 | 268.166-335.392 | 270.539-332.591 | 286.750-306.754 |  |
|  | 90 | 317.443-371.867 | 318.316-366.868 | 337.071-351.954 |  |
|  | 95 | 368.378-432.396 | 372.560-421.307 | 386.817-404.523 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=130.703$ | 5 | 32.831-41.964 | 33.631-41.000 | 36.007-38.339 | WATER FLUX = |
|  | 10 | 41.125-50.918 | 42.350-50.506 | 45.062-48.465 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 48.646-57.109 | 49.376-56.569 | 51.111-54.283 |  |
|  | 20 | 53.785-67.815 | 54.411-66.067 | 56.939-62.190 |  |
|  | 25 | 60.456-75.886 | 61.891-74.316 | 66.062-71.458 |  |
| STD. DEV. = | 30 | 69.986-83.194 | 70.785-81.162 | 73.470-79.521 | FALL DISTANCE = |
| $=86.165$ | 35 | 77.591-92.204 | 78.802-90.792 | 80.507-85.928 | $=500 \mathrm{~cm}$ |
|  | 40 | 83.364-104.720 | 84.632-103.109 | 87.666-96.501 |  |
|  | 45 | 92.190-116.282 | 94.455-114.337 | 100.068-107.736 |  |
|  | 50 | 104.072-122.165 | 105.311-120.884 | 109.629-118.793 |  |
| SAMPLE SIZE = | 55 | 115.861-130.754 | 116.562-129.150 | 120.502-123.320 | AEROSOL MASS |
| $=360$ | 60 | 121.599-144.965 | 122.580-143.602 | 127.317-137.904 | FRACTION REMAINING = |
|  | 65 | 130.471-156.130 | 132.384-152.600 | 142.111-146.777 | $=0.5$ |
|  | 70 | 145.201-168.198 | 146.080-164.669 | 150.093-158.149 |  |
|  | 75 | 156.682-179.889 | 156.952-178.154 | 162.452-172.345 |  |
|  | 80 | 170.658-200.165 | 172.125-198.296 | 178.070-191.294 |  |
|  | 85 | 189.754-231.724 | 192.274-221.914 | 199.393-211.822 |  |
|  | 90 | 213.620-261.032 | 218.596-258.747 | 233.888-252.187 |  |
|  | 95 | 259.433-324.108 | 261.049-322.959 | 272.787-302.453 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{\mathbf{- 1}}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=106.332$ | 5 | 25.414-35.517 | 25.918-34.609 | 29.597-32.497 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 34.689-41.054 | 35.565-40.670 | 37.665-39.668 |  |
|  | 15 | 39.976-46.437 | 40.081-46.205 | 41.755-43.814 |  |
|  | 20 | 43.417-54.347 | 44.263-53.568 | 46.429-49.715 |  |
|  | 25 | 48.849-62.786 | 49.660-61.562 | 53.504-58.068 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =69.432 \end{aligned}$ | 30 | 57.335-69.889 | 57.967-69.484 | 61.015-65.536 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =500 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 63.505-76.328 | 64.958-75.314 | 67.830-72.060 |  |
|  | 40 | 69.948-85.143 | 70.682-84.650 | 74.485-80.154 |  |
|  | 45 | 76.203-90.411 | 77.412-90.044 | 82.563-87.352 |  |
|  | 50 | 84.813-100.684 | 85.722-99.404 | 89.046-93.558 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 90.093-108.721 | 90.486-107.047 | 97.194-103.749 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | 100.219-118.435 | 101.110-116.913 | 105.934-111.472 |  |
|  | 65 | 108.716-124.977 | 110.354-123.881 | 113.693-120.304 |  |
|  | 70 | 118.545-134.183 | 120.038-131.378 | 122.239-126.792 |  |
|  | 75 | 125.709-147.408 | 126.639-145.935 | 129.389-137.994 |  |
|  | 80 | 135.219-161.380 | 137.892-160.363 | 145.613-152.929 |  |
|  | 85 | 152.782-184.923 | 154.204-183.892 | 160.736-177.853 |  |
|  | 90 | 179.446-216.876 | 182.084-207.701 | 186.076-198.985 |  |
|  | 95 | 208.222-275.805 | 217.053-258.056 | 227.611-246.574 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=75.936$ | 5 | 17.121-23.187 | 17.241-23.012 | 19.487-21.118 | WATER FLUX = |
|  | 10 | 23.053-29.490 | 23.445-29.328 | 25.001-27.915 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 28.257-33.165 | 28.376-32.827 | 29.825-31.719 |  |
|  | 20 | 31.644-39.051 | 32.033-38.676 | 33.100-36.195 |  |
|  | 25 | 35.351-44.312 | 35.891-43.992 | 38.628-41.075 |  |
| STD. DEV. = | 30 | 39.668-49.758 | 40.885-48.960 | 43.340-46.880 | FALL DISTANCE $=$ |
| $=51.273$ | 35 | 44.626-52.945 | 46.021-52.135 | 48.576-50.919 | $=500 \mathrm{~cm}$ |
|  | 40 | 49.834-59.236 | 50.084-58.091 | 51.819-55.007 |  |
|  | 45 | 52.627-64.666 | 53.968-64.106 | 56.885-61.116 |  |
|  | 50 | 58.631-70.906 | 59.747-69.146 | 63.361-65.174 |  |
| SAMPLE SIZE = | 55 | 64.363-76.744 | 64.888-75.368 | 67.083-72.548 | AEROSȮL MASS |
| $=360$ | 60 | 70.089-84.541 | 71.723-83.306 | 74.478-78.471 | FRACTION REMAINING $=$ |
|  | 65 | 76.596-91.373 | 78.160-89.588 | 82.668-86.675 | $=0.1$ |
|  | 70 | 84.937-96.711 | 85.686-95.683 | 89.119-93.488 |  |
|  | 75 | 92.038-103.152 | 92.316-101.492 | 95.348-98.624 |  |
|  | 80 | 97.478-114.777 | 98.511-112.557 | 101.409-108.345 |  |
|  | 85 | 107.796-136.532 | 108.594-133.713 | 112.738-120.299 |  |
|  | 90 | 121.091-162.157 | 130.062-156.260 | 138.260-145.994 |  |
|  | 95 | 156.537-203.318 | 162.200-194.298 | 166.840-181.878 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=47.779$ | 5 | 10.299-13.328 | 10.385-12.452 | 10.912-11.594 | $\begin{aligned} & \text { WATER FLUX }= \\ & =.0 .25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 12.495-17.485 | 13.461-17.325 | 15.100-16.514 |  |
|  | 15 | 16.601-21.587 | 16.815-20.989 | 17.913-19.525 |  |
|  | 20 | 19.414-23.709 | 19.710-23.328 | 21.362-22.598 |  |
|  | 25 | 22.101-26.273 | 22.536-25.766 | 23.280-24.396 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =35.133 \end{aligned}$ | 30 | 23.960-29.424 | 24.189-28.642 | 25.733-27.590 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =500 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 26.784-32.678 | 27.146-32.515 | 28.359-31.105 |  |
|  | 40 | 29.652-35.054 | 30.634-34.813 | 31.988-33.121 |  |
|  | 45 | 32.592-39.156 | 32.860-38.419 | 33.832-36.708 |  |
|  | 50 | 34.941-43.034 | 35.223-42.333 | 37.780-40.456 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 38.868-47.938 | 39.480-47.246 | 41.767-44.434 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 42.970-52.316 | 43.456-52.009 | 45.528-49.117 |  |
|  | 65 | 47.894-56.473 | 48.680-55.641 | 51.134-53.726 |  |
|  | 70 | 52.497-60.636 | 53.445-60.215 | 55.418-57.903 |  |
|  | 75 | 56.641-66.377 | 57.450-65.007 | 60.153-63.164 |  |
|  | 80 | 62.434-71.906 | 63.123-70.592 | 64.894-69.110 |  |
|  | 85 | 68.944-83.522 | 69.360-81.999 | 71.635-76.639 |  |
|  | 90 | 79.985-102.424 | 80.724-98.823 | 84.065-94.184 |  |
|  | 95 | 98.849-133.719 | 102.628-132.216 | 106.318-120.545 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=39.459$ | 5 | 7.479-10.051 | 7.768-9.315 | 8.064-8.463 |  |
|  | 10 | 9.348-13.313 | 10.162-13.121 | 11.382-12.578 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 12.599-15.776 | 12.758-15.710 | 13.390-14.859 |  |
|  | 20 | 14.710-17.974 | 14.969-17.480 | 15.755-17.024 |  |
|  | 25 | 16.737-20.044 | 17.006-19.660 | 17.464-18.686 |  |
| STD. DEV. = | 30 | 18,357-22.297 | 18.577-22.057 | 19.492-21.049 | FALL DISTANCE = |
| $=44.391$ | 35 | 20.181-24.869 | 20.567-24.729 | 21.603-23.526 | $=500 \mathrm{~cm}$ |
|  | 40 | 22.484-27.517 | 23.109-26.954 | 24.672-25.511 |  |
|  | 45 | 24.837-30.068 | 25.090-29.840 | 26.066-28.924 |  |
|  | 50 | 27.455-32.748 | 28.243-32.450 | 29.481-30.926 |  |
| SAMPLE SIZE = | 55 | 30.026-36.699 | 30.513-36.355 | 32.087-33.683 |  |
| $=360$ | 60 | $32.564-40.308$ | $33.038-40.056$ | $35.105-38.289$ | FRACTION REMAINING $=$ |
|  | 65 | $36.685-43.672$ | $37.292-43.092$ | $39.569-41.168$ | $=0.001$ |
|  | 70 | 40.396-48.614 | 40.695-47.420 | $42.655-45.560$ |  |
|  | 75 | 44.780-53.293 | 45.198-52.246 | 46.787-49.831 |  |
|  | 80 | 49.364-58.028 | 49.791-57.294 | 52.070-54.479 |  |
|  | 85 | 54.239-67.176 | 56.162-65.009 | 57.680-61.506 |  |
|  | 90 | 62.344-79.268 | 63.224-78.441 | 68.339-76.863 |  |
|  | 95 | 78.631-118.879 | 79.405-115.399 | 88.117-104.330 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{\mathbf{- 1}}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=162.608$ | 5 | 38.875-46.008 | 36.773-45.946 | 39.087-43.357 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 45.946-53.962 | 46.143-52.854 | 48.098-49.726 |  |
|  | 15 | 50.518-68.012 | 51.146-66.783 | 56.979-64.080 |  |
|  | 20 | 63.734-73.124 | 64.786-72.570 | 67.751-69.694 |  |
|  | 25 | 69.086-81.865 | 69.635-81.776 | 72.486-76.183 |  |
| $\begin{aligned} & \text { STD. DEV. = } \\ & =117.010 \end{aligned}$ | 30 | 75.430-91.688 | 76.154-90.239 | 80.929-85.074 | $\begin{aligned} & \text { FALL DISTANCE = } \\ & =853 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 83.398-104.663 | 83.958-102.013 | 89.822-93.735 |  |
|  | 40 | 91.816-117.592 | 92.530-115.915 | 101.273-110.137 |  |
|  | 45 | 104.337-131.233 | 106.949-129.843 | 113.169-122.867 |  |
|  | 50 | 117.444-154.228 | 119.650-150.400 | 128.227-138.510 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 130.354-167.888 | 134.399-166.535 | 147.470-159.673 | AEROSOL MASS <br> FRACTION REMAINING = $=0.9$ |
|  | 60 | 152.948-180.662 | 156.127-179.668 | 163.638-171.108 |  |
|  | 65 | 167.834-198.759 | 170.586-194.933 | 176.591-185.262 |  |
|  | 70 | 180.974-215.694 | 182.995-214.343 | 190.975-207.005 |  |
|  | 75 | 199.470-233.203 | 204.814-227.291 | 213.360-217.866 |  |
|  | 80 | 217.088-257.837 | 217.858-254.234 | 227.183-243.682 |  |
|  | 85 | 240.439-313.511 | 248.189-300.690 | 256.092-274.625 |  |
|  | 90 | 287.947-353.723 | 296.267-348.861 | 320.069-337.157 |  |
|  | 95 | 349.695-403.029 | 355.516-398.835 | 379.474-394.194 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=96.439$ | 5 | 22.557-29.804 | 22.699-29.256 | 24.931-26.741 | WATER FLUX = |
|  | 10 | 29.310-33.939 | 29.871-33.451 | 31.218-32.652 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 32.780-39.932 | 33.019-39.159 | 34.445-37.504 |  |
|  | 20 | 36.450-45.514 | 38.001-45.340 | 39.876-43.864 |  |
|  | 25 | 42.393-52.327 | 43.605-51.792 | 45.310-47.719 |  |
| STD. DEV. $=$ | 30 | 46.725-58.203 | 47.389-56.902 | 51.108-54.490 | FALL DISTANCE = |
| $=66.126$ | 35 | 53.168-64.205 | 53.693-62.834 | 56.067-60.193 | $=853 \mathrm{~cm}$ |
|  | 40 | 58.441-71.046 | 59.416-69.969 | 62.143-67.498 |  |
|  | 45 | 63.836-81.073 | 66.506-80.169 | 69.280-73.740 |  |
|  | 50 | 70.654-90.981 | 71.531-88.291 | 77.661-82.729 |  |
| SAMPLE SIZE = | 55 | 80.389-98.921 | 81.451-98.286 | 84.153-94.281 | AEROSOL MASS |
| $=360$ | 60 | 89.692-108.132 | 91.068-106.534 | 97.058-103.037 | FRACTION REMAINING $=$ |
|  | 65 | 98.889-116.125 | 100.702-115.467 | 105.164-111.361 | $=0.3$ |
|  | 70 | 108.190-122.894 | 109.606-122.207 | 115.223-118.393 |  |
|  | 75 | 116.406-133.651 | 117.192-131.372 | 120.593-125.124 |  |
|  | 80 | 124.030-155.786 | 125.033-153.629 | 131.331-142.524 |  |
|  | 85 | 141.599-179.056 | 143.933-178.234 | 153.741-172.221 |  |
|  | 90 | 173.437-204.845 | 175.959-199.056 | 179.341-188.088 |  |
|  | 95 | 199.222-255.299 | 205.607-251.121 | 217.860-230.778 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=68.901$ | 5 | 15.603-19.687 | 15.657-18.927 | 16.385-17.627 | WATER FLUX = |
|  | 10 | 19.000-24.372 | 19.691-24.171 | 21.485-23.698 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 23.860-27.504 | 24.080-26.940 | 24.619-25.878 |  |
|  | 20 | 25.835-32.785 | 26.058-32.064 | 27.361-30.669 |  |
|  | 25 | 29.718-37.190 | 30.567-36.746 | 31.991-35.260 |  |
| STD. DEV. = | 30 | 33.698-41.479 | 34.692-40.865 | 36.574-38.562 | FALL DISTANCE $=$ |
| $=48.238$ | 35 | 37.758-45.759 | 37.947-44.953 | 40.738-42.973 | $=853 \mathrm{~cm}$ |
|  | 40 | 41.549-50.454 | 42.068-49.666 | 43.543-47.268 |  |
|  | 45 | 45.718-55.945 | 46.721-55.672 | 49.038-52.026 |  |
|  | 50 | 50.374-63.041 | 50.903-61.418 | 53.885-57.275 |  |
| SAMPLE SIZE $=$ | 55 | 55.758-70.260 | 56.120-69.645 | 59.982-65.092 | AEROSOL MASS |
| $=360$ | 60 | 62.585-76.263 | 63.352-75.724 | 68.353-71.765 | FRACTION REMAINING $=$ |
|  | 65 | 70.204-82.828 | 71.094-82.335 | 74.532-77.805 | $=0.1$ |
|  | 70 | 76.580-90.006 | 77.448-88.533 | 80.194-84.520 |  |
|  | 75 | 83.295-97.676 | 84.019-96.009 | 87.781-92.507 |  |
|  | 80 | 91.423-110.062 | 92.391-106.810 | 95.757-100.697 |  |
|  | 85 | 99.835-132.209 | 101.247-127.826 | 108.561-115.075 |  |
|  | 90 | 115.907-153.494 | 121.338-148.608 | 134.257-141.650 |  |
|  | 95 | 150.339-189.701 | 154.047-182.635 | 161.986-176.218 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=43.564$ | 5 | 8.664-10.981 | 8.672-10.562 | 9.079-9.483 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 10.568-14.889 | 11.026-14.579 | 12.753-13.734 |  |
|  | 15 | 14.078-17.369 | 14.340-17.166 | 15.093-15.976 |  |
|  | 20 | 15.841-19.372 | 16.384-19.071 | 17.297-18.331 |  |
|  | 25 | 18.071-22.208 | 18.311-22.038 | 19.036-20.992 |  |
| STD. DEV. $=$$=33.080$ | 30 | 20.174-25.143 | 20.527-24.961 | 21.762-23.660 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =853 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 22.316-28.057 | 23.174-27.238 | 24.749-25.657 |  |
|  | 40 | 25.202-31.266 | 25.356-30.810 | 26.524-28.679 |  |
|  | 45 | 28.017-34.402 | 28.151-33.943 | 30.056-32.462 |  |
|  | 50 | 31.222-38.980 | 31.769-38.747 | 33.343-36.243 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 34.080-42.597 | 35.186-42.435 | 38.266-39.988 | AEROSOL MASS FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 38.937-45.734 | 39.359-44.931 | 41.830-43.767. |  |
|  | 65 | 42.575-50.503 | 43.058-50.251 | 44.390-47.251 |  |
|  | 70 | 45.798-57.620 | 46.620-56.394 | 49.377-53.195 |  |
|  | 75 | 51.753-63.138 | 52.411-62.612 | 56.044-59.421 |  |
|  | 80 | 58.454-68.196 | 59.401-67.473 | 62.564-66.016 |  |
|  | 85 | 65.956-81.502 | 66.246-79.423 | 67.623-73.202 |  |
|  | 90 | 74.323-99.871 | 77.239-95.992 | 82.204-91.371 |  |
|  | 95 | 96.004-128.016 | 100.201-126.639 | 103.566-117.030 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=34.255$ | 5 | 6.283-8.324 | 6.302-8.049 | 6.751-7.121 | WATER FLUX = |
|  | 10 | 8.136-11.388 | 8.336-11.343 | 9.402-10.413 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 10.594-12.851 | 10.800-12.741 | 11.494-12.172 |  |
|  | 20 | 12.104-14.798 | 12.398-14.610 | 12.826-13.936 |  |
|  | 25 | 13.540-16.918 | 13.820-16.845 | 14.610-16.018 |  |
| STD. DEV. = | 30 | 15.429-18.882 | 15.681-18.513 | 16.582-17.747 | FALL DISTANCE = |
| $=27.243$ | 35 | 16.970-21.249 | 17.280-20.833 | 18.199-19.654 | $=853 \mathrm{~cm}$ |
|  | 40 | 18.949-24.355 | 19.359-24.101 | 20.173-22.517 |  |
|  | 45 | 21.178-27.054 | 21.796-26.578 | 23.591-25.060 |  |
|  | 50 | 24.326-29.468 | 24.453-29.190 | 25.743-28.456 |  |
| SAMPLE SIZE $=$ | 55 | 26.754-32.125 | 27.974-31.758 | 28.930-30.877 | AEROSOL MASS |
| $=360$ | 60 | 29.335-36.034 | 29.768-35.696 | 31.565-33.658 | FRACTION REMAINING $=$ |
|  | 65 | 32.120-39.713 | 32.616-38.886 | 34.810-37.902 | $=0.001$ |
|  | 70 | 36.210-44.525 | 37.407-43.670 | 38.177-40.719 |  |
|  | 75 | 39.938-50.347 | 40.425-49.500 | 42.520-47.370 |  |
|  | 80 | 45.756-55.423 | 47.308-54.672 | 49.441-52.397 |  |
|  | 85 | 52.209-63.014 | 52.516-61.482 | 55.395-58.442 |  |
|  | 90 | 59.677-76.909 | 60.560-75.928 | 65.580-72.550 |  |
|  | 95 | 76.030-105.144 | 76.927-103.465 | 82.141-94.062 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=157.848$ | 5 | 32.600-43.203 | 34.424-42.923 | 37.284-40.243 | WATER FLUX = |
|  | 10 | 43.011-53.839 | 43.322-52.706 | 44.969-46.836 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 47.390-63.314 | 48.159-62.837 | 54.368-59.776 |  |
|  | 20 | 59.440-69.195 | 60.124-67.561 | 63.146-65.447 |  |
|  | 25 | 64.454-76.741 | 65.041-76.238 | 67.544-71.156 |  |
| STD. DEV. = | 30 | 70.476-86.899 | 70.835-85.382 | 75.675-79.529 | FALL DISTANCE = |
| $=116.345$ | 35 | 77.385-97.246 | 78.402-94.812 | 84.463-91.377 | $=1000 \mathrm{~cm}$ |
|  | 40 | 87.181-111.476 | 89.172-110.228 | 93.350-101.332 |  |
|  | 45 | 96.820-128.139 | 98.804-126.166 | 106.996-117.872 |  |
|  | 50 | 111.356-148.844 | 115.432-144.414 | 121.340-136.124 |  |
| SAMPLE SIZE = | 55 | 127.335-162.658 | $129.392-160.288$ | $140.643-153.609$ |  |
| $=360$ | $60$ | $147.740-176.220$ | 151.276-173.226 | $155.718-166.369$ | FRACTION REMAINING $=$ |
|  | $65$ | $162.573-196.804$ | $163.737-190.932$ | $170.362-179.208$ | $=0.9$ |
|  | $70$ | $177.116-211.720$ | $178.145-207.004$ | $186.452-202.733$ |  |
|  | 75 | $197.762-224.554$ | $201.614-218.990$ | $205.732-214.886$ |  |
|  | 80 | 213.977-254.190 | 214.763-250.328 | 218.387-234.925 |  |
|  | 85 | 233.687-305.581 | 237:562-294.999 | 251.228-272.144 |  |
|  | 90 | 277.592-351.812 | 287.074-346.965 | 312.847-334.422 |  |
|  | 95 | 347.649-396.822 | 353.672-394.313 | 377.465-392.147 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=114.749$ | 5 | 26.763-34.158 | 27.929-32.920 | 28.947-32.021 | WATER FLUX = |
|  | 10 | 32.999-38.915 | 34.253-38.542 | 35.345-37.710 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 38.037-47.239 | 38.295-45.879 | 39.676-42.219 |  |
|  | 20 | 42.122-52.714 | 42.678-52.051 | 46.729-50.417 |  |
|  | 25 | 50.008-59.345 | 50.277-58.782 | 52.016-55.350 |  |
| STD. DEV. = | 30 | 54.415-64.048 | 54.846-63.652 | 58.319-60.600 | FALL DISTANCE $=$ |
| $=81.263$ | 35 | 59.549-71.884 | 60.195-71.223 | 61.734-68.512 | $=1000 \mathrm{~cm}$ |
|  | 40 | 64.348-84.074 | 65.631-83.333 | 69.907-77.849 |  |
|  | 45 | 71.812-95.246 | 75.081-91.112 | 81.883-87.269 |  |
|  | 50 | 84.033-108.380 | 86.010-107.654 | 89.496-99.013 |  |
| SAMPLE SIZE $=$ | 55 | 94.173-117.818 | 96.279-116.571 | 103.721-111.982 | AEROSOL MASS |
| $=360$ | 60 | 107.886-126.709 | 109.502-126.026 | 115.079-121.518 | FRACTION REMAINING $=$ |
|  | 65 | 117.816-140.540 | 119.595-138.879 | 124.875-131.499 | $=0.5$ |
|  | 70 | 126.841-149.644 | 129.622-148.467 | 137.383-143.064 |  |
|  | 75 | 140.995-164.291 | 142.557-161.293 | 147.458-153.078 |  |
|  | 80 | 152.162-188.870 | 152.982-186.249 | 160.102-171.442 |  |
|  | 85 | 170.780-212.050 | 171.931-211.114 | 187.569-197.301 |  |
|  | 90 | 199.338-246.447 | 205.097-244.232 | 215.885-236.327 |  |
|  | 95 | 244.296-307.474 | 246.534-304.217 | 254.379-275.589 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=93.558$ | 5 | 21.247-27.818 | 21.759-27.695 | 23.599-25.617 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 27.719-31.728 | 27.953-31.513 | 29.448-30.301 |  |
|  | 15 | 30.500-38.115 | 30.663-37.191 | 32.171-35.223 |  |
|  | 20 | 34.915-43.983 | 35.636-43.532 | 37.731-41.296 |  |
|  | 25 | 39.640-49.566 | 41.208-48.388 | 43.387-45.557 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =65.393 \end{aligned}$ | 30 | 44.343-54.120 | 45.233-53.073 | 47.904-51.229 | $\text { FALL DISTANCE }=$ |
|  | 35 | 49.819-61.418 | 50.860-59.433 | 52.203-56.787 |  |
|  | 40 | 54.399-68.142 | 55.411-65.782 | 58.127-62.694 |  |
|  | 45 | 61.391-75.980 | 61.625-75.116 | 64.125-70.821 |  |
|  | 50 | 68.034-86.165 | 68.489-85.202 | 74.114-81.176 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 75.736-96.607 | 78.662-94.793 | 82.476-89.953 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | 85.872-105.771 | 89.147-104.798 | 92.275-98.831 |  |
|  | 65 | 96.366-114.393 | 97.600-113.073 | 103.594-107.566 |  |
|  | 70 | 106.178-120.452 | 106.949-118.749 | $110.727-115.552$ |  |
|  | 75 | 115.054-131.252 | 115.305-129.770 | 118.253-122.898 |  |
|  | 80 | 121.694-154.106 | 122.742-152.267 | 129.270-141.368 |  |
|  | 85 | 140.472-177.140 | 142.588-175.451 | 152.460-168.890 |  |
|  | 90 | 171.436-202.846 | 173.763-196.900 | 177.477-186.293 |  |
|  | 95 | 197.052-252.397 | 203.517-249.096 | 214.421-227.587 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=66.821$ | 5 | 14.465-18.257 | 14.576-17.641 | 15.732-16.772 | WATER FLUX = |
|  | 10 | 17.699-22.860 | 18.439-22.685 | 20.093-22.251 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 22.294-26.087 | 22.380-25.535 | 23.137-24.317 |  |
|  | 20 | 24.232-30.690 | 24.397-30.520 | 25.865-29.256 |  |
|  | 25 | 28.201-34.855 | 29.254-34.283 | 30.467-32.859 |  |
| STD. DEV. = | 30 | 31.801-38.984 | 32.794-38.545 | 34.032-37.583 | FALL DISTANCE = |
| $=47.535$ | 35 | 35.103-43.330 | 36.435-42.601 | 37.866-40.225 | $=1000 \mathrm{~cm}$ |
|  | 40 | 39.105-48.452 | 39.528-47.267 | 41.348-45.452 |  |
|  | 45 | 43.301-52.056 | 43.811-51.680 | 46.541-49.724 |  |
|  | 50 | 48.399-61.921 | 48.711-59.885 | 50.931-55.178 |  |
| SAMPLE SIZE $=$ | 55 | 51.869-68.315 | 52.691-66.317 | 57.727-63.483 | AEROSOL MASS |
| $=360$ | 60 | 60.851-74.327 | 62.688-73.464 | 64.952-70.422 | FRACTION REMAINING $=$ |
|  | 65 | 68.066-81.264 | 68.843-78.611 | 71.859-75.284 | $=0.1$ |
|  | 70 | 74.588-88.652 | 74.970-87.013 | 77.602-82.780 |  |
|  | 75 | 81.946-95.387 | 82.386-93.885 | 86.190-91.195 |  |
|  | 80 | 90.309-107.559 | 91.152-105.367 | 93.446-99.693 |  |
|  | 85 | 98.765-130.900 | 100.408-126.745 | 106.009-113.803 |  |
|  | 90 | 114.570-151.895 | 120.046-146.943 | 133.025-139.536 |  |
|  | 95 | 148.550-187.145 | 152.386-179.834 | 160.630-171.087 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=42.222$ | 5 | 8.055-10.341 | 8.065-10.076 | 8.454-9.267 | WATER FLUX = |
|  | 10 | 10.114-14.062 | 10.412-13.886 | 11.897-13.212 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 13.362-16.290 | 13.446-16.120 | 14.165-14.830 |  |
|  | 20 | 14.795-18.008 | 15.282-17.694 | 16.256-17.112 |  |
|  | 25 | 16.825-20.874 | 17.062-20.487 | 17.669-19.517 |  |
| STD. DEV. $=$ | 30 | 18.752-23.530 | 19.369-23.286 | 20.319-22.317 | FALL DISTANCE $=$ |
| $=32.539$ | 35 | 20.969-26.040 | 21.984-25.714 | 23.068-24.179 | $=1000 \mathrm{~cm}$ |
|  | 40 | 23.605-30.362 | 23.980-29.646 | 25.176-26.831 |  |
|  | 45 | 26.021-33.093 | 26.277-32.810 | 28.595-30.935 |  |
|  | 50 | 30.166-38.429 | 30.452-36.961 | 31.844-34.513 |  |
| SAMPLE SIZE $=$ | 55 | 33.003-40.785 | 33.341-40.047 | 36.307-39.247 | AEROSOL MASS |
| $=360$ | 60 | 37.943-44.070 | 38.656-43.567 | 39.477-41.374 | FRACTION REMAINING $=$ |
|  | 65 | 40.722-49.968 | 41.134-49.216 | 42.356-46.356 | $=0.01$ |
|  | 70 | 44.190-56.264 | 45.463-54.823 | 47.723-52.026 |  |
|  | 75 | 50.584-61.784 | 51.683-61.372 | 54.037-58.963 |  |
|  | 80 | 57.907-67.256 | 58.945-66.800 | 61.256-65.370 |  |
|  | 85 | 65.226-79.641 | 65.517-78.280 | 66.988-72.353 |  |
|  | 90 | 73.479-96.218 | 76.400-95.113 | 81.094-90.470 |  |
|  | 95 | 95.138-126.438 | 96.599-122.327 | 103.034-115.831 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=33.223$ | 5 | 5.858-7.733 | 5.869-7.481 | 6.282-6.840 | WATER FLUX = |
|  | 10 | 7.542-10.732 | 7.894-10.632 | 8.738-9.878 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 9.906-12.345 | 10.316-11.990 | 10.755-11.426 |  |
|  | 20 | 11.346-13.908 | 11.623-13.672 | 12.324-12.981 |  |
|  | 25 | 12.678-16.001 | 12.860-15.729 | 13.668-14.813 |  |
| STD. DEV. = | 30 | 14.390-18.007 | 14.711-17.892 | 15.533-16.737 | FALL DISTANCE $=$ |
| $=26.711$ | 35 | 16.073-20.084 | 16.544-19.659 | 17.297-18.661 | $=1000 \mathrm{~cm}$ |
|  | 40 | 18.026-23.614 | 18.265-23.242 | 19.240-21.082 |  |
|  | 45 | 20.051-26.081 | 20.206-25.240 | 22.437-24.169 |  |
|  | 50 | 23.604-28.887 | 23.732-28.718 | 24.370-27.429 |  |
| SAMPLE SIZE $=$ | 55 | 25.601-31.207 | 26.516-30.701 | 28.257-29.379 | AEROSOL MASS |
| $=360$ | 60 | 28.855-35.093 | 29.163-34.628 | 30.174-31.889 | FRACTION REMAINING $=$ |
|  | 65 | 31.146-38.804 | 31.261-38.112 | 33.607-35.778 | $=0.001$ |
|  | 70 | 35.161-44.062 | 35.493-42.966 | 37.616-39.960 |  |
|  | 75 | 39.325-49.036 | 39.767-48.310 | 42.187-46.108 |  |
|  | 80 | 45.097-54.811 | 45.926-53.655 | 48.174-51.687 |  |
|  | 85 | 51.631-62.010 | 51.828-60.815 | 54.233-57.782 |  |
|  | 90 | 58.030-76.351 | 59.776-75.256 | 64.754-71.780 |  |
|  | 95 | 75.389-103.845 | 76.413-98.508 | 77.798-91.953 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=144.382$ | 5 | 26.338-35.099 | 27.728-34.515 | 30.824-32.880 | WATER FLUX = |
|  | 10 | 34.590-46.083 | 35.167-43.669 | 36.088-38.272 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 39.052-51.446 | 41.149-51.132 | 46.310-50.331 |  |
|  | 20 | 49.984-56.476 | 50.381-55.407 | 51.349-53.384 |  |
|  | 25 | 52.476-62.652 | 53.377-61.986 | 55.309-59.543 |  |
| STD. DEV. = | 30 | 57.632-71.533 | 59.023-69.910 | 61.628-67.440 | FALL DISTANCE = |
| $=114.627$ | 35 | 63.179-82.384 | 65.796-79.761 | 69.342-76.326 | $=1584 \mathrm{~cm}$ |
|  | 40 | 71.755-92.883 | 74.774-92.040 | 77.734-86.303 |  |
|  | 45 | 82.231-115.372 | 84.197-112.043 | 88.412-100.874 |  |
|  | 50 | 92.655-128.004 | 93.911-126.419 | 108.094-118.246 |  |
| SAMPLE SIZE $=$ | 55 | 114.330-148.424 | 116.532-142.756 | 124.351-133.958 | AEROSOL MASS |
| $=360$ | 60 | 127.619-162.792 | 129.680-160.579 | 138.657-154.516 | FRACTION REMAINING = |
|  | 65 | 147.949-176.079 | 150.343-174.243 | 158.163-167.211 | $=0.9$ |
|  | 70 | 163.426-197.100 | 164.936-192.622 | 173.186-182.194 |  |
|  | 75 | 178.271-209.992 | 180.368-208.995 | 190.080-202.830 |  |
|  | 80 | 201.439-240.670 | 202.672-238.968 | 208.861-215.937 |  |
|  | 85 | 215.760-287.877 | 221.195-284.604 | 239.450-261.364 |  |
|  | 90 | 263.399-340.811 | 272.434-336.391 | 297.600-317.514 |  |
|  | 95 | 336.459-389.639 | 340.846-388.093 | 365.532-385.259 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=105.152$ | 5 | 22.658-27.930 | 22.740-27.562 | 23.880-25.329 | WATER FLUX = |
|  | 10 | 27.634-31.803 | 27.952-31.652 | 28.788-30.795 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 30.912-38.174 | 31.260-37.692 | 32.008-35.546 |  |
|  | 20 | 35.455-44.184 | $35.751-43.624$ | 37.905-41.772 |  |
|  | 25 | 41.130-48.769 | 41.494-48.215 | 43.582-46.455 |  |
| STD. DEV. = | 30 | 45.082-53.025 | 45.892-52.426 | 47.917-49.683 | FALL DISTANCE = |
| $=80.061$ | 35 | 48.896-59.788 | 49.474-58.685 | 51.185-54.799 | $=1584 \mathrm{~cm}$ |
|  | 40 | 53.320-69.684 | 54.506-68.362 | 57.037-64.946 |  |
|  | 45 | 59.721-81.490 | 63.069-80.195 | 67.023-72.561 |  |
|  | 50 | 69.349-95.779 | 70.630-94.864 | 78.832-86.987 |  |
| SAMPLE SIZE = | 55 | 81.363-106.594 | 84.716-105.903 | 91.634-99.796 |  |
| $=360$ | $60$ | $95.703-116.020$ | 96.153-114.889 | $102.903-110.708$ | FRACTION REMAINING $=$ |
|  | 65 | $106.505-132.841$ | $107.712-128.368$ | $113.108-122.096$ | $=0.5$ |
|  | 70 | 116.689-143.586 | 118.880-142.290 | $124.640-137.065$ |  |
|  | 75 | 134.531-157.251 | 136.227-153.490 | 141.046-146.354 |  |
|  | 80 | 145.544-180.690 | 146.241-177.344 | 153.468-165.560 |  |
|  | 85 | 164.914-205.718 | 167.023-199.966 | 178.660-186.527 |  |
|  | 90 | 191.684-238.362 | 194.375-237.302 | 206.465-224.575 |  |
|  | 95 | 237.452-297.041 | 238.407-296.049 | 246.475-265.623 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=60.960$ | 5 | 11.549-16.011 | 11.860-15.854 | 12.961-14.243 | WATER FLUX |
|  | 10 | 15.882-18.178 | 16.026-18.175 | 16.762-17.805 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 17.961-21.511 | 18.090-21.047 | 18.238-19.266 |  |
|  | 20 | 19.243-25.428 | 19.553-24.559 | 21.325-23.444 |  |
|  | 25 | 23.151-28.412 | 23.357-27.831 | 24.552-26.176 |  |
| STD. DEV. = | 30 | 25.945-32.143 | 26.162-31.419 | 27.543-30.011 | FALL DISTANCE $=$ |
| $=45.999$ | 35 | 29.099-36.822 | 29.735-36.138 | 31.087-34.255 | $=1584 \mathrm{~cm}$ |
|  | 40 | 32.198-40.157 | 32.728-39.732 | 34.973-37.549 |  |
|  | 45 | 36.814-46.842 | 37.099-45.550 | 39.159-41.606 |  |
|  | 50 | 40.046-53.357 | 40.239-52.963 | 43.873-49.038 |  |
| SAMPLE SIZE $=$ | 55 | 45.703-59.679 | 47.729-58.474 | 51.466-55.663 | AEROSOL MASS |
| $=360$ | 60 | 53.215-68.179 | 53.574-66.198 | 57.566-62.369 | FRACTION REMAINING $=$ |
|  | 65 | 59.563-75.005 | 60.234-74.520 | 63.752-71.852 | $=0.1$ |
|  | 70 | 68.486-84.265 | 69.470-81.636 | 73.346-79.350 |  |
|  | 75 | 75.801-92.284 | 78.048-90.131 | 81.303-87.505 |  |
|  | 80 | 85.939-103.663 | 87.419-102.795 | 90.066-96.621 |  |
|  | 85 | 95.947-124.786 | 97.079-122.851 | 103.274-109.739 |  |
|  | 90 | 110.272-143.848 | 115.276-139.034 | 127.701-134.490 |  |
|  | 95 | 140.151-174.098 | 114.251-173.554 | 152.370-161.149 |  |



|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=30.353$ | 5 | 4.850-6.737 | 4.948-6.289 | 5.139-5.876 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 6.315-8.574 | 6.758-8.490 | 6.974-7.892 |  |
|  | 15 | 7.994-9.798 | 8.233-9.692 | 8.691-9.231 |  |
|  | 20 | 9.221-11.332 | 9.421-11.248 | 9.794-10.679 |  |
|  | 25 | 10.489-13.005 | 10.597-12.698 | 11.233-12.103 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =25.448 \end{aligned}$ | 30 | 11.488-14.992 | 11.793-14.710 | 12.534-13.598 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =1584 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 13.224-17.192 | 13.338-16.802 | 14.565-15.708 |  |
|  | 40 | 15.102-19.902 | 15.458-19.111 | 16.418-18.129 |  |
|  | 45 | 17.179-23.133 | 17.556-22.929 | 18.585-21.195 |  |
|  | 50 | 19.748-25.703 | 20.141-24.647 | 22.411-23.651 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 23.029-28.107 | 23.247-27.834 | 23.931-27.006 | AEROSOL MASS FRACTION REMAINING = $=0.001$ |
|  | 60 | 25.289-31.244 | 25.828-30.708 | 27.683-29.043. |  |
|  | 65 | 28.083-36.480 | 28.272-36.173 | 30.083-33.915 |  |
|  | 70 | 31.425-40.442 | 32.913-39.280 | 35.788-38.186 |  |
|  | 75 | 37.011-47.052 | 38.041-46.681 | 39.000-43.500 |  |
|  | 80 | 42.327-52.538 | 43.409-51.386 | 46.611-49.732 |  |
|  | 85 | 49.648-59.246 | 49.826-58.698 | 51.852-54.107 |  |
|  | 90 | 55.647-73.089 | 57.034-72.418 | 59.486-68.294 |  |
|  | 95 | 72.670-99.845 | 73.161-94.726 | 75.261-87.888 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=138.403$ | 5 | 24.444-30.789 | 25.197-30.432 | 27.879-29.532 | WATER FLUX = |
|  | 10 | 30.510-39.726 | 30.898-38.743 | 32.030-34.451 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 35.626-45.576 | 37.238-45.115 | 40.706-44.586 |  |
|  | 20 | 44.248-51.878 | 44.642-51.068 | 45.404-47.775 |  |
|  | 25 | 47.429-56.188 | 47.763-55.754 | 51.058-53.661 |  |
| STD. DEV. = | 30 | 52.861-65.890 | 53.285-64.169 | $55.384-60.019$ | FALL DISTANCE = |
| $=114.599$ | 35 | 57.347-74.661 | 58.084-71.894 | $62.491-67.787$ | $=2000 \mathrm{~cm}$ |
|  | 40 | 66.053-87.184 | 66.587-85.854 | 69.234-78.235 |  |
|  | 45 | 74.477-104.954 | 75.537-102.255 | 82.011-91.812 |  |
|  | 50 | 86.396-119.933 | 89.913-117.300 | 96.826-110.243 |  |
| SAMPLE SIZE = | 55 | 102.734-139.448 | 109.499-137.038 | 113.708-127.068 | AEROSOL MASS |
| $=360$ | 60 | 119.686-154.978 | 121.636-154.204 | 132.959-145.714 | FRACTION REMAINING $=$ |
|  | 65 | 139.442-169.911 | 140.931-166.790 | 151.551-158.556 | $=0.9$ |
|  | 70 | 155.200-192.563 | 156.161-188.653 | 164.045-175.324 |  |
|  | 75 | 171.349-206.852 | 173.607-205.574 | 187.173-200.277 |  |
|  | 80 | 198.220-242.277 | 199.984-234.193 | 205.436-212.178 |  |
|  | 85 | 210.744-284.483 | 214.539-274.050 | 235.574-256.687 |  |
|  | 90 | 258.763-337.465 | 267.688-334.389 | 296.412-312.170 |  |
|  | 95 | 335.039-385.759 | 337.590-383.297 | 359.275-380.496 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=100.481$ | 5 | 20.348-24.669 | 20.554-24.165 | 21.252-22.675 | WATER FLUX = |
|  | 10 | 24.310-28.079 | 24.718-27.847 | 25.585-27.249 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 27.393-34.217 | 27.550-33.900 | 28.521-31.995 |  |
|  | 20 | 31.885-40.269 | 32.112-39.318 | 34.098-37.269 |  |
|  | 25 | 36.524-43.488 | 37.181-43.084 | 39.190-41.751 |  |
| STD. DEV. = | 30 | 40.704-47.920 | 41.221-47.245 | 42.754-45.277 | FALL DISTANCE $=$ |
| $=79.472$ | 35 | 43.930-56.304 | 44.504-54.430 | 46.504-49.215 | $=2000 \mathrm{~cm}$ |
|  | 40 | 48.081-61.926 | 48.715-61.407 | 51.343-57.862 |  |
|  | 45 | 56.130-78.423 | 56.734-75.454 | 59.705-67.338 |  |
|  | 50 | 61.790-88.673 | 62.933-86.165 | 70.160-79.865 |  |
| SAMPLE SIZE $=$ | 55 | 77.902-101.702 | 78.898-97.781 | 84.432-92.463 |  |
| $=360$ | 60 | 88.099-113.198 | 90.136-111.186 | 94.528-105.790 | FRACTION REMAINING $=$ |
|  | 65 | 101.674-128.822 | 103.010-125.460 | 109.670-118.338 | $=0.5$ |
|  | 70 | 113.502-140.933 | 114.541-139.502 | 123.037-134.802 |  |
|  | 75 | 131.442-153.733 | 133.382-151.175 | 138.950-144.456 |  |
|  | 80 | 143.013-175.551 | 144.276-172.254 | 150.923-161.973 |  |
|  | 85 | 161.644-199.430 | 162.549-195.044 | 174.781-184.096 |  |
|  | 90 | 189.058-234.317 | 189.821-231.738 | 202.890-219.964 |  |
|  | 95 | 232.332-292.814 | 234.391-290.224 | 240.539-261.221 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=81.733$ | 5 | 15.924-19.965 | 16.145-19.833 | 17.492-19.376 | $\begin{aligned} & \text { WATER FLUX = } \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 19.837-23.564 | 19.975-23.439 | 21.119-22.267 |  |
|  | 15 | 22.370-26.955 | 22.728-26.765 | 23.942-25.040 |  |
|  | 20 | 24.935-33.134 | 25.098-32.327 | 26.888-29.721 |  |
|  | 25 | 28.469-36.580 | 29.204-36.338 | 32.312 - 35.003 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =63.308 \end{aligned}$ | 30 | 33.727-40.224 | 34.586-39.415 | 35.974-37.829 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =2000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 36.927-44.124 | 37.101-43.696 | 39.192-41.430 |  |
|  | 40 | 40.484-52.180 | 40.872-50.208 | 43.190-45.243 |  |
|  | 45 | 44.055-62.639 | 44.467-59.756 | 48.727-55.559 |  |
|  | 50 | 52.032-71.232 | 52.764-70.736 | 58.499-65.342 |  |
| $\begin{aligned} & \text { SAMPLE SIZE = } \\ & =360 \end{aligned}$ | 55 | 62.503-80.295 | 64.385-78.012 | 67.255-75.152 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | 71.138-94.536 | 71.992-93.156 | 76.727-84.300. |  |
|  | 65 | 79.704-106.130 | 81.470-104.677 | 88.849-101.069 |  |
|  | 70 | 94.863-113.242 | 96.819-112.335 | 102.705-109.529 |  |
|  | 75 | 108.247-123.268 | 108.963-120.974 | 111.825-116.893 |  |
|  | 80 | 115.134-145.642 | 116.737-142.362 | 120.783-134.926 |  |
|  | 85 | 133.954-167.696 | 135.569-166.260 | 143.507-161.106 |  |
|  | 90 | 164.046-186.569 | 164.554-185.425 | 168.389-176.400 |  |
|  | 95 | 186.021-235.147 | 186.665-226.068 | 198.217-210.870 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=58.349$ | 5 | 10.510-14.228 | 10.610-14.088 | 11.341-12.608 | WATER FLUX = |
|  | 10 | 14.115-16.220 | 14.256-16.199 | 15.271-15.936 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 16.036-18.917 | 16.091-18.728 | 16.342-17.260 |  |
|  | 20 | 17.254-22.825 | 17.351-22.307 | 18.855-20.800 |  |
|  | 25 | 20.278-25.513 | 20.670-25.194 | 22.242-23.459 |  |
| STD. DEV. $=$ | 30 | 23.196-28.885 | 23.382-28.649 | 24.482-27.054 | FALL DISTANCE $=$ |
| $=45.447$ | 35 | 25.728-32.563 | 26.414-32.216 | 28.445-30.400 | $=2000 \mathrm{~cm}$ |
|  | 40 | 29.109-36.976 | 29.831-35.787 | 31.812-34.331 |  |
|  | 45 | 32.484-44.808 | 33.140-44.043 | 34.899-38.106 |  |
|  | 50 | 36.810-48.731 | 37.290-48.267 | 41.186-45.819 |  |
| SAMPLE SIZE = | 55 | 44.436-57.298 | 45.128-56.126 | 47.251-51.812 | AEROSOL MASS |
| $=360$ | 60 | 48.662-66.783 | 49.872-64.749 | 53.236-59.928 | FRACTION REMAINING = |
|  | 65 | 57.221-74.235 | 57.997-73.628 | 62.699-70.290 | $=0.1$ |
|  | 70 | 67.190-83.512 | 68.407-80.927 | 71.587-77.821 |  |
|  | 75 | 74.698-90.455 | 76.506-88.919 | 80.624-86.005 |  |
|  | 80 | 84.664-101.637 | 85.893-101.181 | 88.747-94.547 |  |
|  | 85 | 93.308-121.907 | 95.239-119.688 | 101.536-107.566 |  |
|  | 90 | 108.197-139.155 | 112.953-136.156 | 122.796-131.790 |  |
|  | 95 | 136.640-170.955 | 139.315-169.063 | 146.854-157.433 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=37.092$ | 5 | 5.751-7.634 | 5.769-7.417 | 6.093-7.241 | WATER FLUX = |
|  | 10 | 7.420-10.151 | 7.663-9.965 | 8.692-9.324 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 9.363-11.634 | 9.590-11.453 | 10.360-10.870 |  |
|  | 20 | 10.805-13.162 | 10.933-12.976 | 11.574-12.311 |  |
|  | 25 | 12.130-15.343 | 12.310-15.193 | 12.960-13.959 |  |
| STD. DEV. = | 30 | 13.748-17.719 | 13.919-17.329 | 15.102-16.232 | FALL DISTANCE = |
| $=38.781$ | 35 | 15.518-20.540 | 16.057-20.283 | 16.701-18.621 | $=2000 \mathrm{~cm}$ |
|  | 40 | 17.814-23.574 | 18.195-23.465 | 19.740-21.566 |  |
|  | 45 | 20.498-27.223 | 20.693-27.039 | 23.335-24.748 |  |
|  | 50 | 23.506-29.803 | 23.802-29.499 | 25.847-28.431 |  |
| SAMPLE SIZE = | 55 | 27.209-35.304 | 27.334-34.693 | 29.216-31.549 | AEROSOL MASS |
| $=360$ | 60 | 29.740-40.219 | 30.638-39.733 | 32.540-37.230 | FRACTION REMAINING $=$ |
|  | 65 | 35.213-45.476 | 35.960-45.503 | 38.690-42.216 | $=0.01$ |
|  | 70 | 40.433-51.835 | 41.712-50.539 | 43.760-47.745 |  |
|  | 75 | 46.327-58.663 | 47.322-58.310 | 50.300-55.124 |  |
|  | 80 | 53.670-64.211 | 55.053-63.010 | 58.110-61.929 |  |
|  | 85 | 61.823-75.509 | 61.962-74.202 | 63.506-68.860 |  |
|  | 90 | 69.134-90.752 | 70.545-89.629 | 77.125-83.051 |  |
|  | 95 | 89.710-119.026 | 90.856-115.154 | 97.997-105.418 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=28.911$ | 5 | 4.364-5.821 | 4.440-5.687 | 4.707-5.328 | WATER FLUX = |
|  | 10 | 5.688-7.601 | 5.914-7.548 | 6.251-6.976 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 7.080-8.644 | 7.244-8.472 | 7.662-8.225 |  |
|  | 20 | 8.219-9.972 | 8.334-9.841 | 8.560-9.658 |  |
|  | 25 | 9.340-11.665 | 9.628-11.543 | 9.832-10.600 |  |
| STD. DEV. = | 30 | 10.152-13.477 | 10.466-13.142 | 11.472-12.328 | FALL DISTANCE = |
| $=24.850$ | 35 | 11.796-16.057 | 12.058-15.330 | 13.009-14.197 | $=2000 \mathrm{~cm}$ |
|  | 40 | 13.509-18.114 | 13.914-17.828 | 14.937-16.427 |  |
|  | 45 | 16.022-21.074 | 16.223-20.602 | 17.240-19.438 |  |
|  | 50 | 18.074-23.472 | 18.586-23.202 | 20.030-21.962 |  |
| SAMPLE SIZE = | 55 | 20.783-27.567 | 21.339-27.323 | 22.978-24.794 | AEROSOL MASS |
| $=360$ | 60 | 23.406-30.228 | 23.939-29.555 | 26.309-27.858 | FRACTION REMAINING $=$ |
|  | 65 | 27.542-35.387 | 27.693-34.808 | 29.083-32.837 | $=0.001$ |
|  | 70 | 30.383-39.026 | 32.034-38.433 | 34.312-36.776 |  |
|  | 75 | 35.408-46.003 | 36.243-45.070 | 38.233-42.406 |  |
|  | 80 | 41.672-50.498 | 42.291-50.220 | 44.845-48.147 |  |
|  | 85 | $47.469-57.820$ | 48.596-56.677 | 50.292-52.897 |  |
|  | 90 | 53.350-70.940 | 54.451-70.048 | 58.241-65.364 |  |
|  | 95 | 70.195-97.750 | 71.024-92.745 | 73.788-86.074 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=127.946$ | 5 | 20.269-25.222 | 20.434-25.018 | 22.507-23.518 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 25.022-31.567 | 25.222-30.337 | 25.916-27.639 |  |
|  | 15 | 28.515-36.253 | 29.768-35.782 | 32.964-35.182 |  |
|  | 20 | 35.075-42.786 | 35.340-41.442 | 36.142-39.007 |  |
|  | 25 | 38.058-47.376 | 38.748-46.374 | 41.339-44.457 |  |
| $\begin{aligned} & \text { STD. DEV. = } \\ & =113.145 \end{aligned}$ | 30 | 43.540-53.330 | 44.274-52.233 | 46.109-50.893 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =3000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 48.028-61.314 | 49.869-60.050 | 51.702-55.166 |  |
|  | 40 | 53.812-75.033 | 54.467-72.610 | 58.453-65.236 |  |
|  | 45 | 60.887-88.602 | 62.978-85.859 | 69.440-79.403 |  |
|  | 50 | 74.487-108.078 | 75.466-105.661 | 83.989-91.291 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 86.393-124.552 | 89.002-120.634 | 98.691-111.947 | AEROSOL MASS <br> FRACTION REMAINING = $=0.9$ |
|  | 60 | 107.992-147.445 | 110.002-143.102 | 117.789-129.400 |  |
|  | 65 | 123.688-163.819 | 126.502-158.211 | 138.248-152.262 |  |
|  | 70 | 148.689-186.046 | 150.731-182.390 | 156.086-168.946 |  |
|  | 75 | 164.682-200.625 | 167.326-198.810 | 178.999-194.495 |  |
|  | 80 | 191.794-227.748 | 194.207-221.810 | 198.566-206.242 |  |
|  | 85 | 206.195-265.244 | 208.234-261.649 | 227.208-248.127 |  |
|  | 90 | 251.526-320.789 | 252.802-313.652 | 265.430-299.166 |  |
|  | 95 | 315.454-379.618 | 321.183-378.013 | 339.548-374.872 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=93.042$ | 5 | 16.317-19.925 | 16.549-19.761 | 17.284-19.142 | WATER FLUX = |
|  | 10 | 19.780-22.223 | 19.983-21.942 | 20.589-21.629 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 21.790-28.334 | 21.851-27.385 | 22.708-25.081 |  |
|  | 20 | 25.052-32.368 | 25.331-32.102 | 27.917-30.562 |  |
|  | 25 | 29.958-35.505 | 30.547-35.093 | 32.077-33.809 |  |
| STD. DEV. = | 30 | 32.935-38.921 | 33.274-38.397 | 34.909-36.422 | FALL DISTANCE = |
| $=78.683$ | 35 | 35.840-46.295 | 36.009-45.656 | 37.581-41.955 | $=3000 \mathrm{~cm}$ |
|  | 40 | 39.115-53.841 | 40.060-51.957 | 43.975-48.140 |  |
|  | 45 | 46.251-64.528 | 47.020-63.003 | 49.457-57.316 |  |
|  | 50 | 53.239-75.914 | 55.595-74.112 | 60.442-68.414 |  |
| SAMPLE SIZE = | 55 | 63.646-92.262 | 66.048-90.421 | 71.655-78.987 | AEROSOL MASS |
| $=360$ | 60 | 75.696-109.874 | 76.472-108.161 | 88.074-100.351 | FRACTION REMAINING $=$ |
|  | 65 | 91.904-123.917 | 97.752-121.612 | 104.983-114.963 | $=0.5$ |
|  | 70 | 110.246-136.320 | 112.283-135.312 | 120.225-130.164 |  |
|  | 75 | 124.966-148.539 | 127.233-145.480 | 134.862-139.627 |  |
|  | 80 | 138.014-169.034 | 139.480-167.576 | 144.687-156.527 |  |
|  | 85 | 155.902-191.954 | 157.156-187.062 | 168.327-179.418 |  |
|  | 90 | 180.844-225.762 | 182.912-223.418 | 194.647-210.685 |  |
|  | 95 | 223.937-280.110 | 225.864-260.022 | 232.343-250.353 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=75.662$ | 5 | 12.662-15.970 | 13.211-15.832 | 14.327-15.499 | WATER FLUX = |
|  | 10 | 15.838-18.987 | 16.038-18.707 | 16.576-18.070 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 18.475-21.732 | 18.527-21.275 | 19.455-20.316 |  |
|  | 20 | 20.118-26.326 | 20.491-25.916 | 21.690-24.822 |  |
|  | 25 | 23.983-29.459 | 24.770-28.711 | 25.852-27.829 |  |
| STD. DEV. $=$ | 30 | 27.510-32.177 | 27.787-31.845 | 28.590-30.389 | FALL DISTANCE = |
| $=62.616$ | 35 | 29.678-37.249 | 30.192-35.840 | 31.703-33.634 | $=3000 \mathrm{~cm}$ |
|  | 40 | 32.232-43.943 | 32.931-43.450 | 35.116-39.166 |  |
|  | 45 | 37.162-52.596 | 37.837-51.470 | 41.791-46.029 |  |
|  | 50 | 43.881-62.906 | 44.806-59.950 | 48.749-55.514 |  |
| SAMPLE SIZE = | 55 | 51.707-75.165 | 53.217-74.459 | 57.401-65.529 | AEROSOL MASS |
| $=360$ | 60 | 61.003-91.841 | 63.843-87.939 | 69.448-78.536 | FRACTION REMAINING $=$ |
|  | 65 | 75.113-102.150 | 76.219-100.970 | 87.031-95.301 | $=0.3$ |
|  | 70 | 92.322-110.987 | 93.263-109.320 | 100.466-105.284 |  |
|  | 75 | 103.305-118.767 | 104.909-117.738 | 108.177-112.793 |  |
|  | 80 | 111.823-138.651 | 112.658-134.945 | 117.289-128.343 |  |
|  | 85 | 124.472-161.563 | 131.128-159.624 | 138.423-149.748 |  |
|  | 90 | 155.721-179.821 | 157.956-175.482 | 162.124-169.173 |  |
|  | 95 | 176.285-219.081 | 179.909-214.195 | 191.848-203.475 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=54.005$ | 5 | 8.740-11.330 | 8.861-11.200 | 8.977-9.960 | WATER FLUX = |
|  | 10 | 11.219-13.025 | 11.376-13.019 | 12.306-12.599 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 12.677-15.827 | 12.905-15.459 | 13.098-14.734 |  |
|  | 20 | 14.323-17.823 | 14.883-17.425 | 15.734-16.701 |  |
|  | 25 | 16.395-20.781 | 16.698-19.782 | 17.366-18.674 |  |
| STD. DEV. $=$ | 30 | 18.185-23.593 | 18.464-23.224 | 19.638-21.950 | FALL DISTANCE $=$ |
| $=44.748$ | 35 | 21.014-26.491 | 21.503-26.351 | 22.896-25.100 | $=3000 \mathrm{~cm}$ |
|  | 40 | 23.628-30.625 | 24.400-30.025 | 25.655-27.792 |  |
|  | 45 | 26.477-37.741 | 26.609-36.550 | 29.152-35.208 |  |
|  | 50 | 30.466-43.556 | $31.547-43.076$ | 36.021-38.510 |  |
| SAMPLE SIZE = | 55 | 37.511-51.675 | 37.829-50.265 | 41.151-46.302 |  |
| $=360$ | 60 | $43.389-64.281$ | $44.431-61.619$ | $49.956-56.138$ | FRACTION REMAINING $=$ |
|  | 65 | $51.609-72.585$ | $54.595-71.003$ | $60.928-67.971$ |  |
|  | 70 | 64.685-80.755 | 66.562-78.536 | 69.795-74.971 |  |
|  | 75 | 72.909-87.684 | $73.646-86.817$ | 77.802-83.298 |  |
|  | 80 | 82.261-99.123 | 83.140-97.797 | 86.665-90.178 |  |
|  | 85 | 90.000-118.415 | 92.047-113.183 | 98.103-103.663 |  |
|  | 90 | 104.247-132.710 | 105.802-130.606 | 118.470-126.531 |  |
|  | 95 | 130.853-166.218 | 133.108-164.719 | 140.626-154.134 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=34.326$ | 5 | 4.625-6.246 | 4.696-6.166 | 5.040-5.829 | WATER FLUX = |
|  | 10 | 6.178-8.276 | 6.333-8.045 | 6.960-7.577 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 7.616-9.246 | 7.900-9.129 | $8.373-8.758$ |  |
|  | 20 | 8.750-10.492 | 8.771 - 10.280 | 9.193-9.861 |  |
|  | 25 | 9.743-12.618 | 9.845-12.061 | 10.275-11.416 |  |
| STD. DEV. $=$ | 30 | 10.986-14.447 | 11.228-13.932 | $11.776-13.125$ | $\text { FALL DISTANCE }=$ |
| $=30.054$ | 35 | 12.727-16.475 | 12.914-16.159 | $13.562-15.259$ | $=3000 \mathrm{~cm}$ |
|  | 40 | 14.513-20.026 | 14.733-19.790 | 16.058-18.570 |  |
|  | 45 | 16.436-23.019 | 17.897-22.861 | 19.295-20.973 |  |
|  | 50 | 19.898-28.279 | 20.493-27.082 | 22.498-23.609 |  |
| SAMPLE SIZE $=$ | 55 | 22.924-33.076 | 23.312-31.990 | 25.549-29.099 | AEROSOL MASS |
| $=360$ | 60 | 28.198-38.545 | 28.620-38.138 | 30.979-34.142 | FRACTION REMAINING $=$ |
|  | 65 | 32.883-43.983 | 33.614-42.579 | 36.402-39.891 | $=0.01$ |
|  | 70 | 38.628-49.756 | 39.080-49.232 | 42.114-46.076 |  |
|  | 75 | 44.457-56.832 | 45.617-56.254 | 48.454-52.390 |  |
|  | 80 | 51.464-62.291 | 52.274-61.204 | 55.969-59.558 |  |
|  | 85 | 59.319-71.641 | 59.634-69.932 | 61.462-65.921 |  |
|  | 90 | 66.527-88.076 | 67.533-87.285 | 72.606-81.688 |  |
|  | 95 | 87.424-111.321 | 88.276-110.512 | 95.021-100.560 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=26.827$ | 5 | 3.488-4.855 | 3.513-4.830 | 3.847-4.374 | WATER FLUX = |
|  | 10 | 4.831-6.065 | 4.868-5.990 | 4.994-5.614 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 5.675-6.837 | $5.831-6.776$ | 6.144-6.648 |  |
|  | 20 | 6.622-7.988 | 6.697-7.905 | 6.787-7.595 |  |
|  | 25 | 7.464-9.442 | 7.590-9.274 | 7.902-8.432 |  |
| STD. DEV. = | 30 | 8.125-11.201 | 8.369-10.758 | 9.180-10.228 | FALL DISTANCE = |
| $=24.287$ | 35 | 9.627-12.776 | 9.851-12.458 | 10.554-11.881 | $=3000 \mathrm{~cm}$ |
|  | 40 | 11.247-15.814 | 11.437-15.432 | 12.140-13.881 |  |
|  | 45 | 12.751-17.590 | 12.977-17.180 | 14.870-16.206 |  |
|  | 50 | 15.673-22.155 | 15.936-21.247 | 16.882-18.893 |  |
| SAMPLE SIZE = | 55 | 17.485-26.200 | 17.897-25.598 | 19.972-22.708 | AEROSOL MASS |
| $=360$ | 60 | 22.004-28.590 | 22.256-28.157 | 24.861-26.844 | FRACTION REMAINING $=$ |
|  | 65 | 26.074-34.013 | 26.590-33.611 | 27.361-29.887 | $=0.001$ |
|  | 70 | 28.663-37.514 | 29.124-37.101 | 33.010-35.298 |  |
|  | 75 | 34.210-44.502 | 34.462-42.903 | 36.763-40.446 |  |
|  | 80 | 39.985-49.242 | 40.410-48.681 | 42.871-46.394 |  |
|  | 85 | 45.901-55.683 | 46.789-53.416 | 49.150-51.431 |  |
|  | 90 | 51.576-69.427 | 52.521-68.300 | 56.263-64.698 |  |
|  | 95 | 68.626-89.916 | 69.579-87.932 | 73.075-82.446 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=121.583$ | 5 | 17.110-21.362 | 18.467-21.310 | 18.965-20.058 | WATER FLUX = |
|  | 10 | 21.326-26.431 | 21.484-26.221 | 22.012-23.844 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 24.317-30.580 | 24.936-30.119 | 27.406-29:281 |  |
|  | 20 | 29.110-36.233 | 29.396-35.825 | 30.302-32.527 |  |
|  | 25 | 31.647-40.175 | 32.459-39.317 | 35.730-38.134 |  |
| STD. DEV. = | 30 | 37.139-46.390 | 37.701-45.978 | 39.105-42.987 | FALL DISTANCE = |
| $=112.669$ | 35 | 41.067-54.474 | 42.413-52.936 | 45.075-50.098 | $=4000 \mathrm{~cm}$ |
|  | 40 | 46.467-63.760 | 48.255-62.401 | 52.479-58.036 |  |
|  | 45 | 54.456-78.114 | 54.650-75.539 | 61.388-69.596 |  |
|  | 50 | 63.533-93.959 | 66.476-91.227 | 73.854-84.354 |  |
| SAMPLE SIZE = | 55 | 77.166-118.278 | 80.536-112.428 | 89.081-99.369 | AEROSOL MASS |
| $=360$ | 60 | 92.047-142.269 | 96.927-138.797 | 107.289-126.110 | FRACTION REMAINING = |
|  | 65 | 116.725-156.302 | 121.716-154.732 | 134.828-148.200 | $=0.90$ |
|  | 70 | 143.660-180.503 | 146.749-177.559 | 151.774-165.533 |  |
|  | 75 | 161.123-196.436 | 164.383-195.699 | 169.703-190.874 |  |
|  | 80 | 185.750-218.415 | 190.552-218.320 | 195.689-204.253 |  |
|  | 85 | 204.098-257.822 | 204.528-251.936 | 218.409-237.296 |  |
|  | 90 | 244.619-316.002 | 248.930-309.229 | 258.594-293.299 |  |
|  | 95 | 312.595-376.437 | 316.208-373.027 | 335.504-369.839 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=88.344$ | 5 | 13.796-17.018 | 14.126-16.824 | 14.765-16.028 | WATER FLUX = |
|  | 10 | 16.828-19.150 | 17.068-18.748 | 17.709-18.180 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 18.333-23.823 | 18.499-23.178 | 19.497-21.029 |  |
|  | 20 | 20.830-27.233 | 21.413-27.105 | 23.672-25.552 |  |
|  | 25 | 25.187-30.596 | 25.511-30.139 | 27.086-28.834 |  |
| STD. DEV. = | 30 | 28.066-32.843 | 28.756-32.432 | 29.786-31.016 | FALL DISTANCE $=$ |
| $=78.240$ | 35 | 30.627-40.111 | 30.892-39.421 | 32.202-36.192 | $=4000 \mathrm{~cm}$ |
|  | 40 | 33.213-48.036 | 34.749-47.032 | 38.352-41.918 |  |
|  | 45 | 40.087-57.096 | 40.871-55.347 | 44.447-51.528 |  |
|  | 50 | 47.914-68.062 | 48.304-64.796 | 53.575-59.184 |  |
| SAMPLE SIZE $=$ | 55 | 56.509-89.731 | 58.097-88.050 | 61.775-75.123 | AEROSOL MASS |
| $=360$ | 60 | 65.787-107.340 | 72.288-103.724 | 82.961-98.385 | FRACTION REMAINING $=$ |
|  | 65 | 89.446-120.641 | 93.553-118.302 | 101.493-110.677 | $=0.5$ |
|  | 70 | 107.608-133.334 | 108.430-132.095 | 116.680-125.499 |  |
|  | 75 | 122.291-144.573 | 123.770-141.384 | 131.594-136.325 |  |
|  | 80 | 134.884-165.392 | 136.300-162.862 | 141.319-152.384 |  |
|  | 85 | 151.784-188.331 | 153.100-183.196 | 164.068-175.468 |  |
|  | 90 | 178.407-218.444 | 180.940-216.779 | 190.577-206.531 |  |
|  | 95 | 217.017-272.680 | 218.653-253.195 | 226.735-244.030 |  |



|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=51.263$ | 5 | 7.395-9.728 | 7.512-9.463 | 7.830-8.587 | WATER FLUX $=$ |
|  | 10 | 9.484-11.028 | 9.753-10.985 | 10.210-10.761 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 10.827-13.539 | 10.893-13.245 | 11.143-12.555 |  |
|  | 20 | 12.376-15.170 | 12.584-14.936 | 13.400-14.097 |  |
|  | 25 | 13.898-17.434 | 14.093-16.828 | 14.895-16.157 |  |
| STD. DEV. = | 30 | 15.613-20.179 | 15.872-19.438 | 16.544-18.531 | FALL DISTANCE = |
| $=44.386$ | 35 | 17.825-22.773 | 18.169-22.230 | 19.178-21.056 | $=4000 \mathrm{~cm}$ |
|  | 40 | 20.327-28.686 | 20.956-26.404 | 21.882-23.683 |  |
|  | 45 | 22.647-32.763 | 23.204-31.922 | 25.180-30.019 |  |
|  | 50 | 28.369-41.417 | 29.301-39.688 | 31.066-36.164 |  |
| SAMPLE SIZE = | 55 | 32.199-49.935 | 34.215-48.801 | 37.685-43.108 | AEROSOL MASS |
| $=360$ | 60 | 40.653-62.709 | 42.139-60.409 | 46.339-54.935 | FRACTION REMAINING $=$ |
|  | 65 | 49.679-71.516 | 52.326-69.789 | 58.793-66.110 | $=0.1$ |
|  | 70 | 62.893-78.767 | 65.661-76.380 | 68.217-72.862 |  |
|  | 75 | 71.911-85.730 | 72.250-84.707 | 75.686-81.286 |  |
|  | 80 | 80.500-96.517 | 81.259-95.092 | 84.214-88.152 |  |
|  | 85 | 87.900-115.839 | 89.659-105.488 | 95.718-100.197 |  |
|  | 90 | 100.866-129.603 | 101.459-127.837 | 116.581-123.334 |  |
|  | 95 | 128.367-160.745 | 129.915-154.115 | 136.910-150.322 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=32.570$ | 5 | 3.963-5.625 | 4.071-5.368 | 4.474-4.944 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 5.397-6.877 | 5.628-6.798 | 5.885-6.449 |  |
|  | 15 | 6.535-7.853 | 6.662-7.767 | 7.097-7.421 |  |
|  | 20 | 7.377-8.941 | 7.427-8.796 | 7.829-8.411 |  |
|  | 25 | 8.274-10.650 | 8.410-10.263 | 8.781-9.618 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =29.665 \end{aligned}$ | 30 | 9.330-12.384 | 9.501-12.156 | 10.146-11.060 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =4000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 10.746-14.915 | 10.899-13.901 | 11.918-13.146 |  |
|  | 40 | 12.443-17.280 | 12.725-16.813 | 13.442-15.945 |  |
|  | 45 | 14.894-20.787 | 15.253-19.883 | 16.161-18.934 |  |
|  | 50 | 17.230-26.707 | 17.325-24.867 | 19.421-22.569 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =360 \end{aligned}$ | 55 | 20.542-31.053 | 21.287-30.344 | 23.501-27.955 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 26.483-37.689 | 27.677-36.119 | 29.016-32.976 |  |
|  | 65 | 30.956-42.788 | 32.075-41.341 | 35.272-39.014 |  |
|  | 70 | 37.873-48.662 | 38.234-47.517 | 40.758-44.858 |  |
|  | 75 | 43.581-55.436 | 44.429-54.729 | 47.105-51.390 |  |
|  | 80 | 50.152-59.784 | 51.281-58.987 | 54.720-56.561 |  |
|  | 85 | 56.176-69.757 | 57.860-67.969 | 59.679-63.909 |  |
|  | 90 | 65.146-85.745 | 66.120-85.082 | 71.017-79.712 |  |
|  | 95 | 85.590-107.627 | 85.797-104.675 | 91.038-99.629 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=25.485$ | 5 | 2.962-4.130 | 3.018-4.111 | 3.282-3.703 | WATER FLUX = |
|  | 10 | 4.114-5.114 | 4.152-5.050 | 4.452-4.793 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{3}$ |
|  | 15 | 4.818-6.104 | 4.882-5.843 | 5.312-5.599 |  |
|  | 20 | 5.597-6.752 | 5.672-6.671 | 6.030-6.352 |  |
|  | 25 | 6.323-7.991 | 6.348-7.807 | 6.663-7.188 |  |
| STD. DEV. $=$ | 30 | 6.914-9.544 | 6.997-9.395 | 7.737-8.646 | FALL DISTANCE $=$ |
| $=23.997$ | 35 | 8.080-11.131 | 8.498-10.728 | 9.121-10.023 | $=4000 \mathrm{~cm}$ |
|  | 40 | 9.571-13.539 | 9.682-13.205 | 10.429-12.180 |  |
|  | 45 | 10.990-16.119 | 11.609-15.786 | 12.674-14.248 |  |
|  | 50 | 13.502-20.758 | 13.944-19.811 | 14.826-16.922 |  |
| SAMPLE SIZE = | 55 | 15.802-24.900 | 16.386-23.636 | 18.470-22.020 | AEROSOL MASS |
| $=360$ | 60 | 20.667-28.106 | 21.317-27.170 | 22.943-25.985 | FRACTION REMAINING $=$ |
|  | 65 | 24.800-33.062 | 25.439-32.693 | 26.815-28.960 | $=0.001$ |
|  | 70 | 28.328-36.488 | 28.659-36.119 | 32.193-33.870 |  |
|  | 75 | 33.343-42.049 | 33.768-41.824 | 35.771-39.710 |  |
|  | 80 | 37.984-47.926 | 39.654-46.548 | 41.796-44.711 |  |
|  | 85 | 44.645-54.265 | 45.175-52.297 | 47.173-50.138 |  |
|  | 90 | 50.761-67.258 | 51.447-66.678 | 55.233-63.352 |  |
|  | 95 | 67.106-87.555 | 67.297-85.633 | 70.870-80.704 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=117.276$ | 5 | 15.827-18.894 | 16.171-18.695 | 16.584-17.596 | WATER FLUX = |
|  | 10 | 18.695-23.706 | 18.934-23.316 | 19.500-20.926 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 21.270-26.644 | 21.942-26.255 | 23.840-25.403 |  |
|  | 20 | 25.329-31.694 | 25.562-31.041 | 26.411-28.012 |  |
|  | 25 | 27.381-35.635 | 27.942-34.445 | 30.920-33.126 |  |
| STD. DEV. $=$ | 30 | 32.416-40.724 | 33.051-40.308 | 34.297-37.753 | FALL DISTANCE $=$ |
| $=112.495$ | 35 | 36.229-50.739 | 36.717-48.316 | 39.715-45.003 | $=5000 \mathrm{~cm}$ |
|  | 40 | 41.065-58.636 | 43.086-55.159 | 46.718-53.096 |  |
|  | 45 | 50.445-73.263 | 51.379-66.686 | 54.137-62.323 |  |
|  | 50 | 57.498-85.878 | 59.796-83.549 | 65.440-76.867 |  |
| SAMPLE SIZE $=$ | 55 | 70.859-111.450 | 75.478-110.107 | 80.719-90.732 | AEROSOL MASS |
| $=360$ | 60 | 85.297-140.614 | 89.074-136.918 | 104.312-124.289 | FRACTION REMAINING $=$ |
|  | 65 | 111.052-153.373 | 118.476-151.297 | 131.001-145.253 | $=0.9$ |
|  | 70 | 141.708-177.634 | 143.808-174.684 | 150.075-162.316 |  |
|  | 75 | 155.044-194.749 | 161.110-193.796 | 171.123-187.663 |  |
|  | 80 | 182.978-215.985 | 187.404-213.862 | 192.905-202.119 |  |
|  | 85 | 201.781-252.796 | 202.710-248.316 | 214.297-234.484 |  |
|  | 90 | 240.261-312.396 | 246.726-305.904 | 253.568-288.417 |  |
|  | 95 | 310.479-373.957 | 312.440-370.694 | 332.524-365.953 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=85.048$ | 5 | 12.004-14.877 | 12.421-14.867 | 12.827-14.535 | WATER FLUX = |
|  | 10 | 14.870-16.687 | 14.957-16.499 | 15.388-15.957 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 16.046-20.788 | 16.219-20.372 | 17.173-18.541 |  |
|  | 20 | 18.242-23.732 | 19.429-23.460 | 20.712-22.204 |  |
|  | 25 | 22.011-26.739 | 22.137-26.278 | 23.438-25.136 |  |
| STD. DEV. = | 30 | 24.637-29.987 | 24.906-28.381 | 26.217-27.192 | FALL DISTANCE $=$ |
| $=77.924$ | 35 | 26.873-35.810 | 26.970-34.873 | 28.311-31.634 | $=5000 \mathrm{~cm}$ |
|  | 40 | 30.347-44.288 | 31.331-42.635 | 33.636-37.497 |  |
|  | 45 | 35.806-51.748 | 36.151 - 50.599 | 40.608-46.735 |  |
|  | 50 | 43.134-64.358 | 45.241-58.793 | 47.699-53.529 |  |
| SAMPLE SIZE $=$ | 55 | 51.456-87.873 | 52.364-86.221 | 56.277-72.335 | AEROSOL MASS |
| $=360$ | 60 | 63.169-105.737 | - 67.742-101.931 | 82.087-94.938 | FRACTION REMAINING $=$ |
|  | 65 | 87.850-118.466 | 88.817-115.798 | 99.421-108.027 | $=0.5$ |
|  | 70 | 105.899-131.543 | 107.088-130.459 | 114.446-123.236 |  |
|  | 75 | 120.238-140.954 | 120.683-139.522 | 128.990-133.755 |  |
|  | 80 | 131.956-162.562 | 133.660-160.143 | 139.250-149.273 |  |
|  | 85 | 148.795-183.438 | 150.205-179.680 | 161.972-172.105 |  |
|  | 90 | 174.598-213.963 | 177.006-212.539 | 186.432-203.207 |  |
|  | 95 | 212.878-267.069 | 214.180-249.686 | 223.813-239.079 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=69.150$ | 5 | 9.640-11.767 | 10.032-11.678 | 10.830-11.400 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 11.680-14.151 | 11.835-13.796 | 12.664-13.225 |  |
|  | 15 | 13.378-16.118 | 13.667-15.605 | 14.496-15.053 |  |
|  | 20 | 14.963-19.762 | 15.079-19.361 | 16.009 - 18.505 |  |
|  | 25 | 18.369-21.998 | 18.499-21.668 | 19.346-20.717 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =61.996 \end{aligned}$ | 30 | 20.129-23.851 | 20.579-23.555 | 21.583-22.802 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =5000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 22.201-28.507 | 22.482-27.790 | 23.454-25.314 |  |
|  | 40 | 23.959-34.981 | 24.553-33.902 | 26.426-31.074 |  |
|  | 45 | 28.203-42.082 | 29.393-41.165 | 32.823-38.190 |  |
|  | 50 | 34.397-54.440 | 37.329-50.247 | 39.577-43.410 |  |
| $\begin{aligned} & \text { SAMPLE SIZE = } \\ & =360 \end{aligned}$ | 55 | 41.858-71.636 | 42.558-69.443 | 45.367-62.353 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.3$ |
|  | 60 | 53.775-87.913 | 55.455-85.550 | 64.842-74.312 |  |
|  | 65 | 71.595-99.352 | 72.623-98.131 | 82.285-91.961 |  |
|  | 70 | 88.450-106.087 | 90.329-105.044 | 97.443-100.238 |  |
|  | 75 | 99.647-113.395 | 100.190-111.662 | 104.592-108.981 |  |
|  | 80 | 108.431-132.318 | 108.965-129.782 | 111.474-118.335 |  |
|  | 85 | 117.825-154.205 | 119.835-153.388 | 130.067-147.310 |  |
|  | 90 | 148.595-170.289 | 151.242-168.371 | 154.331-162.141 |  |
|  | 95 | 168.518-209.498 | 170.469-207.313 | 182.325-192.519 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| $\mathrm{MEAN}=49.175$ | 5 | 6.460-8.518 | 6.548-8.380 | 6.945-7.491 | WATER FLUX = |
|  | 10 | 8.397-9.688 | 8.521-9.652 | 8.928-9.447 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 9.478-11.790 | 9.588-11.632 | 9.798-10.964 |  |
|  | 20 | 10.794-13.238 | 11.012-13.111 | $11.766-12.418$ |  |
|  | 25 | 12.155-15.602 | 12.341-15.440 | 13.080-14.115 |  |
| STD. DEV. = | 30 | 13.628-17.757 | 13.912-16.846 | 15.171-16.432 | FALL DISTANCE = |
| $=43.776$ | 35 | 16.055-19.829 | 16.251-19.310 | 16.697-18.337 | $=5000 \mathrm{~cm}$ |
|  | 40 | 17.846-25.384 | 18.094-23.355 | 18.877-21.337 |  |
|  | 45 | 19.561-29.949 | 20.540-28.468 | 22.913-26.783 |  |
|  | 50 | 25.284-39.247 | 25.713-37.178 | 28.085-33.663 |  |
| SAMPLE SIZE $=$ | 55 | 29.649-49.143 | 30.733-47.856 | 35.938-41.924 | AEROSOL MASS |
| $=360$ | 60 | 37.767-62.010 | 40.512-59.862 | 45.439-52.580 | FRACTION REMAINING $=$ |
|  | 65 | 48.943-70.193 | 50.866-68.207 | 57.474-65.019 | $=0.1$ |
|  | 70 | 62.140-77.301 | 63.702-75.226 | 66.704-71.675 |  |
|  | 75 | 70.722-84.293 | 71.387-82.495 | 74.251-80.072 |  |
|  | 80 | 79.017-94.631 | 79.992-92.908 | 82.390-86.580 |  |
|  | 85 | 86.174-113.901 | 86.845-104.041 | 93.389-97.168 |  |
|  | 90 | 98.799-125.670 | 99.381-124.472 | 115.184-120.898 |  |
|  | 95 | 124.565-152.793 | 125.685-151.789 | 133.312-145.146 |  |

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Appendix A


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=24.523$ | 5 | 2.591-3.600 | 2.642-3.572 | 3.007-3.291 | WATER FLUX = |
|  | 10 | 3.576-4.477 | 3.623-4.409 | 3.951-4.148 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 4.193-5.270 | 4.272-5.232 | 4.604-4.923 |  |
|  | 20 | 4.901-5.954 | 4.977-5.902 | 5.258-5.529 |  |
|  | 25 | 5.478-6.928 | 5.520-6.793 | 5.898-6.364 |  |
| STD. DEV. $=$ | 30 | 6.152-8.278 | 6.226-8.154 | 6.742-7.534 | FALL DISTANCE = |
| $=23.718$ | 35 | 7.277-9.774 | 7.510-9.458 | 8.016-8.930 | $=5000 \mathrm{~cm}$ |
| .. | 40 | 8.303-12.138 | 8.574-11.763 | 9.278-10.774 |  |
|  | 45 | 9.723-15.496 | 10.487-14.311 | 11.491-12.485 |  |
|  | 50 | 11.955-19.874 | 12.316-18.634 | 13.505-16.358 |  |
| SAMPLE SIZE $=$ | 55 | 14.527-24.486 | 15.602-22.759 | 16.883-20.841 |  |
| $=360$ | 60 | 19.565-26.751 | 20.249-26.577 | 22.263-25.295 | FRACTION REMAINING $=$ |
|  | 65 | 24.467-32.355 | 24.984-32.116 | 26.262-28.576 | $=0.001$ |
|  | 70 | 26.896-35.964 | 28.058-35.449 | 31.179-33.411 |  |
|  | 75 | 32.459-41.368 | 33.384-40.869 | 35.089-38.780 |  |
|  | 80 | 36.582-47.575 | 38.495-46.098 | 40.861-44.129 |  |
|  | 85 | 43.753-53.642 | 44.342-52.128 | 47.246-50.005 |  |
|  | 90 | 50.176-66.036 | 51.393-64.798 | 54.311-61.002 |  |
|  | 95 | 64.972-84.053 | 66.073-80.984 | 70.008-75.425 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=1.088$ | 5 | 0.252-0.353 | 0.253-0.349 | 0.278-0.317 |  |
|  | $10$ | $0.352-0.430$ | $0.355-0.424$ | $0.378-0.410$ | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.418-0.490 | 0.422-0.483 | 0.435-0.466 |  |
|  | 20 | 0.466-0.547 | 0.467-0.542 | 0.490-0.518 |  |
|  | 25 | 0.512-0.619 | 0.520-0.605 | 0.545-0.587 |  |
| STD. DEV. $=$ | 30 | 0.582-0.677 | 0.585-0.658 | 0.605-0.633 | FALL DISTANCE = |
| $=0.953$ | 35 | 0.624-0.736 | 0.632-0.730 | 0.652-0.709 | $=500 \mathrm{~cm}$ |
|  | 40 | 0.687-0.798 | 0.699-0.790 | 0.725-0.742 |  |
|  | 45 | 0.739-0.856 | 0.739-0.838 | 0.775-0.821 |  |
|  | 50 | 0.801-0.925 | 0.804-0.920 | 0.834-0.859 |  |
| SAMPLE SIZE $=$ | 55 | 0.857-1.003 | 0.857-0.994 | 0.903-0.955 | AEROSOL MASS |
| $=400$ | 60 | 0.926-1.081 | 0.938-1.071 | 0.983-1.050 | FRACTION REMAINING $=$ |
|  | 65 | 1.005-1.169 | 1.030-1.159 | 1.065-1.120 | $=0.9$ |
|  | 70 | 1.101-1.287 | 1.117-1.272 | $1.157-1.243$ |  |
|  | 75 | 1.204-1.409 | 1.237-1.390 | $1.269-1.351$ |  |
|  | 80 | 1.331-1.628 | 1.357-1.608 | 1.394-1.476 |  |
|  | 85 | 1.478-1.832 | 1.538-1.807 | 1.628-1.711 |  |
|  | 90 | 1.762-2.388 | 1.788-2.364 | 1.891-2.227 |  |
|  | 95 | 2.378-2.705 | 2.391-2.705 | 2.474-2.663 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.792$ | 5 | 0.167-0.293 | 0.172-0.290 | 0.202-0.263 | WATER FLUX = |
|  | 10 | 0.292-0.327 | 0.296-0.327 | 0.305-0.318 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.320-0.377 | 0.325-0.365 | 0.334-0.346 |  |
|  | 20 | 0.346-0.420 | 0.353-0.416 | 0.377-0.392 |  |
|  | 25 | 0.387-0.457 | 0.395-0.452 | 0.417-0.440 |  |
| STD. DEV. = | 30 | 0.436-0.502 | 0.439-0.494 | 0.451-0.471 | FALL DISTANCE $=$ |
| $=0.616$ | 35 | 0.470-0.534 | 0.470-0.523 | 0.488-0.508 | $=500 \mathrm{~cm}$ |
|  | 40 | 0.504-0.615 | 0.505-0.597 | 0.518-0.558 |  |
|  | 45 | 0.539-0.682 | 0.556-0.657 | 0.586-0.628 |  |
|  | 50 | 0.621-0.722 | 0.621-0.713 | 0.644-0.694 |  |
| SAMPLE SIZE $=$ | 55 | 0.682-0.757 | 0.687-0.756 | 0.710-0.743 | AEROSOL MASS |
| $=400$ | 60 | 0.724-0.836 | 0.733-0.827 | 0.746-0.778 | FRACTION REMAINING $=$ |
|  | 65 | 0.765-0.910 | 0.768-0.904 | 0.826-0.844 | $=0.5$ |
|  | 70 | 0.838-0.987 | 0.844-0.970 | 0.898-0.943 |  |
|  | 75 | 0.925-1.041 | 0.943-1.022 | 0.968-1.006 |  |
|  | 80 | 1.002-1.117 | 1.008-1.087 | 1.023-1.047 |  |
|  | 85 | 1.047-1.260 | 1.073-1.241 | 1.112-1.164 |  |
|  | 90 | 1.204-1.615 | 1.227-1.552 | 1.262-1.477 |  |
|  | 95 | 1.595-2.151 | 1.625-2.018 | 1.680-1.892 |  |


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.647$ | 5 | 0.143-0.232 | 0.147-0.232 | 0.180-0.219 | WATER FLUX = |
|  | 10 | 0.232-0.201 | 0.240-0.279 | 0.252-0.272 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.276-0.305 | 0.276-0.303 | 0.283-0.295 |  |
|  | 20 | 0.295-0.339 | 0.296-0.335 | 0.305-0.325 |  |
|  | 25 | 0.318-0.373 | 0.325-0.373 | 0.336-0.355 |  |
| STD. DEV. = | 30 | 0.352-0.402 | 0.355-0.399 | 0.372-0.391 | FALL DISTANCE = |
| $=0.456$ | 35 | 0.381-0.447 | 0.389-0.443 | 0.399-0.412 | $=500 \mathrm{~cm}$ |
|  | 40 | 0.404-0.501 | 0.408-0.496 | 0.438-0.461 |  |
|  | 45 | 0.448-0.552 | 0.459-0.551 | 0.489-0.518 |  |
|  | 50 | 0.510-0.609 | 0.512-0.591 | 0.539-0.559 |  |
| SAMPLE SIZE $=$ | 55 | 0.552-0.659 | 0.558-0.647 | 0.574-0.627 | AEROSOL MASS |
| $=400$ | 60 | 0.616-0.694 | 0.624-0.689 | 0.639-0.668 | FRACTION REMAINING $=$ |
|  | 65 | 0.666-0.747 | 0.667-0.737 | 0.679-0.704 | $=0.3$ |
|  | 70 | 0.696-0.784 | 0.698-0.775 | 0.736-0.766 |  |
|  | 75 | 0.749-0.857 | 0.763-0.848 | 0.774-0.802 |  |
|  | 80 | 0.799-0.929 | 0.804-0.919 | 0.852-0.898 |  |
|  | 85 | 0.898-1.023 | 0.901-1.000 | 0.928-0.962 |  |
|  | 90 | 0.987-1.232 | 0.997-1.196 | 1.063-1.073 |  |
|  | 95 | 1.222-1.796 | 1.264-1.618 | 1.410-1.523 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.463$ | 5 | 0.101-0.160 | 0.102-0.156 | 0.128-0.145 |  |
|  | $10$ | $0.159-0.197$ | $0.162-0.195$ | $0.180-0.187$ | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
| $\checkmark$ - | 15 | 0.191-0.224 | 0.194-0.221 | 0.200-0.212 |  |
| - | 20 | 0.212-0.249 | 0.217-0.247 | 0.224-0.234 |  |
|  | 25 | 0.232-0.264 | 0.236-0.262 | 0.247-0.253 |  |
| STD. DEV. = | 30 | 0.250-0.291 | 0.253-0.284 | 0.261-0.276 | FALL DISTANCE = |
| $=0.326$ | 35 | 0.273-0.315 | 0.275-0.314 | 0.278-0.301 | $=500 \mathrm{~cm}$ |
|  | 40 | 0.293-0.359 | 0.295-0.353 | 0.314-0.324 |  |
|  | 45 | 0.316-0.393 | 0.322-0.392 | 0.344-0.368 |  |
|  | 50 | 0.359-0.432 | 0.359-0.429 | 0.379-0.412 |  |
| SAMPLE SIZE $=$ | 55 | 0.400-0.461 | 0.406-0.456 | 0.428-0.444 | AEROSOL MASS |
| $=400$ | 60 | 0.434-0.498 | 0.435-0.496 | 0.454-0.468 | FRACTION REMAINING $=$ |
|  | 65 | 0.461-0.538 | 0.465-0.523 | 0.490-0.512 | $=0.10$ |
|  | 70 | 0.503-0.583 | 0.512-0.571 | 0.520-0.544 |  |
|  | 75 | 0.542-0.612 | 0.542-0.605 | 0.569-0.590 |  |
|  | 80 | 0.590-0.649 | 0.591-0.644 | 0.605-0.631 |  |
|  | 85 | 0.632-0.747 | 0.637-0.736 | 0.649-0.702 |  |
|  | 90 | 0.709-0.908 | 0.719-0.904 | 0.779-0.823 |  |
|  | 95 | 0.907-1.387 | 0.910-1.315 | 0.994-1.105 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.295$ | 5 | 0.060-0.096 | 0.061-0.091 | 0.072-0.087 | $\begin{aligned} & \text { WATER FLUX = } \\ & =0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 0.096-0.118 | 0.097-0.116 | 0.106-0.111 |  |
|  | 15 | 0.112-0.134 | 0.114-0.132 | 0.119-0.128 |  |
|  | 20 | 0.127-0.156 | 0.130-0.150 | 0.134-0.141 |  |
|  | 25 | 0.141-0.172 | 0.142-0.170 | 0.154-0.164 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =0.210 \end{aligned}$ | 30 | 0.163-0.184 | 0.164-0.183 | 0.170-0.177 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =500 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 0.174-0.200 | 0.177-0.196 | 0.181-0.185 |  |
|  | 40 | 0.184-0.219 | 0.184-0.216 | 0.195-0.207 |  |
|  | $\begin{aligned} & 45 \\ & 50 \end{aligned}$ | $\begin{aligned} & 0.201-0.239 \\ & 0.223-0.263 \end{aligned}$ | $\begin{aligned} & 0.203-0.237 \\ & 0.228-0.256 \end{aligned}$ | $\begin{aligned} & 0.210-0.230 \\ & 0.235-0.252 \end{aligned}$ |  |
|  |  |  |  |  |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 0.241-0.284 | 0.248-0.280 | 0.255-0.271 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 0.264-0.308 | 0.267-0.307 | 0.279-0.291 |  |
|  | 65 | 0.285-0.329 | 0.288-0.326 | 0.301-0.313 |  |
|  | 70 | 0.311-0.360 | 0.313-0.356 | 0.325-0.336 |  |
|  | 75 | 0.331-0.397 | 0.335-0.393 | 0.356-0.383 |  |
|  | 80 | 0.377-0.456 | 0.384-0.438 | $0.393-0.405$ |  |
|  | 85 | 0.405-0.512 | 0.415-0.508 | 0.455-0.483 |  |
|  | 90 | 0.501-0.609 | $0.508-0.596$ | 0.522-0.580 |  |
|  | 95 | 0.607-0.895 | 0.633-0.833 | 0.658-0.710 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.231$ | 5 | 0.044-0.070 | 0.046-0.069 | 0.056-0.065 | WATER FLUX = |
|  | 10 | 0.070-0.088 | 0.072-0.087 | 0.078-0.083 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.086-0.104 | 0.086-0.103 | 0.090-0.099 |  |
|  | 20 | 0.099-0.118 | 0.100-0.115 | 0.104-0.111 |  |
|  | 25 | 0.108-0.134 | 0.111-0.132 | 0.116-0.123 |  |
| STD. DEV. = | 30 | 0.121-0.148 | 0.122-0.146 | 0.132-0.142 | FALL DISTANCE = |
| $=0.171$ | 35 | 0.137-0.153 | 0.141-0.153 | 0.145-0.151 | $=500 \mathrm{~cm}$ |
|  | 40 | 0.149-0.172 | 0.151-0.164 | 0.152-0.159 |  |
|  | 45 | 0.153-0.185 | 0.155-0.184 | 0.163-0.177 |  |
|  | 50 | 0.174-0.200 | 0.175-0.199 | 0.181-0.193 |  |
| SAMPLE SIZE = | 55 | 0.185-0.211 | 0.190-0.210 | 0.197-0.202 | AEROSOL MASS |
| $=400$ | 60 | 0.201:0.238 | 0.201-0.234 | 0.206-0.220 | FRACTION REMAINING $=$ |
|  | 65 | 0.213-0.254 | 0.215-0.252 | 0.233-0.245 | $=0.001$ |
|  | 70 | 0.241-0.280 | 0.244-0.276 | 0.250-0.269 |  |
|  | 75 | 0.264-0.312 | 0.269-0.310 | 0.275-0.302 |  |
|  | 80 | 0.287-0.362 | 0.303-0.336 | 0.310-0.319 |  |
|  | 85 | 0.319-0.417 | 0.321-0.415 | 0.359-0.404 |  |
|  | 90 | 0.408-0.489 | 0.411-0.489 | 0.425-0.448 |  |
|  | 95 | 0.489-0.702 | 0.490-0.668 | 0.524-0.571 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=1.058$ | 5 | 0.248-0.348 | 0.252-0.342 | 0.267-0.317 | WATER FLUX = |
|  | 10 | 0.348-0.424 | 0.351-0.423 | 0.364-0.400 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.401-0.486 | 0.417-0.471 | 0.429-0.452 |  |
|  | 20 | 0.451-0.544 | 0.455-0.535 | 0.487-0.511 |  |
|  | 25 | 0.505-0.602 | 0.515-0.593 | 0.539-0.561 |  |
| STD. DEV. = | 30 | 0.553-0.657 | 0.559-0.649 | 0.589-0.623 | FALL DISTANCE $=$ |
| $=0.912$ | 35 | 0.607-0.706 | 0.619-0.695 | 0.649-0.690 | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.665-0.774 | 0.676-0.765 | 0.693-0.733 |  |
|  | 45 | 0.711-0.830 | 0.727-0.817 | 0.758-0.807 |  |
|  | 50 | 0.777-0.900 | 0.796-0.882 | 0.815-0.832 |  |
| SAMPLE SIZE = | 55 | 0.830-0.992 | 0.830-0.980 | 0.881-0.927 ${ }^{\text {- }}$ |  |
| $=400$ | 60 | 0.903-1.057 | 0.910-1.045 | $0.949-0.997$ | FRACTION REMAINING $=$ |
|  | 65 | 0.993-1.165 | 0.996-1.135 | 1.029-1.087 | $=0.9$ |
|  | 70 | 1.079-1.263 | 1.085-1.251 | 1.124-1.193 |  |
|  | 75 | 1.166-1.372 | 1.189-1.363 | 1.251-1.318 |  |
|  | 80 | 1.308-1.601 | 1.319-1.579 | 1.365-1.470 |  |
|  | 85 | 1.470-1.819 | 1.494-1.784 | 1.600-1.674 |  |
|  | 90 | 1.707-2.270 | 1.747-2.257 | 1.852-2.217 |  |
|  | 95 | 2.265-2.616 | 2.308-2.615 | 2.454-2.533 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.773$ | 5 | 0.168-0.282 | 0.176-0.282 | 0.201-0.260 | WATER FLUX $=$ |
|  | 10 | 0.282-0.324 | 0.286-0.321 | 0.298-0.312 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s-cm}{ }^{2}$ |
|  | 15 | 0.319-0.369 | 0.321-0.365 | 0.331-0.345 |  |
|  | 20 | 0.345-0.409 | 0.347-0.405 | 0.369-0.389 |  |
|  | 25 | 0.385-0.453 | 0.390-0.449 | 0.407-0.432 |  |
| STD. DEV. $=$ | 30 | 0.428-0.476 | 0.431-0.475 | 0.449-0.468 | FALL DISTANCE = |
| $=0.590$ | 35 | 0.461-0.522 | 0.467-0.516 | 0.475-0.484 | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.477-0.598 | 0.482-0.591 | 0.508-0.544 |  |
|  | 45 | 0.535-0.654 | 0.543-0.640 | 0.578-0.625 |  |
|  | 50 | 0.599-0.709 | 0.600-0.701 | 0.636-0.669 |  |
| SAMPLE SIZE = | 55 | 0.655-0.742 | 0.664-0.739 | 0.697-0.723. | AEROSOL MASS ${ }^{\text {- }}$ |
| $=400$ | 60 | 0.710-0.820 | 0.722-0.798 | 0.732-0.765 | FRACTION REMAINING $=$ |
|  | 65 | 0.744-0.886 | 0.758-0.876 | 0.787-0.834 | $=0.5$ |
|  | 70 | 0.826-0.965 | 0.833-0.952 | 0.871-0.918 |  |
| . | 75 | 0.912-1.014 | 0.918-1.011 | 0.952-0.996 |  |
|  | 80 | 0.995-1.079 | 0.997-1.072 | 1.012-1.041 |  |
|  | 85 | 1.041-1.255 | 1.042-1.223 | 1.078-1.151 |  |
|  | 90 | 1.184-1.562 | 1.203-1.496 | 1.259-1.431 |  |
|  | 95 | 1.554-2.029 | 1.615-1.957 | 1.658-1.798 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.629$ | 5 | 0.143-0.224 | 0.147-0.224 | 0.177-0.213 | WATER FLUX = |
|  | 10 | 0.224-0.273 | 0.228-0.273 | 0.246-0.267 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.271-0.297 | 0.271-0.296 | 0.275-0.289 |  |
|  | 20 | 0.288-0.337 | 0.293-0.332 | 0.297-0.315 |  |
|  | 25 | 0.310-0.370 | 0.316-0.364 | 0.335-0.351 |  |
| STD. DEV. = | 30 | 0.344-0.391 | 0.348-0.386 | 0.360-0.373 | FALL DISTANCE = |
| $=0.456$ | 35 | 0.373-0.434 | 0.373-0.427 | 0.385-0.404 | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.394-0.496 | 0.399-0.483 | 0.423-0.454 |  |
|  | 45 | 0.434-0.528 | 0.442-0.525 | 0.477-0.505 |  |
|  | 50 | 0.498-0.589 | 0.498-0.572 | 0.519-0.545 |  |
| SAMPLE SIZE = | 55 | 0.529-0.636 | 0.533-0.635 | 0.568-0.620 | AEROSOL MASS . |
| $=400$ | 60 | 0.599-0.677 | 0.615-0.671 | 0.634-0.646 | FRACTION REMAINING $=$ |
|  | 65 | 0.640-0.721 | 0.646-0.718 | 0.666-0.689 | $=0.3$ |
|  | 70 | 0.683-0.767 | 0.684-0.761 | 0.716-0.744 |  |
|  | 75 | 0.735-0.838 | 0.743-0.837 | 0.760-0.790 |  |
|  | 80 | 0.775-0.901 | 0.791-0.897 | 0.837-0.863 |  |
|  | 85 | 0.866-0.999 | 0.886-0.974 | 0.900-0.949 |  |
|  | 90 | 0.957-1.199 | 0.966-1.190 | 1.024-1.059 |  |
|  | 95 | 1.196-1.683 | 1.214-1.572 | 1.392-1.478 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.450$ | 5 | 0.100-0.154 | 0.101-0.148 | 0.126-0.139 | WATER FLUX = |
|  | 10 | 0.153-0.191 | 0.159-0.189 | 0.171-0.180 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.183-0.218 | 0.186-0.215 | 0.195-0.202 |  |
|  | 20 | 0.202-0.243 | 0.206-0.239 | 0.218-0.230 |  |
|  | 25 | 0.228-0.259 | 0.230-0.259 | 0.239-0.249 |  |
| STD. DEV. $=$ | 30 | 0.248-0.283 | 0.249-0.275 | 0.259-0.263 | FALL DISTANCE = |
| $=0.313$ | 35 | 0.260-0.309 | 0.262-0.305 | 0.273-0.293 | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.289-0.346 | 0.291-0.340 | 0.304-0.321 |  |
|  | 45 | 0.313-0.386 | 0.319-0.369 | 0.334-0.358 |  |
|  | 50 | 0.347-0.423 | 0.352-0.422 | 0.365-0.406 |  |
| SAMPLE SIZE $=$ | 55 | 0.389-0.455 | 0.399-0.451 | 0.411-0.427 | AEROSOL MASS |
| $=400$ | 60 | 0.425-0.492 | 0.426-0.482 | 0.439-0.465 | FRACTION REMAINING $=$ |
|  | 65 | 0.459-0.521 | 0.464-0.517 | 0.475-0.495 | $=0.1$ |
|  | 70 | 0.493-0.574 | 0.495-0.549 | 0.516-0.528 |  |
|  | 75 | 0.525-0.604 | 0.526-0.590 | 0.548-0.586 |  |
|  | 80 | 0.586-0.643 | 0.586-0.636 | 0.592-0.615 |  |
|  | 85 | 0.615-0.718 | 0.620-0.713 | 0.642-0.685 |  |
|  | 90 | 0.701-0.871 | 0.705-0.871 | 0.749-0.795 |  |
|  | 95 | 0.871-1.344 | 0.906-1.253 | 0.945-1.073 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.287$ | 5 | 0.058-0.090 | 0.061-0.089 | 0.070-0.083 | WATER FLUX = |
|  | 10 | 0.090-0.112 | 0.093-0.111 | 0.101-0.107 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.108-0.131 | 0.109-0.130 | 0.116-0.125 |  |
|  | 20 | 0.125-0.149 | 0.127-0.147 | 0.131-0.141 |  |
|  | 25 | 0.138-0.169 | 0.141-0.168 | 0.147-0.162 |  |
| STD. DEV. = | 30 | 0.157-0.178 | 0.162-0.176 | $0.167-0.171$ | FALL DISTANCE = |
| $=0.206$ | 35 | $0.170-0.195$ | $0.170-0.194$ | $0.174-0.182$ | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.179-0.209 | 0.181-0.206 | 0.190-0.201 |  |
|  | 45 | 0.197-0.236 | 0.198-0.234 | 0.205-0.225 |  |
|  | 50 | 0.217-0.254 | 0.222-0.254 | 0.231-0.241 |  |
| SAMPLE SIZE = | 55 | 0.237-0.282 | 0.239-0.273 | 0.248-0.263 |  |
| $=400$ | $60$ | $0.255-0.298$ | $0.261-0.293$ | $0.271-0.286$ | FRACTION REMAINING $=$ |
|  | $65$ | $0.283-0.321$ | $0.285-0.318$ | 0.289-0.310 |  |
|  | 70 | 0.301-0.348 | 0.304-0.340 | 0.317-0.330 |  |
|  | 75 | 0.322-0.387 | 0.327-0.381 | 0.340-0.375 |  |
|  | 80 | 0.370-0.449 | 0.375-0.422 | 0.382-0.404 |  |
|  | 85 | 0.404-0.497 | 0.405-0.491 | 0.447-0.475 |  |
|  | 90 | 0.478-0.594 | 0.482-0.594 | 0.510-0.548 |  |
|  | 95 | 0.594-0.869 | 0.595-0.808 | 0.637-0.688 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{hr}^{-1}\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.224$ | 5 | 0.044-0.068 | 0.046-0.066 | 0.053-0.063 | WATER FLUX = |
|  | 10 | 0.068-0.086 | 0.069-0.084 | 0.075-0.080 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.081-0.103 | 0.082-0.100 | 0.088-0.094 |  |
|  | 20 | 0.094-0.113 | 0.096-0.112 | 0.103-0.107 |  |
|  | 25 | 0.106-0.131 | 0.107-0.130 | 0.113-0.120 |  |
| STD. DEV. = | 30 | 0.117-0.142 | 0.119-0.141 | 0.130-0.134 | FALL DISTANCE $=$ |
| $=0.166$ | 35 | 0.134-0.150 | 0.134-0.150 | 0.140-0.145 | $=5000 \mathrm{~cm}$ |
|  | 40 | 0.143-0.165 | 0.143-0.163 | 0.148-0.154 |  |
|  | 45 | 0.151-0.183 | 0.152-0.178 | . $0.162-0.172$ |  |
|  | 50 | 0.165-0.198 | 0.171-0.194 | 0.177-0.190 |  |
| SAMPLE SIZE = | 55 | 0.184-0.206 | 0.185-0.203 | 0.192-0.200 | AEROSOL MASS |
| $=400$ | 60 | 0.198-0.230 | 0.199-0.228 | 0.202-0.212 | FRACTION REMAINING $=$ |
|  | 65 | 0.208-0.247 | 0.210-0.243 | 0.221-0.238 | $=0.001$ |
|  | 70 | 0.236-0.271 | 0.237-0.271 | 0.242-0.266 |  |
|  | 75 | 0.260-0.304 | 0.265-0.304 | 0.271-0.288 |  |
|  | 80 | 0.282-0.343 | 0.291-0.328 | 0.304-0.312 |  |
|  | 85 | 0.312-0.405 | 0.318-0.404 | 0.342-0.385 |  |
|  | 90 | 0.400-0.487 | 0.404-0.478 | 0.409-0.437 |  |
|  | 95 | 0.486-0.677 | 0.488-0.647 | 0.500-0.588 |  |

## Appendix B

## Uncertainty Distributions for $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$

Cumulative probability distributions for $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ are shown in the tables of this appendix. The distributions of $\lambda\left(m_{\mathrm{f}}\right) / \lambda\left(m_{\mathrm{f}}=0.9\right)$ are, of course, identical to distributions of $\mathrm{E} / \mathrm{D}\left(\mathrm{m}_{\mathrm{f}}\right) /$ $\mathrm{E} / \mathrm{D}\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$. The distributions are essentially independent of the fall distance of the spray droplets. Consequently $\dot{3}_{2}$ distributions have only been tabulated for $\mathrm{H}=3000 \mathrm{~cm}$ and $\mathrm{Q}=0.001$, 0.01 , and $0.25 \mathrm{~cm}^{3} / \mathrm{cm}^{2}$-s.


|  | Quantile (\%) | Range for $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.622$ | 5 | 0.417-0.432 | 0.418-0.432 | 0.420-0.425 | WATER FLUX = |
|  | 10 | 0.432-0.460 | 0.432-0.460 | 0.439-0.452 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.453-0.473 | 0.454-0.472 | 0.462-0.466 |  |
|  | 20 | 0.465-0.487 | 0.466-0.486 | 0.473-0.484 |  |
|  | 25 | 0.480-0.503 | 0.483-0.501 | 0.486-0.496 |  |
| STD. DEV. = | 30 | 0.490-0.534 | 0.494-0.530 | 0.501-0.522 | FALL DISTANCE = |
| $=0.142$ | 35 | 0.509-0.559 | 0.515-0.558 | 0.528-0.541 | $=3000 \mathrm{~cm}$ |
|  | 40 | 0.534-0.585 | 0.538-0.579 | 0.546-0.567 |  |
|  | 45 | 0.559-0.613 | 0.563-0.609 | 0.576-0.597 |  |
|  | 50 | 0.582-0.635 | 0.590-0.631 | 0.601-0.618 |  |
|  | 55 | 0.613-0.663 | 0.614-0.660 | 0.625-0.643 | AEROSOL MASS |
| $=360$ | 60 | 0.635-0.686 | 0.638-0.683 | 0.655-0.674 | FRACTION REMAINING $=$ |
|  | 65 | 0.662-0.713 | 0.666-0.709 | 0.680-0.696 | $=0.3$ |
|  | 70 | 0.687-0.737 | 0.690-0.734 | 0.706-0.721 |  |
|  | 75 | 0.715-0.766 | 0.720-0.762 | 0.727-0.752 |  |
|  | 80 | 0.746-0.803 | 0.752-0.798 | 0.762-0.788 |  |
|  | 85 | 0.787-0.820 | 0.790-0.819 | 0.801-0.810 |  |
|  | 90 | 0.814-0.843 | 0.815-0.842 | 0.821-0.831 |  |
|  | 95 | 0.842-0.872 | 0.843-0.869 | 0.853-0.867 |  |

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|  | Quantile (\%) | Range for $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.458$ | 5 | 0.238-0.257 | 0.239-0.256 | 0.244-0.251 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 0.256-0.277 | 0.257-0.275 | 0.260-0.269 |  |
|  | 15 | 0.271-0.293 | 0.274-0.290 | 0.279-0.287 |  |
|  | 20 | 0.286-0.309 | 0.287-0.308 | 0.291-0.300 |  |
|  | 25 | 0.298-0.326 | 0.300-0.322 | 0.308-0.316 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =0.164 \end{aligned}$ | 30 | 0.314-0.352 | 0.315-0.346 | 0.319-0.336 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =3000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 0.328-0.373 | 0.333-0.370 | 0.345-0.357 |  |
|  | 40 | 0.353-0.400 | 0.356-0.395 | 0.365-0.382 |  |
|  | 45 | 0.372-0.430 | 0.379-0.427 | 0.391-0.410 |  |
|  | 50 | 0.398-0.460 | 0.405-0.453 | 0.423-0.438 |  |
| $\begin{aligned} & \text { SAMPLE SIZE = } \\ & =360 \end{aligned}$ | 55 | 0.430-0.489 | 0.433-0.485 | 0.445-0.465 | AEROSOL MASS FRACTION REMAINING = $=0.1$ |
|  | 60 | 0.456-0.516 | 0.463-0.512 | 0.479-0.499 |  |
|  | 65 | 0.488-0.547 | 0.493-0.541 | 0.509-0.528 |  |
|  | 70 | 0.516-0.579 | 0.521-0.575 | 0.540-0.560 |  |
|  | 75 | 0.549"-0.625 | 0.554-0.618 | 0.567-0.604 |  |
|  | 80 | 0.592-0.669 | 0.603-0.662 | 0.615-0.650 |  |
|  | 85 | 0.647-0.699 | 0.653-0.697 | 0.666-0.682 |  |
|  | 90 | 0.684-0.733 | 0.685-0.732 | 0.700-0.716 |  |
|  | 95 | 0.732-0.773 | 0.733-0.770 | 0.745-0.765 |  |


|  | Quantile <br> (\%) | Range for $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.302$ | 5 | 0.112-0.128 | 0.114-0.128 | 0.117-0.125 | WATER FLUX = |
|  | 10 | 0.128-0.141 | 0.128-0.140 | 0.132-0.137 | $=0.25 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.138-0.152 | 0.139-0.151 | 0.142-0.148 |  |
|  | 20 | 0.148-0.170 | 0.150-0.170 | 0.151-0.161 |  |
|  | 25 | 0.158-0.186 | 0.161-0.182 | 0.169-0.175 |  |
| STD. DEV. = | 30 | 0.173-0.200 | 0.175-0.197 | 0.180-0.189 | FALL DISTANCE = |
| $=0.155$ | 35 | 0.187-0.218 | 0.188-0.217 | 0.196-0.207 | $=3000 \mathrm{~cm}$ |
|  | 40 | 0.200-0.236 | 0.204-0.235 | 0.215-0.224 |  |
|  | 45 | 0.218-0.258 | 0.221-0.256 | 0.230-0.245 |  |
|  | 50 | 0.236-0.286 | 0.240-0.285 | 0.252-0.263 |  |
| SAMPLE SIZE $=$ | 55 | 0.258-0.313 | 0.258-0.308 | 0.277-0.292 | AEROSOL MASS |
| $=360$ | 60 | 0.285-0.337 | 0.288-0.330 | 0.304-0.320 | FRACTION REMAINING $=$ |
|  | 65 | 0.312-0.364 | 0.316-0.363 | 0.328-0.354 | $=0.01$ |
|  | 70 | 0.338-0.399 | 0.347-0.396 | 0.361-0.378 |  |
|  | 75 | 0.367-0.453 | 0.370-0.445 | 0.389-0.423 |  |
|  | 80 | 0.419-0.502 | 0.422-0.496 | 0.443-0.479 |  |
|  | 85 | 0.479-0.536 | 0.482-0.532 | 0.497-0.516 |  |
|  | 90 | 0.517-0.581 | 0.530-0.577 | 0.540-0.559 |  |
|  | 95 | 0.577-0.630 | 0.582-0.626 | 0.595-0.618 |  |

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|  | Quantile (\%) | Range for $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.246$ | 5 | 0.079-0.087 | 0.080-0.086 | 0.081-0.084 | WATER FLUX = |
|  | 10 | 0.087-0.104 | 0.088-0.103 | 0.093-0.100 | $=0.01 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.101-0.118 | 0.102-0.117 | 0.105-0.110 |  |
|  | 20 | 0.109-0.131 | 0.113-0.130 | . $0.119-0.127$ |  |
|  | 25 | 0.123-0.147 | 0.127-0.145 | 0.131-0.140 |  |
| STD. DEV. = | 30 | 0.137-0.163 | 0.139-0.160 | 0.145-0.154 | FALL DISTANCE $=$ |
| $=0.136$ | 35 | 0.150-0.178 | 0.152-0.177 | 0.159-0.168 | $=3000 \mathrm{~cm}$ |
|  | 40 | 0.164-0.190 | 0.167-0.185 | 0.176-0.182 |  |
|  | 45 | 0.179-0.204 | 0.179-0.203 | 0.184-0.198 |  |
|  | 50 | 0.191-0.223 | 0.194-0.218 | 0.202-0.210 |  |
| SAMPLE SIZE $=$ | 55 | 0.204-0.249 | 0.208-0.247 | 0.216-0.236 | AEROSOL MASS |
| $=400$ | 60 | 0.226-0.272 | 0.232-0.267 | 0.246-0.258 | FRACTION REMAINING $=$ |
|  | 65 | 0.251-0.295 | 0.254-0.294 | 0.266-0.278 | $=0.001$ |
|  | 70 | 0.275-0.333 | 0.277-0.323 | 0.293-0.304 |  |
|  | 75 | 0.301-0.364 | 0.304-0.361 | 0.320-0.346 |  |
|  | 80 | 0.342-0.412 | 0.348-0.408 | 0.361-0.384 |  |
|  | 85 | 0.384-0.438 | 0.391-0.437 | 0.412-0.428 |  |
|  | 90 | 0.430-0.491 | 0.432-0.490 | 0.451-0.471 |  |
|  | 95 | 0.490-0.541 | 0.494-0.540 | 0.507-0.525 |  |


Appendix B


|  | Quantile (\%) | Range for $\lambda\left(\mathrm{m}_{\mathrm{f}}\right) / \lambda\left(\mathrm{m}_{\mathrm{f}}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.631$ | 5 | 0.423-0.437 | 0.424-0.435 | 0.430-0.431 | WATER FLUX = |
|  | 10 | 0.437-0.459 | 0.438-0.459 | 0.447-0.452 | $=0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2}$ |
|  | 15 | 0.455-0.475 | 0.458-0.473 | 0.464-0.468 |  |
|  | 20 | 0.468-0.492 | 0.470-0.491 | 0.475-0.483 |  |
|  | 25 | 0.483-0.519 | 0.484-0.517 | 0.492-0.506 |  |
| STD. DEV. $=$ | 30 | 0.501-0.540 | 0.506-0.540 | 0.517-0.532 | FALL DISTANCE $=$ |
| $=0.142$ | 35 | 0.527-0.565 | 0.530-0.559 | 0.540-0.548 | $=3000 \mathrm{~cm}$ |
|  | 40 | 0.541-0.583 | 0.544-0.580 | 0.559-0.571 |  |
|  | 45 | 0.568-0.626 | 0.571-0.624 | 0.576-0.599 |  |
|  | 50 | 0.584-0.660 | 0.594-0.658 | 0.612-0.645 |  |
| SAMPLE SIZE = | 55 | 0.629-0.683 | 0.639-0.682 | 0.654-0.670 | AEROSOL MASS |
| $=400$ | 60 | 0.663-0.697 | 0.667-0.691 | 0.674-0.687 | FRACTION REMAINING $=$ |
|  | 65 | 0.684-0.720 | 0.686-0.719 | 0.689-0.707 | $=0.30$ |
|  | 70 | 0.704-0.761 | 0.707-0.756 | 0.718-0.740 |  |
|  | 75 | 0.726-0.775 | 0.740-0.773 | 0.755-0.768 |  |
|  | 80 | 0.768-0.797 | 0.768-0.796 | 0.773-0.784 |  |
|  | 85 | 0.784-0.821 | 0.787-0.820 | 0.797-0.813 |  |
|  | 90 | 0.817-0.840 | 0.820-0.839 | 0.825-0.830 |  |
|  | 95 | 0.840-0.872 | 0.840-0.872 | 0.851-0.865 |  |

## NUREG/CR-5966



|  | Quantile (\%) | Range for $\lambda\left(m_{f}\right) / \lambda\left(m_{f}=0.9\right)$ at a confidence level of |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 95\% | 90\% | 50\% |  |
| MEAN $=0.311$ | 5 | 0.116-0.131 | 0.117-0.127 | 0.120-0.124 | $\begin{aligned} & \text { WATER FLUX }= \\ & =0.001 \mathrm{~cm}^{3} / \mathrm{s}-\mathrm{cm}^{2} \end{aligned}$ |
|  | 10 | 0.130-0.147 | 0:132-0.146 | 0.138-0.141 |  |
|  | 15 | 0.141-0.160 | 0.144-0.158 | 0.148-0.154 |  |
|  | 20 | 0.154-0.174 | 0.155-0.172 | 0.160-0.168 |  |
|  | 25 | 0.168-0.198 | 0.169-0.194 | 0.173-0.183 |  |
| $\begin{aligned} & \text { STD. DEV. }= \\ & =0.151 \end{aligned}$ | 30 | 0.180-0.213 | 0.183-0.208 | 0.193-0.203 | $\begin{aligned} & \text { FALL DISTANCE }= \\ & =3000 \mathrm{~cm} \end{aligned}$ |
|  | 35 | 0.202-0.231 | 0.203-0.222 | 0.207-0.216 |  |
|  | 40 | 0.214-0.248 | 0.214-0.248 | 0.220-0.237 |  |
|  | 45 | 0.234-0.284 | 0.236-0.280 | 0.247-0.260 |  |
|  | 50 | 0.248-0.315 | 0.255-0.313 | 0.276-0.292 |  |
| $\begin{aligned} & \text { SAMPLE SIZE }= \\ & =400 \end{aligned}$ | 55 | 0.284-0.333 | 0.286-0.324 | 0.303-0.322 | AEROSOL MASS <br> FRACTION REMAINING $=$ $=0.01$ |
|  | 60 | 0.317-0.354 | 0.317-0.351 | 0.323-0.336 |  |
|  | 65 | 0.334-0.372 | 0.335-0.372 | 0.348-0.361 |  |
|  | 70 | 0.356-0.423 | 0.359-0.423 | 0.369-0.398 |  |
|  | 75 | 0.386-0.454 | 0.396-0.454 | 0.420-0.439 |  |
|  | 80 | 0.437-0.483 | 0.440-0.483 | 0.454-0.464 |  |
|  | 85 | 0.464-0.520 | 0.475-0.520 | 0.488-0.510 |  |
|  | 90 | 0.519-0.556 | 0.520-0.556 | 0.532-0.541 |  |
|  | 95 | 0.560-0.625 | 0.567-0.625 | 0.578-0.611 |  |

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[^0]:    *Taken at a location 86 cm radially displaced from the axis of the nozzle and 305 cm below the nozzle.
    **mean, $\mu$, and geometric standard deviation obtained by a least squares fit to a log-normal distribution.

[^1]:    *Throughout this document $\lambda$ is given in units of reciprocal hours. It is useful to remember in examining the values of $\lambda$ presented here that $1 / \lambda$ is the time (in hours) required to reduce the aerosol concentration by a factor of $\mathrm{e} \approx 2.72$

[^2]:    *The ranges defining percentile levels can be reduced by taking a larger number of samples. The ranges narrow with the square root of the number of samples. For this work, sample sizes were selected so that it was at least 95 percent certain that 95 percent of the range of values of $\lambda$ had been sampled. See Appendix A of Reference 11 for further discussion of this point.

[^3]:    *Means and standard deviations of the distributions are also presented in the tables in Appendix A. Because the uncertainty distributions for $\lambda$ are not simple, normal or log-normal distributions, means and standard deviations are not especially significant.

